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54 **Crystalline aluminosilicate compositions, the preparation thereof and their use in the conversion of synthesis gas to low molecular weight hydrocarbons.**

57 **Crystalline platinum or palladium aluminosilicates are prepared by incorporating platinum or palladium onto the aluminosilicate and mixing with a methanol synthesis catalyst. Conversion of synthesis gas to low molecular weight hydrocarbons with high selectivity employing these platinum or palladium aluminosilicates as catalysts are also disclosed.**

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CRYSTALLINE ALUMINOSILICATE COMPOSITIONS, THE
PREPARATION THEREOF AND THEIR USE IN THE CONVERSION
OF SYNTHESIS GAS TO LOW MOLECULAR WEIGHT HYDROCARBONS

5 The present invention relates to aluminosilicate compositions and the catalytic conversion of synthesis gas to low molecular weight hydrocarbons utilizing these compositions.

10 Zeolite materials, both natural and synthetic, are known to have catalytic capability for various types of reactions, especially hydrocarbon conversions. The well known crystalline aluminosilicate zeolites are commonly referred to as "molecular sieves" and are characterized by their highly ordered crystalline structure and uniformly dimensioned pores, and are distinguishable from each other on
15 the basis of composition, crystal structure, adsorption properties and the like. The term "molecular sieves" is derived from the ability of the zeolite materials to selectively adsorb molecules on the basis of their size and form.

20 The processes for producing such crystalline synthetic zeolites are well known in the art. A family of crystalline aluminosilicate zeolites, designated ZSM-5, is disclosed in U.S. Patent No. 3,702,886, said patent being herein incorporated by reference.

25 U.S. Patent No. 3,941,871 relates to novel crystalline metal organosilicates which are essentially free of Group IIIA metals, i.e., aluminum and/or gallium. This patent is herein incorporated by reference. It is noted therein that the amount of alumina present in the known
30 zeolites appears directly related to the acidity characteristics of the resultant product and that a low alumina

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1 content has been recognized as being advantageous in
attaining a low degree of acidity which in many catalytic
reactions is translated into low coke making properties and
low aging rates. A typical procedure for making the organo-
5 silicates is to react a mixture containing a tetraalkyl-
ammonium compound, sodium hydroxide, an oxide of a metal
other than a metal of Group IIIA, an oxide of silicon, and
water until crystals of said metal organosilicates are
formed. It is also noted in the patent that the family of
.0 crystalline metal organosilicates have a definite X-ray
diffraction pattern which is similar to that of the ZSM-5
zeolites. Minor amounts of alumina are contemplated in the
patent and are attributable primarily to the presence of
aluminum impurities in the reactants and/or equipment
5 employed.

U.S. Patent No. 3,884,835 discloses crystalline
silica compositions. The crystalline silica materials may
also contain a metal promoter which may be selected from
Group IIIA, Group VB or Group VIB elements. Boron is
20 disclosed as one of the metal promoters.

U.S. Patent No. 4,088,605 is directed to the
synthesis of a zeolite, such as ZSM-5, which contains an
outer shell free from aluminum. The patent states at column
10, the paragraph beginning at line 20, that to produce the
25 outer aluminum-free shell, it is also essential that the
reactive aluminum be removed from the reaction mixture. It
is therefore necessary, as noted therein, to process the
zeolite and to replace the crystallization medium with an
aluminum-free mixture to obtain crystallization of SiO_2 on
30 the surface of the zeolite which can be accomplished by a
total replacement of the reaction mixture or by complexing
from the original reaction mixture any remaining aluminum
ions with reagents such as gluconic acid or ethylene-
diaminotertra-acetic acid (EDTA).

1 Crystalline borosilicate compositions are disclosed
in German Offenlegungsschrift 2,746,790. This application
relates specifically to borosilicates which are prepared
using the usual procedures for making the aluminosilicate
5 zeolites. It is noted therein that in instances where a
deliberate effort is made to eliminate aluminum from the
borosilicate crystal structure because of its adverse
influence on particular conversion processes, the molar
ratios of $\text{SiO}_2/\text{Al}_2\text{O}_3$ can easily exceed 2000-3000 and that
10 this ratio is generally only limited by the availability of
aluminum-free raw materials.

German Offenlegungsschrift 2,848,849 relates to
crystalline aluminosilicates of the ZSM-5 zeolite series.
These particular zeolites have a silica to alumina mole ratio
15 greater than 20 and are prepared from a reaction mixture
containing a source of silica, alumina, a quaternary alkyl
ammonium compound and a metal compound including such group
VIII metals as ruthenium, palladium and platinum. In example
2, the crystalline aluminosilicate is prepared from a
20 reaction mixture containing RuCl_3 and in Example 3, the
reaction mixture contains $\text{H}_2\text{PtCl}_6 \cdot n\text{H}_2\text{O}$.

U.S. Patent No. 4,468,474 discloses hydrogen
activated catalyst compositions comprising iron, silicon and
carbon that selectively convert gaseous mixtures to $\text{C}_2\text{-C}_6$
25 alkenes. It is further noted that the catalysts maintained
their activity and high selectivity over a long period and
that regeneration of partially deactivated catalysts can be
accomplished by treatment with hydrogen at elevated
temperature.

30 U.S. Patent No. 4,298,695 discloses the conversion
of synthesis gas to a liquid hydrocarbon, e.g. naphtha. The
process employs unpromoted catalysts which need promoters and
high activity without aging is characteristic of these
catalysts.

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1 U.S. Patent No. 4,418,155 discloses a process for
the conversion of synthesis gas utilizing a catalyst which
comprises a ZSM-5 type zeolite and a carbon oxide reducing
component. This process yields a particular product, e.g.
5 linear alpha-olefins, (C₄-C₆ olefins)..

