

10-8

100132

743

Item #16

### Computation of combustion temperatures of mixtures consisting of H<sub>2</sub>S and CO<sub>2</sub>

#### Presumptions

Net calorific value of H<sub>2</sub>S = 5587 kg. cal./m<sup>3</sup>, 0°C./760mm Hg  
 True specific heats according to table 4 of gas constants, Eckhard-Kah. Gases before the combustion are free from water, volume 0'. 760 mm. of Hg. No formation of SO<sub>3</sub>.  
 Such an excess of air that the dry combustion gases contain 1% oxygen.  
 Oxygen content of the air: 20.9%

#### Combustion temperatures

##### 1. H<sub>2</sub>S-CO<sub>2</sub> mixture with 20% H<sub>2</sub>S

from 200 vol. H<sub>2</sub>S  
 800 " CO<sub>2</sub>  
 and 1540 " air

are obtained:

- 200 vol. SO<sub>2</sub> = 8.2%
- 200 " H<sub>2</sub>O = 8.2%
- 800 " CO<sub>2</sub> = 32.8%
- 1218 " N<sub>2</sub> = 49.9%
- 22 " O<sub>2</sub> = 0.9% = 1% in the dry gas mixture.

Total 2,440 vol. moist combustion gases or 100 vol. H<sub>2</sub>S generate 1,220 vol. combustion gases.

For such a composition of the combustion gases the true specific heat at 1200°C. is:

$$\frac{(8.2 \times 0.583) + (8.2 \times 0.443) + (32.8 \times 0.583) + (50.8 \times 0.337)}{100} =$$

0.446 kg. cal./Nm<sup>3</sup>

The temperature increase of the gases is  $\frac{100 \times 5,587}{1,220 \times 0.446} = 1,023^{\circ}\text{C}.$

##### 2. H<sub>2</sub>S-CO<sub>2</sub> mixture with 40% H<sub>2</sub>S

From 400 vol. H<sub>2</sub>S, 600 vol. CO<sub>2</sub> and 3,038 vol. air are obtained:

- 400 vol. SO<sub>2</sub> = 10.4%
- 400 " H<sub>2</sub>O = 10.4%
- 600 " CO<sub>2</sub> = 15.6%
- 403 " H<sub>2</sub> = 62.7%
- 35 " O<sub>2</sub> = 0.9% = 1.0% in the dry combustion gases.

Total 3,838 vol. moist combustion gases, or 100 vol. H<sub>2</sub>S generate 960 vol. combustion gases.

For such a composition the true spec. heat at 1,300°C. is

$$\frac{(10.4 \times 0.629) + (10.4 \times 0.489) + (15.6 \times 0.629) + (63.6 \times 0.352)}{100} =$$

0.438 kcal/Nm<sup>3</sup>

The temperature increase is  $\frac{100 \times 5,587}{960 \times 0.438} = 1,325^{\circ}\text{C}.$

##### 3. H<sub>2</sub>S-CO<sub>2</sub> mixture with 60% H<sub>2</sub>S

From 600 vol. H<sub>2</sub>S, 400 vol. CO<sub>2</sub> and 4,520 vol. air are obtained:

- 600 vol. SO<sub>2</sub> = 11.5%

600 vol. H<sub>2</sub>O = 11.5%  
 400 " CO<sub>2</sub> = 7.7%  
 3574 " N<sub>2</sub> = 68.4%  
 46 " O<sub>2</sub> = 0.9% = 1.0% in the dry combustion gases

Total 5,220 vol. moist combustion gases, or 100 vol. H<sub>2</sub>S generate 870 vol. combustion gases.

For such a composition the true spec. heat at 1,450°C. is 0.437 k.g. cal. per Nm<sup>3</sup>.

The temperature increase is  $\frac{100 \times 5,587}{870 \times 0.437} = 1,468^{\circ}\text{C}.$

4. H<sub>2</sub>S=CO<sub>2</sub> mixture with 80% H<sub>2</sub>S

From 800 vol. H<sub>2</sub>S, 200 vol. CO<sub>2</sub>, and 6,020 vol. air are obtained:

800 vol. SO<sub>2</sub> = 12.1%  
 800 vol. H<sub>2</sub>O = 12.1%  
 200 vol. CO<sub>2</sub> = 3.0%  
 4763 vol. N<sub>2</sub> = 72.0%  
 57 vol. O<sub>2</sub> = 0.8% = 1.0% of the dry combustion gases

Total 6,620 vol. moist combustion gases, or 100 vol. H<sub>2</sub>S generate 828 vol. combustion gases.

For such a composition the true spec. heat at 1,550°C. = 0.436 k. cal. per Nm<sup>3</sup>.

The temperature increase of the combustion gases is 1,547°C.

5. 100% H<sub>2</sub>S

From 1000 vol. H<sub>2</sub>S and 7,520 vol. air are obtained:

1000 vol. SO<sub>2</sub> = 12.45%  
 1000 vol. H<sub>2</sub>O = 12.45%  
 5950 vol. N<sub>2</sub> = 74.20%  
 70 vol. O<sub>2</sub> = 0.90% = 1.0% of the dry combustion gases.

Total 8,020 vol. moist combustion gases or 100 vol. H<sub>2</sub>S generate 802 vol. combustion gases. For such a composition the true spec. heat at 1,600°C. is 0.433 k.cal./Nm<sup>3</sup>.

The temperature increase of the combustion gases is

$$\frac{100 \times 5587}{802 \times 0.433} = 1,610^{\circ}\text{C}.$$

COMBUSTION TEMPERATURES OF  
 $H_2S - CO_2$  MIXTURES  
(FOR THE CLAUSS REACTION)

