

Nr.

## Drucksynthese D.-V.-A.

Ofen-Nr. 111

Füllung 13

Dat. 6. 2. 8. 43

Zeit

Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,40         | 34,5           | 50,1                   | 38,3                                 | 36,4                  |
| Kondens.-Öl    | 5,70         | 44,6           | 57,4                   | 43,8                                 | 34,0                  |
| Paraffingatsch | 2,62         | 20,9           | 33,5                   | 17,9                                 | 15,9                  |
|                | 12,72        | 100,0          | 131,0                  | 100,0                                | 76,3                  |

|  | AK-Benzin         | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |   |
|--|-------------------|---------|---------------------|----------------|--------|----------------------|---|
|  | Vol. %            | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |   |
| 1  | 2                 | 3       | 4                   | 5              | 6      | 7                    | 8 |
| Dichte bei 20 °C   | 0,690             | 0,714   | 0,89                |                |        | 0,998                |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. %    |                   |         |                     |                |        |                      |   |
| Jodzahl (Wijss)  |                   |         |                     |                |        |                      |   |
| N.Z. / V.Z.  |                   |         |                     |                |        |                      |   |
| Siede-Analyse  | Siedebeginn °C    |         |                     |                | 4%     |                      |   |
|  | — 40              |         |                     |                |        |                      |   |
|  | 60                |         |                     |                | 6,0    |                      |   |
|  | 80                |         |                     |                | 13,0   |                      |   |
|  | 100               |         |                     |                | 21,0   |                      |   |
|  | 120               |         |                     |                | 29,0   | 51,1                 |   |
|  | 140               |         |                     |                | 37,0   |                      |   |
|  | 160               |         |                     |                | 44,0   |                      |   |
|  | 180               |         |                     |                | 50,0   |                      |   |
|  | 200               |         |                     |                | 55,0   |                      |   |
|  | 220               |         |                     |                | 59,0   |                      |   |
|  | 240               |         |                     |                | 62,0   |                      |   |
|  | 260               |         |                     |                | 65,0   |                      |   |
|  | 280               |         |                     |                | 68,0   | 23,5                 |   |
|  | 300               |         |                     |                | 70,0   |                      |   |
|  | 320               |         |                     |                | 72,0   |                      |   |
| 340  |                   |         |                     |                |        |                      |   |
| 360  |                   |         |                     |                |        |                      |   |
| Siede-Ende °C  |                   |         |                     |                |        | 85,0                 |   |
| Rückstand  |                   |         |                     |                |        | 0,4                  |   |
| Verlust  |                   |         |                     |                |        |                      |   |
| Stockpunkt °C  |                   |         |                     |                |        |                      |   |
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) |         |                     | 60             |        |                      |   |
|  | Öl (200—320°)     |         |                     | 40             |        |                      |   |

Bemerkungen:

00000

Nr.

# Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 13 Dat. 5.6.8.43 Zeit          Betr.Tage         

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 3,84      | 31,8       | 46,3                   | 35,4                                 | 34,3                  |
| Kondens.-Öl    | 5,40      | 45,2       | 52,6                   | 44,8                                 | 34,6                  |
| Paraffingatsch | 3,75      | 32,0       | 35,8                   | 19,8                                 | 17,6                  |
|                | 11,95     | 100,0      | 130,7                  | 100,0                                | 26,5                  |

|   | AK-Benzin      | Ölkond. | Paraffingatsch | Gesamt-Produkt |        | Reaktionswasser |   |
|---|----------------|---------|----------------|----------------|--------|-----------------|---|
|   | Vol. %         | Vol. %  | Vol. %         | Vol. %         | Vol. % | 7               | 8 |
| Dichte bei 20 °C  | 0,687          | 0,774   | 0,89           |                |        | 0,984           |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |                |         |                |                |        |                 |   |
| Jodzahl (Wijss)   |                |         |                |                |        |                 |   |
| N.Z. / V.Z.   |                |         |                |                |        |                 |   |
| Siede-Analyse   | Siedebeginn °C |         |                |                | 47     |                 |   |
|   | — 40           |         |                |                |        |                 |   |
|   | 60             |         |                |                | 5,0    |                 |   |
|   | 80             |         |                |                | 11,0   |                 |   |
|   | 100            |         |                |                | 19,0   |                 |   |
|   | 120            |         |                |                | 32,0   | 48,7            |   |
|   | 140            |         |                |                | 35,0   |                 |   |
|   | 160            |         |                |                | 41,0   |                 |   |
|   | 180            |         |                |                | 46,0   |                 |   |
|   | 200            |         |                |                | 50,0   |                 |   |
|   | 220            |         |                |                | 55,0   |                 |   |
|   | 240            |         |                |                | 62,0   |                 |   |
|   | 260            |         |                |                | 65,0   | 34,6            |   |
|   | 280            |         |                |                | 65,0   |                 |   |
|   | 300            |         |                |                | 65,0   |                 |   |
| 320   |                |         |                | 75,0           |        |                 |   |
| 340   |                |         |                |                |        |                 |   |
| 360   |                |         |                |                |        |                 |   |
| Siede-Ende °C   |                |         |                |                |        | 25,4            |   |
| Rückstand   |                |         |                |                |        | 2,2             |   |
| Verlust   |                |         |                |                |        |                 |   |
| Stockpunkt °C   |                |         |                |                |        |                 |   |

|  |                   |    |
|--|-------------------|----|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 60 |
|  | Öl (200-320°)     | 39 |

Bemerkungen:

000002

Nr.

**Drucksynthese D.-V.-A.**Ofen Nr. 11 Füllung 13 Dat. 4.8.43 Zeit Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | -g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|------------------------|
| A.K.-Benzin    | 4,58         | 36,8           | 53,6                   | 40,8                                 | 28,0                   |
| Kondens.-Öl    | 4,90         | 40,1           | 52,0                   | 39,6                                 | 30,6                   |
| Paraffingatsch | 2,81         | 23,1           | 25,7                   | 19,6                                 | 17,6                   |
|                | 12,29        | 100,0          | 131,3                  | 100,0                                | 26,2                   |

|   | AK-Benzin<br>Vol. % | Ölkond.<br>Vol. % | Paraffin-<br>gatsch<br>Vol. % | Gesamt-Produkt<br>Vol. % |     | Reaktions-<br>wasser |       |
|---|---------------------|-------------------|-------------------------------|--------------------------|-----|----------------------|-------|
| 1   | 2                   | 3                 | 4                             | 5                        | 6   | 7                    | 8     |
| Dichte bei 20 °C  | 0,688               | 0,772             | 0,90                          |                          |     |                      | 0,883 |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |                     |                   |                               |                          |     |                      |       |
| Jodzahl (Wijss)   |                     |                   |                               |                          |     |                      |       |
| N.Z. / V.Z.   |                     |                   |                               |                          |     |                      |       |
| Siede-Analyse   | Siedebeginn °C      |                   |                               |                          | 44  |                      |       |
|   | — 40                |                   |                               |                          |     |                      |       |
|   | 60                  |                   |                               |                          | 60  |                      |       |
|   | 80                  |                   |                               |                          | 140 |                      |       |
|   | 100                 |                   |                               |                          | 220 |                      |       |
|   | 120                 |                   |                               |                          | 300 | 51,0                 |       |
|   | 140                 |                   |                               |                          | 370 |                      |       |
|   | 160                 |                   |                               |                          | 420 |                      |       |
|   | 180                 |                   |                               |                          | 500 |                      |       |
|   | 200                 |                   |                               |                          | 550 |                      |       |
|   | 220                 |                   |                               |                          | 590 |                      |       |
|   | 240                 |                   |                               |                          | 620 |                      |       |
|   | 260                 |                   |                               |                          | 700 | 22,2                 |       |
|   | 280                 |                   |                               |                          | 740 |                      |       |
|   | 300                 |                   |                               |                          | 740 |                      |       |
| 320   |                     |                   |                               | 770                      |     |                      |       |
| 340   |                     |                   |                               |                          |     |                      |       |
| 360   |                     |                   |                               |                          |     |                      |       |
| Siede-Ende °C   |                     |                   |                               |                          |     |                      |       |
| Rückstand   |                     |                   |                               |                          |     | 25,4                 |       |
| Verlust   |                     |                   |                               |                          |     | 0,9                  |       |
| Stockpunkt °C   |                     |                   |                               |                          |     |                      |       |

|  |                   |    |
|--|-------------------|----|
| — Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 58 |
|  | Öl (200—320°)     | 37 |

Bemerkungen:

000003

Nr. 2

## Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 13 Dat. 3.4.8.43 Zeit Betr. Tage

| Produkt        | Anfaß<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,30        | 34,5           | 50,3                   | 38,5                                 | 26,4                  |
| Kondens.-Öl    | 5,00        | 41,6           | 53,8                   | 41,2                                 | 31,9                  |
| Paraffingatsch | 3,96        | 33,9           | 26,5                   | 20,3                                 | 18,3                  |
|                | 13,96       | 100,0          | 130,6                  | 100,0                                | 76,6                  |

|   | AK-Benzin      | Ölkönd. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |       |
|---|----------------|---------|---------------------|----------------|--------|----------------------|-------|
|   | Vol. %         | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |       |
| 1   | 2              | 3       | 4                   | 5              | 6      | 7                    | 8     |
| Dichte bei 20 °C  | 0,688          | 0,774   | 0,990               |                |        |                      | 0,924 |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |                |         |                     |                |        |                      |       |
| Jodzahl (Wijss)   |                |         |                     |                |        |                      |       |
| N.Z. / V.Z.   |                |         |                     |                |        |                      |       |
| Siede-Analyse   | Siedebeginn °C |         |                     |                | 43     |                      |       |
|   | — 40           |         |                     |                |        |                      |       |
|   | 60             |         |                     |                | 2,0    |                      |       |
|   | 80             |         |                     |                | 14,0   |                      |       |
|   | 100            |         |                     |                | 33,0   |                      |       |
|   | 120            |         |                     |                | 20,0   |                      | 7,5   |
|   | 140            |         |                     |                | 27,0   |                      |       |
|   | 160            |         |                     |                | 43,0   |                      |       |
|   | 180            |         |                     |                | 49,0   |                      |       |
|   | 200            |         |                     |                | 54,0   |                      |       |
|   | 220            |         |                     |                | 58,0   |                      |       |
|   | 240            |         |                     |                | 62,0   |                      |       |
|   | 260            |         |                     |                | 62,0   |                      | 2,0   |
|   | 280            |         |                     |                | 70,0   |                      |       |
| 300   |                |         |                     | 73,0           |        |                      |       |
| 320   |                |         |                     | 75,0           |        |                      |       |
| 340   |                |         |                     |                |        |                      |       |
| 360   |                |         |                     |                |        |                      |       |
| Siede-Ende °C   |                |         |                     |                |        |                      |       |
| Rückstand   |                |         |                     |                |        |                      | 1,8   |
| Verlust   |                |         |                     |                |        |                      | 2,5   |
| Stockpunkt °C   |                |         |                     |                |        |                      |       |

Olefine Vol. % Benzin (bis 200°)  
(H<sub>2</sub>SO<sub>4</sub>-P<sub>2</sub>O<sub>5</sub>) Öl (200—320°)

60

41

Bemerkungen:

000004

Nr.

Drucksynthese D.-V.-A.Ofen Nr. 11 Füllung 13 Dat. 2.3.8.43 Zeit Betr.Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% <sub>an</sub> | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|------------------------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,3          | 34,6                         | 50,0                   | 38,2                                 | 26,4                  |
| Kondens.-Öl    | 5,4          | 43,6                         | 56,3                   | 43,1                                 | 33,4                  |
| Paraffingätsch | 2,2          | 17,8                         | 24,5                   | 18,7                                 | 16,6                  |
|                | 12,4         | 100,0                        | 130,8                  | 100,0                                | 26,4                  |

|   | AK-Benzin      | Ölkond. | Paraffin-<br>gätsch | Gesamt-Produkt |        | Reaktions-<br>wasser |       |
|---|----------------|---------|---------------------|----------------|--------|----------------------|-------|
|   | Vol. %         | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |       |
| 1   | 2              | 3       | 4                   | 5              | 6      | 7                    | 8     |
| Dichte bei 20 °C  | 0,692          | 0,725   | 0,89                |                |        |                      | 0,990 |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |                |         |                     |                |        |                      |       |
| Jodzahl (Wijss)   |                |         |                     |                |        |                      |       |
| N. Z. / V. Z.   |                |         |                     |                |        |                      |       |
| Siede-Analyse   | Siedebeginn °C |         |                     |                | 51     |                      |       |
|   | 40             |         |                     |                |        |                      |       |
|   | 60             |         |                     |                | 2,0    |                      |       |
|   | 80             |         |                     |                | 2,0    |                      |       |
|   | 100            |         |                     |                | 16,0   |                      |       |
|   | 120            |         |                     |                | 34,0   | 48,8                 |       |
|   | 140            |         |                     |                | 32,0   |                      |       |
|   | 160            |         |                     |                | 39,0   |                      |       |
|   | 180            |         |                     |                | 46,0   |                      |       |
|   | 200            |         |                     |                | 52,0   |                      |       |
|   | 220            |         |                     |                | 56,0   |                      |       |
|   | 240            |         |                     |                | 61,0   |                      |       |
|   | 260            |         |                     |                | 65,0   | 22,2                 |       |
|   | 280            |         |                     |                | 70,0   |                      |       |
|   | 300            |         |                     |                | 72,0   |                      |       |
| 320   |                |         |                     | 75,0           |        |                      |       |
| 340   |                |         |                     |                |        |                      |       |
| 360   |                |         |                     |                |        |                      |       |
| Siede-Ende °C   |                |         |                     |                |        |                      |       |
| Rückstand   |                |         |                     |                |        | 28,0                 |       |
| Verlust   |                |         |                     |                |        | 1,0                  |       |
| Stockpunkt °C   |                |         |                     |                |        |                      |       |

Olefine Vol. %  
(H<sub>2</sub>SO<sub>4</sub>-P<sub>2</sub>O<sub>5</sub>)

Benzin (bis 200°)

60

Öl (200-320°)

40

Bemerkungen:

000005

Nr.

## Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 13 Dat. 1.2.84 Zeit Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A. K.-Benzin   | 4,10         | 30,3           | 43,8                   | 33,8                                 | 33,4                  |
| Kondens.-Öl    | 5,60         | 41,4           | 53,4                   | 41,3                                 | 33,0                  |
| Paraffingatsch | 3,81         | 28,3           | 32,3                   | 24,9                                 | 21,9                  |
|                | 13,51        | 100,0          | 129,4                  | 100,0                                | 87,3                  |

|   | AK-Benzin      | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |   |
|---|----------------|---------|---------------------|----------------|--------|----------------------|---|
|   | Vol. %         | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |   |
| 1   | 2              | 3       | 4                   | 5              | 6      | 7                    | 8 |
| Dichte bei 20 °C  | 0,691          | 0,745   | 0,82                |                |        | 0,788                |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |                |         |                     |                |        |                      |   |
| Jodzahl (Wjss)  |                |         |                     |                |        |                      |   |
| N. Z. / V. Z.   |                |         |                     |                |        |                      |   |
| Siede-Analyse   | Siedebeginn °C |         |                     | 52             |        |                      |   |
|   | 40             |         |                     |                |        |                      |   |
|   | 60             |         |                     | 2,0            |        |                      |   |
|   | 80             |         |                     | 8,2            |        |                      |   |
|   | 100            |         |                     | 15,9           |        |                      |   |
|   | 120            |         |                     | 23,0           |        |                      |   |
|   | 140            |         |                     | 29,0           |        | 42,4                 |   |
|   | 160            |         |                     | 35,0           |        |                      |   |
|   | 180            |         |                     | 41,0           |        |                      |   |
|   | 200            |         |                     | 46,9           |        |                      |   |
|   | 220            |         |                     | 51,0           |        |                      |   |
|   | 240            |         |                     | 56,0           |        |                      |   |
|   | 260            |         |                     | 61,0           |        | 33,8                 |   |
|   | 280            |         |                     | 65,0           |        |                      |   |
| 300   |                |         | 68,5                |                |        |                      |   |
| 320   |                |         | 70,2                |                |        |                      |   |
| 340   |                |         |                     |                |        |                      |   |
| 360   |                |         |                     |                |        |                      |   |
| Siede-Ende °C   |                |         |                     |                |        |                      |   |
| Rückstand   |                |         |                     |                |        | 33,7                 |   |
| Verlust   |                |         |                     |                |        | 1,1                  |   |
| Stockpunkt °C   |                |         |                     |                |        |                      |   |

Olefine Vol. %  
(H<sub>2</sub>SO<sub>4</sub>-P<sub>2</sub>O<sub>5</sub>)

Benzin (bis 200°)

Öl (200—320°)

30

37

Bemerkungen:

000006

Nr.

Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 13 Dat. 31.11.1933 Zeit Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 42           | 312            | 448                    | 349                                  | 243                   |
| Kondens.-Öl    | 58           | 386            | 498                    | 387                                  | 300                   |
| Paraffingatsch | 466          | 302            | 359                    | 264                                  | 235                   |
|                | 1546         | 1000           | 1285                   | 1000                                 | 978                   |

|   | AK-Benzin      | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |   |
|---|----------------|---------|---------------------|----------------|--------|----------------------|---|
|   | Vol. %         | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |   |
| I   | 2              | 3       | 4                   | 5              | 6      | 7                    | 8 |
| Dichte bei 20 °C  | 0,654          | 0,715   | 0,89                |                |        | 0,758                |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |                |         |                     |                |        |                      |   |
| Jodzahl (Wijsse)  |                |         |                     |                |        |                      |   |
| N. Z. / V. Z.   |                |         |                     |                |        |                      |   |
| Siede-Analyse   | Siedebeginn °C |         |                     | 50             |        |                      |   |
|   | — 40           |         |                     |                |        |                      |   |
|   | 60             |         |                     | 80             |        |                      |   |
|   | 80             |         |                     | 80             |        |                      |   |
|   | 100            |         |                     | 100            |        |                      |   |
|   | 120            |         |                     | 230            | 449    |                      |   |
|   | 140            |         |                     | 290            |        |                      |   |
|   | 160            |         |                     | 350            |        |                      |   |
|   | 180            |         |                     | 400            |        |                      |   |
|   | 200            |         |                     | 450            |        |                      |   |
|   | 220            |         |                     | 500            |        |                      |   |
|   | 240            |         |                     | 540            |        |                      |   |
|   | 260            |         |                     | 580            | 219    |                      |   |
|   | 280            |         |                     | 610            |        |                      |   |
|   | 300            |         |                     | 640            |        |                      |   |
|   | 320            |         |                     | 645            |        |                      |   |
|   | 340            |         |                     |                |        |                      |   |
| 360   |                |         |                     |                |        |                      |   |
| Siede-Ende °C   |                |         |                     |                |        |                      |   |
| Rückstand   |                |         |                     |                | 392    |                      |   |
| Verlust   |                |         |                     |                | 10     |                      |   |
| Stockpunkt °C   |                |         |                     |                |        |                      |   |

|  |                   |    |
|--|-------------------|----|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 61 |
|  | Öl (200—320°)     | 46 |

Bemerkungen:

000007

DVA

# Untersuchung der flüssigen Produkte

 Ofen-Nr. 11 Füllung 13 Dat. 30.31.7.43 Zeit Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,57         | 38,0           | 55,4                   | 43,1                                | 39,0                  |
| Kondens.-Öl    | 3,40         | 36,9           | 47,8                   | 36,3                                | 28,1                  |
| Paraffingatsch | 3,31         | 35,1           | 38,5                   | 31,6                                | 10,0                  |
| Ges.-Prod.     | 4,21         | 100,0          | 131,7                  | 100,0                               | 76,1                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,688       | 0,773   | 0,88                |                | 0,485                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijs)       |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

| Siedeanalyse      | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|-------------|--------|--------|--------|--------|--------|--------|
|                   | - 40 °C     |        |        |        |        | 42     |        |
|                   | 60 "        |        |        |        |        | 50     |        |
|                   | 80 "        |        |        |        |        | 14,0   |        |
|                   | 100 "       |        |        |        |        | 33,0   |        |
|                   | 120 "       |        |        |        |        | 30,0   | 51,5   |
|                   | 140 "       |        |        |        |        | 37,0   |        |
|                   | 160 "       |        |        |        |        | 43,0   |        |
|                   | 180 "       |        |        |        |        | 49,0   |        |
|                   | 200 "       |        |        |        |        | 54,0   |        |
|                   | 220 "       |        |        |        |        | 58,0   |        |
|                   | 240 "       |        |        |        |        | 62,0   |        |
|                   | 260 "       |        |        |        |        | 66,0   | 21,0   |
|                   | 280 "       |        |        |        |        | 70,0   |        |
|                   | 300 "       |        |        |        |        | 73,0   |        |
| 320 "             |             |        |        |        | 75,0   |        |        |
| 340 "             |             |        |        |        |        |        |        |
| 360 "             |             |        |        |        |        |        |        |
| Siede-Ende °C     |             |        |        |        |        |        |        |
| Rückstand         |             |        |        |        |        |        | 10,5   |
| Verlust           |             |        |        |        |        |        | 1,0    |
| Stockpunkt °C     |             |        |        |        |        |        |        |
| Destill.-Prod.    | SPL         | N Z    | V Z    |        |        |        |        |
| Benzin (bis 200°) |             |        |        |        |        | 60     |        |
| Öl (200-320°)     |             |        |        |        |        | 37     |        |

Bemerkungen:

000008



# Untersuchung der flüssigen Produkte

Ofen-Nr. 11 Füllung 15 Dat. 29.10.47 Zeit 4.45 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 48           | 370            | 543                    | 414                                 | 282                   |
| Kondens.-Öl    | 43           | 330            | 424                    | 326                                 | 252                   |
| Paraffingatsch | 35           | 300            | 344                    | 260                                 | 229                   |
| Ges.-Prod.     | 130          | 1000           | 1311                   | 1000                                | 763                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0.682       | 0.744   | 0.88                |                | 0.920                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | — 40 °C     |        |        |        |        |        | 38     |
| 60 "          |             |        |        |        |        | 100    |        |
| 80 "          |             |        |        |        |        | 140    |        |
| 100 "         |             |        |        |        |        | 240    |        |
| 120 "         |             |        |        |        |        | 300    | 48.7   |
| 140 "         |             |        |        |        |        | 360    |        |
| 160 "         |             |        |        |        |        | 410    |        |
| 180 "         |             |        |        |        |        | 460    |        |
| 200 "         |             |        |        |        |        | 510    |        |
| 220 "         |             |        |        |        |        | 550    | 17.9   |
| 240 "         |             |        |        |        |        | 580    |        |
| 260 "         |             |        |        |        |        | 610    |        |
| 280 "         |             |        |        |        |        | 640    |        |
| 300 "         |             |        |        |        |        | 670    |        |
| 320 "         |             |        |        |        |        | 700    |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        | 318    |
| Rückstand     |             |        |        |        |        |        | 16     |
| Verlust       |             |        |        |        |        |        |        |

| Stockpunkt °C     | SPL   | N Z   | V Z | Destill.-Prod. |
|-------------------|-------|-------|-----|----------------|
|                   |       |       |     | 46.11          |
| Benzin (bis 200°) | 0.709 | 0.508 |     | 60             |
| Öl (200–320°)     | 0.745 | 0.595 |     | 36             |

Bemerkungen:

000009

000010

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| 1  |
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|----------------------|-----|------|
| Patent               | 80% | 100% |
| Pro 70               | 665 | 100  |
| Pro 80               | 47  | 100  |
| $\Sigma$             | 719 | + 83 |
| cost <sub>2</sub> -h | 450 |      |

Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 27.3.27.43 Zeit Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 2,10      | 43,7       | 62,4                   | 40,3                                 | 32,2                  |
| Kondens.-Öl    | 4,20      | 56,3       | 92,8                   | 53,7                                 | 41,5                  |
| Paraffingatsch | 0,0       | 0,0        | 0,0                    | 0,0                                  | 0,0                   |
| Ges.-Prod.     | 4,80      | 100,0      | 135,7                  | 100,0                                | 73,7                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20 °C     | 0,676       | 0,774   | —              | —              | 0,987           |
| Olefine „SPL“ Vol. % | —           | —       | —              | —              | —               |
| Jodzahl (Wijss)      | —           | —       | —              | —              | —               |
| N-Z / V-Z            | —           | —       | —              | —              | —               |

| Siedebeginn   | Vol. % |        |        |        |        | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
|               | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % |        |
| - 40 °C       | 41     | 82     | —      | 41     | 52     | —      |
| 60 "          | 26     | —      | —      | 32     | 30     | —      |
| 80 "          | 29,0   | —      | —      | 13,4   | 10,0   | —      |
| - 100 "       | 42,0   | 3,0    | —      | 33,3   | 20,0   | —      |
| 120 "         | 63,0   | 6,0    | —      | 32,4   | 30,0   | 0,0    |
| 140 "         | 55,0   | 10,0   | —      | 29,6   | 40,0   | —      |
| 160 "         | 24,0   | 16,0   | 84,6   | 23,4   | 49,0   | —      |
| 180 "         | 29,0   | 16,0   | —      | 55,2   | 56,0   | —      |
| 200 "         | 33,0   | 26,0   | —      | 62,3   | 63,0   | —      |
| 220 "         | 45,0   | 46,0   | —      | 71,0   | 69,0   | —      |
| 240 "         | —      | 73,0   | —      | 74,0   | 74,0   | —      |
| 260 "         | —      | —      | —      | 89,0   | 90,0   | 9,0    |
| 280 "         | —      | 82,0   | —      | 92,1   | 93,0   | —      |
| 300 "         | —      | 94,0   | —      | 96,9   | 93,0   | —      |
| 320 "         | —      | 95,0   | —      | 99,2   | 92,0   | —      |
| 340 "         | —      | —      | —      | —      | —      | —      |
| 360 "         | —      | —      | —      | —      | —      | —      |
| Siede-Ende °C | 350    | —      | —      | —      | —      | —      |
| Rückstand     | 2,8    | 15,4   | —      | 9,9    | 8,9    | —      |
| Verlust       | 2,4    | 0,0    | —      | 0,5    | 0,5    | —      |

|                   |     |     |     |   |    |   |
|-------------------|-----|-----|-----|---|----|---|
| Stockpunkt °C     | —   | —   | —   | — | —  | — |
| Destill.-Prod.    | SPL | N Z | V Z | — | —  | — |
| Benzin (bis 200°) | —   | —   | —   | — | 58 | — |
| Öl (200—320°)     | —   | —   | —   | — | 14 | — |