U.S. Patent No. 4,432,535 discloses a process for
the conversion of synthesis gas to an exclusive hydrocarbon
product with selectivity to ethane. The catalysts comprise a
crystalline zeolite component and a metal component. The
10 zeolites employed are primarily synthetic zeolites such as
ZSM-5, ZSM-11 and the like, that have a silica:alumina ratio
of at least 12:1 and preferably 30:1. The metal component may
be derived from one or more metals. Suitable metals or
combinations of metals are those which may be employed for
15 the synthesis of alcohols from synthesis gas. The metal
components may be introduced into the zeolite by impregnation
from liquid ammonia solutions. In Example 10, the effect of
using different zeolites, e.g. erionite (a natural zeolite)
is shown in the conversion of synthesis gas. Erionite shows
20 significantly lower selectivity for ethane.

While the art has provided zeolitic catalysts
having a wide variety of catalytic and adsorbative properties,
the need still exists for crystalline materials having
different and/or enhanced catalytic properties. For example,
25 an important use for a catalytic material is the conversion
of synthesis gas to low molecular weight hydrocarbons.
Further, many hydrocarbon conversion processes are performed
employing zeolites, i.e. alkylation and isomerization. As is
well-known in the art, it is important to maximize
30 selectivity for a desired product.

1 In the present invention, palladium or platinum is
incorporated onto the aluminosilicates and the alumino-
silicates are mixed with a methanol synthesis catalyst for
use in converting synthesis gas to low molecular weight
5 hydrocarbons. Briefly, this invention relates to novel
platinum or palladium aluminosilicate compositions that can
be physically mixed with a methanol synthesis catalyst, the
preparation of these compositions and the use of these
compositions to convert synthesis gas to low molecular weight
10 hydrocarbons, preferably ethane. Consequently, when
compositions prepared in accordance with the present invention
are used in the conversion of synthesis gas to low molecular
weight hydrocarbons, the compositions exhibit high catalytic
activity in the conversion of synthesis gas to C₂-C₄ alkanes,
15 with high selectivity specifically for ethane. These
properties are contrary to the results expected from this
type of crystalline zeolite composition.

The compositions of this invention are prepared by
a method which comprises:

20 (a) contacting a crystalline aluminosilicate with
a platinum or palladium salt solution to provide a platinum
or palladium crystalline aluminosilicate;

(b) calcining the platinum or palladium
crystalline aluminosilicate in air at a temperature of about
25 300°C to about 600°C for at least 4 hours;

(c) heating the calcined platinum or palladium
aluminosilicate in the presence of hydrogen from ambient
temperature to an elevated temperature of about 300°C to
about 400°C at a rate of temperature increase of about 0.5 to
30 about 2.0°C per minute;

(d) maintaining said silicate at said temperature
for about 0.5 to about 4 hours; and

1 (e) cooling said aluminosilicate to ambient
temperature in the presence of hydrogen.

5 In another embodiment, this invention relates to
aluminosilicate compositions that are prepared by the method
described above.

Still another embodiment of this invention relates
to a method for the conversion of synthesis gas comprising:

0 contacting synthesis gas which comprises hydrogen
and carbon monoxide with a catalytically effective amount of
the silicate compositions described above under conversion
conditions effective to provide ethane at a carbon
selectivity of at least 40%.

5 This invention relates to a method of preparing
aluminosilicates and the catalytic conversion of synthesis
gas utilizing these aluminosilicates to C₂₋₄ alkanes, with
high selectivity for ethane.

10 Zeolitic materials, both natural and synthetic, in
naturally occurring and modified forms have been demonstrated
as having catalytic capabilities for hydrocarbon conversion.
Such zeolitic materials are ordered crystalline aluminosilicates
having definite crystalline structure within which
there are passages, pores, or cavities of definite ranges of
sizes. Since the dimensions of these pores are such as to
accept for adsorption molecules of certain dimensions while
15 rejecting those of larger dimension, these materials have
been referred to as "molecular sieves" and utilized in many
ways taking advantage of these properties.

20 The aluminosilicates of this invention may be
prepared by incorporating platinum or palladium onto various
known zeolites. Platinum is the preferred species because of
the improved catalyst stability it provides. The
incorporation of either metal may be achieved by
ion-exchange or impregnation.

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1 Ion-exchange techniques known to those in the art
may be utilized. For example, typical ion-exchange
techniques include contacting the aluminosilicates with a
salt solution of the desired replacing cation or cations.
5 Although, a wide variety of salts can be employed, particular
preference is given to chlorides, nitrates and sulfates.

Representative ion-exchange techniques are
disclosed in a wide variety of patents including U.S. Patent
Nos. 3,140,249, 3,140,251 and 3,140,253, which are
10 incorporated herein by reference.

Alternatively, platinum or palladium may be
impregnated into the aluminosilicate by the addition of an
ammonia solution or an aqueous solution of an appropriate
platinum or palladium salt. The ammonia solvent which is
15 used may be liquid ammonia or aqueous ammonia containing
greater than 50 weight percent ammonia. Prior to
impregnation with either solution, the aluminosilicate
should, if necessary, be calcined at about 300°C to about
600°C for at least 4 hours in air or an inert atmosphere to
20 drive off any organic cations which remain after formation of
the aluminosilicate and which would tend to block the pore
structure of the aluminosilicate.

Addition of the ammonia solvent dissolves the
platinum or palladium and the resulting solution is added
25 to the aluminosilicate. To complete the impregnation, the
aluminosilicate is dried, generally under mild conditions, to
drive off the solvent and fix the platinum or palladium on
the aluminosilicate. Temperatures of up to about 200°C,
preferably about 110°C to about 130°C are suitable for this
30 purpose.