Bemerkungen:

000011

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 26.2.7.43 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 23           | 36,0           | 52,4                   | 39,8                                | 32,4                  |
| Kondens.-Öl    | 6,1          | 21,5           | 53,7                   | 46,9                                | 31,6                  |
| Paraffingatsch | 3,3          | 33,5           | 35,3                   | 13,3                                | 12,2                  |
| Ges.-Prod.     | 14,7         | 100,0          | 131,4                  | 100,0                               | 76,2                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,689       | 0,773   | 0,89                |                | 0,985                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijs)       |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |      |
|---------------|-------------|--------|--------|--------|--------|--------|--------|------|
|               | — 40 °C     |        |        |        |        |        | 50     |      |
|               | 60 „        |        |        |        |        |        | 30     |      |
|               | 80 „        |        |        |        |        |        | 0      |      |
|               | 100 „       |        |        |        |        |        | 12,0   |      |
|               | 120 „       |        |        |        |        |        | 5,0    | 47,3 |
|               | 140 „       |        |        |        |        |        | 3,0    |      |
|               | 160 „       |        |        |        |        |        | 2,0    |      |
|               | 180 „       |        |        |        |        |        | 2,0    |      |
|               | 200 „       |        |        |        |        |        | 3,0    |      |
|               | 220 „       |        |        |        |        |        | 5,0    |      |
|               | 240 „       |        |        |        |        |        | 2,0    |      |
|               | 260 „       |        |        |        |        |        | 2,0    | 31,2 |
|               | 280 „       |        |        |        |        |        | 2,0    |      |
|               | 300 „       |        |        |        |        |        | 1,0    |      |
| 320 „         |             |        |        |        |        | 2,0    |        |      |
| 340 „         |             |        |        |        |        |        |        |      |
| 360 „         |             |        |        |        |        |        |        |      |
| Siede-Ende °C |             |        |        |        |        |        |        |      |
| Rückstand     |             |        |        |        |        |        |        |      |
| Verlust       |             |        |        |        |        |        |        |      |

|                   |     |     |     |  |    |      |
|-------------------|-----|-----|-----|--|----|------|
| Stockpunkt °C     |     |     |     |  |    |      |
| Destill.-Prod.    | SPL | N Z | V Z |  |    |      |
| Benzin (bis 200°) |     |     |     |  | 58 | 37,8 |
| Öl (200–320°)     |     |     |     |  | 38 | 1,3  |

Bemerkungen: 000012

## Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 10 Dat. 25.11.74 Zeit 7:43 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 40           | 300            | 436                    | 334                                 | 233                   |
| Kondens.-Öl    | 525          | 430            | 556                    | 428                                 | 331                   |
| Paraffingatsch | 96           | 870            | 304                    | 235                                 | 209                   |
| Ges.-Prod.     | 1335         | 1000           | 1296                   | 1000                                | 773                   |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20 °C     | 0.688       | 0.949   | 0.89                |                | 0.944                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| NZ / VZ              |             |         |                     |                |                      |

| Siedeanalyse      | Siedebeginn | Vol. % | Vol. ‰ | Vol. ‰ | Vol. ‰ | Vol. ‰ | Gew. % |
|-------------------|-------------|--------|--------|--------|--------|--------|--------|
|                   | - 40 °C     |        |        |        |        |        | 46     |
| 60 "              |             |        |        |        |        | 50     |        |
| 80 "              |             |        |        |        |        | 130    |        |
| 100 "             |             |        |        |        |        | 200    |        |
| 120 "             |             |        |        |        |        | 240    | 463    |
| 140 "             |             |        |        |        |        | 350    |        |
| 160 "             |             |        |        |        |        | 400    | 208    |
| 180 "             |             |        |        |        |        | 460    |        |
| 200 "             |             |        |        |        |        | 510    |        |
| 220 "             |             |        |        |        |        | 550    |        |
| 240 "             |             |        |        |        |        | 590    | 208    |
| 260 "             |             |        |        |        |        | 630    |        |
| 280 "             |             |        |        |        |        | 640    |        |
| 300 "             |             |        |        |        |        | 710    | 323    |
| 320 "             |             |        |        |        |        | 720    |        |
| 340 "             |             |        |        |        |        |        | 0.6    |
| 360 "             |             |        |        |        |        |        |        |
| Siede-Ende °C     |             |        |        |        |        |        |        |
| Rückstand         |             |        |        |        |        |        |        |
| Verlust           |             |        |        |        |        |        |        |
| Stockpunkt °C     |             |        |        |        |        |        |        |
| Destill.-Prod.    | SPL         | NZ     | VZ     |        |        |        |        |
| Benzin (bis 200°) |             |        |        |        |        | 60     |        |
| Öl (200-320°)     |             |        |        |        |        | 38     |        |

Bemerkungen:

000013

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 24.11.43 Zeit 43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 49        | 36,6       | 53,7                   | 40,9                                | 37,8                  |
| Kondens.-Öl    | 5,5       | 41,0       | 33,1                   | 20,4                                | 31,8                  |
| Paraffingatsch | 3,0       | 32,0       | 30,6                   | 18,7                                | 17,0                  |
| Ges.-Prod.     | 3,4       | 100,0      | 33,4                   | 100,0                               | 76,0                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,881       | 0,874   | 0,81           |                | 0,885           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedeanalyse      | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|-------------|--------|--------|--------|--------|--------|--------|
|                   | - 40 °C     |        |        |        |        | 45     |        |
|                   | 60 "        |        |        |        |        | 5,0    |        |
|                   | 80 "        |        |        |        |        | 12,0   |        |
|                   | 100 "       |        |        |        |        | 29,0   |        |
|                   | 120 "       |        |        |        |        | 32,0   |        |
|                   | 140 "       |        |        |        |        | 35,0   | 49,9   |
|                   | 160 "       |        |        |        |        | 47,0   |        |
|                   | 180 "       |        |        |        |        | 50,0   |        |
|                   | 200 "       |        |        |        |        | 50,0   |        |
|                   | 220 "       |        |        |        |        | 50,0   |        |
|                   | 240 "       |        |        |        |        | 50,0   |        |
|                   | 260 "       |        |        |        |        | 50,0   |        |
|                   | 280 "       |        |        |        |        | 50,0   |        |
|                   | 300 "       |        |        |        |        | 50,0   |        |
| 320 "             |             |        |        |        | 50,0   |        |        |
| 340 "             |             |        |        |        |        |        |        |
| 360 "             |             |        |        |        |        |        |        |
| Siede-Ende °C     |             |        |        |        |        |        |        |
| Rückstand         |             |        |        |        |        | 26,0   |        |
| Verlust           |             |        |        |        |        | 1,6    |        |
| Stockpunkt °C     |             |        |        |        |        |        |        |
| Destill.-Prod.    | SPL         | N Z    | V Z    |        |        |        |        |
| Benzin (bis 200°) |             |        |        |        | 49     |        |        |
| Öl (200-320°)     |             |        |        |        | 24     |        |        |

Bemerkungen:

000014

DVA

# Untersuchung der flüssigen Produkte

 Ofen Nr. 11 Füllung 12 Dat. 23.04.70 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% <sup>o</sup> | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|-----------------------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 45           | 32,2                        | 4,3                    | 3,9                                  | 3,4                   |
| Kondens.-Öl    | 65           | 46,4                        | 5,1                    | 4,8                                  | 3,4                   |
| Paraffingatsch | 30           | 21,4                        | 2,4                    | 1,8                                  | 1,3                   |
| Ges.-Prod.     | 140          | 100,0                       | 12,5                   | 10,6                                 | 7,1                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |  |  | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|--|--|----------------------|
| Dichte bei 20° C     | 0,721       | 0,741   | 0,99                |                |  |  | 0,98                 |
| Olefine „SPL“ Vol. % |             |         |                     |                |  |  |                      |
| Jodzahl (Wijss)      |             |         |                     |                |  |  |                      |
| N Z / V Z            |             |         |                     |                |  |  |                      |

| Siedeanalyse  | Siedebeginn | Vol. % <sup>o</sup> | Vol. % <sup>o</sup> | Vol. % <sup>o</sup> | Vol. % <sup>o</sup> | Vol. % <sup>o</sup> | Gew. % <sup>o</sup> |
|---------------|-------------|---------------------|---------------------|---------------------|---------------------|---------------------|---------------------|
|               | - 40 °C     |                     |                     |                     |                     | 44                  |                     |
|               | 60 „        |                     |                     |                     |                     | 58                  |                     |
|               | 80 „        |                     |                     |                     |                     | 12,10               |                     |
|               | 100 „       |                     |                     |                     |                     | 25,91               |                     |
|               | 120 „       |                     |                     |                     |                     | 37,0                | 47,5                |
|               | 140 „       |                     |                     |                     |                     | 42,0                |                     |
|               | 160 „       |                     |                     |                     |                     | 47,0                |                     |
|               | 180 „       |                     |                     |                     |                     | 42,0                |                     |
|               | 200 „       |                     |                     |                     |                     | 47,0                |                     |
| 220 „         |             |                     |                     |                     | 52,0                |                     |                     |
| 240 „         |             |                     |                     |                     | 57,0                |                     |                     |
| 260 „         |             |                     |                     |                     | 62,0                | 7,6                 |                     |
| 280 „         |             |                     |                     |                     | 67,0                |                     |                     |
| 300 „         |             |                     |                     |                     | 72,0                |                     |                     |
| 320 „         |             |                     |                     |                     | 77,0                |                     |                     |
| 340 „         |             |                     |                     |                     | 82,0                |                     |                     |
| 360 „         |             |                     |                     |                     | 87,0                |                     |                     |
| Siede-Ende °C |             |                     |                     |                     |                     |                     |                     |
| Rückstand     |             |                     |                     |                     |                     |                     | 25,4                |
| Verlust       |             |                     |                     |                     |                     |                     | 1,0                 |

|                   |     |     |     |  |  |  |  |
|-------------------|-----|-----|-----|--|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |  |
| Öl (200–320°)     |     |     |     |  |  |  |  |

Bemerkungen:

000015

Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 5.3.1943 Zeit Betr. Tage

| Produkt        | Anfall kg | Gewichts % | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 46        | 32.0       | 47.6                   | 36.0                                 | 38.4                  |
| Kondens.-Öl    | 60        | 41.6       | 53.9                   | 41.2                                 | 31.4                  |
| Paraffingatsch | 38        | 26.4       | 30.0                   | 22.9                                 | 10.2                  |
| Ges.-Prod.     | 144       | 100.0      | 131.4                  | 100.0                                | 46.3                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0.679       | 0.473   | 0.88           |                | 0.84            |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        |        | 4.8    |
| 60 „          |             |        |        |        |        | 5.0    |        |
| 80 „          |             |        |        |        |        | 11.5   |        |
| 100 „         |             |        |        |        |        | 14.0   |        |
| 120 „         |             |        |        |        |        | 26.0   | 4.69   |
| 140 „         |             |        |        |        |        | 33.0   |        |
| 160 „         |             |        |        |        |        | 39.0   |        |
| 180 „         |             |        |        |        |        | 45.0   |        |
| 200 „         |             |        |        |        |        | 51.0   |        |
| 220 „         |             |        |        |        |        | 55.0   |        |
| 240 „         |             |        |        |        |        | 59.0   |        |
| 260 „         |             |        |        |        |        | 63.0   | 19.9   |
| 280 „         |             |        |        |        |        | 66.0   |        |
| 300 „         |             |        |        |        |        | 69.0   |        |
| 320 „         |             |        |        |        |        | 71.0   |        |
| 340 „         |             |        |        |        |        |        |        |
| 360 „         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 31.6   |
| Verlust       |             |        |        |        |        |        | 1.6    |

| Stockpunkt °C     | SPL   | N Z   | V Z |
|-------------------|-------|-------|-----|
| Destill.-Prod.    |       |       |     |
| Benzin (bis 200°) | 0.412 | 1.01  |     |
| Öl (200-320°)     | 0.445 | 0.932 |     |

Bemerkungen: 000016



Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 2/23.7.43 Zeit            Betr. Tage           

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,10      | 33,6       | 28,3                   | 36,8                                | 35,2                  |
| Kondens.-Öl    | 5,30      | 42,7       | 56,9                   | 42,6                                | 33,1                  |
| Paraffingatsch | 3,03      | 24,3       | 37,0                   | 26,6                                | 19,5                  |
| Ges.-Prod.     | 12,43     | 100,0      | 130,0                  | 100,0                               | 26,2                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,684       | 0,746   | 0,80           |                | 0,723           |
| Ölefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedebeginn   | Vol. %   |         | Vol. % |         | Gew. % |        |
|---------------|----------|---------|--------|---------|--------|--------|
|               | Vol. %   | Vol. %  | Vol. % | Vol. %  | Vol. % | Gew. % |
| - 40 °C       | 29       | 49      | 2,60   | 37      | 43     |        |
| 60 „          | 32       |         |        | 85      | 107    |        |
| 80 „          | 33       |         |        | 158     | 137    |        |
| 100 „         | 37       | 50      |        | 231     | 239    |        |
| 120 „         | 41,0     | 89      |        | 295     | 320    | 49,2   |
| 140 „         | 41,0 159 | 100 159 |        | 352 203 | 370    |        |
| 160 „         | 42,0     | 83,0    |        | 42,6    | 43,0   |        |
| 180 „         | 43,0     | 23,0    |        | 47,9    | 48,0   |        |
| 200 „         | 43,0     | 42,0    |        | 52,9    | 53,0   |        |
| 220 „         | 43,0     |         |        | 57      | 51,0   |        |
| 240 „         | 43,0     |         |        | 61,0    | 61,0   |        |
| 260 „         | 43,0     |         |        | 64,2    | 65,0   | 28,2   |
| 280 „         | 43,0     | 2,0     |        | 67,0    | 69,0   |        |
| 300 „         | 43,0     | 2,0     |        | 70,0    | 70,0   |        |
| 320 „         | 43,0     | 2,0     |        | 72,0    | 71,0   |        |
| 340 „         |          |         |        |         |        |        |
| 360 „         |          |         |        |         |        |        |
| Siede-Ende °C |          |         |        |         |        |        |
| Rückstand     | 1,8      | 13,2    | 93,1   | 92,7    |        | 22,2   |
| Verlust       | 2,3      | 5,0     | 0,0    | 1,1     |        | 1,3    |

| Stockpunkt °C     | Destill.-Prod. |           |
|-------------------|----------------|-----------|
|                   | SPL            | N Z / V Z |
| Benzin (bis 200°) |                |           |
| Öl (200-320°)     |                |           |

Bemerkungen: 000017

## Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 10.11.43 Zeit            Betr. Tage           

| Produkt        | Anfall-<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|---------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 52            | 33,8           | 493                    | 378                                 | 259                   |
| Kondens.-Öl    | 64            | 41,8           | 576                    | 440                                 | 345                   |
| Paraffingatsch | 95            | 61,4           | 238                    | 182                                 | 164                   |
| Ges.-Prod.     | 159           | 100,0          | 1304                   | 1000                                | 466                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,666       | 0,718   | 0,90                |                | 0,88                 |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        | 47     |        |
|               | 60 „        |        |        |        |        | 30     |        |
|               | 80 „        |        |        |        |        | 100    |        |
|               | 100 „       |        |        |        |        | 120    |        |
|               | 120 „       |        |        |        |        | 260    | 489    |
|               | 140 „       |        |        |        |        | 340    |        |
|               | 160 „       |        |        |        |        | 420    |        |
|               | 180 „       |        |        |        |        | 480    |        |
|               | 200 „       |        |        |        |        | 520    |        |
|               | 220 „       |        |        |        |        | 560    |        |
|               | 240 „       |        |        |        |        | 600    |        |
|               | 260 „       |        |        |        |        | 640    | 221    |
|               | 280 „       |        |        |        |        | 680    |        |
|               | 300 „       |        |        |        |        | 720    |        |
|               | 320 „       |        |        |        |        | 745    |        |
| 340 „         |             |        |        |        |        |        |        |
| 360 „         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 278    |
| Verlust       |             |        |        |        |        |        | 19     |

| Stockpunkt °C     |       |       |     |    |
|-------------------|-------|-------|-----|----|
| Destill.-Prod.    | SPL   | N Z   | V Z |    |
| Benzin (bis 200°) | 0,717 | 1,265 |     | 62 |
| Öl (200—320°)     | 0,745 | 0,53  |     | 42 |

Bemerkungen:

000018



9

Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 19.10.74 Zeit 7.43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,90      | 33,0       | 48,3                   | 36,9                                 | 25,3                  |
| Kondens.-Öl    | 6,80      | 45,8       | 59,0                   | 44,9                                 | 34,2                  |
| Paraffingatsch | 3,15      | 21,2       | 23,9                   | 18,2                                 | 16,3                  |
| Ges.-Prod.     | 14,85     | 100,0      | 131,2                  | 100,0                                | 76,3                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,685       | 0,728   | 0,89           | 0,728          | 0,986           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl — (Wijss)    |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       | 3,9    | 1,5    | 2,5    | 3,9    | 2,0    |        |
| 60 "          | 2,0    |        |        | 2,4    | 1,0    |        |
| 80 "          | 4,0    |        |        | 14,2   | 15,0   |        |
| 100 "         | 5,0    | 2,0    |        | 12,3   | 17,0   |        |
| 120 "         | 2,0    | 2,0    |        | 12,5   | 15,0   | 48,3   |
| 140 "         | 2,0    | 9,0    | 0      | 33,9   | 24,0   |        |
| 160 "         | 2,0    | 12,0   | 18,0   | 4,4    | 19,0   |        |
| 180 "         | 3,0    | 26,0   |        | 2,0    | 4,2    |        |
| 200 "         | 5,0    | 23,0   |        | 21,1   | 1,0    |        |
| 220 "         |        | 22,0   |        | 5,2    | 5,0    |        |
| 240 "         |        | 2,0    |        | 6,3    | 6,0    |        |
| 260 "         |        | 5,0    |        | 6,3    | 6,0    | 13,9   |
| 280 "         |        | 2,0    | 2,0    | 6,1    | 6,0    |        |
| 300 "         |        | 24,0   | 4,0    | 7,5    | 23,0   |        |
| 320 "         |        | 24,0   | 2,0    | 2,9    | 24,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C | 220    |        |        |        |        |        |
| Rückstand     | 1,8    | 1,5    | 4,1    | 28,0   |        | 32,2   |
| Verlust       | 1,6    | 2,7    | 1,4    | 0,6    |        | 1,0    |

| Stockpunkt °C | Destill.-Prod.    | SPL | N Z | V Z |
|---------------|-------------------|-----|-----|-----|
|               | Benzin (bis 200°) |     |     |     |
|               | Öl (200—320°)     |     |     |     |

Bemerkungen:

000019

## Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 10 Dat. 18.10.1945 Zeit        Betr. Tage       

| Produkt        | Anfall / kg | Gewichts- % | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-------------|-------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 475         | 325         | 443                    | 363                                  | 249                   |
| Kondens.-Öl    | 63          | 432         | 556                    | 424                                  | 332                   |
| Paraffingatsch | 355         | 243         | 273                    | 210                                  | 144                   |
| Ges.-Prod.     | 793         | 1000        | 1302                   | 1000                                 | 468                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin- gatsch | Gesamt-Produkt | Reaktions- wasser |
|----------------------|-------------|---------|------------------|----------------|-------------------|
| Dichte bei 20° C     | 0.687       | 0.777   | 0.891            |                | 0.985             |
| Olefine „SPL“ Vol. % |             |         |                  |                |                   |
| Jodzahl (Wijss)      |             |         |                  |                |                   |
| N Z / V Z            |             |         |                  |                |                   |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        |        | 43     |
| 60 "          |             |        |        |        |        | 60     |        |
| 80 "          |             |        |        |        |        | 130    |        |
| 100 "         |             |        |        |        |        | 200    |        |
| 120 "         |             |        |        |        |        | 270    | 481    |
| 140 "         |             |        |        |        |        | 340    |        |
| 160 "         |             |        |        |        |        | 400    |        |
| 180 "         |             |        |        |        |        | 460    |        |
| 200 "         |             |        |        |        |        | 510    |        |
| 220 "         |             |        |        |        |        | 550    |        |
| 240 "         |             |        |        |        |        | 590    |        |
| 260 "         |             |        |        |        |        | 630    | 211    |
| 280 "         |             |        |        |        |        | 670    |        |
| 300 "         |             |        |        |        |        | 700    |        |
| 320 "         |             |        |        |        |        | 720    |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 294    |
| Verlust       |             |        |        |        |        |        | 14     |

| Stockpunkt °C     | SPL | N Z | V Z |  |  |    |
|-------------------|-----|-----|-----|--|--|----|
| Destill.-Prod.    |     |     |     |  |  |    |
| Benzin (bis 200°) |     |     |     |  |  | 64 |
| Öl (200-320°)     |     |     |     |  |  | 42 |

Bemerkungen: 000020

Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 17.10.7.43 Zeit          Betr. Tage         

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 5,44      | 32,6       | 47,8                   | 36,6                                | 8,5,0                 |
| Kondens.-Öl    | 6,14      | 39,3       | 57,1                   | 43,8                                | 34,0                  |
| Paraffingatsch | 3,27      | 23,1       | 8,57                   | 6,57                                | 17,7                  |
| Ges.-Prod.     | 14,85     | 100,0      | 113,0,6                | 100,0                               | 26,7                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,684       | 0,746   | 0,90           |                | 0,995           |
| Olefine „SPL“ Vol.-% |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        | 4,5    |        |
|               | 60 „        |        |        |        |        | 5,0    |        |
|               | 80 „        |        |        |        |        | 12,0   |        |
|               | 100 „       |        |        |        |        | 35,0   |        |
|               | 120 „       |        |        |        |        | 52,0   | 9,2    |
|               | 140 „       |        |        |        |        | 75,0   |        |
|               | 160 „       |        |        |        |        | 85,0   |        |
|               | 180 „       |        |        |        |        | 92,0   |        |
|               | 200 „       |        |        |        |        | 95,0   |        |
|               | 220 „       |        |        |        |        | 97,0   |        |
|               | 240 „       |        |        |        |        | 98,0   |        |
|               | 260 „       |        |        |        |        | 99,0   | 2,8    |
|               | 280 „       |        |        |        |        | 100,0  |        |
|               | 300 „       |        |        |        |        | 100,0  |        |
|               | 320 „       |        |        |        |        | 100,0  |        |
| 340 „         |             |        |        |        |        |        |        |
| 360 „         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        |        |
| Verlust       |             |        |        |        |        |        | 1,3    |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200—320°)     |     |     |     |  |  |  |

Bemerkungen: 000021

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 16/17.1.43 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 53           | 356            | 525                    | 399                                  | 291                   |
| Kondens.-Öl    | 60           | 402            | 518                    | 394                                  | 306                   |
| Paraffingatsch | 36           | 242            | 242                    | 204                                  | 184                   |
| Ges.-Prod.     | 149          | 1000           | 1315                   | 1000                                 | 761                   |

| Kondens.-Prod.      | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|---------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C    | 0,649       | 0,744   | 0,792               |                | 0,712                |
| Olefin „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)     |             |         |                     |                |                      |
| N Z / V Z           |             |         |                     |                |                      |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        |        | 46     |
| 60 "          |             |        |        |        |        | 46     |        |
| 80 "          |             |        |        |        |        | 190    |        |
| 100 "         |             |        |        |        |        | 230    |        |
| 120 "         |             |        |        |        |        | 310    | 306    |
| 140 "         |             |        |        |        |        | 340    | 306    |
| 160 "         |             |        |        |        |        | 450    |        |
| 180 "         |             |        |        |        |        | 510    |        |
| 200 "         |             |        |        |        |        | 550    |        |
| 220 "         |             |        |        |        |        | 580    |        |
| 240 "         |             |        |        |        |        | 630    |        |
| 260 "         |             |        |        |        |        | 690    | 184    |
| 280 "         |             |        |        |        |        | 700    |        |
| 300 "         |             |        |        |        |        | 720    |        |
| 320 "         |             |        |        |        |        | 735    |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 293    |
| Verlust       |             |        |        |        |        |        | 17     |

|                   |     |     |     |        |  |
|-------------------|-----|-----|-----|--------|--|
| Stockpunkt °C     |     |     |     |        |  |
| Destill.-Prod.    | SPL | N Z | V Z |        |  |
| Benzin (bis 200°) |     |     |     | 51/100 |  |
| Öl (200-320°)     |     |     |     | 103    |  |
|                   |     |     |     | 42     |  |