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The percent by weight of platinum or palladium that is used to ion-exchange or impregnate the aluminosilicate significantly affects the catalytic activity, stability and selectivity for C₂-C₃ alkanes in the conversion of synthesis gas. The percent by wt. of platinum or palladium present in the aluminosilicate should be about 0.1% wt. to about 10% wt., with about 0.2 % wt. to about 5.0 % wt. being preferred. The aluminosilicate must have at least 0.1 % wt. of platinum or palladium present in the composition in order to obtain good selectivity and stability for the conversion of synthesis gas to C₂₋₄ alkanes.

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Various metals may be ion-exchanged or alternatively impregnated onto the aluminosilicates in accordance with this invention. Group VIII metals are intended to be included in the scope of this invention, with platinum and palladium being preferred and platinum being specifically preferred. The description herein will utilize platinum for illustrative purposes.

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The aluminosilicates that are prepared in accordance with the present invention and used in the conversion of synthesis gas are known in the art. The term aluminosilicate is meant to include synthetically produced and naturally occurring aluminosilicates. The aluminosilicates intended to be included in the scope of this invention include ZSM-5, ZSM-11, ZSM-34, ZSM-38, chabazite, erionite, and of which ZSM-5, and chabazite are preferred.

ZSM-5 is fully disclosed in U.S. Patent No. 3,702,886, the disclosure of which is herein incorporated by reference.

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ZSM-11 is more particularly described in U.S. Patent No. 3,702,979, the entire contents of which are herein incorporated by reference.

1 ZSM-12 is more particularly described in U.S.
Patent No. 3,832,449, the entire contents of which are being
incorporated by reference.

5 ZSM-38 is described in U.S. Patent No. 4,016,859,
the entire contents of which are incorporated herein by
reference.

10 Platinum or palladium exchanging the alumino-
silicates in accordance with the present invention affects
the selectivity and stability of the aluminosilicates in the
conversion of synthesis gas to low molecular weight C_2-C_3
alkanes.

15 In an optional embodiment of this invention, the
physical mixing of commercially available methanol synthesis
catalysts, such as for example, a copper oxide-zinc oxide or
a chromium oxide-zinc oxide catalyst with the platinum
aluminosilicate increases the catalytic conversion of
20 synthesis gas to C_{2-3} alkanes. The copper-zinc catalyst
available from United Catalyst Inc. under the designation
"Cl8HC", has a high activity and its composition is a 1:1
ratio of ZnO to CuO plus 10% alumina. The chromium-zinc
25 catalyst, available from Harshaw Chemical Co. under the
designation "Zn-0312 T," is composed of 74% ZnO, 21% chromium
oxide and 600 parts per million of aluminum. High
hydrocarbon yields result when the methanol synthesis
catalyst is added in a weight ratio of about 0.1 to 10
preferably about 0.3 to 5, in relation to the amount of
platinum aluminosilicate.

30 The methanol synthesis catalyst may be physically
mixed with the platinum aluminosilicate composition by any
known method, such as for example, blending, ultrasonic
mixing and the like.

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1 After the aluminosilicates of this invention are
impregnated or ion-exchanged with platinum or palladium, they
are heat treated, i.e., calcined, in air at about 300°C to
about 600°C for at least 4 hours, typically at 540°C for 4
5 hours, and then cooled to ambient temperature. The
aluminosilicates are then subjected to a hydrogen treatment
during which the treating temperature is increased from
ambient conditions to about 200°C to about 500°C, preferably
about 300°C to about 400°C. The rate of temperature increase
must be controlled. A temperature increase of about 0.1°C to
10 about 5.0°C per minute with a temperature increase of about
0.5°C to 2.0°C per minute being preferred. After reaching the
desired temperature, the composition is maintained at this
temperature for about 0.5 to about 4 hours, preferably about
0.75 hour to about 1.25 hour. The composition is then cooled
15 to ambient temperature in the presence of an inert gas or
hydrogen. The treatment of the composition with hydrogen
during the heat treatment and cooling steps increases the
C₂₋₃ alkane selectivity and activity when the composition is
employed in the conversion of synthesis gas to low molecular
20 weight hydrocarbons.

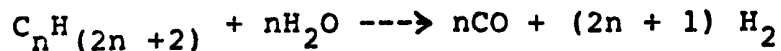
The present invention provides physical mixtures of
crystalline aluminosilicates and methanol synthesis catalysts
which exhibit superior catalytic activity for the highly
selective conversion of synthesis gas (carbon monoxide and
25 hydrogen) to low molecular weight hydrocarbons (C₂-C₃
alkanes). Moreover, these compositions of the present
invention maintain their catalytic activity and high
selectivity over relatively long periods of time. An
advantage of this process is that any water formed reacts
30 with the CO in the water gas shift reaction to provide

1 additional quantities of hydrogen. For this reason there is
little need to employ a water gas shifted synthesis gas as
the feed in the process of this invention.

5 Synthesis gas is provided commercially by such well
known processes as the steam reforming of naphtha or natural
gas or the partial oxidation of carbonaceous materials, such
as coal or heavy petroleum distillates. The reactions
involved are:

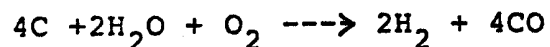
Stream Reforming:

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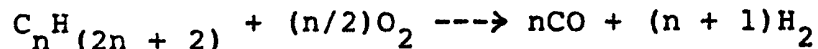
Partial Oxidation

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or

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The process for conversion of mixtures of gaseous
carbon monoxide and hydrogen in the presence of an effective
amount of the compositions of the present invention is
conveniently conducted at a temperature in the range of about
250° to about 500°C, normally 325°-500°C, a pressure in the
range of about 0 psig (101 kPa) to about 1500 psig (10,442
kPa), preferably 50 psig (446 kPa)-1000 psig (6995 kPa), in a
batch or flow reactor system. The volume ratio of carbon
monoxide to hydrogen is conveniently in the range of 0.5:1 to
about 6:1, normally about 1:1.