Bemerkungen: 000022

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 15.10.74 Zeit 43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 44        | 29,9       | 43,9                   | 33,9                                | 23,1                  |
| Kondens.-Öl    | 0,0       | 40,8       | 3,6                    | 40,8                                | 31,6                  |
| Paraffingatsch | ?         | 9,3        | 33,6                   | 35,3                                | 22,8                  |
| Ges.-Prod.     | 147       | 100,0      | 121,1                  | 109,9                               | 77,5                  |

| Kondens.-Prod.       | A K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20 °C     | 0,671       | 0,746   | 0,90           |                | 0,985           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn    | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|----------------|--------|--------|--------|--------|--------|--------|
| - 40 °C        |        |        |        |        | 0      |        |
| 60 „           |        |        |        |        | 5,0    |        |
| 80 „           |        |        |        |        | 13,0   |        |
| 100 „          |        |        |        |        | 20,0   |        |
| 120 „          |        |        |        |        | 37,0   | 44,7   |
| 140 „          |        |        |        |        | 33,0   |        |
| 160 „          |        |        |        |        | 39,0   |        |
| 180 „          |        |        |        |        | 40,0   |        |
| 200 „          |        |        |        |        | 20,0   |        |
| 220 „          |        |        |        |        | 50,0   |        |
| 240 „          |        |        |        |        | 56,0   |        |
| 260 „          |        |        |        |        | 20,0   | 21,3   |
| 280 „          |        |        |        |        | ?      |        |
| 300 „          |        |        |        |        | ?      |        |
| 320 „          |        |        |        |        | 5      |        |
| 340 „          |        |        |        |        |        |        |
| 360 „          |        |        |        |        |        |        |
| •Siede-Ende °C |        |        |        |        |        |        |
| Rückstand      |        |        |        |        |        | 32,4   |
| Verlust        |        |        |        |        |        | 1,5    |

| Stockpunkt °C     | SPL | N. Z | V. Z |
|-------------------|-----|------|------|
| Destill.-Prod.    |     |      |      |
| Benzin (bis 200°) |     |      | 62   |
| Öl (200-320°)     |     |      | 39   |

Bemerkungen:

000023

DVA

# Untersuchung der flüssigen Produkte

Ofen-Nr. 11 Füllung 13 Dat. 14.10.74 Zeit 43 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,3          | 28,3           | 41,6                   | 32,3                                | 22,0                  |
| Kondens.-Öl    | 6,2          | 41,4           | 53,5                   | 41,5                                | 33,3                  |
| Paraffingatsch | 4,6          | 30,3           | 33,7                   | 26,2                                | 23,6                  |
| Ges.-Prod.     | 15,2         | 100,0          | 128,8                  | 100,0                               | 78,9                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,680       | 0,746   | 0,90                |                | 0,995                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn       | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|--------|--------|--------|--------|--------|--------|
| 40 °C             |        |        |        |        | 4,9    |        |
| 60 "              |        |        |        |        | 4,0    |        |
| 80 "              |        |        |        |        | 11,0   |        |
| 100 "             |        |        |        |        | 18,0   |        |
| 120 "             |        |        |        |        | 65,0   |        |
| 140 "             |        |        |        |        | 62,0   | 33,9   |
| 160 "             |        |        |        |        | 38,0   |        |
| 180 "             |        |        |        |        | 43,0   |        |
| 200 "             |        |        |        |        | 42,0   |        |
| 220 "             |        |        |        |        | 30     |        |
| 240 "             |        |        |        |        | 20     |        |
| 260 "             |        |        |        |        | 17     | 21,8   |
| 280 "             |        |        |        |        | 5,0    |        |
| 300 "             |        |        |        |        | 0,0    |        |
| 320 "             |        |        |        |        | 0,0    |        |
| 340 "             |        |        |        |        | 0,0    |        |
| 360 "             |        |        |        |        | 0,0    |        |
| Siede-Ende °C     |        |        |        |        |        |        |
| Rückstand         |        |        |        |        |        | 33,8   |
| Verlust           |        |        |        |        |        | 1,3    |
| Stockpunkt °C     |        |        |        |        |        |        |
| Destill.-Prod.    | SPL    | N Z    | V Z    |        |        |        |
| Benzin (bis 200°) |        |        |        |        |        |        |
| Öl (200-320°)     |        |        |        |        | 6,2    |        |
|                   |        |        |        |        | 3,9    |        |

Bemerkungen:

000024



# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Fällung 13 Dat. 13.11.47 Zeit 42 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,2          | 31,3           | 46,1                   | 35,4                                | 24,0                  |
| Kondens.-Öl    | 6,5          | 48,8           | 55,9                   | 42,9                                | 33,2                  |
| Paraffingatsch | 3,8          | 25,4           | 38,2                   | 29,7                                | 19,6                  |
| Ges.-Prod.     | 15,0         | 100,0          | 130,2                  | 100,0                               | 76,8                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,680       | 0,725   | 0,90                |                | 0,723                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z V Z              |             |         |                     |                |                      |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | — 40 °C     |        |        |        |        |        | 4,2    |
| 60 "          |             |        |        |        |        | 6,0    |        |
| 80 "          |             |        |        |        |        | 13,0   |        |
| 100 "         |             |        |        |        |        | 20,0   |        |
| 120 "         |             |        |        |        |        | 27,0   |        |
| 140 "         |             |        |        |        |        | 34,0   | 48,6   |
| 160 "         |             |        |        |        |        | 40,0   |        |
| 180 "         |             |        |        |        |        | 46,0   |        |
| 200 "         |             |        |        |        |        | 51,0   |        |
| 220 "         |             |        |        |        |        | 56,0   |        |
| 240 "         |             |        |        |        |        | 60,0   |        |
| 260 "         |             |        |        |        |        | 64,0   | 22,6   |
| 280 "         |             |        |        |        |        | 67,0   |        |
| 300 "         |             |        |        |        |        | 70,0   |        |
| 320 "         |             |        |        |        |        | 73,0   |        |
| 340 "         |             |        |        |        |        | 75,0   |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 27,5   |
| Verlust       |             |        |        |        |        |        | 1,3    |

|                   |     |     |     |  |  |
|-------------------|-----|-----|-----|--|--|
| Stockpunkt °C     |     |     |     |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |
| Benzin (bis 200°) |     |     |     |  |  |
| Öl (200—320°)     |     |     |     |  |  |

Bemerkungen:

000025

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 18.12.43 Zeit 43 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 49           | 31,2           | 46,1                   | 35,6                                | 241                   |
| Kondens.-Öl    | 63           | 40,1           | 51,7                   | 39,8                                | 309                   |
| Paraffingatsch | 45           | 28,7           | 31,9                   | 24,6                                | 22,2                  |
| Ges.-Prod.     | 157          | 100,0          | 109,7                  | 100,0                               | 47,2                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20 °C     | 0,677       | 0,796   | 0,90                |                | 0,983                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 40     |        |
| 60 "          |        |        |        |        | 50     |        |
| 80 "          |        |        |        |        | 100    |        |
| 100 "         |        |        |        |        | 100    |        |
| 120 "         |        |        |        |        | 27,0   | 4,4    |
| 140 "         |        |        |        |        | 26,0   |        |
| 160 "         |        |        |        |        | 40,0   |        |
| 180 "         |        |        |        |        | 45,0   |        |
| 200 "         |        |        |        |        | 50,0   |        |
| 220 "         |        |        |        |        | 54,0   |        |
| 240 "         |        |        |        |        | 58,0   |        |
| 260 "         |        |        |        |        | 62,0   | 21,2   |
| 280 "         |        |        |        |        | 66,0   |        |
| 300 "         |        |        |        |        | 69,0   |        |
| 320 "         |        |        |        |        | 71,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 21,8   |
| Verlust       |        |        |        |        |        | 2,6    |

|                   |     |     |     |    |  |
|-------------------|-----|-----|-----|----|--|
| Stockpunkt °C     |     |     |     |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |    |  |
| Benzin (bis 200°) |     |     |     | 62 |  |
| Öl (200-320°)     |     |     |     | 38 |  |

Bemerkungen:

000026

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 11.12.73 Zeit      Betr.-Tage     

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 47           | 322            | 496                    | 367                                 | 247                   |
| Kondens.-Öl    | 64           | 438            | 565                    | 432                                 | 336                   |
| Paraffingatsch | 35           | 240            | 267                    | 267                                 | 184                   |
| Ges.-Prod.     | 146          | 1000           | 1308                   | 1000                                | 467                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20 °C     | 0.674       | 0.796   | 0.910               |                | 0.796                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        |        | 47     |
| 60 "          |             |        |        |        |        | 50     |        |
| 80 "          |             |        |        |        |        | 190    |        |
| 100 "         |             |        |        |        |        | 200    |        |
| 120 "         |             |        |        |        |        | 280    |        |
| 140 "         |             |        |        |        |        | 350    | 483    |
| 160 "         |             |        |        |        |        | 410    |        |
| 180 "         |             |        |        |        |        | 470    |        |
| 200 "         |             |        |        |        |        | 520    |        |
| 220 "         |             |        |        |        |        | 580    |        |
| 240 "         |             |        |        |        |        | 600    |        |
| 260 "         |             |        |        |        |        | 645    | 267    |
| 280 "         |             |        |        |        |        | 670    |        |
| 300 "         |             |        |        |        |        | 700    |        |
| 320 "         |             |        |        |        |        | 725    |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        | 1100   |
| Rückstand     |             |        |        |        |        |        | 23     |
| Verlust       |             |        |        |        |        |        |        |

|                   |     |     |     |    |  |
|-------------------|-----|-----|-----|----|--|
| Stockpunkt °C     |     |     |     |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |    |  |
| Benzin (bis 200°) |     |     |     | 62 |  |
| Öl (200-320°)     |     |     |     | 42 |  |

**Bemerkungen:**

000027

# Untersuchung der flüssigen Produkte

Ofen Nr. M Füllung B Dat. 14/12/44 Zeit 11:43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 64        | 356        | 529                    | 401                                  | 240                   |
| Kondens.-Öl    | 80        | 449        | 567                    | 430                                  | 334                   |
| Paraffingatsch | 36        | 200        | 222                    | 169                                  | 158                   |
| Ges.-Prod.     | 180       | 7000       | 1318                   | 1000                                 | 186                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0,673       | 0,777   | 0,80            |                | 0,982            |
| Olefine „SPL“ Vol. % |             |         |                 |                |                  |
| Jodzahl (Wijss)      |             |         |                 |                |                  |
| N Z / V Z            |             |         |                 |                |                  |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 49     |        |
| 60 „          |        |        |        |        | 50     |        |
| 80 „          |        |        |        |        | 150    |        |
| 100 „         |        |        |        |        | 240    |        |
| 120 „         |        |        |        |        | 340    |        |
| 140 „         |        |        |        |        | 370    | 5,17   |
| 160 „         |        |        |        |        | 430    |        |
| 180 „         |        |        |        |        | 440    |        |
| 200 „         |        |        |        |        | 550    |        |
| 220 „         |        |        |        |        | 590    |        |
| 240 „         |        |        |        |        | 620    |        |
| 260 „         |        |        |        |        | 650    | 14,2   |
| 280 „         |        |        |        |        | 680    |        |
| 300 „         |        |        |        |        | 710    |        |
| 320 „         |        |        |        |        | 730    |        |
| 340 „         |        |        |        |        |        |        |
| 360 „         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 84     |
| Verlust       |        |        |        |        |        | 30     |

| Stockpunkt °C     | SPL | N Z | V Z |
|-------------------|-----|-----|-----|
| Destill.-Prod.    |     |     |     |
| Benzin (bis 200°) |     |     |     |
| Öl (200-320°)     |     |     |     |

Bemerkungen:

000028

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 16.7.4 Zeit 11.15 Betr. Tage 1

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4.5       | 35.2       | 4.4                    | 34.1                                | 193.2                 |
| Kondens.-Öl    | 6.9       | 56.3       | 5.7                    | 46.2                                | 25.8                  |
| Paraffingatsch | 3.5       | 28.5       | 2.9                    | 19.9                                | 18.1                  |
| Ges.-Prod.     | 14.9      | 100.0      | 13.0                   | 100.0                               | 227.1                 |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0.69        | 0.776   | 0.91           |                | 0.784           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol.-% | Vol.-% | Vol.-% | Vol.-% | Vol.-% | Gew.-% |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 „          |        |        |        |        |        |        |
| 80 „          |        |        |        |        |        |        |
| 100 „         |        |        |        |        |        |        |
| 120 „         |        |        |        |        |        |        |
| 140 „         |        |        |        |        |        |        |
| 160 „         |        |        |        |        |        |        |
| 180 „         |        |        |        |        |        |        |
| 200 „         |        |        |        |        |        |        |
| 220 „         |        |        |        |        |        |        |
| 240 „         |        |        |        |        |        |        |
| 260 „         |        |        |        |        |        |        |
| 280 „         |        |        |        |        |        |        |
| 300 „         |        |        |        |        |        |        |
| 320 „         |        |        |        |        |        |        |
| 340 „         |        |        |        |        |        |        |
| 360 „         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        |        |

|                   |     |     |     |    |  |  |
|-------------------|-----|-----|-----|----|--|--|
| Stockpunkt °C     |     |     |     |    |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |    |  |  |
| Benzin (bis 200°) |     |     |     | 61 |  |  |
| Öl (200-320°)     |     |     |     | 29 |  |  |

Bemerkungen:

000029

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 8/9 243 Zeit Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 43        | 286        | 419                    | 323                                 | 277                   |
| Kondens.-Öl    | 65        | 451        | 570                    | 42                                  | 342                   |
| Paraffingatsch | 41        | 273        | 350                    | 253                                 | 212                   |
| Ges.-Prod.     | 1505      | 1000       | 1219                   | 1000                                | 746                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,68        | 0,715   | 0,74           |                | 0,53            |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedebeginn   | Vol. % |        |        |        |        |        | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|--------|
|               | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % |        |
| -40 °C        |        |        |        |        |        | 148    |        |
| 60 "          |        |        |        |        |        | 40     |        |
| 80 "          |        |        |        |        |        | 110    |        |
| 100 "         |        |        |        |        |        | 180    |        |
| 120 "         |        |        |        |        |        | 370    | 472    |
| 140 "         |        |        |        |        |        | 300    |        |
| 160 "         |        |        |        |        |        | 360    |        |
| 180 "         |        |        |        |        |        | 470    |        |
| 200 "         |        |        |        |        |        | 440    |        |
| 220 "         |        |        |        |        |        | 520    |        |
| 240 "         |        |        |        |        |        | 570    |        |
| 260 "         |        |        |        |        |        | 640    | 215    |
| 280 "         |        |        |        |        |        | 740    |        |
| 300 "         |        |        |        |        |        | 690    |        |
| 320 "         |        |        |        |        |        | 830    |        |
| 340 "         |        |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        | 341    |
| Verlust       |        |        |        |        |        |        | 15     |

| Stockpunkt °C     | SPL | N Z | V Z |
|-------------------|-----|-----|-----|
| Destill.-Prod.    |     |     |     |
| Benzin (bis 200°) |     |     |     |
| Öl (200-320°)     |     |     |     |

Bemerkungen:

000030

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 2.8.74 Zeit 1 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,40      | 32,0       | 46,5                   | 35,9                                 | 24,0                  |
| Kondens.-Öl    | 5,90      | 42,8       | 54,7                   | 43,4                                 | 33,1                  |
| Paraffingatsch | 3,48      | 25,2       | 32,0                   | 21,2                                 | 14,5                  |
| Ges.-Prod.     | 13,78     | 100,0      | 42,2                   | 30,0                                 | 20,0                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20 °C     | 0,727       | 0,781   | 0,760          | 0,760          | 0,727           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z   V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       | 0      | 0      | 37,0   | 1,9    | 4,3    |        |
| 60 "          | 0      | 0      |        | 2,2    | 5,0    |        |
| 80 "          | 0      | 0      |        | 1,1    | 12,0   |        |
| 100 "         | 0      | 0      |        | 1,1    | 13,0   |        |
| 120 "         | 0      | 0      |        | 1,1    | 25,0   | 47,0   |
| 140 "         | 0      | 0      |        | 3,0    | 22,0   |        |
| 160 "         | 0      | 0      |        | 3,9    | 37,0   |        |
| 180 "         | 0      | 0      |        | 4,9    | 45,0   |        |
| 200 "         | 0      | 0      |        | 7,4    | 50,0   |        |
| 220 "         | 0      | 0      |        | 5,0    | 55,0   |        |
| 240 "         | 0      | 0      |        | 5,5    | 50,0   |        |
| 260 "         | 0      | 0      |        | 3,3    | 30,0   | 32,0   |
| 280 "         | 0      | 0      |        | 1,3    | 15,0   |        |
| 300 "         | 0      | 0      |        | 0,7    | 10,0   |        |
| 320 "         | 0      | 0      |        | 0,7    | 2,0    |        |
| 340 "         | 0      | 0      |        | 2,3    | 4,0    |        |
| 360 "         | 0      | 0      |        |        |        |        |
| Siede-Ende °C | 320    |        |        |        |        |        |
| Rückstand     | 3,9    | 12,4   | 2,2    | 3,4    | 5,9    |        |
| Verlust       | 0,0    | 0,0    | 0,0    | 0,0    | 0,0    |        |

|                   |     |     |     |  |    |  |
|-------------------|-----|-----|-----|--|----|--|
| Stockpunkt °C     |     |     |     |  |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |    |  |
| Benzin (bis 200°) |     |     |     |  | 65 |  |
| Öl (200-320°)     |     |     |     |  | 42 |  |

Bemerkungen:

000031

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 15 Dat. 6.11.1913 Zeit 11.15 Betr. Tage     

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 1.2       | 24.5       | 35.3                   | 28.4                                 | 19.5                  |
| Kondens.-Öl    | 1.5       | 30.3       | 38.5                   | 31.0                                 | 24.4                  |
| Paraffingatsch | 2.25      | 45.4       | 56.5                   | 45.6                                 | 36.5                  |
| Ges.-Prod.     | 4.95      | 100.0      | 72.3                   | 100.0                                | 100.0                 |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|------------------|
|                      |             |         |                 |                |                  |
| Dichte bei 20° C     | 0.688       | 0.787   | 0.80            |                | 0.84             |
| Olefine „SPL“ Vol. % |             |         |                 |                |                  |
| Jodzahl (Wijss)      |             |         |                 |                |                  |
| N.Z / V.Z            |             |         |                 |                |                  |

Siedeanalyse

| Siedebeginn       | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|--------|--------|--------|--------|--------|--------|
| 40 °C             |        |        |        |        | 50     |        |
| 60 "              |        |        |        |        | 20     |        |
| 80 "              |        |        |        |        | 40     |        |
| 100 "             |        |        |        |        | 120    |        |
| 120 "             |        |        |        |        | 140    |        |
| 140 "             |        |        |        |        | 280    | 33.0   |
| 160 "             |        |        |        |        | 240    |        |
| 180 "             |        |        |        |        | 320    |        |
| 200 "             |        |        |        |        | 360    |        |
| 220 "             |        |        |        |        | 460    |        |
| 240 "             |        |        |        |        | 190    |        |
| 260 "             |        |        |        |        | 440    | 18.0   |
| 280 "             |        |        |        |        | 500    |        |
| 300 "             |        |        |        |        | 530    |        |
| 320 "             |        |        |        |        | 54.5   |        |
| 340 "             |        |        |        |        |        |        |
| 360 "             |        |        |        |        |        |        |
| Siede-Ende °C     |        |        |        |        |        |        |
| Rückstand         |        |        |        |        |        | 44.5   |
| Verlust           |        |        |        |        |        | 7.1    |
| Stockpunkt °C     |        |        |        |        |        |        |
| Destill.-Prod.    | SPL %  | N.Z    | V.Z    |        |        |        |
| Benzin (bis 200°) |        |        |        |        | 69     |        |
| Öl (200-320°)     |        |        |        |        | 51     |        |

Bemerkungen:

000032



# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 6.7.43 Zeit 1 Betr. Tage

| Produkt        | Anfall kg | Ge wichts- % | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|--------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 438       | 36,4         | 28,9                   | 20,3                                 | 2,8                   |
| Kondens.-Öl    | 42        | 4,5          | 0                      | 4,5                                  | 3,5                   |
| Paraffingatsch | 45        | 3,7          | 29,9                   | 34,0                                 | 3,16                  |
| Ges.-Prod.     | 1641      | 100,0        | 168,8                  | 100,0                                | 11,5                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin- gatsch | Gesamt-Produkt | Reaktions- wasser |
|----------------------|-------------|---------|------------------|----------------|-------------------|
|                      | 0,92        | 0,744   | 0,90             |                | 0,92              |
| Dichte bei 20° C     |             |         |                  |                |                   |
| Olefine „SPL“ Vol. % |             |         |                  |                | 0,92              |
| Jodzahl (Wijss)      |             |         |                  |                |                   |
| N Z / V Z            |             |         |                  |                |                   |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| 140 °C        |        |        |        |        | 5,2    |        |
| 60 "          |        |        |        |        | 3,0    |        |
| 80 "          |        |        |        |        | 19,9   |        |
| 100 "         |        |        |        |        | 12,0   |        |
| 120 "         |        |        |        |        | 33,0   |        |
| 140 "         |        |        |        |        | 34,9   | 5,1    |
| 160 "         |        |        |        |        | 38,0   |        |
| 180 "         |        |        |        |        | 41,0   |        |
| 200 "         |        |        |        |        | 48,0   |        |
| 220 "         |        |        |        |        | 50,0   |        |
| 240 "         |        |        |        |        | 59,0   |        |
| 260 "         |        |        |        |        | 62,0   |        |
| 280 "         |        |        |        |        | 63,0   |        |
| 300 "         |        |        |        |        | 60,0   |        |
| 320 "         |        |        |        |        | 60,0   |        |
| 340 "         |        |        |        |        | 60,0   |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 0,9    |

|                   |     |     |     |  |     |  |
|-------------------|-----|-----|-----|--|-----|--|
| Stockpunkt °C     |     |     |     |  |     |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |     |  |
| Benzin (bis 200°) |     |     |     |  | 2,8 |  |
| Öl (200-320°)     |     |     |     |  | 4,0 |  |

Bemerkungen:

000033

# Untersuchung der flüssigen Produkte

Ofen-Nr. 114 Füllung 113 Dat. 9.5.74 Zeit Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 45        | 30,7       | 447                    | 345                                  | 237                   |
| Kondens.-Öl    | 164       | 43,7       | 365                    | 435                                  | 337                   |
| Paraffingatsch | 375       | 25,6       | 285                    | 220                                  | 198                   |
| Ges.-Prod.     | 1465      | 100,0      | 1237                   | 1000                                 | 442                   |

| Kondens.-Prod.       | A K - Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|--------------|---------|-----------------|----------------|------------------|
| Dichte bei 20 °C     | 0,688        | 0,714   | 0,7             |                | 0,688            |
| Olefine „SPL“ Vol. % |              |         |                 |                |                  |
| Jodzahl (Wijss)      |              |         |                 |                |                  |
| N Z / V Z            |              |         |                 |                |                  |

| Siedeanalyse       | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|--------------------|-------------|--------|--------|--------|--------|--------|--------|
|                    | — 40 °C     |        |        |        |        | 53     |        |
|                    | 60 „        |        |        |        |        | 20     |        |
|                    | 80 „        |        |        |        |        | 10     |        |
|                    | 100 „       |        |        |        |        | 10     |        |
|                    | 120 „       |        |        |        |        | 230    | 465    |
|                    | 140 „       |        |        |        |        | 300    |        |
|                    | 160 „       |        |        |        |        | 370    |        |
|                    | 180 „       |        |        |        |        | 430    |        |
|                    | 200 „       |        |        |        |        | 430    |        |
|                    | 220 „       |        |        |        |        | 520    | 195    |
|                    | 240 „       |        |        |        |        | 540    |        |
|                    | 260 „       |        |        |        |        | 610    |        |
|                    | 280 „       |        |        |        |        | 640    |        |
|                    | 300 „       |        |        |        |        | 670    |        |
| 320 „              |             |        |        |        | 670    |        |        |
| 340 „              |             |        |        |        |        |        |        |
| 360 „              |             |        |        |        |        |        |        |
| Siede-Ende °C      |             |        |        |        |        |        |        |
| Rückstand          |             |        |        |        |        |        | 333    |
| Verlust            |             |        |        |        |        |        | 28     |
| Stockpunkt °C      |             |        |        |        |        |        |        |
| Destill.-Prod.     | SPL         | N Z    | V Z    |        |        |        |        |
| Benzin (bis 200 °) |             |        |        |        |        | 63     |        |
| Öl (200—320 °)     |             |        |        |        |        | 42     |        |

Bemerkungen:

000034

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 3/4.74 Zeit 45 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 44        | 320        | 466                    | 363                                  | 249                   |
| Kondens.-Öl    | 56        | 398        | 485                    | 376                                  | 295                   |
| Paraffingatsch | 495       | 307        | 336                    | 264                                  | 235                   |
| Ges.-Prod.     | 1595      | 1000       | 1287                   | 1000                                 | 1419                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0.686       | 0.750   | 0.90           |                | 0.995           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| 40 °C         |        |        |        |        | 49     |        |
| 60 "          |        |        |        |        | 36     |        |
| 80 "          |        |        |        |        | 100    |        |
| 100 "         |        |        |        |        | 180    |        |
| 120 "         |        |        |        |        | 260    | 449    |
| 140 "         |        |        |        |        | 336    |        |
| 160 "         |        |        |        |        | 398    |        |
| 180 "         |        |        |        |        | 440    |        |
| 200 "         |        |        |        |        | 495    |        |
| 220 "         |        |        |        |        | 536    |        |
| 240 "         |        |        |        |        | 576    |        |
| 260 "         |        |        |        |        | 600    | 203    |
| 280 "         |        |        |        |        | 650    |        |
| 300 "         |        |        |        |        | 690    |        |
| 320 "         |        |        |        |        | 740    |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 342    |
| Verlust       |        |        |        |        |        | 0%     |

|                   |     |     |     |  |    |  |
|-------------------|-----|-----|-----|--|----|--|
| Stockpunkt °C     |     |     |     |  |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |    |  |
| Benzin (bis 200°) |     |     |     |  | 63 |  |
| Öl (200-320°)     |     |     |     |  | 41 |  |

Bemerkungen:

000035

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 2.3.74 Zeit 43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 5,1       | 10,0       | 44,3                   | 36,2                                 | 24,5                  |
| Kondens.-Öl    | 6,2       | 42,9       | 50,1                   | 22,1                                 | 29,2                  |
| Paraffingatsch | 4,9       | 25,2       | 32,3                   | 11,7                                 | 19,3                  |
| Ges.-Prod.     | 15,9      | 100,0      | 130,8                  | 70,0                                 | 73,0                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|------------------|
| Dichte bei 20 ° C    | 0,678       | 0,777   | 0,77            |                | 0,925            |
| Olefine „SPL“ Vol. % |             |         |                 |                |                  |
| Jodzahl (Wijss)      |             |         |                 |                |                  |
| N Z / V Z            |             |         |                 |                |                  |

Siedeanalyse

| Siedebeginn       | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. %       |
|-------------------|--------|--------|--------|--------|--------|--------------|
| - 40 ° C          |        |        |        |        |        |              |
| 60 "              |        |        |        |        | 2,2    |              |
| 80 "              |        |        |        |        | 2,7    |              |
| 100 "             |        |        |        |        | 10,7   |              |
| 120 "             |        |        |        |        | 11,8   |              |
| 140 "             |        |        |        |        | 22,0   |              |
| 160 "             |        |        |        |        | 24,0   | 2,4          |
| 180 "             |        |        |        |        | 40,0   |              |
| 200 "             |        |        |        |        | 43,0   |              |
| 220 "             |        |        |        |        | 50,0   |              |
| 240 "             |        |        |        |        | 50,0   |              |
| 260 "             |        |        |        |        | 50,0   |              |
| 280 "             |        |        |        |        | 53,0   | 21,4         |
| 300 "             |        |        |        |        | 53,0   |              |
| 320 "             |        |        |        |        | 50,0   |              |
| 340 "             |        |        |        |        | 50,0   |              |
| 360 "             |        |        |        |        |        |              |
| Siede-Ende ° C    |        |        |        |        |        |              |
| Rückstand         |        |        |        |        |        |              |
| Verlust           |        |        |        |        |        | 1,0 0<br>2,0 |
| Stockpunkt) ° C   |        |        |        |        |        |              |
| Destill.-Prod.    | SPL    | N Z    | V Z    |        |        |              |
| Benzin (bis 200°) |        |        |        |        | 59     |              |
| Öl (200-320°)     |        |        |        |        | 49     |              |

Bemerkungen:

000036

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 1.12.77 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,96         | 29,3           | 42,5                   | 33,3                                | 22,7                  |
| Kondens.-Öl    | 6,3          | 42,8           | 54,9                   | 42,1                                | 32,7                  |
| Paraffingatsch | 4,75         | 28,5           | 31,7                   | 24,6                                | 22,1                  |
| Ges.-Prod.     | 14,91        | 100,0          | 109,0                  | 100,0                               | 87,5                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,683       | 0,796   | 0,80                |                | 0,745                |
| Öloline „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijs)       |             |         |                     |                |                      |
| N.Z. / V.Z.          |             |         |                     |                |                      |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 44     |        |
| 60 "          |        |        |        |        | 80     |        |
| 80 "          |        |        |        |        | 116    |        |
| 100 "         |        |        |        |        | 152    |        |
| 120 "         |        |        |        |        | 188    |        |
| 140 "         |        |        |        |        | 224    | 15,3   |
| 160 "         |        |        |        |        | 260    |        |
| 180 "         |        |        |        |        | 296    |        |
| 200 "         |        |        |        |        | 332    |        |
| 220 "         |        |        |        |        | 368    |        |
| 240 "         |        |        |        |        | 404    |        |
| 260 "         |        |        |        |        | 440    | 18,8   |
| 280 "         |        |        |        |        | 476    |        |
| 300 "         |        |        |        |        | 512    |        |
| 320 "         |        |        |        |        | 548    |        |
| 340 "         |        |        |        |        | 584    |        |
| 360 "         |        |        |        |        | 620    |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 34,7   |
| Verlust       |        |        |        |        |        | 1,5    |

|                   |     |     |     |     |  |
|-------------------|-----|-----|-----|-----|--|
| Stockpunkt °C     |     |     |     |     |  |
| Destill.-Prod.    | SPL | N Z | V Z |     |  |
| Benzin (bis 200°) |     |     |     | 6,1 |  |
| Öl (200-320°)     |     |     |     | 4,4 |  |

Bemerkungen: 9

000037

**Untersuchung der flüssigen Produkte**

Ofen Nr. 11 Füllung 13 Dat. 30.6.48 Zeit 17.48 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,20         | 22,5           | 43,3                   | 33,3                                 | 22,4                  |
| Kondens.-Öl    | 6,20         | 42,5           | 16,2                   | 43,3                                 | 33,5                  |
| Paraffingatsch | 3,85         | 22,0           | 30,4                   | 33,4                                 | 20,8                  |
| Ges.-Prod.     | 14,25        | 100,0          | 129,9                  | 100,0                                | 76,0                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,683       | 0,725   | 0,77                | 0,76           | 0,475                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jödzahl (Wijss)      |             |         |                     |                |                      |
| N.Z. / V.Z.          |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       | 2,9    | 1,4    | 1,0    | 3,0    | 4,9    |        |
| 60 "          | 2,9    |        |        | 8,3    | 6,9    |        |
| 80 "          |        |        |        | 13,3   | 15,2   |        |
| 100 "         | 2,9    | 1,0    |        | 20,2   | 19,0   |        |
| 120 "         |        | 1,0    |        | 21,2   | 20,5   |        |
| 140 "         |        | 15,0   |        | 33,6   | 37,0   | 25,9   |
| 160 "         |        | 23,0   |        | 37,7   | 37,7   |        |
| 180 "         |        | 26,0   |        | 40,7   | 37,7   |        |
| 200 "         | 9,0    | 32,0   |        | 47,7   | 37,7   |        |
| 220 "         |        | 32,0   |        | 52,7   | 37,7   |        |
| 240 "         |        | 32,0   |        | 52,7   | 37,7   |        |
| 260 "         |        | 32,0   |        | 52,7   | 37,7   |        |
| 280 "         |        | 32,0   |        | 52,7   | 37,7   |        |
| 300 "         |        | 32,0   |        | 52,7   | 37,7   |        |
| 320 "         |        | 32,0   |        | 52,7   | 37,7   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     | 3,1    | 1,0    | 8,2    | 30,2   | 32,9   |        |
| Verlust       | 2,2    | 0,0    | 0,8    | 2,7    | 1,1    |        |

| Stockpunkt °C | Destill.-Prod.    | SPL | N.Z. | V.Z.     |
|---------------|-------------------|-----|------|----------|
|               | Benzin (bis 200°) |     |      |          |
|               | Öl (200-320°)     |     |      | 61<br>40 |

Bemerkungen:

000038

824  
 392 482 48.5  
 58 143  
 334 339  
 334

Jan  
 Mar  
 Mar  
 Jan  
 Jan

1.02 67.3  
79.7 40

Ch 13 90

CO2 36 20

36.5  
 11.2  
 24.8

441.67

18  
 38  
 35  
 41  
 41  
 39  
 67  
279

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 29/30.6.45 Zeit      Betr. Tage     

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|----------------------|
| A.K.-Benzin    | 41        | 24,7       | 404                    | 314                                 | 215                  |
| Kondens.-Öl    | 65        | 40,9       | 565                    | 438                                 | 341                  |
| Paraffingatsch | 47        | 28,4       | 319                    | 248                                 | 221                  |
| Ges.-Prod.     | 148       | 100,0      | 1288                   | 1000                                | 477                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,686       | 0,747   | 0,81           |                | 1,15            |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wjss)       |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| 40 °C         |        |        |        |        | 52     |        |
| 60 "          |        |        |        |        | 15     |        |
| 80 "          |        |        |        |        | 115    |        |
| 100 "         |        |        |        |        | 168    |        |
| 120 "         |        |        |        |        | 26     | 455    |
| 140 "         |        |        |        |        | 320    |        |
| 160 "         |        |        |        |        | 30     |        |
| 180 "         |        |        |        |        | 440    |        |
| 200 "         |        |        |        |        | 490    |        |
| 220 "         |        |        |        |        | 490    |        |
| 240 "         |        |        |        |        | 1530   |        |
| 260 "         |        |        |        |        | 590    |        |
| 280 "         |        |        |        |        | 070    | 199    |
| 300 "         |        |        |        |        | 640    |        |
| 320 "         |        |        |        |        | 170    |        |
| 340 "         |        |        |        |        | 615    |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 334    |
| Verlust       |        |        |        |        |        | 112    |

|                   |     |     |     |          |  |  |
|-------------------|-----|-----|-----|----------|--|--|
| Stockpunkt °C     |     |     |     |          |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |          |  |  |
| Benzin (bis 200°) |     |     |     | 0,611 mm |  |  |
| Öl (200-320°)     |     |     |     | 160      |  |  |
|                   |     |     |     | 40       |  |  |

Bemerkungen:

000040



# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 28. 2. 6. 43 Zeit 1 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,60      | 31,4       | 46,1                   | 35,3                                 | 24,1                  |
| Kondens.-Öl    | 6,30      | 43,0       | 55,4                   | 48,6                                 | 33,9                  |
| Paraffingatsch | 3,75      | 25,6       | 38,8                   | 32,1                                 | 18,6                  |
| Ges.-Prod.     | 14,65     | 100,0      | 130,6                  | 100,0                                | 76,6                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20 °C     | 0,685       | 0,723   | 0,89           |                | 0,984           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       | 2,0    | 3,0    | 9,0    | 1,0    | 2,0    |        |
| 60 „          | 1,0    |        |        |        |        |        |
| 80 „          | 43,0   | 1,0    |        | 15,0   | 2,0    |        |
| 100 „         | 5,0    | 5,0    |        | 2,0    | 1,0    |        |
| 120 „         | 0,0    | 5,0    |        | 1,0    |        |        |
| 140 „         | 0,0    | 13,0   |        | 2,0    | 2,0    |        |
| 160 „         | 0,0    | 2,0    |        | 2,0    | 5,0    |        |
| 180 „         | 0,0    | 3,0    |        | 2,0    | 0,0    |        |
| 200 „         | 0,0    | 4,0    |        | 2,0    | 2,0    |        |
| 220 „         | 0,0    | 4,0    |        | 2,0    | 5,0    |        |
| 240 „         | 0,0    | 3,0    |        | 2,0    | 2,0    |        |
| 260 „         | 0,0    | 2,0    |        | 2,0    | 2,0    |        |
| 280 „         | 0,0    | 2,0    |        | 2,0    |        |        |
| 300 „         | 0,0    | 2,0    | 4,0    | 2,0    |        | 3,0    |
| 320 „         | 0,0    | 2,0    | 2,0    | 2,0    |        |        |
| 340 „         | 0,0    |        |        | 2,0    |        |        |
| 360 „         | 0,0    |        |        |        |        |        |
| Siede-Ende °C | 310    |        |        |        |        |        |
| Rückstand     | 2,0    | 1,0    | 2,0    | 2,0    |        |        |
| Verlust       | 0,0    | 0,0    | 1,0    | 1,0    |        |        |

| Stockpunkt °C     | SPL | N Z | V Z        |
|-------------------|-----|-----|------------|
| Destill.-Prod.    |     |     |            |
| Benzin (bis 200°) |     |     |            |
| Öl (200-320°)     |     |     | 0,5<br>3,9 |

Bemerkungen:

000041

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 15 Dat. 29. IX. 63 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,2          | 29,3           | 43,0                   | 33,2                                | 22,6                  |
| Kondens.-Öl    | 6,0          | 41,7           | 53,4                   | 41,6                                | 32,2                  |
| Paraffingatsch | 4,15         | 29,0           | 32,6                   | 25,2                                | 22,7                  |
| Ges.-Prod.     | 14,35        | 100,0          | 109,5                  | 100,0                               | 47,5                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,684       | 0,714   | 0,89                |                | 0,96                 |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 4,6    |        |
| 60 "          |        |        |        |        | 1,0    |        |
| 80 "          |        |        |        |        | 1,0    |        |
| 100 "         |        |        |        |        | 2,0    |        |
| 120 "         |        |        |        |        | 2,0    | 4,0    |
| 140 "         |        |        |        |        | 2,0    |        |
| 160 "         |        |        |        |        | 3,0    |        |
| 180 "         |        |        |        |        | 4,0    |        |
| 200 "         |        |        |        |        | 4,0    |        |
| 220 "         |        |        |        |        | 5,0    |        |
| 240 "         |        |        |        |        | 5,0    |        |
| 260 "         |        |        |        |        | 5,0    | 18,8   |
| 280 "         |        |        |        |        | 6,0    |        |
| 300 "         |        |        |        |        | 6,0    |        |
| 320 "         |        |        |        |        | 6,0    |        |
| 340 "         |        |        |        |        | 6,0    |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 34,0   |
| Verlust       |        |        |        |        |        | 1,9    |

|                   |     |     |     |     |  |
|-------------------|-----|-----|-----|-----|--|
| Stockpunkt °C     |     |     |     |     |  |
| Destill.-Prod.    | SPL | N Z | V Z |     |  |
| Benzin (bis 200°) |     |     |     | 1,6 |  |
| Öl (200-320°)     |     |     |     | 3,9 |  |

Bemerkungen:

000042

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 26.11.43 Zeit 10.43 Betr. Tage

| Produkt        | Anfäll kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 5,3       | 34,8       | 78,3                   | 27,9                                | 27,8                  |
| Kondens.-Öl    | 6,1       | 39,4       | 78,2                   | 29,2                                | 30,6                  |
| Paraffingatsch | 4,1       | 26,4       | 78,5                   | 21,2                                | 20,6                  |
| Ges.-Prod.     | 15,5      | 100,0      | 78,1                   | 100,0                               | 22,6                  |

| Kondens.-Prod.       | A K-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,782      | 0,748   | 0,79           |                |                 |
| Oleline „SPL“ Vol. % |            |         |                |                | 0,984           |
| Jodzahl (Wijs)       |            |         |                |                |                 |
| N Z / V Z            |            |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        |        |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        |        |        |
| 140 "         |        |        |        |        |        |        |
| 160 "         |        |        |        |        |        |        |
| 180 "         |        |        |        |        |        |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        |        |        |
| 240 "         |        |        |        |        |        |        |
| 260 "         |        |        |        |        |        |        |
| 280 "         |        |        |        |        |        |        |
| 300 "         |        |        |        |        |        |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 89,2   |

| Stockpunkt °C     | SPL | N Z | V Z |
|-------------------|-----|-----|-----|
| Destill.-Prod.    |     |     |     |
| Benzin (bis 200°) |     |     |     |
| Öl (200-320°)     |     |     |     |

Bemerkungen:

000043

# Untersuchung der flüssigen Produkte

Ofen Nr. M Füllung 1.5 Dat. 5/26. 6. 53 Zeit          Betr. Tage         

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 41        | 28.9       | 142.6                  | 33.0                                 | 27.4                  |
| Kondens.-Öl    | 54        | 38.0       | 152                    | 13.2                                 | 39.5                  |
| Paraffingatsch | 47        | 33.1       | 31.2                   | 2.88                                 | 25.6                  |
| Ges.-Prod.     | 142       | 100        | 120                    | 13.0                                 | 29.5                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0.677       | 0.775   | 0.829          |                |                 |
| Olefine „SPL“ Vol. % |             |         |                |                | 1.140           |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z. V Z             |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 43     |        |
| 60 "          |        |        |        |        | 70     |        |
| 80 "          |        |        |        |        | 110    |        |
| 100 "         |        |        |        |        | 150    |        |
| 120 "         |        |        |        |        | 260    | 440    |
| 140 "         |        |        |        |        | 320    |        |
| 160 "         |        |        |        |        | 380    |        |
| 180 "         |        |        |        |        | 430    |        |
| 200 "         |        |        |        |        | 480    |        |
| 220 "         |        |        |        |        | 520    |        |
| 240 "         |        |        |        |        | 560    |        |
| 260 "         |        |        |        |        | 600    | 195    |
| 280 "         |        |        |        |        | 650    |        |
| 300 "         |        |        |        |        | 680    |        |
| 320 "         |        |        |        |        | 720    |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 351    |

| Stockpunkt °C | Destill.-Prod.    | SPL | N Z | V Z |
|---------------|-------------------|-----|-----|-----|
|               | Benzin (bis 200°) |     |     | 63  |
|               | Öl (200-320°)     |     |     | 40  |

Bemerkungen: 000044

# Untersuchung der flüssigen Produkte

Ofen-Nr. 11 Füllung 13 Dat. 24.12.56 Zeit 6.43 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 2,35         | 54,5           | 24,2                   | 22,8                                | 119,5                 |
| Kondens.-Öl    | 2,20         | 39,8           | 36,8                   | 35,3                                | 33,0                  |
| Paraffingatsch | 4,37         | 45,7           | 3,6                    | 5,9                                 | 24,2                  |
| Ges.-Prod.     | 4,92         | 100,0          | 19,7                   | 100,0                               | 176,7                 |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,659       | 0,774   | 0,789               |                | 0,535                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z + V Z            |             |         |                     |                |                      |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 42     |        |
| 60 "          |        |        |        |        | 50     |        |
| 80 "          |        |        |        |        | 70     |        |
| 100 "         |        |        |        |        | 150    |        |
| 120 "         |        |        |        |        |        |        |
| 140 "         |        |        |        |        | 250    | 324    |
| 160 "         |        |        |        |        | 350    |        |
| 180 "         |        |        |        |        |        |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        | 450    |        |
| 240 "         |        |        |        |        | 470    |        |
| 260 "         |        |        |        |        | 570    |        |
| 280 "         |        |        |        |        | 560    |        |
| 300 "         |        |        |        |        | 570    |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 2,2    |

|                   |     |     |     |  |  |
|-------------------|-----|-----|-----|--|--|
| Stockpunkt °C     |     |     |     |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |
| Benzin (bis 200°) |     |     |     |  |  |
| Öl (200-320°)     |     |     |     |  |  |

Bemerkungen:

000045

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Datum 11.11.69 Zeit      Betr. Tage     

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 39        | 293        | 426                    | 329                                  | 226                   |
| Kondens.-Öl    | 58        | 436        | 503                    | 435                                  | 337                   |
| Paraffingatsch | 36        | 271        | 305                    | 236                                  | 110                   |
| Ges.-Prod.     | 133       | 1000       | 1234                   | 1000                                 | 673                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,684       | 0,415   | 0,89           |                |                 |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        | 43     |        |
|               | 60 „        |        |        |        |        | 51     |        |
|               | 80 „        |        |        |        |        | 56     | 156    |
|               | 100 „       |        |        |        |        | 56     |        |
|               | 120 „       |        |        |        |        | 54     |        |
|               | 140 „       |        |        |        |        | 51     | 172    |
|               | 160 „       |        |        |        |        | 55     |        |
|               | 180 „       |        |        |        |        | 49     | 138    |
|               | 200 „       |        |        |        |        | 46     |        |
|               | 220 „       |        |        |        |        | 53     |        |
|               | 240 „       |        |        |        |        | 54     | 119    |
|               | 260 „       |        |        |        |        | 61     |        |
|               | 280 „       |        |        |        |        | 65     |        |
|               | 300 „       |        |        |        |        | 68     | 119    |
| 320 „         |             |        |        |        | 71     |        |        |
| 340 „         |             |        |        |        |        |        |        |
| 360 „         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 244    |
| Verlust       |             |        |        |        |        |        | 08     |

| Stockpunkt °C | Destill.-Prod.    | SPL   | N Z    | V Z |
|---------------|-------------------|-------|--------|-----|
|               | Benzin (bis 200°) | 0,618 | 0,425  |     |
|               | Öl (200-320°)     | 0,423 | 1,13   |     |
|               | Bemerkungen:      | 0,151 | 1,23   |     |
|               | 200-250           | 0,467 | 0,662  |     |
|               | 250-320           | 0,120 | 0,1815 |     |

000046

# Untersuchung der flüssigen Produkte

Ofen Nr. 18 Füllung 13 Dat. 21.12.42 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,4          | 30,9           | 45,0                   | 34,8                                | 92,9                  |
| Kondens.-Öl    | 4,8          | 43,6           | 56,3                   | 43,4                                | 22,7                  |
| Paraffingatsch | 2,8          | 25,5           | 28,3                   | 21,9                                | 18,6                  |
| Ges.-Prod.     | 11,0         | 100,0          | 29,5                   | 100,0                               |                       |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,729       | 0,776   | 0,90                | 0,862          | 0,900                |
| Olefins „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z   V Z            |             |         |                     |                |                      |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| 40 °C         | 2,0    | 2,7    | 3,5    | 5,2    | 6,9    |        |
| 60 „          | 12,0   |        |        | 19,0   | 25,9   |        |
| 80 „          | 25,0   |        |        | 34,0   | 45,0   |        |
| 100 „         | 38,0   | 3,0    |        | 47,0   | 62,0   |        |
| 120 „         | 50,0   | 7,0    |        | 54,0   | 71,0   |        |
| 140 „         | 62,0   | 12,0   |        | 66,0   | 87,0   | 57,4   |
| 160 „         | 75,0   | 17,0   |        | 73,0   | 95,0   |        |
| 180 „         | 80,0   | 20,0   |        | 78,0   | 100,0  |        |
| 200 „         | 88,0   | 24,0   |        | 82,0   | 100,0  |        |
| 220 „         | 92,0   | 27,0   |        | 85,0   | 100,0  |        |
| 240 „         | 95,0   | 28,0   |        | 87,0   | 100,0  |        |
| 260 „         |        | 29,0   | 1,0    | 88,0   | 100,0  |        |
| 280 „         |        | 30,0   | 2,0    | 89,0   | 100,0  | 82,9   |
| 300 „         |        | 31,0   | 3,0    | 90,0   | 100,0  |        |
| 320 „         |        | 32,0   | 4,0    | 91,0   | 100,0  |        |
| 340 „         |        | 33,0   | 5,0    | 92,0   | 100,0  |        |
| 360 „         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     | 3,2    | 15,9   | 89,0   | 20,0   |        | 1,9    |
| Verlust       | 1,1    | 0,0    | 0,0    | 0,0    |        | 0,9    |

| Stockpunkt °C     | SPL | N Z | V Z |  |    |  |
|-------------------|-----|-----|-----|--|----|--|
| Destill.-Prod.    |     |     |     |  |    |  |
| Benzin (bis 200°) |     |     |     |  | 60 |  |
| Öl (200-320°)     |     |     |     |  | 37 |  |

Bemerkungen:

000047

Untersuchung der flüssigen Produkte

Ofen-Nr. 11 Füllung 13 Dat. 20.10.64 Zelt 43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,2       | 39,4       | 47,1                   | 33,2                                 | 39,7                  |
| Kondens.-Öl    | 6,1       | 49,5       | 55,2                   | 49,6                                 | 39,9                  |
| Paraffingatsch | 4,0       | 38,0       | 31,4                   | 52,9                                 | 31,6                  |
| Ges.-Prod.     | 14,3      | 100,0      | 43,9                   | 45,0                                 | 37,2                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20 °C     | 0,723       | 0,723   | 0,721          |                | 0,985           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijs)       |             |         |                |                |                 |
| NZ / VZ              |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 48     |        |
| 60 "          |        |        |        |        | 50     |        |
| 80 "          |        |        |        |        | 51,5   |        |
| 100 "         |        |        |        |        | 52,9   |        |
| 120 "         |        |        |        |        | 54,5   | 55,0   |
| 140 "         |        |        |        |        | 56,0   |        |
| 160 "         |        |        |        |        | 57,0   |        |
| 180 "         |        |        |        |        | 58,0   |        |
| 200 "         |        |        |        |        | 59,0   |        |
| 220 "         |        |        |        |        | 60,0   |        |
| 240 "         |        |        |        |        | 61,0   |        |
| 260 "         |        |        |        |        | 62,0   | 9,1    |
| 280 "         |        |        |        |        | 63,0   |        |
| 300 "         |        |        |        |        | 64,0   |        |
| 320 "         |        |        |        |        | 65,0   |        |
| 340 "         |        |        |        |        | 66,0   |        |
| 360 "         |        |        |        |        | 67,0   |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 9,1    |
| Verlust       |        |        |        |        |        |        |

|                   |     |    |    |    |  |  |
|-------------------|-----|----|----|----|--|--|
| Stockpunkt °C     |     |    |    |    |  |  |
| Destill.-Prod.    | SPL | NZ | VZ |    |  |  |
| Benzin (bis 200°) |     |    |    | 29 |  |  |
| Öl. (200-320°)    |     |    |    | 29 |  |  |