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The process of the present invention is conducted for a time sufficient to form a product mixture containing methane, C₂-C₆ alkenes and alkanes, carbon dioxide, water and less than 5.0% alcohols and ethers. The product mixture may be entrapped in a suitable trapping means such as a condenser and thereafter separated by standard techniques, e.g., distillation. For example, when utilizing the subject process in a batch-wise fashion, contact times of about 0.1 to about 3.0, preferably about 0.5 to about 2 minutes are found to be effective. When reacting the subject process continuously, space velocities of about 0.1 to about 20, preferably about 0.5 to about 10 weight hourly space velocity (WHSV) should be utilized.

The activity of the compositions of the present invention is achieved at temperatures of about 325°-450°C. Furthermore, the composition deactivates faster at temperatures of about 450°C to about 500°C. The activity of the composition is decreased at temperatures of about 300°C to about 325°C. Temperatures in the range of about 325°C to about 450°C were preferred for maximizing catalytic activity, service lifetime and selectivity to C₂-C₄ alkanes.

The process of the present invention can be operated in batch or continuous mode. A continuous flow reactor minimizes secondary reactions of initially formed products and extends the service lifetime of the composition.

Synthetic crystalline aluminosilicate compositions of this invention, when evaluated for catalytic properties without having been calcined, are inactive, possibly because the intracrystalline free space is occupied by organic cations from the forming solution. They may, however, be activated by heat treatment using known techniques such as heating in an inert atmosphere or air at 200°-900°C, for 1 to

1 60 hours. This may be followed by ion-exchange with ammonium
salts and further heat treatment at 200°-900°C, if desired.
Typical ion-exchange techniques as described above may be
employed to platinum or palladium exchange the
5 aluminosilicate.

Regardless of the cations replacing the sodium in
the synthesized form of the compositions, the spatial
arrangement of the atoms which form the basic crystal
lattices in any given composition of this invention remain
essentially unchanged by the described replacement of sodium
10 or other alkali metal as determined by taking an X-ray powder
diffraction pattern of the ion-exchanged material.

The aluminosilicate compositions prepared by the
instant invention are formed in a wide variety of particular
sizes. Generally speaking, the particles can be in the form
15 of a powder, a granule, or a molded product, such as
extrudate having a particle size sufficient to pass through a
2 mesh (Tyler) screen and be retained on a 100 mesh (Tyler)
screen. In cases where the composition is molded, such by
20 extrusion, the composition can be extruded before drying or
dried or partially dried and then extruded.

In the case of the mixtures of methanol synthesis
catalyst and platinum aluminosilicate the mixing can occur
before or after the extrusion process. It should be
25 remembered that where the methanol synthesis catalyst is
present before the heat treatment, the treatment conditions
should be chosen not to adversely affect the methanol
synthesis catalyst.

In the case of many catalysts, it is desired to
30 incorporate the aluminosilicate composition of this invention
with another material resistant to the temperatures and other
conditions employed in organic conversion processes. Such

1 materials include active and inactive materials and synthetic
or naturally occurring crystalline compositions as well as
inorganic materials such as clays, silica and/or metal
oxides. The latter may be either naturally occurring or in
5 the form of gelatinous precipitates or gels including
mixtures of silica and metal oxides. Use of these materials
in conjunction with the present composition tends to improve
the conversion and/or selectivity of the catalyst in certain
organic conversion processes. Inactive materials suitably
0 serve as diluents to control the amount of conversion in a
given process so that products can be obtained economically
and in an orderly manner without employing other means for
controlling the rate of reaction. Normally, zeolite
5 materials have been incorporated into naturally occurring
clays, e.g., bentonite and kaolin, to improve the crush
strength of the composition under commercial operating
conditions. These materials, e.g., clays, oxides, etc.
function as binders for the composition. It is desirable to
provide a composition having good crush strength, because in
0 a chemical process the composition is often subjected to
handling or use which tends to break the composition down
into powder-like materials which cause problems in
processing. These clay binders have been employed for the
purpose of improving the crush strength of the composition.

5 In addition to the foregoing materials, the
aluminosilicate can be composited with a porous matrix
material such as silica-alumina, silica-magnesia,
silica-zirconia, silica-thoria, silica-beryllia,
silica-titania as well as ternary compositions such as
0 silica-alumina-thoria, silica alumina-zirconia,
silica-alumina-magnesia and silica- magnesia-zirconia. The
matrix can be in the form of a cogel.

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The following examples are presented as specific
embodiments of the present invention and show some of the
unique characteristics of the claimed crystalline
compositions and are not to be considered as constituting a
limitation on the present invention.

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EXAMPLE 1

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A. Ion Exchange1. NH_4^+ or H^+ Chabazite

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25 grams of aluminosilicate (Linde AW500 Chabazite) were added to a solution of 15 grams NH_4Cl dissolved in 400 ml deionized water and refluxed for 16 hours. The solution was then decanted and additional solution containing 15 grams NH_4Cl dissolved in 400 ml deionized water were added. After 4 hours of reflux the solid was washed by repetitive

10 decantation and isolated by filtration. Drying at 110°C overnight yielded NH_4^+ - chabazite. If the H^+ form was desired, the NH_4^+ form was calcined at 540°C in air or inert gas for 4 hours.