Bemerkungen:

000048



DVA

# Untersuchung der flüssigen Produkte

 Ofen Nr. 11 Füllung 13 Dat. 19/10/65 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 41           | 283            | 411                    | 319                                 | -211                  |
| Kondens.-Öl    | 65           | 448            | 598                    | 447                                 | 398                   |
| Paraffingatsch | 39           | 269            | 367                    | 234                                 | 108                   |
| Ges.-Prod.     | 145          | 1000           | 1274                   | 1000                                | 1115                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0.689       | 0.976   | 0.89                |                | 0.385                |
| Olefine „SPL“ Vol.-% |             |         |                     |                | 8                    |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 55     |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        |        |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        | 250    |        |
| 140 "         |        |        |        |        | 120    | 468    |
| 160 "         |        |        |        |        | 220    |        |
| 180 "         |        |        |        |        | 450    |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        |        |        |
| 240 "         |        |        |        |        | 550    |        |
| 260 "         |        |        |        |        | 590    |        |
| 280 "         |        |        |        |        | 680    | 290    |
| 300 "         |        |        |        |        |        |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 310    |
| Verlust       |        |        |        |        |        | (1)    |

| Stockpunkt °C     | Destill.-Prod. | SPL | N Z | V Z |
|-------------------|----------------|-----|-----|-----|
| Benzin (bis 200°) |                |     |     |     |
| Öl (200-320°)     |                |     |     |     |

Bemerkungen:

000049

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 18/19.6.43 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 3,70         | 24,6           | 35,8                   | 28,2                                 | 19,3                  |
| Kondens.-Öl    | 6,65         | 44,3           | 54,0                   | 44,8                                 | 34,7                  |
| Paraffingatsch | 4,70         | 31,3           | 32,3                   | 27,0                                 | 24,6                  |
| Ges.-Prod.     | 15,05        | 100,0          | 122,1                  | 100,0                                | 78,6                  |

| Kondens.-Prod.       | A-K-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |  |  | Reaktions-<br>wasser |
|----------------------|------------|---------|---------------------|----------------|--|--|----------------------|
| Dichte bei 20 °C     | 0,680      | 0,726   | 0,91                |                |  |  | 0,983                |
| Olefine „SPL“ Vol. % |            |         |                     |                |  |  |                      |
| Jodzahl (Wijss)      |            |         |                     |                |  |  |                      |
| N Z / V Z            |            |         |                     |                |  |  |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        |        |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        |        |        |
| 140 "         |        |        |        |        |        |        |
| 160 "         |        |        |        |        |        |        |
| 180 "         |        |        |        |        |        |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        |        |        |
| 240 "         |        |        |        |        |        |        |
| 260 "         |        |        |        |        |        |        |
| 280 "         |        |        |        |        |        |        |
| 300 "         |        |        |        |        |        |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 560 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        |        |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200-320°)     |     |     |     |  |  |  |

Bemerkungen:         

000050

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Fällung 15 Dat. 19/12/63 Zeit 10:00 Betr. Tage 1

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 40        | 288        | 420                    | 326                                 | 223                   |
| Kondens.-Ol    | 59        | 424        | 548                    | 426                                 | 334                   |
| Paraffingatsch | 40        | 288        | 320                    | 248                                 | 223                   |
| Ges.-Prod.     | 139       | 1000       | 1288                   | 1000                                | 779                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
|                      |             |         |                |                |                 |
| Dichte bei 20° C     | 0.685       | 0.796   | 0.90           |                |                 |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 42     |        |
| 60 "          |        |        |        |        | 60     |        |
| 80 "          |        |        |        |        | 120    |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        | 240    | 42.4   |
| 140 "         |        |        |        |        | 300    |        |
| 160 "         |        |        |        |        | 360    |        |
| 180 "         |        |        |        |        | 320    |        |
| 200 "         |        |        |        |        | 440    |        |
| 220 "         |        |        |        |        | 520    |        |
| 240 "         |        |        |        |        | 540    |        |
| 260 "         |        |        |        |        | 640    | 22.3   |
| 280 "         |        |        |        |        | 640    |        |
| 300 "         |        |        |        |        | 670    |        |
| 320 "         |        |        |        |        | 125    |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 33.9   |
| Verlust       |        |        |        |        |        | 1.5    |

|                   |     |       |     |  |    |  |
|-------------------|-----|-------|-----|--|----|--|
| Stockpunkt °C     |     |       |     |  |    |  |
| Destill.-Prod.    | SPL | N Z   | V Z |  |    |  |
| Benzin (bis 200°) |     | 12.65 |     |  | 62 |  |
| Öl (200-320°)     |     | 0.65  |     |  | 41 |  |

Bemerkungen:

000051

Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 10 Dat. 10/11.6.49 Zeit 1 Betr. Tage

| Produkt        | Anfall<br>kr | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 40           | 26,1           | 380                    | 27,4                                 | 26,9                  |
| Kondens.-Öl    | 65           | 42,5           | 596                    | 42,7                                 | 39,2                  |
| Paraffingatsch | 48           | 31,4           | 353                    | 27,6                                 | 24,6                  |
| Ges.-Prod.     | 153          | 100            | 1299                   | 100,0                                | 98,7                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,687       | 0,718   | 0,87                |                |                      |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z V Z              |             |         |                     |                |                      |

| Siedebeginn   | Vol. % |         | Vol. % |         | Gew. % |        |
|---------------|--------|---------|--------|---------|--------|--------|
|               | Vol. % | Vol. %  | Vol. % | Vol. %  | Vol. % | Gew. % |
| - 40 °C       | 35     | 2,2     | 2,50   |         | 45     |        |
| 60 "          | 35     |         |        |         | 40     |        |
| 80 "          | 35     |         |        |         | 30     |        |
| 100 "         | 35     |         |        |         | 25     |        |
| 120 "         | 35     | 45      |        | 3,6     | 210    | 313    |
| 140 "         | 35     | 50      |        | 10,2    | 275    |        |
| 160 "         | 35     | 66      |        | 27,6    | 275    |        |
| 180 "         | 35     | 83      |        | 41,9    | 375    |        |
| 200 "         | 35     | 310/111 |        | 42 (52) | 425    |        |
| 220 "         | 35     | 405     |        | 49,1    | 460    |        |
| 240 "         | 35     | 49      |        | 42,1    | 320    |        |
| 260 "         | 35     | 58      |        | 37,1    | 375    |        |
| 280 "         | 35     | 66      | 1,7    | 10,2    | 320    | 240    |
| 300 "         | 35     | 75      | 2,7    | 10,2    | 320    |        |
| 320 "         | 35     |         | 6,5    | 10,2    | 65     |        |
| 340 "         | 35     |         |        |         |        |        |
| 360 "         | 35     |         |        |         |        |        |
| Siede-Ende °C | 25     |         |        |         |        |        |
| Rückstand     | 30     | 112     | 5,9    | 40,9    | 39,1   |        |
| Verlust       | 10     | 0,4     | 0,4    | 3,5     | 8,6    |        |

| Stockpunkt °C     | Destill.-Prod. |     |     |
|-------------------|----------------|-----|-----|
|                   | SPL            | N Z | V Z |
| Benzin (bis 200°) |                |     |     |
| Öl (200-320°)     |                |     |     |

Bemerkungen:

000052

# Untersuchung der flüssigen Produkte

Ofen Nr. 177 Füllung 73 Dat. 18/11/43 Zeit 10:15 Betr. Tage 1

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 2.14         | 100            | 1.00                   | 1.00                                 | 1.00                  |
| Kondens.-Öl    |              |                |                        |                                      |                       |
| Paraffingatsch |              |                |                        |                                      |                       |
| Ges.-Prod.     | 2.14         | 100            | 1.00                   | 1.00                                 | 1.00                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     |             |         |                     |                |                      |
| Oleline „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            | M           |         |                     |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        |        |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        |        |        |
| 140 "         |        |        |        |        |        |        |
| 160 "         |        |        |        |        |        |        |
| 180 "         |        |        |        |        |        |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        |        |        |
| 240 "         |        |        |        |        |        |        |
| 260 "         |        |        |        |        |        |        |
| 280 "         |        |        |        |        |        |        |
| 300 "         |        |        |        |        |        |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        |        |

|                   |     |     |     |  |  |
|-------------------|-----|-----|-----|--|--|
| Stockpunkt °C     |     |     |     |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |
| Benzin (bis 200°) |     |     |     |  |  |
| Öl (200-320°)     |     |     |     |  |  |

**Bemerkungen:**

000053

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13.11 Dat. 19/11/56 Zeit 6.45 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 33        | 370        | 53%                    | 403                                  | 298                   |
| Kondens.-Öl    | 48        | 540        | 69%                    | 522                                  | 406                   |
| Paraffingatsch | 08        | 90         | 10%                    | 75                                   | 08                    |
| Ges.-Prod.     | 89        | 1000       | 132%                   | 1000                                 | 152                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch. | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|-----------------|----------------|-----------------|
| Dichte bei 20° C     | 0.630       | 0.796   | 0.851           |                |                 |
| Olefine „SPL“ Vol. % |             |         |                 |                |                 |
| Jodzahl (Wijss)      |             |         |                 |                |                 |
| N Z / V Z            |             |         |                 |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| 40 °C         |        |        |        |        | 33     |        |
| 60 „          |        |        |        |        | 37     |        |
| 80 „          |        |        |        |        | 10     |        |
| 100 „         |        |        |        |        |        |        |
| 120 „         |        |        |        |        |        |        |
| 140 „         |        |        |        |        | 53     |        |
| 160 „         |        |        |        |        |        |        |
| 180 „         |        |        |        |        |        |        |
| 200 „         |        |        |        |        | 80     |        |
| 220 „         |        |        |        |        |        |        |
| 240 „         |        |        |        |        |        |        |
| 260 „         |        |        |        |        |        |        |
| 280 „         |        |        |        |        |        |        |
| 300 „         |        |        |        |        |        |        |
| 320 „         |        |        |        |        |        |        |
| 340 „         |        |        |        |        |        |        |
| 360 „         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        |        |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200-320°)     |     |     |     |  |  |  |

Bemerkung: 000054

Untersuchung der flüssigen Produkte

Ofen-Nr. 11 Füllung 12 Dat. \_\_\_\_\_ Zeit \_\_\_\_\_ Betr. Tage \_\_\_\_\_

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 500          | 100,0          |                        |                                      |                       |
| Kondens.-Öl    |              |                |                        |                                      |                       |
| Paraffingatsch |              |                |                        |                                      |                       |
| Ges.-Prod.     | 1460         | 100,0          |                        |                                      |                       |

| Kondens.-Prod.      | A.K. Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|---------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20 °C    |             |         |                     |                |                      |
| Olefin „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)     |             |         |                     |                |                      |
| N Z / V Z           |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        |        |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        |        |        |
| 140 "         |        |        |        |        |        |        |
| 160 "         |        |        |        |        |        |        |
| 180 "         |        |        |        |        |        |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        |        |        |
| 240 "         |        |        |        |        |        |        |
| 260 "         |        |        |        |        |        |        |
| 280 "         |        |        |        |        |        |        |
| 300 "         |        |        |        |        |        |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        |        |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200—320°)     |     |     |     |  |  |  |

Bemerkungen:

000055

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 12/11/65 Zeit 6:15 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 409       | 31,5       | 485                    | 354                                 | 24,3                  |
| Kondens.-Öl    | 54        | 4,2        | 531                    | 413                                 | 32,1                  |
| Paraffingatsch | 36        | 2,75       | 239                    | 253                                 | 21,4                  |
| Ges.-Prod.     | 1394      | 100,0      | 1185                   | 1000                                | 79,8                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt |  | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|--|-----------------|
| Dichte bei 20° C     | 0,685       | 0,776   | 0,72           |                |  | 0,010           |
| Olefine „SPL“ Vol. % |             |         |                |                |  |                 |
| Jodzahl (Wijss)      |             |         |                |                |  |                 |
| N Z / V Z            |             |         |                |                |  |                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40° C     |        |        |        |        | 4,5    |        |
|               | 60 "        |        |        |        |        | 50     |        |
|               | 80 "        |        |        |        |        | 16     |        |
|               | 100 "       |        |        |        |        | 150    |        |
|               | 120 "       |        |        |        |        | 225    | 44,3   |
|               | 140 "       |        |        |        |        | 360    |        |
|               | 160 "       |        |        |        |        | 420    |        |
|               | 180 "       |        |        |        |        | 480    |        |
|               | 200 "       |        |        |        |        | 480    |        |
|               | 220 "       |        |        |        |        | 540    |        |
|               | 240 "       |        |        |        |        | 570    |        |
|               | 260 "       |        |        |        |        | 640    |        |
|               | 280 "       |        |        |        |        | 670    |        |
|               | 300 "       |        |        |        |        | 670    |        |
| 320 "         |             |        |        |        | 715    |        |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 33,2   |
| Verlust       |             |        |        |        |        |        | 0,7    |

|                   |     |     |     |  |    |  |
|-------------------|-----|-----|-----|--|----|--|
| Stockpunkt °C     |     |     |     |  |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |    |  |
| Benzin (bis 200°) |     |     |     |  | 59 |  |
| Öl (200-320°)     |     |     |     |  | 58 |  |

Bemerkungen:

000056



Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 15 Dat. 11/17 6:43 Zeit Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 26           | 29.2           | 485                    | 330                                  | 227                   |
| Kondens.-Öl    | 55           | 42.8           | 553                    | 413                                  | 325                   |
| Paraffingatsch | 54.5         | 28.0           | 344                    | 241                                  | 204                   |
| Ges.-Prod.     | 235          | 100.0          | 429                    | 304                                  | 224                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0.686       | 0.90    |                |                |                 |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        |        |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        |        |        |
| 140 "         |        |        |        |        |        |        |
| 160 "         |        |        |        |        |        |        |
| 180 "         |        |        |        |        |        |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        |        |        |
| 240 "         |        |        |        |        |        |        |
| 260 "         |        |        |        |        |        |        |
| 280 "         |        |        |        |        |        |        |
| 300 "         |        |        |        |        |        |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 35     |
| Verlust       |        |        |        |        |        |        |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200-320°)     |     |     |     |  |  |  |

Bemerkungen:

000057

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 14 Füllung 13 Dat. 10.11.23 Zeit 13:20 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,03      | 11,9       | 53,6                   | 40,8                                | 32,0                  |
| Kondens.-Öl    | 5,68      | 16,9       | 54,2                   | 41,4                                | 33,0                  |
| Paraffingatsch | 4,24      | 12,8       | 43,2                   | 37,8                                | 16,3                  |
| Ges.-Prod.     | 13,95     | 41,6       | 50,4                   | 40,0                                | 26,3                  |

| Kondens.-Prod.       | AK-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-----------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,686     | 0,723   | 0,74           |                | 0,924           |
| Olefine „SPL“ Vol. % |           |         |                |                |                 |
| Jodzahl (Wijss)      |           |         |                |                |                 |
| N Z / V Z            |           |         |                |                |                 |

Siedeanalyse

| Siedebeginn       | Vol. %    | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|-----------|--------|--------|--------|--------|--------|
| - 40 °C           | 4,0       | 9      | 10     | 10     | 5      |        |
| 60 "              | 24,0      |        |        | 9      |        |        |
| 80 "              | 11,0      |        |        | 6      |        |        |
| 100 "             | 5,0       | 9,0    |        | 2,2    | 4,0    |        |
| 120 "             | 6,0       |        |        | 2,5    | 5,0    |        |
| 140 "             | 25,0, 9,0 |        |        | 3,3    | 7,0    |        |
| 160 "             | 2,0       |        |        | 0,7    |        | 7,1    |
| 180 "             | 2,0       | 2,0    |        | 0,7    |        |        |
| 200 "             | 3,0       |        |        | 0,9    |        |        |
| 220 "             | 3,0       |        |        | 0,9    |        |        |
| 240 "             |           |        |        |        |        |        |
| 260 "             |           |        | 1,0    | 0,9    |        |        |
| 280 "             |           |        | 0,7    | 0,5    |        |        |
| 300 "             |           |        |        | 1,1    |        | 3,3    |
| 320 "             |           |        |        | 2,2    |        |        |
| 340 "             |           |        |        | 2,2    |        |        |
| 360 "             |           |        |        |        |        |        |
| Siede-Ende °C     |           |        |        |        |        |        |
| Rückstand         | 2,0       | 1,0    | 0,5    | 2,0    |        |        |
| Verlust           | 2,5       | 0,1    | 1,0    | 0,9    |        | 1,2    |
| Stockpunkt °C     |           |        |        |        |        |        |
| Destill.-Prod.    | SPL       | N Z    | V Z    |        |        |        |
| Benzin (bis 200°) |           |        |        |        | 53     |        |
| Öl (200-320°)     |           |        |        |        | 33     |        |

Bemerkungen:

000058

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 2/10.6.73 Zeit          Betr. Tage         

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 49        | 36,2       | 530                    | 469                                  | 246                   |
| Kondens.-Öl    | 54        | 39,9       | 549                    | 3914                                 | 205                   |
| Paraffingatsch | 323       | 23,9       | 260                    | 199                                  | 183                   |
| Ges.-Prod.     | 1353      | 100,0      | 1409                   | 1000                                 | 164                   |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0,684       | 0,769   | 0,92            | 0,81           | 0,915            |
| Olefine „SPL“-Vol. % |             |         |                 |                |                  |
| Jodzahl (Wijs)       |             |         |                 |                |                  |
| N Z / V Z            |             |         |                 |                |                  |

Siedeanalyse

| Siedebeginn   | Vol.-% | Vol.-% | Vol.-% | Vol.-% | Vol.-% | Gew.-% |
|---------------|--------|--------|--------|--------|--------|--------|
| -40 °C        | 10     | 18     | 260    | 0,4    | 56     |        |
| 60 "          | 210    |        |        | 75     | 16     |        |
| 80 "          | 390    |        |        | 152    | 80     |        |
| 100 "         | 550    | 20     |        | 222    | 140    |        |
| 120 "         | 640    | 40     |        | 286    | 240    |        |
| 140 "         | 780    | 95     | 40     | 332    | 310    | 463    |
| 160 "         | 840    | 160    |        | 344    | 380    |        |
| 180 "         | 900    | 260    |        | 465    | 450    |        |
| 200 "         | 920    | 340    | 225    | 516    | 500    |        |
| 220 "         | 950    | 460    |        | 566    | 540    |        |
| 240 "         |        | 560    |        | 605    | 520    |        |
| 260 "         |        | 650    |        | 644    | 620    | 214    |
| 280 "         |        | 720    | 10     | 670    | 660    |        |
| 300 "         |        | 790    | 30     | 702    | 690    |        |
| 320 "         |        | 840    | 80     | 722    | 715    |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C | 220-28 |        |        |        |        |        |
| Rückstand     | 29     | 49,2   | 915    | 799    | -      | 315    |
| Verlust       | 1,1    | 0,3    | 10     | 0,4    |        | 15     |

| Stockpunkt °C     | SPL | N Z | V Z | Reaktion |
|-------------------|-----|-----|-----|----------|
| Destill.-Prod.    |     |     |     |          |
| Benzin (bis 200°) |     |     |     | 54       |
| Öl (200-320°)     |     |     |     | 34       |

Bemerkungen:

000059

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 8/9.6.43 Zeit          Betr. Tage         

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 5,33      | 25,3       | 516                    | 29,5                                 | 37,0                  |
| Kondens.-Öl    | 6,44      | 39,8       | 415                    | 29,5                                 | 29,6                  |
| Paraffingatsch | 3,78      | 24,9       | 374                    | 31,0                                 | 19,1                  |
| Ges.-Prod.     | 15,55     | 100,0      | 130,5                  | 100,0                                | 85,7                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt |  | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|--|------------------|
|                      |             |         |                 |                |  |                  |
| Dichte bei 20 °C     | 0,685       | 0,724   | 0,71            |                |  | 0,493            |
| Olefine „SPL“ Vol. % |             |         |                 |                |  |                  |
| Jodzahl (Wijss)      |             |         |                 |                |  |                  |
| N Z / V Z            |             |         |                 |                |  |                  |

Siedeanalyse

| Siedebeginn   | Vol. % |        |        |        |        | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
|               | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % |        |
| - 40 °C       | 27     | 28     | 9,60   | 39     | 38     |        |
| 60 "          | 39     |        |        | 41     | 40     |        |
| 80 "          | 70     |        |        | 12     | 12,0   |        |
| 100 "         | 10     | 40     |        | 29     | 29,0   |        |
| 120 "         | 40     | 60     |        | 22     | 27,0   | 47,1   |
| 140 "         | 55     | 100    |        | 27     | 34,0   |        |
| 160 "         | 80     | 180    |        | 36     | 43,0   |        |
| 180 "         | 70     | 22     |        | 21     | 42,0   |        |
| 200 "         | 140    | 240    | 23,6   | 20,6   | 101    |        |
| 220 "         | 39     | 22     |        | 53     | 50     |        |
| 240 "         | 50     | 22     |        | 12     | 29,0   |        |
| 260 "         |        | 60     |        | 2      | 3,0    |        |
| 280 "         |        | 20     | 2,9    | 27     | 64,0   | 14,4   |
| 300 "         |        | 60     | 4,6    | 20,6   | 29,0   |        |
| 320 "         |        | 22     | 2,0    | 3,6    | 21,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C | 100    |        |        |        |        |        |
| Rückstand     | 2,1    | 12,4   |        | 29,6   | 30,3   |        |
| Verlust       | 13,9   | 2,0    |        | 1,4    |        |        |

| Stockpunkt °C     | Destill.-Prod. |     |      |
|-------------------|----------------|-----|------|
|                   | SPL            | N Z | V. Z |
| Benzin (bis 200°) |                |     |      |
| Öl (200-320°)     |                |     |      |

Bemerkungen:

000060

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 1/8.6.43 Zeit      Betr. Tage     

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 57        | 300        | 440                    | 338                                  | 231                   |
| Kondens.-Öl    | 19        | 405        | 538                    | 413                                  | 310                   |
| Paraffingatsch | 56        | 195        | 324                    | 249                                  | 224                   |
| Ges.-Prod.     | 190       | 1000       | 1302                   | 1000                                 | 464                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0.681       | 0.754   | 0.91           |                | 0.982           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 38     |        |
| 60 "          |        |        |        |        | 140    |        |
| 80 "          |        |        |        |        | 150    |        |
| 100 "         |        |        |        |        | 230    |        |
| 120 "         |        |        |        |        | 300    | 476    |
| 140 "         |        |        |        |        | 340    |        |
| 160 "         |        |        |        |        | 420    |        |
| 180 "         |        |        |        |        | 440    |        |
| 200 "         |        |        |        |        | 590    |        |
| 220 "         |        |        |        |        | 560    |        |
| 240 "         |        |        |        |        | 590    |        |
| 260 "         |        |        |        |        | 610    | 182    |
| 280 "         |        |        |        |        | 650    |        |
| 300 "         |        |        |        |        | 680    |        |
| 320 "         |        |        |        |        | 465    |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 324    |
| Verlust       |        |        |        |        |        | 15     |

|                   |     |     |     |  |      |  |
|-------------------|-----|-----|-----|--|------|--|
| Stockpunkt °C     |     |     |     |  |      |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |      |  |
| Benzin (bis 200°) |     |     |     |  | 0.11 |  |
| Öl (200-320°)     |     |     |     |  | 55   |  |
|                   |     |     |     |  | 35   |  |

Bemerkungen:

000061

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung A3 Dat. 6.9.6.43 Zeit Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,95      | 33,1       | 48,3                   | 3,73                                 | 25,6                  |
| Kondens.-Öl    | 6,00      | 40,1       | 5,14                   | 40,0                                 | 3,11                  |
| Paraffingatsch | 6,00      | 36,2       | 1,91                   | 3,37                                 | 3,09                  |
| Ges.-Prod.     | 14,95     | 100,0      | 55,34                  | 100,0                                | 31,6                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch. | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|-----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,685       | 0,723   | 0,920           |                | 0,983           |
| Olefine „SPL“ Vol. % |             |         |                 |                | 1               |
| Jodzahl (Wijss)      |             |         |                 |                |                 |
| N Z / V Z            |             |         |                 |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| 40 °C         |        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        | 3,0    |        |
| 100 "         |        |        |        |        | 10,0   |        |
| 120 "         |        |        |        |        | 2,0    |        |
| 140 "         |        |        |        |        | 2,0    | 45,3   |
| 160 "         |        |        |        |        | 2,0    |        |
| 180 "         |        |        |        |        | 2,0    |        |
| 200 "         |        |        |        |        | 2,0    |        |
| 220 "         |        |        |        |        | 2,0    |        |
| 240 "         |        |        |        |        | 2,0    |        |
| 260 "         |        |        |        |        | 2,0    | 3,07   |
| 280 "         |        |        |        |        | 2,0    |        |
| 300 "         |        |        |        |        | 2,0    |        |
| 320 "         |        |        |        |        | 2,0    |        |
| 340 "         |        |        |        |        | 2,0    |        |
| 360 "         |        |        |        |        | 2,0    |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 3,07   |
| Verlust       |        |        |        |        |        |        |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200-320°)     |     |     |     |  |  |  |