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2. Pt-Chabazite

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A 25 gram sample of NH_4^+ -Chabazite aluminosilicate was added to a solution containing 0.53 gram Pt $(\text{NH}_3)_4\text{Cl}_2$ (56.15%Pt) dissolved in 400 ml deionized water. After being stirred at reflux for 16 hours, the solution was decanted and another charge of $\text{Pt}(\text{NH}_3)_4\text{Cl}_2$ and water was added, followed by stirring at reflux for 4 hours. After cooling the solid was washed by repeated decantation with water, collected by filtration, and dried overnight at 110°C .

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B. Catalyst Pretreatment

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Before charging Pt-aluminosilicate to the reactor, the preferred pretreatment was to calcine 25 grams of platinum- aluminosilicate in air at 540°C . for 4 hours and then cool to ambient temperature. The calcined solid was treated with 5% hydrogen in nitrogen at a temperature program of $1^\circ\text{C}/\text{minute}$ to 350°C and held for 1 hour. The catalyst was then cooled to ambient temperature in 5% hydrogen.

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1 C. Physical Mixture

The Pt-aluminosilicate was physically mixed with a methanol synthesis catalyst (Harshaw's Zn-0312 T). Typically, 3 ml (4.1 grams) of the Cr-Zn methanol synthesis catalyst were added to the 6 ml (3.2 grams) of platinum-chabazite. The mixture was blended and charged to the reactor.

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EXAMPLE 2

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A physical mixture of a platinum - ZSM-5 and a
methanol synthesis catalyst was prepared in accordance with
5 the procedure of Example 1 except that ZSM-5 was substituted
for chabazite.

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EXAMPLE 3

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This example compares the catalytic activities of platinum chabazite (platinum exchanged ammonium form of Linde AW500), a Cr-Zn methanol synthesis catalyst (Harshaw's Zn-0312 T), Cr-Zn followed by Pt-AW500, and a physical mixture of these two materials. The platinum compositions were prepared in accordance with Example 1 and all runs were conducted at 735 psig (5169 kPa) in a 310 stainless steel tubular reactor.

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TABLE III
SYNGAS REACTIONS (1)

Catalyst (2)	Cr-Zn	Pt-AW500	Cr-Zn(3) Pt-AW500	Cr-Zn Pt-AW500 (physical mixture)
<u>HC Yield, % (4)</u>	5	5	11	40
<u>HC Sel., % (4)</u>				
C ₁	69	21	22	10
C ₂	27	46	44	53
C ₃	4	33	31	33
C ₄	0	0	4	5
C ₅₊	0	0	0	0
Ar	0	0	0	0
<u>CO₂ Yield, % (4)</u>	5	4	9	36
<u>CO Conv., % (4)</u>	11	9	20	76

(1) 400°C, H₂/CO = 1,735 psig (5169 kPa), 9.86 l/h STP.

(2) 3 ml Cr-Zn, Harshaw Zn-0312 T and/or
6 ml Pt-AW500, Pt exchanged NH₄⁺ AW500, prepared from
Linde AW500.

(3) Cr-Zn followed by 1/2" glass wool followed by Pt-AW500.

(4) Based on carbon.

The data show that the physically mixed Cr-Zn/-
Pt-AW500 composition of the present invention has a higher
carbon monoxide conversion and the highest C₂ selectivity for
the conversion of synthesis gas. Both the Cr-Zn and the
Pt-AW500 catalysts show low carbon monoxide conversion, with
the layered Cr-Zn/Pt-AW500 composition demonstrating a CO
conversion equal to the sum of the conversion of the Cr-Zn
and Pt-AW500 catalysts.

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EXAMPLE 4

This example shows the effect of incorporating
5 platinum onto chabazite (AW500) which is physically mixed
with a Cr-Zn methanol synthesis catalyst for the conversion
of synthesis gas. Both compositions were prepared in
accordance with Example 1 and only differ in Pt content. All
runs were conducted at 735 psig (5169 kPa) in a 310 stainless
10 steel tubular reactor at an actual hourly space velocity of
60.

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TABLE IV
SYNGAS REACTIONS
EFFECT OF PLATINUM ON AW500 MIXED WITH CHROMIUM-ZINC

Pt, wt. %	0					2.0							
Time on Stream, hrs.	4	24	29	98	101	2	22	26	46	51	70	74	92
HC Yield, % (2)	32	20	19	14	14	42	41	40	40	39	39	39	38
HC Sel., % (2)													
C ₁	13	19	20	23	26	12	10	10	10	9	9	9	9
C ₂	25	38	40	44	43	50	47	48	46	46	45	47	46
C ₃	50	31	30	29	28	34	38	37	39	40	40	39	39
C ₄	7	8	7	3	3	4	5	5	5	5	5	5	6
C ₅₊ & Ar	5	5	4	0	0	0	0	0	0	0	0	0	0
CO ₂ Yield, % (2)	31	19	18	14	14	35	34	33	32	33	32	33	33
CO Conv., %	63	39	37	28	28	75	75	73	72	72	71	72	71

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(1) 400°C, H₂/CO=1, 735 psig (5169 kPa), Actual Hourly
Space Velocity=60

(2) Based on carbon.

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The data show that platinum-exchanged AW500 which is mixed with Cr-Zn provides improved catalytic stability, higher C₂ selectivity, and higher hydrocarbon yield for synthesis gas conversion than the H⁺-AW500 (prior art type) composition.

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This example compares the effect of the platinum content on the catalytic properties of physically mixed Cr-Zn/AW500 compositions for the conversion of synthesis gas. All of the compositions were prepared in accordance with Example 1, except that platinum was impregnated onto the NH_4^+ form of the compositions with aqueous $\text{Pt}(\text{NH}_3)_4\text{Cl}_2$. All runs were conducted at 735 psig (5169 kPa) in a 310 stainless steel tubular reactor at an actual hourly space velocity of 50.