Bemerkungen:

000062

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 5.11.64 Zeit 13:43 Betr. Tage 1

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 567       | 377        | 506                    | 390                                  | 267                   |
| Kondens.-Öl    | 66        | 402        | 518                    | 400                                  | 311                   |
| Paraffingatsch | 44        | 251        | 273                    | 210                                  | 193                   |
| Ges.-Prod.     | 1637      | 1030       | 1297                   | 1000                                 | 771                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,6852      | 0,996   | 0,99           |                |                 |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Völ. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| — 40 °C       |        |        |        |        | 48     |        |
| 60 "          |        |        |        |        | 40     |        |
| 80 "          |        |        |        |        | 175    |        |
| 100 "         |        |        |        |        | 180    |        |
| — 120 "       |        |        |        |        | 200    | 76,9   |
| 140 "         |        |        |        |        | 340    |        |
| 160 "         |        |        |        |        | 420    |        |
| 180 "         |        |        |        |        | 470    |        |
| 200 "         |        |        |        |        | 570    |        |
| 220 "         |        |        |        |        | 550    |        |
| 240 "         |        |        |        |        | 510    |        |
| 260 "         |        |        |        |        | 630    | 21,0   |
| 280 "         |        |        |        |        | 640    |        |
| 300 "         |        |        |        |        | 700    |        |
| 320 "         |        |        |        |        | 725    |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 30,6   |

| Stockpunkt °C     | SPL | N Z | V Z |      |  |
|-------------------|-----|-----|-----|------|--|
| Destill.-Prod.    |     |     |     |      |  |
| Benzin (bis 200°) |     |     |     | 21,1 |  |
| Öl (200–320°)     |     |     |     | 59   |  |
|                   |     |     |     | 39   |  |

Bemerkungen:

000063

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 18 Dat. 25.11.48 Zeit 11.45 Betr. Tage

| Produkt        | Anfall - kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-------------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 0,26        | 4,4        | 20,0                   | 52,5                                | 0,59                  |
| Kondens.-Öl    | 5,04        | 82,7       | 41,2                   | 30,8                                | 3,40                  |
| Paraffingatsch | 2,22        | 36,8       | 33,3                   | 16,7                                | 1,83                  |
| Ges.-Prod.     | 7,52        | 100,0      | 100,0                  | 100,0                               | 2,57                  |

| Kondens.-Prod.       | A K - Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|--------------|---------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0,72         | 0,74    | 0,71            |                | 0,72             |
| Olefine „SPL“ Vol. % |              |         |                 |                |                  |
| Jodzahl (Wijss)      |              |         |                 |                |                  |
| N Z / V Z            |              |         |                 |                |                  |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        |        |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        |        |        |
| 140 "         |        |        |        |        |        |        |
| 160 "         |        |        |        |        |        |        |
| 180 "         |        |        |        |        |        |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        |        |        |
| 240 "         |        |        |        |        |        |        |
| 260 "         |        |        |        |        |        |        |
| 280 "         |        |        |        |        |        |        |
| 300 "         |        |        |        |        |        |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        |        |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V-Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200-320°)     |     |     |     |  |  |  |

Bemerkungen:

000064



# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung AS Dat. 3.19.64 Zeit 6.43 Betr. Tage

| Produkt        | Anfall, kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|------------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 12,17      | 57,4       | 84,7                   | 619                                  | 419                   |
| Kondens.-Öl    | 5,8        | 27,5       | 35,3                   | 258                                  | 202                   |
| Paraffingatsch | 3,2        | 15,1       | 16,8                   | 125                                  | 111                   |
| Ges.-Prod.     | 21,17      | 100,0      | 136,8                  | 1000                                 | 133,8                 |

| Kondens.-Prod.       | A K - Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|--------------|---------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0,678        | 0,780   | 0,90            | 0,80           | 0,978            |
| Olefine „SPL“ Vol. % |              |         |                 |                |                  |
| Jodzahl (Wijs)       |              |         |                 |                |                  |
| N Z / V Z            |              |         |                 |                |                  |

Siedeanalyse

| Siedebeginn   | Vok <sup>3</sup> % | Vol. % | Vol. % | Vok <sup>3</sup> % | Vol. % | Gew. % |
|---------------|--------------------|--------|--------|--------------------|--------|--------|
| - 40 °C       | 30                 | 85     | 220    | 19                 | 42     |        |
| 60 "          | 220                |        |        | 136                | 60     |        |
| 80 "          | 420                |        |        | 260                | 180    |        |
| 100 "         | 540                | 30     |        | 370                | 300    |        |
| 120 "         | 720                | 45     |        | 460                | 400    | 65,4   |
| 140 "         | 820                | 60     |        | 535                | 500    |        |
| 160 "         | 880                | 70     |        | 600                | 570    |        |
| 180 "         | 920                | 78     |        | 659                | 620    |        |
| 200 "         | 930                | 80     | 84,4   | 685                | 660    |        |
| 220 "         | 940                | 81     |        | 712                | 690    |        |
| 240 "         | 950                | 82     |        | 730                | 720    |        |
| 260 "         |                    | 83     |        | 760                | 740    | 13,5   |
| 280 "         |                    | 84     |        | 784                | 760    |        |
| 300 "         |                    | 85     |        | 800                | 780    |        |
| 320 "         |                    | 86     |        | 819                | 800    |        |
| 340 "         |                    | 87     |        |                    |        |        |
| 360 "         |                    |        |        |                    |        |        |
| Siede-Ende °C | 1000               |        |        |                    |        |        |
| Rückstand     | 35                 | 15,3   | 91,4   | 200                | 194    |        |
| Verlust       | 26                 | 12,3   | 82     | 15                 | 29     |        |

| Stockpunkt °C     | Destill.-Prod. |  |  | SPL |  | N Z |  | V Z |  |
|-------------------|----------------|--|--|-----|--|-----|--|-----|--|
| Benzin (bis 200°) |                |  |  |     |  |     |  |     |  |
| Öl (200-320°)     |                |  |  |     |  |     |  |     |  |

Bemerkungen:

000065

990000

67.10.1877  
73.1  
7.17  
-88  
109  
7.08.84  
Z

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 2/3. 1922 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 14,44        | 68,3           | 11,6                   | 23,1                                | 47,9                  |
| Kondens.-Öl    | 5,30         | 28,1           | 4,5                    | 12,3                                | 19,4                  |
| Paraffingatsch | 2,92         | 14,6           | 1,5                    | 3,6                                 | 12,7                  |
| Ges.-Prod.     | 22,66        | 100,0          | 13,6                   | 39,0                                | 80,0                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     |             |         |                     |                | 0,920                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z V Z              |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn     | - Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-----------------|----------|--------|--------|--------|--------|--------|
| -40 °C          |          |        |        |        |        |        |
| 60 „            |          |        |        |        |        |        |
| 80 „            |          |        |        |        |        |        |
| 100 „           |          |        |        |        |        |        |
| 120 „           |          |        |        |        |        |        |
| 140 „           |          |        |        |        |        |        |
| 160 „           |          |        |        |        |        |        |
| 180 „           |          |        |        |        |        |        |
| 200 „           |          |        |        |        |        |        |
| 220 „           |          |        |        |        |        |        |
| 240 „           |          |        |        |        |        |        |
| 260 „           |          |        |        |        |        |        |
| 280 „           |          |        |        |        |        |        |
| 300 „           |          |        |        |        |        |        |
| 320 „           |          |        |        |        |        |        |
| 340 „           |          |        |        |        |        |        |
| 360 „           |          |        |        |        |        |        |
| Siede-Ende 10 C |          |        |        |        |        |        |
| Rückstand       |          |        |        |        |        |        |
| Verlust         |          |        |        |        |        |        |

|                   |     |     |     |  |  |
|-------------------|-----|-----|-----|--|--|
| Stockpunkt °C     |     |     |     |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |
| Benzin (bis 200°) |     |     |     |  |  |
| Öl (200-320°)     |     |     |     |  |  |

Bemerkungen:

000067

# Untersuchung der flüssigen Produkte

Ofen-Nr. 11 Füllung 13. Dat. 1/12. 6. 45 Zeit          Betr. Tage         

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 25.04     | 73.6       | 109.4                  | 47.6                                 | 52.1                  |
| Kondens.-Öl    | 5.3       | 15.5       | 20.1                   | 14.2                                 | 11.0                  |
| Paraffingatsch | 3.71      | 10.9       | 11.6                   | 8.2                                  | 8.9                   |
| Ges.-Prod.     | 34.04     | 100.0      | 141.1                  | 70.0                                 | 70.8                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20 °C     | 0.672       | 0.773   | 0.94           |                | 0.982           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedebeginn   | Vol. %  |          | Vol. %  |          | Gew. %  |          |
|---------------|---------|----------|---------|----------|---------|----------|
|               | Vol. 1% | Vol. 10% | Vol. 1% | Vol. 10% | Vol. 1% | Vol. 10% |
| -40 °C        | 10      | 85       | 230     | 48       | 10      |          |
| 60 "          | 180     |          |         | 140      | 20      |          |
| 80 "          | 400     |          |         | 340      | 240     |          |
| 100 "         | 600     | 30       |         | 460      | 340     |          |
| 120 "         | 1150    | 91.4     | 10      | 580      | 500     | 72.4     |
| 140 "         | 140     | 100      |         | 680      | 600     |          |
| 160 "         | 240     | 200      |         | 730      | 600     |          |
| 180 "         | 330     | 300      |         | 760      | 700     |          |
| 200 "         | 350     | 400      | 86.3    | 770      | 730     |          |
| 220 "         |         | 500      |         | 790      | 750     |          |
| 240 "         |         | 600      |         | 800      | 770     |          |
| 260 "         |         | 700      | 10      | 820      | 780     | 10.2     |
| 280 "         |         | 760      | 20      | 830      | 790     |          |
| 300 "         |         | 820      | 30      | 830      | 800     |          |
| 320 "         |         | 870      | 40      | 850      | 820     |          |
| 340 "         |         |          |         |          |         |          |
| 360 "         |         |          |         |          |         |          |
| Siede-Ende °C | 781     |          |         |          |         |          |
| Rückstand     | 62      | 13.7     | 94      | 170      | 148     |          |
| Verlust       | 24      | 60       | 61      | 16       | 30      |          |

| Stockpunkt °C     | SPL | N Z | V Z |
|-------------------|-----|-----|-----|
| Destill.-Prod.    |     |     |     |
| Benzin (bis 200°) |     |     |     |
| Öl (200-320°)     |     |     |     |

Bemerkungen:

000068

# Untersuchung der flüssigen Produkte

Ofen Nr. M Füllung 13 Dat. 21.11.63 Zeit      Betr. Tage     

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 247       | 137        | 1084                   | 1144                                | 523                   |
| Kondens.-Öl    | 56        | 167        | 215                    | 153                                 | 119                   |
| Paraffingatsch | 32        | 96         | 102                    | 113                                 | 19                    |
| Ges.-Prod.     | 335       | 105        | 1406                   | 1600                                | 111                   |

| Kondens.-Prod.       | A.K. Benzin | Ölkönd. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|------------------|
| Dichte bei 20 °C     | 0.697       | 0.745   | 0.94            |                | 0.982            |
| Olefine „SPL“ Vol. % |             |         |                 |                |                  |
| Jodzahl (Wijss)      |             |         |                 |                |                  |
| N Z / V Z            |             |         |                 |                |                  |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     | 40     | 83     | 130    | 40     | 41     |        |
| 60 "          | 150         |        |        | 110    | 80     |        |        |
| 80 "          | 420         |        |        | 308    | 210    |        |        |
| 100 "         | 620         | 30     |        | 453    | 410    |        |        |
| 120 "         | 160         | 954-60 |        | 516    | 560    | 1143   |        |
| 140 "         | 270         | 100    |        | 448    | 660    |        |        |
| 160 "         | 370         | 110    |        | 432    | 420    |        |        |
| 180 "         | 390         | 290    |        | 440    | 450    |        |        |
| 200 "         | 250         | 400    | 845    | 495    | 411    |        |        |
| 220 "         |             | 510    |        | 412    | 200    |        |        |
| 240 "         |             | 600    |        | 426    | 220    |        |        |
| 260 "         |             | 620    | 10     | 439    | 230    | 83     |        |
| 280 "         |             | 760    | 10     | 451    | 240    |        |        |
| 300 "         |             | 810    | 20     | 460    | 250    |        |        |
| 320 "         |             | 860    | 10     | 470    | 265    |        |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C | 196.5       |        |        |        |        |        |        |
| Rückstand     | 28          | 154    | 341    | 158    |        | 127    |        |
| Verlust       | 18          | 01     | 02     | 14     |        | 47     |        |

|                   |     |     |     |    |  |
|-------------------|-----|-----|-----|----|--|
| Stockpunkt °C     |     |     |     |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |    |  |
| Benzin (bis 200°) |     |     |     | 67 |  |
| Öl (200-320°)     |     |     |     | 38 |  |
|                   |     |     |     | 35 |  |

**Bemerkungen:**

000069

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 30.3.15.43 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 17,2         | 59,0           | 265                    | 140                                  | 42,6                  |
| Kondens.-Öl    | 6,8          | 23,2           | 30,0                   | 33,3                                 | 12,3                  |
| Paraffingatsch | 5,2          | 17,8           | 182                    | 130                                  | 12,1                  |
| Ges.-Prod.     | 29,2         | 100,0          | 185,3                  | 190,0                                | 23,4                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,732       | 0,744   | 0,95                |                | 0,732                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z F V Z            |             |         |                     |                |                      |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        |        | 12     |
| 60 "          |             |        |        |        |        | 140    |        |
| 80 "          |             |        |        |        |        | 190    |        |
| 100 "         |             |        |        |        |        | 220    |        |
| 120 "         |             |        |        |        |        | 270    | 13,5   |
| 140 "         |             |        |        |        |        | 270    |        |
| 160 "         |             |        |        |        |        | 270    |        |
| 180 "         |             |        |        |        |        | 270    |        |
| 200 "         |             |        |        |        |        | 270    |        |
| 220 "         |             |        |        |        |        | 270    |        |
| 240 "         |             |        |        |        |        | 270    |        |
| 260 "         |             |        |        |        |        | 270    | 13,5   |
| 280 "         |             |        |        |        |        | 270    |        |
| 300 "         |             |        |        |        |        | 270    |        |
| 320 "         |             |        |        |        |        | 270    |        |
| 340 "         |             |        |        |        |        | 270    |        |
| 360 "         |             |        |        |        |        | 270    |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        |        |
| Verlust       |             |        |        |        |        |        |        |

|                   |     |     |     |           |  |  |
|-------------------|-----|-----|-----|-----------|--|--|
| Stockpunkt °C     | SPL | N Z | V Z | Distillat |  |  |
| Destill.-Prod.    |     |     |     |           |  |  |
| Benzin (bis 200°) |     |     |     | 27        |  |  |
| Öl (200—320°)     |     |     |     | 29        |  |  |

**Bemerkungen:** 7

000070

# Untersuchung der flüssigen Produkte

Ofen Nr. M Füllung 15 Dat. 29.10.54 Zeit 5.45 Betr. Tage     

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100-g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 209       | 47.2       | 105.0                  | 153                                 | 509                   |
| Kondens.-Öl    | 1506      | 47.2       | 22.2                   | 159                                 | 12.3                  |
| Paraffingatsch | 349       | 11.6       | 12.2                   | 88                                  | 84                    |
| Ges.-Prod.     | 2959      | 100.0      | 129.4                  | 1100                                | 411.6                 |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0.644       | 0.745   | 0.95            |                | 0.932            |
| Ölefine „SPL“ Vol.-% |             |         |                 |                |                  |
| Jodzahl (Wijss)      |             |         |                 |                |                  |
| N Z / V Z            |             |         |                 |                |                  |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        | 71     |        |
| 80 "          |        |        |        |        | 40     |        |
| 100 "         |        |        |        |        | 250    |        |
| 120 "         |        |        |        |        | 420    |        |
| 140 "         |        |        |        |        | 570    | 144    |
| 160 "         |        |        |        |        | 640    |        |
| 180 "         |        |        |        |        | 750    |        |
| 200 "         |        |        |        |        | 770    |        |
| 220 "         |        |        |        |        | 770    |        |
| 240 "         |        |        |        |        | 790    |        |
| 260 "         |        |        |        |        | 810    |        |
| 280 "         |        |        |        |        | 830    | 11.0   |
| 300 "         |        |        |        |        | 850    |        |
| 320 "         |        |        |        |        | 870    |        |
| 340 "         |        |        |        |        | 880    |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 120    |
| Verlust       |        |        |        |        |        | 26     |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200-320°)     |     |     |     |  |  |  |

Bemerkungen:

000071

# Untersuchung der flüssigen Produkte

Ofen Nr. M Füllung 13 Dat. 28/29. 5. 43 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 928          | 522            | 1993                   | 541                                 | 386                   |
| Kondens.-Öl    | 45           | 255            | 328                    | 242                                 | 184                   |
| Paraffingatsch | 40           | 215            | 253                    | 184                                 | 166                   |
| Ges.-Prod.     | 1013         | 1000           | 1354                   | 1000                                | 736                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0.676       | 0.711   | 0.89                |                | 0.83                 |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

|  | Siedebeginn   | Vol. %  | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|--|---------------|---------|--------|--------|--------|--------|--------|
|  | Siedeanalyse  | — 40 °C |        |        |        |        | 40     |
|  | 60 „          |         |        |        |        | 50     |        |
|  | 80 „          |         |        |        |        | 160    |        |
|  | 100 „         |         |        |        |        | 260    |        |
|  | 120 „         |         |        |        |        | 360    | 545    |
|  | 140 „         |         |        |        |        | 440    |        |
|  | 160 „         |         |        |        |        | 490    |        |
|  | 180 „         |         |        |        |        | 530    |        |
|  | 200 „         |         |        |        |        | 540.5  |        |
|  | 220 „         |         |        |        |        | 600    |        |
|  | 240 „         |         |        |        |        | 630    |        |
|  | 260 „         |         |        |        |        | 650    | 155    |
|  | 280 „         |         |        |        |        | 670    |        |
|  | 300 „         |         |        |        |        | 690    |        |
|  | 320 „         |         |        |        |        | 710    |        |
|  | 340 „         |         |        |        |        |        |        |
|  | 360 „         |         |        |        |        |        |        |
|  | Siede-Ende °C |         |        |        |        |        |        |
|  | Rückstand     |         |        |        |        |        | 973    |
|  | Verlust       |         |        |        |        |        | 24     |

|                   |     |     |     |    |  |
|-------------------|-----|-----|-----|----|--|
| Stockpunkt °C     |     |     |     |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |    |  |
| Benzin (bis 200°) |     |     |     | 40 |  |
| Öl (200–320°)     |     |     |     | 45 |  |

Bemerkungen: 9

000072



# Untersuchung der flüssigen Produkte

Ofen Nr. M Füllung 15 Dat. 16.11.54 Zeit 5.45 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 17.7      | 63.4       | 9.1                    | 6.9                                 | 45.4                  |
| Kondens.-Öl    | 9.65      | 27.3       | 35.2                   | 25.3                                | 19.6                  |
| Paraffingatsch | 2.6       | 9.3        | 10.4                   | 7.5                                 | 6.4                   |
| Ges.-Prod.     | 29.95     | 100.0      | 139.7                  | 100.0                               | 71.4                  |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|------------------|
| Dichte bei 20 ° C    | 0.675       | 0.776   | 0.89            |                | 0.934            |
| Olefine „SPL“ Vol. % |             |         |                 |                |                  |
| Jodzahl (Wijss)      |             |         |                 |                |                  |
| N Z / V Z            |             |         |                 |                |                  |

Siedeanalyse

| Siedebeginn    | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. %    |
|----------------|--------|--------|--------|--------|--------|-----------|
| - 40 ° C       |        |        |        |        |        |           |
| 60 "           |        |        |        |        | 41     |           |
| 80 "           |        |        |        |        | 80     |           |
| 100 "          |        |        |        |        | 210    |           |
| 120 "          |        |        |        |        | 360    |           |
| 140 "          |        |        |        |        | 410    | 684       |
| 160 "          |        |        |        |        | 580    |           |
| 180 "          |        |        |        |        | 650    |           |
| 200 "          |        |        |        |        | 680    |           |
| 220 "          |        |        |        |        | 1110   |           |
| 240 "          |        |        |        |        | 1140   |           |
| 260 "          |        |        |        |        | 1160   |           |
| 280 "          |        |        |        |        | 1180   | 190       |
| 300 "          |        |        |        |        | 1190   |           |
| 320 "          |        |        |        |        | 1200   |           |
| 340 "          |        |        |        |        | 125    |           |
| 360 "          |        |        |        |        |        |           |
| Siede-Ende ° C |        |        |        |        |        |           |
| Rückstand      |        |        |        |        |        |           |
| Verlust        |        |        |        |        |        | 158<br>38 |

| Stockpunkt ° C | Destill.-Prod.    | SPL | N Z | V Z |
|----------------|-------------------|-----|-----|-----|
|                | Benzin (bis 200°) |     |     | 41  |
|                | Öl (200-320°)     |     |     | 36  |

Bemerkungen:

000073

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 25.10.53 Zeit 43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 15,65     | 69,7       | 458                    | 684                                 | 461                   |
| Kondens.-Öl    | 60        | 24,6       | 320                    | 229                                 | 144                   |
| Paraffingatsch | 26        | 10,7       | 129                    | 87                                  | 77                    |
| Ges.-Prod.     | 24,25     | 100,0      | 1400                   | 1000                                | 145                   |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,676       | 0,770   | 0,88           |                | 0,945           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijs)       |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        | 10     |        |
|               | 60 "        |        |        |        |        | 20     |        |
|               | 80 "        |        |        |        |        | 200    |        |
|               | 100 "       |        |        |        |        | 360    |        |
|               | 120 "       |        |        |        |        | 480    | 104    |
|               | 140 "       |        |        |        |        | 540    |        |
|               | 160 "       |        |        |        |        | 650    |        |
|               | 180 "       |        |        |        |        | 690    |        |
|               | 200 "       |        |        |        |        | 730    |        |
|               | 220 "       |        |        |        |        | 760    |        |
|               | 240 "       |        |        |        |        | 780    |        |
|               | 260 "       |        |        |        |        | 800    | 11,1   |
|               | 280 "       |        |        |        |        | 810    |        |
|               | 300 "       |        |        |        |        | 820    |        |
| 320 "         |             |        |        |        | 835    |        |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 13,6   |
| Verlust       |             |        |        |        |        |        | 4,9    |

|                   |     |     |     |  |        |  |  |
|-------------------|-----|-----|-----|--|--------|--|--|
| Stockpunkt °C     |     |     |     |  |        |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |        |  |  |
| Benzin (bis 200°) |     |     |     |  | Qualim |  |  |
| Öl (200-320°)     |     |     |     |  | 42     |  |  |
|                   |     |     |     |  | 35     |  |  |

Bemerkungen:

000074

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 12 Dat. 1.12.19 Zeit 11:00 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>%o | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|-----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 10.4         | 2.4             | 165.6                  | 25.0                                | 27.6                  |
| Kondens.-Öl    | 3.9          | 0.9             | 34.2                   | 5.4                                 | 8.8                   |
| Paraffingatsch | 3.7          | 0.9             | 12.5                   | 2.0                                 | 3.2                   |
| Ges.-Prod.     | 18.0         | 4.2             | 212.3                  | 32.4                                | 49.6                  |

| Kondens.-Prod.        | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|-----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C      | 0.74        | 0.82    | 0.82                |                |                      |
| Olefine „SPL“ Vol. %o |             |         |                     |                |                      |
| Jodzahl (Wijss)       |             |         |                     |                |                      |
| N Z / V Z             |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. %o | Vol. %o | Vol. %o | Vol. %o | Vol. %o | Gew. %o |
|---------------|---------|---------|---------|---------|---------|---------|
| - 40° C       |         |         |         |         |         |         |
| 60° „         |         |         |         |         |         |         |
| 80° „         |         |         |         |         |         |         |
| 100° „        |         |         |         |         |         |         |
| 120° „        |         |         |         |         |         |         |
| 140° „        |         |         |         |         |         |         |
| 160° „        |         |         |         |         |         |         |
| 180° „        |         |         |         |         |         |         |
| 200° „        |         |         |         |         |         |         |
| 220° „        |         |         |         |         |         |         |
| 240° „        |         |         |         |         |         |         |
| 260° „        |         |         |         |         |         |         |
| 280° „        |         |         |         |         |         |         |
| 300° „        |         |         |         |         |         |         |
| 320° „        |         |         |         |         |         |         |
| 340° „        |         |         |         |         |         |         |
| 560° „        |         |         |         |         |         |         |
| Siede-Ende °C |         |         |         |         |         |         |
| Rückstand     |         |         |         |         |         |         |
| Verlust       |         |         |         |         |         | 15.6    |

|                   |     |     |     |  |     |  |
|-------------------|-----|-----|-----|--|-----|--|
| Stockpunkt °C     |     |     |     |  |     |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |     |  |
| Benzin (bis 200°) |     |     |     |  | 4.0 |  |
| Öl (200-320°)     |     |     |     |  |     |  |

Bemerkungen:

000075

# Untersuchung der flüssigen Produkte

Ofen Nr. M Füllung 13 Dat. 13/14 5-93 Zeit            Betr. Tage           

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 92        | 56,4       | 822                    | 60,1                                | 412                   |
| Kondens.-Öl    | 57        | 33,0       | 448                    | 32,8                                | 157                   |
| Paraffingatsch | 14        | 8,6        | 97                     | 7,1                                 | 3,5                   |
| Ges.-Prod.     | 163       | 100,0      | 1367                   | 100,0                               | 60,9                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,686       | 0,782   | 0,89           |                | 0,985           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 47     |        |
| 60 „          |        |        |        |        | 40     |        |
| 80 „          |        |        |        |        | 150    |        |
| 100 „         |        |        |        |        | 250    |        |
| 120 „         |        |        |        |        | 360    | 69,1   |
| 140 „         |        |        |        |        | 440    |        |
| 160 „         |        |        |        |        | 580    |        |
| 180 „         |        |        |        |        | 650    |        |
| 200 „         |        |        |        |        | 700    |        |
| 220 „         |        |        |        |        | 730    | 11,1   |
| 240 „         |        |        |        |        | 760    |        |
| 260 „         |        |        |        |        | 790    |        |
| 280 „         |        |        |        |        | 830    |        |
| 300 „         |        |        |        |        | 850    |        |
| 320 „         |        |        |        |        | 865    |        |
| 340 „         |        |        |        |        |        |        |
| 360 „         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 12,2   |

|                   |     |     |     |  |  |    |
|-------------------|-----|-----|-----|--|--|----|
| Stockpunkt... °C  |     |     |     |  |  | 16 |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |    |
| Benzin (bis 200°) |     |     |     |  |  |    |
| Öl (200-320°)     |     |     |     |  |  |    |

**Bemerkungen:** *Definitiv für ...* **000076**  
*... 62 49*

# Untersuchung der flüssigen Produkte

Ofen Nr. M Füllung 13 Dat. 22/23.5.49 Zeit ..... Betr. Tage .....

| P r o d u k t  | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 12,25        | 62,5           | 921                    | 661                                 | 44,9                  |
| Kondens.-Öl    | 5,35         | 24,3           | 350                    | 252                                 | 19,4                  |
| Paraffingatsch | 2,0          | 10,2           | 120                    | 84                                  | 14                    |
| Ges.-Prod.     | 19,6         | 100,0          | 1391                   | 1000                                | 72,0                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,680       | 0,481   | 0,85                |                | 0,982                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 44     |        |
| 60 „          |        |        |        |        | 80     |        |
| 80 „          |        |        |        |        | 200    |        |
| 100 „         |        |        |        |        | 310    |        |
| 120 „         |        |        |        |        | 410    | 69,5   |
| 140 „         |        |        |        |        | 530    |        |
| 160 „         |        |        |        |        | 620    |        |
| 180 „         |        |        |        |        | 690    |        |
| 200 „         |        |        |        |        | 720    |        |
| 220 „         |        |        |        |        | 750    | 140    |
| 240 „         |        |        |        |        | 780    |        |
| 260 „         |        |        |        |        | 810    |        |
| 280 „         |        |        |        |        | 840    |        |
| 300 „         |        |        |        |        | 855    |        |
| 320 „         |        |        |        |        |        |        |
| 340 „         |        |        |        |        |        |        |
| 360 „         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 120    |
| Verlust       |        |        |        |        |        | 45     |

|                   |     |     |     |  |    |  |
|-------------------|-----|-----|-----|--|----|--|
| Stockpunkt °C     |     |     |     |  |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |    |  |
| Benzin (bis 200°) |     |     |     |  | 49 |  |
| Öl (200-320°)     |     |     |     |  | 47 |  |

**Bemerkungen:**

000077

Nr.

# Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 13 Dat. 21/22. 5 43 Zeit 12:20 Betr. Tage 1

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A. K.-Benzin   | 22.85        | 49.03          | 10.81                  | 9.14                                 | 64.2                  |
| Kondens.-Öl    | 2.3          | 4.94           | 12.1                   | 8.6                                  | 6.9                   |
| Paraffingatsch | 23.45        | 100.0          | 14.62                  | 100.0                                | 14.14                 |

|   | AK-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |   |
|---|-----------|---------|---------------------|----------------|--------|----------------------|---|
|   | Vol. %    | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |   |
| 1 | 2         | 3       | 4                   | 5              | 6      | 7                    | 8 |

Dichte bei 20 °C 0.7104 0.7198

Olefine (H<sub>2</sub>SO<sub>4</sub>-P<sub>2</sub>O<sub>5</sub>) Vol. %

Jodzahl (Wijs)

N. Z. / V. Z.

| Siede-Analyse | Siedebeginn °C |  |  |  |
|---------------|----------------|--|--|--|
|               | -40            |  |  |  |
| 60            |                |  |  |  |
| 80            |                |  |  |  |
| 100           |                |  |  |  |
| 120           |                |  |  |  |
| 140           |                |  |  |  |
| 160           |                |  |  |  |
| 180           |                |  |  |  |
| 200           |                |  |  |  |
| 220           |                |  |  |  |
| 240           |                |  |  |  |
| 260           |                |  |  |  |
| 280           |                |  |  |  |
| 300           |                |  |  |  |
| 320           |                |  |  |  |
| 340           |                |  |  |  |
| 360           |                |  |  |  |
| Siede-Ende °C |                |  |  |  |
| Rückstand     |                |  |  |  |
| Verlust       |                |  |  |  |
| Stockpunkt °C |                |  |  |  |

|  |                   |    |
|--|-------------------|----|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 46 |
|  | Öl (200-320°)     | 49 |

Bemerkungen:

000078

Nr.

# Drucksynthese D.-V.-A.

Ofen Nr. M Füllung 13 Dat. 10/11.5.43 Zeit            Betr. Tage           

| Produkt       | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|---------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin   | 69           | 43,2           | 637                    | 468                                  | 378                   |
| Kondens.-Öl   | 655          | 41,1           | 527                    | 386                                  | 308                   |
| Paraffingasch | 25           | 15,7           | 198                    | 146                                  | 116                   |
|               | 1595         | 100,0          | 1359                   | 1080                                 | 834                   |

|  | AK-Benzin<br>Vol. % | Ölkond.<br>Vol. % | Paraffin-<br>gasch<br>Vol. % | Gesamt-Produkt |   | Reaktions-<br>wasser |  |
|--|---------------------|-------------------|------------------------------|----------------|---|----------------------|--|
|  | 1                   | 2                 | 3                            | 4              | 5 | 6                    |  |

|   |       |       |       |  |  |       |  |
|---|-------|-------|-------|--|--|-------|--|
| Dichte bei 20 °C  | 0,680 | 0,985 | 0,494 |  |  | 0,983 |  |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |       |       |       |  |  |       |  |
| Jodzahl (Wijs)  |       |       |       |  |  |       |  |
| N. Z. / V. Z.   |       |       |       |  |  |       |  |

| Siede-Analyse | Siedebeginn °C |  |  |     |    |     |  |
|---------------|----------------|--|--|-----|----|-----|--|
|               | — 40           |  |  |     | 44 |     |  |
| 60            |                |  |  | 80  |    |     |  |
| 80            |                |  |  | 180 |    |     |  |
| 100           |                |  |  | 220 |    |     |  |
| 120           |                |  |  | 550 |    | 596 |  |
| 140           |                |  |  | 430 |    |     |  |
| 160           |                |  |  | 500 |    |     |  |
| 180           |                |  |  | 560 |    |     |  |
| 200           |                |  |  | 610 |    |     |  |
| 220           |                |  |  | 650 |    |     |  |
| 240           |                |  |  | 690 |    |     |  |
| 260           |                |  |  | 730 |    | 233 |  |
| 280           |                |  |  | 760 |    |     |  |
| 300           |                |  |  | 790 |    |     |  |
| 320           |                |  |  | 830 |    |     |  |
| 340           |                |  |  |     |    |     |  |
| 360           |                |  |  |     |    |     |  |
| Siede-Ende °C |                |  |  |     |    |     |  |
| Rückstand     |                |  |  |     |    | 145 |  |
| Verlust       |                |  |  |     |    | 86  |  |
| Stockpunkt °C |                |  |  |     |    |     |  |

|  |                   |    |  |  |  |
|--|-------------------|----|--|--|--|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 66 |  |  |  |
|  | Öl (200–320°)     | 55 |  |  |  |

Bemerkungen: Handanlöser alk 49  
49 62 000079

Nr.

## Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 13 Dat. 19.10.53 Zeit

Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 85           | 48,7           | 71,4                   | 51,4                                 | 35,2                  |
| Kondens.-Öl    | 6,85         | 3,93           | 49,4                   | 36,5                                 | 28,9                  |
| Paraffingatsch | 2,1          | 1,20           | 15,1                   | 11,1                                 | 8,8                   |
|                | 19,45        | 100,0          | 136,2                  | 100,0                                | 113,4                 |

| 1  | AK-Benzin         | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser | 8 |
|--|-------------------|---------|---------------------|----------------|--------|----------------------|---|
|  | Vol. %            | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |   |
| Dichte bei 20 °C   | 0,683             | 0,752   | 0,793               | 0,714          |        | 0,786                |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. %    |                   |         |                     |                |        |                      |   |
| Jodzahl (Wijss)  |                   |         |                     |                |        |                      |   |
| N. Z. / V. Z.  |                   |         |                     |                |        |                      |   |
| Siedebeginn °C   | 32                | 83      | 160                 | 32             | 45     |                      |   |
| 40   | 60                |         |                     | 31             |        |                      |   |
| 60   | 32                |         |                     | 183            | 160    |                      |   |
| 80   | 50                |         |                     | 252            | 200    |                      |   |
| 100  | 690               | 168     | 50                  | 368            | 210    |                      |   |
| 120  | 780               | 100     |                     | 444            | 360    | 725                  |   |
| 140  | 290               | 150     |                     | 510            | 440    |                      |   |
| 160  | 920               | 210     |                     | 558            | 520    |                      |   |
| 180  | 940               | 320     |                     | 611            | 510    |                      |   |
| 200  | 950               | 440     | 890                 | 648            | 620    |                      |   |
| 220  |                   | 590     | 15                  | 696            | 660    |                      |   |
| 240  |                   | 630     | 30                  | 730            | 690    |                      |   |
| 260  |                   | 720     | 50                  | 765            | 720    | 122                  |   |
| 280  |                   | 810     | 70                  | 800            | 750    |                      |   |
| 300  |                   | 860     | 70                  | 826            | 780    |                      |   |
| 320  |                   | 910     | 260                 | 856            | 820    |                      |   |
| 340  |                   |         |                     |                |        |                      |   |
| 360  |                   |         |                     |                |        |                      |   |
| Siede-Ende °C  | 190               |         |                     |                |        |                      |   |
| Rückstand  | 19                | 110     | 453                 | 143            | 130    |                      |   |
| Verlust  | 13                | 180     | 0,1                 | 0,2            | 23     |                      |   |
| Stockpunkt °C  |                   |         |                     |                |        |                      |   |
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) |         |                     | 62             |        |                      |   |
|  | Öl (200-320°)     |         |                     | 37             |        |                      |   |

Bemerkungen:

000080



Nr. 19

# Drucksynthese D.-V.-A.

Ofen Nr. M Füllung 19 Dat. 18.11.1954 Zeit 12 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A. K.-Benzin   | 9,8          | 46,4           | 68,4                   | 50,3                                 | 54,2                  |
| Kondens.-Öl    | 63           | 34,4           | 48,1                   | 35,3                                 | 27,4                  |
| Paraffingatsch | 26           | 15,6           | 19,4                   | 14,4                                 | 11,4                  |
|                | 164          | 100,0          | 136,5                  | 100,0                                | 43,3                  |

|  | AK-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |  |
|--|-----------|---------|---------------------|----------------|--------|----------------------|--|
|  | Vol. %    | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |  |

| 1   | 2              | 3     | 4     | 5   | 6 | 7     | 8 |
|---|----------------|-------|-------|-----|---|-------|---|
| Dichte bei 20 °C  | 0,680          | 0,784 | 0,793 |     |   | 0,984 |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |                |       |       |     |   |       |   |
| Jodzahl (Wijss)   |                |       |       |     |   |       |   |
| N. Z. / V. Z.   |                |       |       |     |   |       |   |
| Siede-Analyse   | Siedebeginn °C |       |       | 46  |   |       |   |
|   | — 40           |       |       |     |   |       |   |
|   | 60             |       |       | 130 |   |       |   |
|   | 80             |       |       | 250 |   |       |   |
|   | 100            |       |       | 350 |   |       |   |
|   | 120            |       |       | 440 |   | 660   |   |
|   | 140            |       |       | 510 |   |       |   |
|   | 160            |       |       | 580 |   |       |   |
|   | 180            |       |       | 630 |   |       |   |
|   | 200            |       |       | 680 |   |       |   |
|   | 220            |       |       | 720 |   |       |   |
|   | 240            |       |       | 760 |   |       |   |
|   | 260            |       |       | 790 |   | 20,5  |   |
|   | 280            |       |       | 820 |   |       |   |
|   | 300            |       |       | 850 |   |       |   |
|   | 320            |       |       | 875 |   |       |   |
| 340   |                |       |       |     |   |       |   |
| 360   |                |       |       |     |   |       |   |
| Siede-Ende °C   |                |       |       |     |   |       |   |
| Rückstand   |                |       |       |     |   | 11,7  |   |
| Verlust   |                |       |       |     |   | 1,8   |   |
| Stockpunkt °C   |                |       |       |     |   |       |   |

|  |                   |    |
|--|-------------------|----|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 61 |
|  | Öl (200–320°)     | 54 |

Bemerkungen:

000081

Nr. ....

# Drucksynthese D.-V.-A.

Ofen Nr. M Füllung 1/3 Dat. 17.10.55 Zeit 4.5 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100-g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A. K.-Benzin   | 44           | 455            | 676                    | 494                                  | 333                   |
| Kondens.-Öl    | 41           | 421            | 537                    | 393                                  | 308                   |
| Paraffingatsch | 21           | 124            | 155                    | 113                                  | 90                    |
|                | 169          | 1000           | 1368                   | 1000                                 | 431                   |

|   | AK-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |   |
|---|-----------|---------|---------------------|----------------|--------|----------------------|---|
|   | Vol. %    | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |   |
| 1 | 2         | 3       | 4                   | 5              | 6      | 7                    | 8 |

Dichte bei 20 °C 0.674 0.785 0.498 0.981

Olefine (H<sub>2</sub>SO<sub>4</sub>-P<sub>2</sub>O<sub>5</sub>) Vol. %

Jodzahl (Wijs)

N. Z. / V. Z.

| Siede-Analyse | Siedebeginn °C |  |  |     |     |     |  |
|---------------|----------------|--|--|-----|-----|-----|--|
|               | - 40           |  |  |     | 43  |     |  |
| 60            |                |  |  | 120 |     |     |  |
| 80            |                |  |  | 230 |     |     |  |
| 100           |                |  |  | 310 |     |     |  |
| 120           |                |  |  | 390 | 635 |     |  |
| 140           |                |  |  | 440 |     |     |  |
| 160           |                |  |  | 550 |     |     |  |
| 180           |                |  |  | 610 |     |     |  |
| 200           |                |  |  | 650 |     |     |  |
| 220           |                |  |  | 690 |     |     |  |
| 240           |                |  |  | 730 | 221 |     |  |
| 260           |                |  |  | 760 |     |     |  |
| 280           |                |  |  | 790 |     |     |  |
| 300           |                |  |  | 820 |     |     |  |
| 320           |                |  |  | 855 |     |     |  |
| 340           |                |  |  |     |     |     |  |
| 360           |                |  |  |     |     |     |  |
| Siede-Ende °C |                |  |  |     |     |     |  |
| Rückstand     |                |  |  |     |     | 118 |  |
| Verlust       |                |  |  |     |     | 26  |  |
| Stockpunkt °C |                |  |  |     |     |     |  |

| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) |    | Öl (200-320°) |
|--|-------------------|----|---------------|
|  |                   | 61 | 59            |

Bemerkungen:

000082

Nr.

# Drucksynthese D.-V.-A.

Ofen Nr. 12 Füllung 13. Dat. 16.11.54 Zeit      Betr. Tage     

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A. K.-Benzin   | 61        | 57.0       | 195                    | 57.7                                 | 39.2                  |
| Kondens.-Öl    | 22        | 21.5       | 359                    | 26.7                                 | 20.6                  |
| Paraffingatsch | 20        | 19.4       | 225                    | 16.2                                 | 12.9                  |
|                | 113       | 106.0      | 1279                   | 100.0                                | 72.7                  |

|   | AK-Benzin      | Ölkond. | Paraffin-gatsch | Gesamt-Produkt |        | Reaktions-wasser |   |
|---|----------------|---------|-----------------|----------------|--------|------------------|---|
|   | Vol. %         | Vol. %  | Vol. %          | Vol. %         | Vol. % |                  |   |
| 1   | 2              | 3       | 4               | 5              | 6      | 7                | 8 |
| Dichte bei 20°C   | 0.680          | 0.795   | 0.796           |                |        | 0.785            |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |                |         |                 |                |        |                  |   |
| Jodzahl - (Wijss)   |                |         |                 |                |        |                  |   |
| N.Z. / V.Z.   |                |         |                 |                |        |                  |   |
| Siede-Analyse   | Siedebeginn °C |         |                 | 43             |        |                  |   |
|   | — 40           |         |                 |                |        |                  |   |
|   | 60             |         |                 | 10             |        |                  |   |
|   | 80             |         |                 | 190            |        |                  |   |
|   | 100            |         |                 | 290            |        |                  |   |
|   | 120            |         |                 | 390            |        | 60.6             |   |
|   | 140            |         |                 | 460            |        |                  |   |
|   | 160            |         |                 | 520            |        |                  |   |
|   | 180            |         |                 | 580            |        |                  |   |
|   | 200            |         |                 | 630            |        |                  |   |
|   | 220            |         |                 | 690            |        |                  |   |
|   | 240            |         |                 | 710            |        |                  |   |
|   | 260            |         |                 | 740            |        | 21.3             |   |
|   | 280            |         |                 | 740            |        |                  |   |
|   | 300            |         |                 | 780            |        |                  |   |
| 320   |                |         | 730             |                |        |                  |   |
| 340   |                |         |                 |                |        |                  |   |
| 360   |                |         |                 |                |        |                  |   |
| Siede-Ende °C   |                |         |                 |                |        |                  |   |
| Rückstand   |                |         |                 |                |        | 14.8             |   |
| Verlust   |                |         |                 |                |        | 3.5              |   |
| Stockpunkt °C   |                |         |                 |                |        |                  |   |

|  |                   |    |
|--|-------------------|----|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 61 |
|  | Öl (200-320°)     | 57 |

Bemerkungen: 000083

Nr.

# Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 1/2 Dat. 15/11.5.43 Zeit Betr. Tage

| Produkt         | Anfall<br>kg | Gewichts-<br>% <sub>o</sub> | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|-----------------|--------------|-----------------------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin     | 84           | 49.1                        | 683                    | 50.3                                 | 398                   |
| Kondens.-Öl     | 44           | 49.6                        | 532                    | 39.2                                 | 307                   |
| Paraffingatsch. | 20           | 11.3                        | 192                    | 16.5                                 | 84                    |
|                 | 148          | 100.0                       | 1357                   | 100.0                                | 459                   |

|  | AK-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |
|--|-----------|---------|---------------------|----------------|--------|----------------------|
|  | Vol. %    | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |

Dichte bei 20 °C 0.692 0.784 0.795 5 6 7 8

Olefine (H<sub>2</sub>SO<sub>4</sub>-P<sub>2</sub>O<sub>5</sub>) Vol. % 0.983

Jodzahl (Wijs) :

N. Z. / V. Z.

| Siede-Analyse | Siedebeginn °C |  |     |      |     |  |
|---------------|----------------|--|-----|------|-----|--|
|               | 40             |  |     | 35   |     |  |
|               | 60             |  |     | 110  |     |  |
|               | 80             |  |     | 200  |     |  |
|               | 100            |  |     | 250  |     |  |
|               | 120            |  |     | 340  | 646 |  |
|               | 140            |  |     | 350  |     |  |
|               | 160            |  |     | 530  |     |  |
|               | 180            |  |     | 610  |     |  |
|               | 200            |  |     | 660  |     |  |
|               | 220            |  |     | 710  |     |  |
|               | 240            |  |     | 750  |     |  |
|               | 260            |  |     | 790  | 233 |  |
|               | 280            |  |     | 820  |     |  |
|               | 300            |  |     | 850  |     |  |
| 320           |                |  | 110 |      |     |  |
| 340           |                |  |     |      |     |  |
| 360           |                |  |     |      |     |  |
| Siede-Ende °C |                |  |     |      |     |  |
| Rückstand     |                |  |     | 10.6 |     |  |
| Verlust       |                |  |     | 15   |     |  |
| Stockpunkt °C |                |  |     |      |     |  |

|  |                   |    |
|--|-------------------|----|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 73 |
|  | Öl (200-320°)     | 58 |

Bemerkungen:

000084

Nr.

# Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 12 Dat. 14.7.52 Zeit 1 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% <sub>0</sub> | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|-----------------------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 3,8          | 16,3                        | 38,1                   | 31,2                                 | 11,9                  |
| Kondens.-Öl    | 3,7          | 5,5                         | 70,4                   | 17,1                                 | 23,9                  |
| Paraffingatsch | 1,65         | 3,69                        | 1,4                    | 1,2                                  | 19,4                  |
|                | 9,15         | 100,0                       | 109,9                  | 50,9                                 | 55,2                  |

|  | AK-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt |        | Reaktions-<br>wasser |
|--|-----------|---------|---------------------|----------------|--------|----------------------|
|  | Vol. %    | Vol. %  | Vol. %              | Vol. %         | Vol. % |                      |

|   |   |   |   |   |   |       |   |
|---|---|---|---|---|---|-------|---|
| 1   | 2 | 3 | 4 | 5 | 6 | 7     | 8 |
| Dichte bei 20°C   |   |   |   |   |   | 0,693 |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |   |   |   |   |   |       |   |
| Jodzahl (Wijss)   |   |   |   |   |   |       |   |
| N. Z. / V. Z.   |   |   |   |   |   |       |   |

Siede-Analyse

| Siedebeginn °C |  |  |  |  |  |  |  |
|----------------|--|--|--|--|--|--|--|
| 40             |  |  |  |  |  |  |  |
| 60             |  |  |  |  |  |  |  |
| 80             |  |  |  |  |  |  |  |
| 100            |  |  |  |  |  |  |  |
| 120            |  |  |  |  |  |  |  |
| 140            |  |  |  |  |  |  |  |
| 160            |  |  |  |  |  |  |  |
| 180            |  |  |  |  |  |  |  |
| 200            |  |  |  |  |  |  |  |
| 220            |  |  |  |  |  |  |  |
| 240            |  |  |  |  |  |  |  |
| 260            |  |  |  |  |  |  |  |
| 280            |  |  |  |  |  |  |  |
| 300            |  |  |  |  |  |  |  |
| 320            |  |  |  |  |  |  |  |
| 340            |  |  |  |  |  |  |  |
| 360            |  |  |  |  |  |  |  |
| Siede-Ende °C  |  |  |  |  |  |  |  |
| Rückstand      |  |  |  |  |  |  |  |
| Verlust        |  |  |  |  |  |  |  |
| Stockpunkt °C  |  |  |  |  |  |  |  |

|  |                   |  |  |
|--|-------------------|--|--|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) |  |  |
|  | Öl (200-320°)     |  |  |

Bemerkungen:

000085

Nr.