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TABLE V A
SYNGAS REACTIONS
THE EFFECT OF PLATINUM CONTENT IN PT-AW500 MIXED WITH
CHROMIUM-ZINC(1)

5	Pt, Wt.%(2)	0.2						0.5					
	Time, hrs.	3	26	45	50	70	74	3	20	25	45	49	68
	HC Yield, %(4)	35	33	28	27	25	24	36	33	34	33	33	32
10	HC Sel., %(4)												
	C ₁	6	7	10	10	11	12	6	7	8	8	8	8
	C ₂	31	27	35	36	38	38	36	36	36	36	36	36
	C ₃	56	58	48	48	45	44	52	51	50	50	49	49
	C ₄	7	7	6	6	5	5	6	6	6	6	6	6
15	C ₅₊	0	0	0	0	0	0	0	0	0	0	0	0
	Ar	0	0	0	0	0	0	0	0	0	0	0	0
	CO ₂ Yield, %(4)	31	30	26	25	23	24	30	31	28	27	27	26
	CO Conv., %	66	63	54	52	48	48	66	64	62	60	60	58

- 20 (1) 400°C, H₂/CO = 1, 735 psig (5169 kPa), Actual Hourly Space Velocity = 50.
- (2) Nominal Values, Pt impregnated NH₄⁺- AW500.
- (3) All catalysts mixed with Harshaw Cr-Zn weight ratio: Cr-Zn/Pt-AW500 = 1.3.
- 25 (4) Based on carbon.

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TABLE V B
SYNGAS REACTIONS
THE EFFECT OF PLATINUM CONTENT IN PT-AW500 MIXED WITH
CHROMIUM-ZINC

Pt, wt.%(2)	1.0						2.0					
Time, hrs.	3	22	26	45	50	68	3	22	26	45	50	68
HC Yield, %(4)	30	28	28	27	27	26	35	33	33	32	31	30
HC Sel., %(4)												
C ₁	6	7	8	8	8	8	6	6	6	7	6	7
C ₂	39	37	38	37	36	36	47	45	46	45	46	46
C ₃	49	49	48	49	49	49	42	43	42	42	42	42
C ₄	6	7	6	7	7	6	5	5	5	6	5	6
C ₅₊	0	0	0	0	0	0	0	0	0	0	0	0
Ar	0	0	0	0	0	0	0	0	0	0	0	0
CO ₂ Yield, %(4)	27	24	24	23	24	23	30	28	28	27	27	26
CO Conv., %	57	52	52	50	51	49	65	61	61	59	58	56

- (1) 400°C H₂/CO = 1, 735 psig (5169 kPa), Actual Hourly Space Velocity = 50.
- (2) Nominal Values, Pt impregnated NH₄⁺- AW500.
- (3) All catalysts mixed with Harshaw Cr-Zn weight ratio: Cr-Zn/Pt-AW500 = 1.3.
- (4) Based on carbon.

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TABLE V C
SYNGAS REACTION
THE EFFECT OF PLATINUM CONTENT ON Pt-AW500 MIXED WITH
CHROMIUM-ZINC (1)

5 Pt, wt.%(2)	3.0						3.0					
Time, hrs.	3	20	25	45	49	68	4	23	27	46	51	69
HC Yield, %(4)	30	26	26	24	24	22	34	32	31	30	30	29
HC Sel., %(4)												
10 C ₁	7	8	8	10	10	10	7	7	7	8	8	7
C ₂	39	41	41	41	42	42	47	45	44	44	45	45
C ₃	48	46	44	43	43	41	41	43	42	43	42	43
C ₄	6	6	6	6	6	6	5	6	6	6	6	6
C ₅₊	0	0	0	0	0	0	0	0	0	0	0	0
15 Ar	0	0	0	0	0	0	0	0	0	0	0	0
CO ₂ Yield, %(4)	24	22	21	20	20	19	29	27	26	25	25	24
CO Conv., %	54	48	47	44	44	44	63	59	57	55	55	53

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(1) 400°C, H₂/CO=1, 735 psig (5169 kPa), Actual Hourly Space Velocity = 50.

(2) Nominal Values, Pt impregnated NH₄⁺- AW500.

(3) All catalysts mixed with Harshaw Cr-Zn Weight ratio: Cr-Zn/Pt AW500 = 1.3.

(4) Based on carbon.

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The data show that all of the compositions have high C₂₋₃ selectivity for the conversion of synthesis gas. Further, all compositions have higher C₂₋₃ selectivity and better stability than platinum free compositions (See Table

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This example compares the effect of different weight ratios of chromium-zinc and platinum-AW500 on the catalytic properties of compositions of the present invention for the conversion of synthesis gas. All catalysts contain 5 equivalent amounts of Pt-AW500 and the syngas feed rate was constant. However total catalyst volume varied with the amount of methanol catalyst added. All of the compositions were prepared in accordance with Example 1 and all runs were 0 conducted at 735 psig (5169 kPa) in a 310 stainless steel tubular reactor.

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TABLE VI A
SYNGAS REACTIONS
THE EFFECT OF Zn-Cr/Pt AW500 RATIO (1)

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Weight Ratio		<u>0.3</u>				<u>0.7</u>		
Zn-Cr/Pt-AW500								
	Time, hrs	3	21	26	44	3	25	43
	HC Yield %	23	22	23	22	31	30	28
	HC Sel., %(2)							
10	C ₁	10	9	12	8	8	8	6
	C ₂	47	45	44	46	47	46	45
	C ₃	38	41	40	42	40	41	43
	C ₄	4	4	4	4	5	5	4
	C ₅₊ & Ar	0	0	0	0	0	0	0
15	CO ₂ Yield, %(2)	19	18	18	18	26	24	24
	CO Conversion, %	42	40	41	40	57	54	52

(1) 400°C, H₂/CO = 1, 735 psig (5169 kPa), Actual Space Velocity = 65.

(2) Based on carbon.

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TABLE VI B

SYNGAS REACTIONSTHE EFFECT OF Cr-Zn/Pt-AW500 RATIO (1)

Weight Ratio		<u>1.3</u>					<u>1.9</u>			
5	Cr-Zn/Pt-AW500									
	Time, hrs	3	22	26	46	50	3	21	25	43
	HC Yield, %(2)	39	36	36	35	35	42	41	39	39
	HC Sel., %(2)									
	C ₁	9	8	7	7	7	8	9	7	8
10	C ₂	49	46	46	45	43	49	46	46	43
	C ₃	37	41	41	43	44	39	40	41	43
	C ₄	5	5	5	5	5	5	5	6	6
	C ₅₊ & Ar	0	0	0	0	0	0	0	0	0
	CO ₂ Yield, %(2)	32	31	30	29	29	35	33	32	0
15	CO conversion, %	71	67	66	64	64	77	74	71	69

(1) 400°C, H₂/CO = 1, 735 psig, Actual Hourly Space Velocity = 40-50.

(2) Based on carbon.

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TABLE VI C
SYNGAS REACTIONS
THE EFFECT OF Cr-Zn/Pt-AW500 RATIO(1)

5		Weight Ratio				
Cr-Zn/Pt-AW500		2.6				
	Time, Hrs.	3	21	26	44	49
	HC Yield, %(2)	47	45	44	43	43
	HC Sel., %(2)					
10	C ₁	8	6	7	7	7
	C ₂	51	48	47	47	47
	C ₃	37	41	41	41	41
	C ₄	4	4	5	5	5
	C ₅₊ & Ar	0	0	0	0	0
15	CO ₂ Yield, %(2)	38	37	38	37	37
	CO conversion, %	.85	82	82	80	80

(1) 400°C, H₂/CO = 1, 735 psig (5169 kPa), Actual Hourly Space Velocity = 50.

(2) Based on carbon.

The data show that the weight ratio of Cr-Zn and Pt-AW500 has little effect on the C₂₋₃ selectivity for the conversion of synthesis gas. However, CO conversion increased as the amount of methanol catalyst (Cr-Zn) is increased. (See Table VI A - compositions having a Zn-Cr/Pt-AW500 ratio of 0.3 versus Table VI C - compositions having a Zn-Cr/Pt-AW500 of 2.6.)

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This example compares the effect of various methanol catalysts on the catalytic properties of the compositions of the present invention for the conversion of synthesis gas. All of the compositions were prepared in accordance with Example 1 and all runs were conducted at 735 psig (5169 kPa) in a 310 stainless steel tubular reactor at an actual hourly space velocity of 80.

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TABLE VII
SYNGAS REACTIONS
VARIOUS METHANOL CATALYSTS MIXED WITH Pt-AW500

Catalyst	<u>HC Yield, %</u>	<u>C₂H₆ Sel., %</u>
Cu-Zn (UCI C18HC)	24	47
Cu-Zn (COS treated)	15	53
Cu-Cr	29	41
Cu-Co-Cr	23	26
Control (Pt-AW500 alone)	5	46

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400°C, H₂/CO = 1, 735 psig (5169 kPa), Actual Hourly
Space Velocity 80.

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The data show methanol synthesis catalysts other
than Cr-Zn that enhance the catalytic properties of
Pt-chabazite.

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5 This example compares the effect of reaction
temperatures on the catalytic properties and C₂ selectivity
of a physically mixed composition of the present invention
for the conversion of synthesis gas. The composition was
prepared in accordance with Example 1, except that NH₄⁺-AW500
zeolite was impregnated with aqueous Pt (NH₃)₄Cl₂. All runs
were conducted at 735 psig (5169 kPa) in a 310 stainless
10 steel tubular reactor at an actual hourly space velocity of
50.

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TABLE VIII

EFFECT OF REACTION TEMPERATURE
ON Cr-Zn/Pt-AW500 FOR SYNGAS CONVERSION

Temp, °C	350	400	450
CO Conv., %.	41	52	53
HC Yield, %.	20	29	29
HC Sel., %.			
C ₁	11	5	8
C ₂	30	37	46
C ₃	50	51	42

H₂/CO = 1, 735 psig (5169 kPa), Actual Hourly Space Velocity = 50.

The data show that a Cr-Zn physically mixed Pt-AW500 composition has a higher C₂ selectivity as the reaction temperature is increased. Compare test data prepared at 350°C versus 450°C.

EXAMPLE 9

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This example compares the effect of the H₂/CO molar ratio on the catalytic properties of a composition of the present invention for the conversion of synthesis gas. The composition was prepared in accordance with Example 1 and all runs were conducted at 735 psig (5169 kPa) in a 310 stainless steel tubular reactor at an actual hourly space velocity of 50.

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TABLE IX
SYNGAS REACTIONS

THE EFFECT OF HYDROGEN-CARBON MONOXIDE RATIO ON Cr-Zn/Pt
AW500 MIXTURES (1)

H ₂ /CO, molar	0.5				1.0					2.0		
Time, hrs.	4	23	27	46	3	22	26	46	50	3	22	26
HC Yield, %(2)	26	21	20	17	39	36	36	35	35	49	44	43
HC Sel., %(2)												
C ₁	8	9	11	12	9	8	7	7	7	12	8	9
C ₂	53	52	50	51	49	46	46	45	43	44	45	44
C ₃	36	35	34	33	37	41	41	43	44	38	40	41
C ₄	3	4	5	3	5	5	5	5	5	6	7	7
C ₅₊	0	0	0	0	0	0	0	0	0	0	0	0
Ar	0	0	0	0	0	0	0	0	0	0	0	0
CO ₂ Yield, %(2)	24	20	18	16	32	31	30	29	29	32	32	32
CO Conv., %(2)	50	41	38	33	71	67	66	64	64	81	76	75

(1) 400°C, 735 psig (5169 kPa), Actual Hourly Space
Velocity = 50.

(2) Based on carbon.

The data show that as the molar ratio of H₂ to CO increases, the C₂ selectivity of the composition decreases. Compare the C₂ selectivity at a ratio of 0.5 versus the C₂ selectivity at a ratio of 2.0.

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The example compares the catalytic properties of a
prior art composition with a composition of the present
invention for the conversion of synthesis gas. All of the
5 compositions were prepared in accordance with Example 1,
except that ZSM-5 was used in place of AW500. All runs were
conducted at 735 psig (5169 kPa) in a 310 stainless steel
tubular reactor at an actual hourly space velocity of 50.

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TABLE X

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SYNGAS REACTIONSCr-Zn PHYSICAL MIXTURES WITH H⁺ OR Pd-ZSM-5(1)

5	Catalyst(2)	HZSM-5 (Prior Art Type)						Pd-ZSM-5			
	10	Time, hrs.	3	22	26	45	50	68	3	22	26
	HC Yield, %(3)	28	26	26	30	29	28	32	32	31	31
	HC Sel., %(3)										
	C ₁	7	7	8	6	6	7	9	7	7	8
	C ₂	14	11	12	10	10	10	44	33	33	32
	C ₃	39	35	33	27	28	28	41	44	45	47
	C ₄	13	18	16	20	21	21	5	9	9	9
	C ₅₊	4	8	10	20	21	21	0	3	3	2
	Ar	22	20	21	17	14	13	0	3	3	3
15	CO ₂ Yield, %(3)	29	29	29	27	27	27	29	28	28	28

(1) 400°C, H₂/CO = 1, 735 psig, Actual Hourly Space Velocity = 50.

(2) Molar Ratio: Cr:Zn:Al:Pd:ZSM-5(Al).

H ZSM-5 20:51:0.3:0:1.

Pd-ZSM-5 20:51:0.3:0.5:1.

(3) Based on Carbon.

The data show that palladium-exchange of ZSM-5 in accordance with the present invention gave a much higher C₂₋₃ selectivity than prior art (H⁺-ZSM-5) compositions.

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- 1 1. A method of preparing a crystalline
aluminosilicate composition which comprises:
- 5 (a) contacting a crystalline aluminosilicate with a
platinum or palladium salt solution to provide a platinum or
palladium crystalline aluminosilicate;
- (b) calcining the platinum or palladium
crystalline aluminosilicate in air at a temperature of about
300 °C to about 600 °C for at least 4 hours;
- 10 (c) heating the calcined palladium or platinum
aluminosilicate in the presence of hydrogen from ambient
temperature to an elevated temperature of about 300 °C to
about 400 °C at a rate of temperature increase of about 0.5
to about 2.0 °C per minute;
- 15 (d) maintaining said silicate at said temperature
for about 0.5 to about 4 hours; and
- (e) cooling said aluminosilicate to ambient
temperature in the presence of hydrogen.
- 20 2. A method as defined in Claim 1, wherein said
crystalline aluminosilicate is ZSM-5 or chabazite.
3. A method as defined in Claim 1 or 2, where in
step (a) said platinum or palladium salt solution is
ion-exchanged onto said crystalline aluminosilicate.
- 25 4. A method of Claim 1 or 2, where in step (a)
step platinum or palladium salt solution is impregnated onto
said crystalline aluminosilicate.
5. A method as defined in any of Claims 1 to 4
wherein in step (d) the temperature is maintained from 0.75
to 1.25 hours.
- 30 6. A method as defined in any of Claims 1 to 5,
including the following additional steps:

1 (f) mixing said aluminosilicate with a methanol
synthesis catalyst in a weight ratio of methanol synthesis
catalyst to aluminosilicate of about 0.3 to about 5.

5 7. A method as defined in Claim 6, wherein said
methanol synthesis catalyst comprises chromium oxide-zinc
oxide or copper oxide-zinc oxide.

8. A method as defined in any of Claims 1 to 7
wherein the resulting composition contains from 0.1% to 10%
by weight of palladium or platinum.

10 9. A crystalline aluminosilicate composition
prepared in accordance with the method of any of Claims 1 to
8.

15 10. A crystalline aluminosilicate composition when
prepared according to any of Claims 1 to 8 in catalytic
amounts for contacting synthesis gas containing hydrogen and
carbon monoxide under conversion conditions to provide ethane
at a carbon selectivity of at least 40%.

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DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 4)
A	CHEMICAL ABSTRACTS, vol. 93, no. 6, August 1980, page 217, abstract no. 50260a, Columbus, Ohio, US; & DD-A-136 345 (VEB LEUNA-WERKE "WALTER ULBRICHT") 04-07-1979 * Abstract; claim; pages 9-11; examples 1,2 *		B 01 J 29/32 C 07 C 1/04
A	--- US-A-4 429 175 (J.L. CIHONSKI) * Column 3, lines 12-52 *		
A	--- EP-A-0 145 289 (EXXON) * Page 28, line 19 - page 30, line 22 *		
			TECHNICAL FIELDS SEARCHED (Int. Cl. 4)
			B 01 J 29/00
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 16-10-1986	Examiner DEVISME F.R.
<p>CATEGORY OF CITED DOCUMENTS</p> <p>X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document</p> <p>T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document</p>			