# Drucksynthese D.-V.-A.

Ofen Nr. 11 Füllung 13 Dat. 11/11/43 Zeit Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4.5       | 4.2        | 6.1                    | 4.9                                  | 31.3                  |
| Kondens.-Öl    | 4.2       | 4.5        | 8.7                    | 4.2                                  | 33.4                  |
| Paraffingatsch | 2.38      | 2.2        | 16.3                   | 12.0                                 | 9.5                   |
|                | 10.68     | 10.9       | 15.4                   | 11.1                                 | 74.3                  |

| 1 | AK-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt |        | Reaktionswasser | 8 |
|---|-----------|---------|----------------|----------------|--------|-----------------|---|
|   | Vol. %    | Vol. %  | Vol. %         | Vol. %         | Vol. % |                 |   |

Dichte bei 20 °C 0.683 0.795 0.786

Olefine (H<sub>2</sub>SO<sub>4</sub>-P<sub>2</sub>O<sub>5</sub>) Vol. % 0.98

Jodzahl (Wijss)

N. Z. / V. Z.

Siede-Analyse

| Siedebeginn °C | AK-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------|-----------|---------|----------------|----------------|-----------------|
| — 40           |           |         |                | 3.9            |                 |
| 60             |           |         |                |                |                 |
| 80             |           |         |                |                |                 |
| 100            |           |         |                |                |                 |
| 120            |           |         |                |                |                 |
| 140            |           |         |                | 3.8            |                 |
| 160            |           |         |                |                |                 |
| 180            |           |         |                |                |                 |
| 200            |           |         |                |                |                 |
| 220            |           |         |                |                |                 |
| 240            |           |         |                |                |                 |
| 260            |           |         |                |                |                 |
| 280            |           |         |                |                |                 |
| 300            |           |         |                |                |                 |
| 320            |           |         |                |                |                 |
| 340            |           |         |                |                |                 |
| 360            |           |         |                |                |                 |
| Siede-Ende °C  |           |         |                |                |                 |
| Rückstand      |           |         |                |                |                 |
| Verlust        |           |         |                |                | 4.2             |
| Stockpunkt °C  |           |         |                |                |                 |

|  |                   |     |
|--|-------------------|-----|
| Olefine Vol. %<br>(H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) | Benzin (bis 200°) | 4.4 |
|  | Öl (200—320°)     | 4.2 |

Bemerkungen:

000086







|   |   |  |  |                       |                                |                      |  |      |                            |              |  |
|---|---|--|--|-----------------------|--------------------------------|----------------------|--|------|----------------------------|--------------|--|
| <b>Druckversuchsanlage</b>                                  |   | <b>Produktionsbericht</b> vom 27.12.11 194.7 |  |                       |                                |                      |  |      |                            |              |  |
| Ofen-Nr. .... 11  | Betriebsstunden .... 24 / 5885            | Füllfug: .... 13                             | Gasdruck .... 20.0 atü                 |                       |                                |                      |  |      |                            |              |  |
| Co-Fe-Inhalt ..... kg                                       | Temperatur 20.0 - 20.5 atü °C             |  |  |                       |                                |                      |  |      |                            |              |  |
| Sy-W-Gas .... 299 Nm <sup>3</sup>                           | Restgas .... 185 Nm <sup>3</sup>          | " " " " " "                                  | Nm <sup>3</sup> /h                     |                       |                                |                      |  |      |                            |              |  |
| " " " " " "   | Kreislaufgas .... 720 Nm <sup>3</sup>     | " " " " " "                                  | Nm <sup>3</sup>                        |                       |                                |                      |  |      |                            |              |  |
| " " " " " "   | Kreislauf .... 1:260                      |  |  |                       |                                |                      |  |      |                            |              |  |
| Belastung ..... A.100 Nm <sup>3</sup> /kg Co, h             |   | Nm <sup>3</sup> /Norm.-Vol., h               |  |                       |                                |                      |  |      |                            |              |  |
| <b>Analysen:</b>  | CO <sub>2</sub>                           | CmHn   | O <sub>2</sub>                         | CO                    | H <sub>2</sub>                 | CH <sub>4</sub>      | N <sub>2</sub>                           | C-Z  | N <sub>2</sub> -F          | Litergewicht |  |
| Sygas   | 5.8                                       | —  | 0.1                                    | 39.4                  | 49.5                           | 0.3                  | 4.9                                      | —    | 47.7                       |              |  |
| Restgas   | 18.3                                      | 0.3  | 0.1                                    | 30.3                  | 40.7                           | 2.7                  | 7.6                                      | 1.00 | 7.53                       |              |  |
|   |   |  |  | 31.9                  | 43.4                           |                      |  |      |                            |              |  |
|   |   |  |  | 11                    | 13.6                           |                      |  |      |                            |              |  |
| Gesamt-Inerte .... 11.1 %                                   | Kondensation nach Menge .... 38.6 %       |  | H <sub>2</sub> CO im Sygas .... 1.96 % |                       | " " N <sub>2</sub> .... 36.5 % |                      | H <sub>2</sub> CO im Restgas .... 1.34 % |      | " " CO <sub>2</sub> .... % |              |  |
| Verbrauch von H <sub>2</sub> : CO .... 1.12                 | Durchschnittliche Kontraktion .... 37.3 % |  |  |                       |                                |                      |  |      |                            |              |  |
| umgesetzt   | %CO                                       | %H <sub>2</sub>                              | %CO+H <sub>2</sub>                     |                       |                                |                      |  |      |                            |              |  |
| verflüssigt   | 51.4                                      | 47.8   | 47.6                                   |                       |                                |                      |  |      |                            |              |  |
| Verfl.-Grad A   | 33.1                                      |  |  |                       |                                |                      |  |      |                            |              |  |
| " " P   | 64.4                                      |  |  |                       |                                |                      |  |      |                            |              |  |
| CH <sub>4</sub> + CmHn .... 7.0                             |   | CO <sub>2</sub> .... 28.5                    |  | bezogen auf CO-Umsatz |                                |                      |  |      |                            |              |  |
| <b>Produkte</b>   |   |  |  |                       |                                | <b>Gesamtprodukt</b> |  |      |                            |              |  |
| Paraffingatsch .... 3.10 kg                                 |   |  |  |                       |                                | SB                   | °C                                       |      |                            |              |  |
| O-Kondensat .... 6.60 "                                     |   |  |  |                       |                                | — 100°               | %  |      |                            |              |  |
| A.-K. Benzin .... 2.80 "                                    |   |  |  |                       |                                | — 200°               | %  |      |                            |              |  |
| Flüssige Prod. .... 12.50 "                                 |   |  |  |                       |                                | — 320°               | %  |      |                            |              |  |
| Sywasser .... 18.50 kg = 1.48 × flüss. Produkte             |   |  |  |                       |                                | Olefine              | Vol. %                                   |      |                            |              |  |
|   |   |  |  |                       |                                | — 200°               | 200 - 320°                               |      |                            |              |  |
| <b>Ausbeute</b>   |   |  |  |                       |                                |                      |  |      |                            |              |  |
| Flüssige Prod. .... 41.9 g/Nm <sup>3</sup> Sygas            | 47.2 g/Nm <sup>3</sup> Nutzgas            |  | c Nm <sup>3</sup> Idealgas             |                       |                                |                      |  |      |                            |              |  |
| Gasol   |   |  |  |                       |                                |                      |  |      |                            |              |  |
| Gesamt-Produkt  |   |  |  |                       |                                |                      |  |      |                            |              |  |
| Sywasser  | 17.8                                      |  | 64.6                                   |                       |                                |                      |  |      |                            |              |  |
| <b>Bemerkungen:</b> Temperatur minimal auf 60.5°C gehalten. |   |  |  |                       |                                |                      |  |      |                            |              |  |

000089





















# Druckversuchsanlage

Produktionsbericht vom 10.11.1949

Ofen-Nr. 11  
 Füllung: 18  
 Co-Fe-Inhalt: kg

Betriebsstunden 24 / 562.1  
 Gasdruck 20 atü  
 Temperatur 19.0 atü 211.4 °C

Sy-W-Gas 30.7 Nm<sup>3</sup>  
 " " " " " "  
 " " " " " "  
 " 17.8 Nm<sup>3</sup>/h

Restgas 18.6 Nm<sup>3</sup>  
 " " " " " "  
 Kreislaufgas 6.14 Nm<sup>3</sup>  
 Kreislauf 1520.1

Belastung: Nm<sup>3</sup>/kg Co, h Nm<sup>3</sup>/Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO                 | H <sub>2</sub>       | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|------|----------------|--------------------|----------------------|-----------------|----------------|------|-------------------|--------------|
| Sygas     | 6.4             | -    | 0.1            | 38.9               | 49.3                 | 0.3             | 5.0            | -    | 4.91              |              |
| Restgas   | 15.8            | 0.3  | 0.1            | 32.9<br>35.6<br>17 | 41.8<br>44.5<br>1.94 | 2.7             | 1.7            | 1.00 | 4.66              |              |

Gesamt-Inerte 11.8 %  
 H<sub>2</sub>CO im Sygas 18.7  
 H<sub>2</sub>CO im Restgas 130  
 Verbrauch von H<sub>2</sub>: CO 1.25

Kontraktion nach Menge 39.9 %  
 " " N<sub>2</sub> 35.5 %  
 " " CO<sub>2</sub> " %  
 Durchschnittliche Kontraktion 37.5 %

umgesetzt %CO 46.7 %H<sub>2</sub> 45.3 %CO+H<sub>2</sub> 46.6  
 verflüssigt 34.1  
 Verf.-Grad A 73.0  
 " " P

CH<sub>4</sub> + CmHn 15.8 CO<sub>2</sub> 41.0 bezogen auf CO-Umsatz

## Produkte

Paraffingatsch 330 kg 26.2 %  
 Öl-Kondensat 5.90 " 46.8 %  
 A.-K. Benzin 3.40 " 27.0 %  
 Flüssige Prod. 12.60 " 100 %  
 Sywasser 18.70 kg = 14.9 % flüss. Produkte

## Gesamtprodukt

SB °C  
 - 100° 54.2 %  
 - 200° 22.8 % > 23.0  
 - 320°  
 Olefine Vol. %  
 - 200° 75 : 200 - 320° 66

## Ausbeute

Flüssige Prod. 11.2 g/Nm<sup>3</sup> Sygas 46.1 g/Nm<sup>3</sup> Nutzgas  
 Gasol 10.77 " " 11.63 " " Idealgas  
 Gesamt-Produkt 51.47 " " 16.30 " " " "  
 Sywasser 6.14 " " 6.18 " " " "

## Bemerkungen:

Gasol 64% Olefine

000099



























|  |  |   |                               |  |             |                        |            |            |             |             |              |
|--|--|---|-------------------------------|--|-------------|------------------------|------------|------------|-------------|-------------|--------------|
| <b>Druckversuchsanlage</b>                     |  |   |                               | Versuchsbericht vom <u>26.12.12</u> 194 <u>8</u> |             |                        |            |            |             |             |              |
| Ofen-Nr. <u>11</u>                             |  | Füllung: <u>13</u>                              |                               | Betriebsstunden <u>23/53.17</u>                  |             | Gasdruck <u>16</u> alü |            |            |             |             |              |
| 26-Fe-Inhalt                                   |  | kg  |                               | Temperatur <u>170</u> alü                        |             | <u>206</u> °C          |            |            |             |             |              |
| W-Gas <u>218</u>                               |  | Nm³   |                               | Restgas <u>143</u>                               |             | Nm³                    |            |            |             |             |              |
| " " " "  |  | " " " "   |                               | " " " "  |             | Nm³/h                  |            |            |             |             |              |
| " " " "  |  | <u>9.1</u> Nm³/h                                |                               | Kreislaufgas <u>801</u>                          |             | Nm³                    |            |            |             |             |              |
| " " " "  |  | " " " "   |                               | Kreislauf <u>133.85</u>                          |             | " " " "                |            |            |             |             |              |
| Belastung                                      |  |   |                               | Nm³ / kg, h                                      |             |                        |            |            |             |             |              |
| Analysen:                                      |  | CO₂   | C <sub>m</sub> H <sub>n</sub> | O₂   | CO          | H₂                     | CH₄        | N₂         | C-Z         | N₂-F        | Litergewicht |
| Sygas  |  | <u>6.3</u>                                      | <u>0.1</u>                    | <u>0.1</u>                                       | <u>38.8</u> | <u>49.4</u>            | <u>0.3</u> | <u>5.1</u> | -           | <u>4.98</u> |              |
| Restgas  |  | <u>16.0</u>                                     | <u>0.3</u>                    | <u>0.1</u>                                       | <u>32.3</u> | <u>41.2</u>            | <u>2.2</u> | <u>8.9</u> | <u>1.10</u> | <u>8.81</u> |              |
|  |  |   |                               |  | <u>33.6</u> | <u>42.2</u>            |            |            |             |             |              |
|  |  |   |                               |  | <u>15</u>   | <u>12.2</u>            |            |            |             |             |              |
| Gesamt-Inerte (Idealgas) <u>11.8</u> %         |  |   |                               | Kontraktion nach Menge <u>31.2</u> %             |             |                        |            |            |             |             |              |
| H₂:CO im Sygas <u>1.27</u>                     |  |   |                               | " " N₂ <u>36.2</u> %                             |             |                        |            |            |             |             |              |
| H₂:CO im Restgas <u>1.27</u>                   |  |   |                               | " " CO₂ <u>    </u> %                            |             |                        |            |            |             |             |              |
| Verbrauch von H₂:CO <u>1.27</u>                |  |   |                               | Durchschnittliche Kontraktion <u>    </u> %      |             |                        |            |            |             |             |              |
|  |  | % CO  |                               | % H₂   |             | % CO+H₂                |            |            |             |             |              |
| umgesetzt                                      |  | <u>47.0</u>                                     |                               | <u>46.9</u>                                      |             | <u>46.95</u>           |            |            |             |             |              |
| verflüssigt                                    |  | <u>34.2</u>                                     |                               |  |             |                        |            |            |             |             |              |
| Verfl.-Grad A                                  |  | <u>1.27</u>                                     |                               |  |             |                        |            |            |             |             |              |
| " " P  |  |   |                               |  |             |                        |            |            |             |             |              |
| CH₄ + C <sub>m</sub> H <sub>n</sub> <u>6.1</u> |  | CO₂ <u>21.3</u>                                 |                               | bezogen auf CO-Umsatz                            |             |                        |            |            |             |             |              |
| <b>Produkte</b>                                |  |   |                               | <b>Gesamtprodukt:</b>                            |             |                        |            |            |             |             |              |
| Paraffingas                                    |  | <u>2.50</u> kg                                  | <u>2.52</u> %                 | SB <u>47</u> °C                                  |             |                        |            |            |             |             |              |
| Ol-Kondensat                                   |  | <u>4.10</u> "                                   | <u>4.14</u> %                 | - 200 °C <u>50.1</u> %                           |             |                        |            |            |             |             |              |
| A.-K. Benzin                                   |  | <u>2.30</u> "                                   | <u>2.32</u> %                 | 200 - 320 °C <u>22.8</u> %                       |             |                        |            |            |             |             |              |
| Flüssige Prod.                                 |  | <u>9.90</u> "                                   | 100 %                         | > 320 °C <u>26.3</u> %                           |             |                        |            |            |             |             |              |
| Sywasser                                       |  | <u>13.60</u> kg = <u>1.37</u> × flüss. Produkte |                               | Olefine Vol. %                                   |             |                        |            |            |             |             |              |
|  |  |   |                               | - 200° <u>7.5</u> ; 200-320° <u>7.2</u>          |             |                        |            |            |             |             |              |
| <b>Ausbeute</b>                                |  |   |                               |  |             |                        |            |            |             |             |              |
| Flüssige Prod.                                 |  | <u>47.6</u> g/Nm³ Sygas                         | <u>54.0</u> g/Nm³ Nutzgas     | <u>(16+12)</u> g/Nm³ Idealgas                    |             |                        |            |            |             |             |              |
| Gasol  |  | " "   | " "                           | " "  |             |                        |            |            |             |             |              |
| Gesamt-Produkt                                 |  | " "   | " "                           | " "  |             |                        |            |            |             |             |              |
| Sywasser                                       |  | " "   | " "                           | " "  |             |                        |            |            |             |             |              |
| Bemerkungen:                                   |  |   |                               |  |             |                        |            |            |             |             |              |

000112



# Druckversuchsanlage

Versuchsbericht vom 25/26.12 1943

Ofen-Nr. 11  
 Füllung: 13  
 Gf.-Inhalt kg

Betriebsstunden 24/5294  
 Gasdruck 24 atü  
 Temperatur 172.1 atü 206 °C

Sy-W-Gas 209 Nm³  
 " " "  
 " " "  
 " 8.7 Nm³/h

Restgas 125 Nm³  
 " " Nm³/h  
 Kreislaufgas 215 Nm³  
 Kreislauf 1.326

Belastung Nm³ / kg,h Nm³ / Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|-----|-------------------|--------------|
| Sygas     | 6.6             | -                             | 0.1            | 38.5 | 50.1           | 1.3             | 4.4            | -   | 4.27              |              |
| Restgas   | 16.5            | 0.3                           | 0.1            | 31.8 | 41.2           | 2.2             | 2.4            | 100 | 2.33              |              |
| Kupf      |                 |                               |                | 33.3 | 43.0           |                 |                |     |                   |              |
|           |                 |                               |                | 1.   | 12.9           |                 |                |     |                   |              |

Gesamt-Inerte (Idealgas) 11.4%  
 H<sub>2</sub>:GO im Sygas 1.30  
 H<sub>2</sub>:CO im Restgas 7.31  
 Verbrauch von H<sub>2</sub>:CO 1.29

Kontraktion nach Menge 40.5 %  
 " " N<sub>2</sub> 4.6 %  
 " " CO<sub>2</sub> %  
 Durchschnittliche Kontraktion 47.15 %

umgesetzt % CO 51.6 % H<sub>2</sub> 51.7 % CO + H<sub>2</sub> 51.45  
 verflüssigt 49.3  
 Verfl.-Grad A 79.8  
 " " P

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 5.0 CO<sub>2</sub> 15.3 bezogen auf CO-Umsatz

**Produkte**

|                |       |                             |      |       |
|----------------|-------|-----------------------------|------|-------|
| Paraffingasch  | 2.30  | kg                          | 25.5 | %     |
| Ol-Kondensat   | 4.21  | "                           | 46.4 | %     |
| A.-K. Benzin   | 2.55  | "                           | 28.2 | %     |
| Flüssige Prod. | 9.05  | "                           |      | 100 % |
| Sywasser       | 14.60 | kg = 1.61 × flüss. Produkte |      |       |

**Gesamtprodukt**

|                       |        |
|-----------------------|--------|
| SB                    | °C     |
| - 200 °C              | %      |
| 200 - 320 °C          | %      |
| > 320 °C              | %      |
| Olefine               | Vol. % |
| - 200 °C ; 200-320 °C |        |

**Ausbeute**

Flüssige Prod. 43.3 g/Nm³ Sygas 49.0 g/Nm³ Nutzgaz 180 + 42 g/Nm³ Idealgas  
 Gasol " " " " " " " "  
 Gesamt-Produkt " " " " " " " "  
 Sywasser " " " " " " " "

Bemerkungen:

000113

# Druckversuchsanlage

Versuchsbericht vom 24.12.12 194 3

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt \_\_\_\_\_ kg

Betriebsstunden 24/5270  
 Gasdruck 16 atü  
 Temperatur 18 atü 209 °C

Sy-W-Gas 211 Nm<sup>3</sup>  
 " " " "  
 " " 8,8 Nm<sup>3</sup>/h

Restgas 124 Nm<sup>3</sup>  
 " " " "  
 Kreislaufgas 808 Nm<sup>3</sup>  
 Kreislauf 1.383

Belastung \_\_\_\_\_ Nm<sup>3</sup> / kg, h

| Analysen: | Nm <sup>3</sup> / kg, h |                               |                |             |                |                 |                | Nm <sup>3</sup> / Norm.-Vol., h |                   |              |
|-----------|-------------------------|-------------------------------|----------------|-------------|----------------|-----------------|----------------|---------------------------------|-------------------|--------------|
|           | CO <sub>2</sub>         | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO          | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z                             | N <sub>2</sub> -F | Litergewicht |
| Sygas     | <u>6,4</u>              | -                             | <u>0,1</u>     | <u>38,8</u> | <u>50,2</u>    | <u>0,3</u>      | <u>4,2</u>     | -                               | <u>4,10</u>       |              |
| Restgas   | <u>12,0</u>             | <u>0,2</u>                    | <u>0,1</u>     | <u>32,2</u> | <u>41,0</u>    | <u>2,4</u>      | <u>7,7</u>     | <u>1,02</u>                     | <u>2,02</u>       |              |
|           |                         |                               |                | <u>33,6</u> | <u>42,7</u>    |                 |                |                                 |                   |              |
|           |                         |                               |                | <u>7</u>    | <u>12,4</u>    |                 |                |                                 |                   |              |

Gesamt-Inerte (Idealgas) 110 %  
 H<sub>2</sub>:CO im Sygas 19,9  
 H<sub>2</sub>:CO im Restgas 1,27  
 Verbrauch von H<sub>2</sub>:CO 1,32

Kontraktion nach Menge 41,2 %  
 " " N<sub>2</sub> 40,2 %  
 " " CO<sub>2</sub> \_\_\_\_\_ %  
 Durchschnittliche Kontraktion 41,0 %

|               |             |                  |                       |
|---------------|-------------|------------------|-----------------------|
|               | % CO        | % H <sub>2</sub> | % CO + H <sub>2</sub> |
| umgesetzt     | <u>50,6</u> | <u>52,0</u>      | <u>51,3</u>           |
| verflüssigt   | <u>39,0</u> |                  |                       |
| Verfl.-Grad A | <u>26,2</u> |                  |                       |
| " " P         |             |                  |                       |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 5,6 CO<sub>2</sub> 11,7 bezogen auf CO-Umsatz

### Produkte

| Produkt        | Menge        | Einheit | Werte                         | %     |
|----------------|--------------|---------|-------------------------------|-------|
| Paraffingatsch | <u>2,60</u>  | kg      | <u>28,3</u>                   |       |
| Ol-Kondensat   | <u>4,20</u>  | "       | <u>45,6</u>                   |       |
| A.-K. Benzin   | <u>2,40</u>  | "       | <u>26,1</u>                   |       |
| Flüssige Prod. | <u>9,20</u>  | "       |                               | 100 % |
| Sywasser       | <u>14,60</u> | kg =    | <u>1,59</u> × flüss. Produkte |       |

### Gesamtprodukt

| SB <sup>1</sup> | Temperatur   | Werte | %      |
|-----------------|--------------|-------|--------|
|                 | <u>44</u> °C |       |        |
| -200 °C         | <u>49,4</u>  |       |        |
| 200 - 320 °C    | <u>23,2</u>  |       |        |
| > 320 °C        | <u>26,6</u>  |       |        |
| Olefine         |              |       | Vol. % |
| -200 °C         | <u>24</u>    |       |        |
| 200-320 °C      | <u>23</u>    |       |        |

### Ausbeute

Flüssige Prod. 43,6 g/Nm<sup>3</sup> Sygas 49,0 g/Nm<sup>3</sup> Nutzgas (20 + 12) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

Bemerkungen:

000114

# Druckversuchsanlage

Versuchsbericht vom

23/24.12

1943

Ofen-Nr. 11

Betriebsstunden

24/5246

Füllung: 13

Gasdruck

2,7 atü

Co-Fe-Inhalt

kg

Temperatur

18 atü 219 °C

Sy-W-Gas

213

Nm³

Restgas

140

Nm³

"

"

Nm³/h

"

"

Kreislaufgas

693

Nm³

"

8,9

Nm³/h

Kreislauf

1.325

Belastung

Nm³ / kg,h

Nm³ / Norm.-Vol., h

Analysen:

CO₂

CmHn

O₂

CO

H₂

CH₄

N₂

C-Z

N₂-F

Litergewicht

Sygas

6,5

-

0,1

38,7

50,7

0,3

4,2

-

4,10

Restgas

14,6

0,2

0,1

34,3

41,8

2,0

2,1

1,00

6,90

Korff

35,6

43,9

1,23

Gesamt-Inerte (Idealgas)

11,9 %

Kontraktion nach Menge

34,2 %

H₂:CO im Sygas

1,31

"

"

N₂

40,5 %

H₂:CO im Restgas

1,22

"

"

CO₂

%

Verbrauch von H₂:CO

1,41

Durchschnittliche Kontraktion

%

umgesetzt

% CO  
47,3

% H₂  
57,0

% CO + H₂  
49,2

verflüssigt

39,3

Verfl.-Grad A

83,1

"

"

P

CH₄ + CmHn

4,9

CO₂

12,0

bezogen auf CO-Umsatz

Produkte

Paraffingasch

2,80

kg

32,5

%

Öl-Kondensat

3,80

"

44,2

%

A.-K. Benzin

2,00

"

23,3

%

Flüssige Prod.

8,60

"

100 %

Sywasser

14,50

kg =

1,69

× flüss. Produkte

Gesamtprodukt

SB

4,2

°C

- 200 °C

48,8

%

200 - 320 °C

21,9

%

> 320 °C

27,9

%

Olefine

Vol. %

- 200 °C

25

;

200-320 °C

6,8

Ausbeute

Flüssige Prod.

40,4

g/Nm³ Sygas

45,4

g/Nm³ Nutzgas

(50 + 15)

g/Nm³ Idealgas

Gasol

"

"

"

"

"

"

Gesamt-Produkt

"

"

"

"

"

"

Sywasser

"

"

"

"

"

"

Bemerkungen:

000115

# Druckversuchsanlage

Versuchsbericht vom 22./33. 10. 1943

Ofen-Nr. 11  
 Füllung: 13.  
 C-Fe-Inhalt - kg

Betriebsstunden 22/5222  
 Gasdruck 20.0 atü  
 Temperatur 17.0 atü 206,2 °C

Sy-W-Gas 302 Nm<sup>3</sup>  
 " " " " " "  
 " 9.2 Nm<sup>3</sup>/h

Restgas 129 Nm<sup>3</sup>  
 " " " " " "  
 Kreislaufgas 692 Nm<sup>3</sup>/h  
 Kreislauf 1.313

Belastung 0.75 Nm<sup>3</sup>/kg.h

| Analyse | Nm <sup>3</sup> /Norm.-Vol., h |                               |                |      |                |                 |                |                  |                   |              |
|---------|--------------------------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------------------|-------------------|--------------|
|         | CO <sub>2</sub>                | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C <sub>2</sub> Z | N <sub>2</sub> -F | Litergewicht |
| Sygas   | 6.2                            | -                             | 0.1            | 38.7 | 57.1           | 0.3             | 4.6            | -                | 4.50              | -            |
| Restgas | 15.8                           | 0.2                           | 0.1            | 38.5 | 40.6           | 2.1             | 7.7            | 1.05             | 7.63              | -            |
| Krllf   |                                |                               |                | 34.8 | 43.0           |                 |                |                  |                   |              |
|         |                                |                               |                | 1.   | 12.3           |                 |                |                  |                   |              |

Gesamt-Inerte (Idealgas) 11.2 %  
 H<sub>2</sub>:CO im Sygas 1.29  
 H<sub>2</sub>:CO im Restgas 1.21  
 Verbrauch von H<sub>2</sub>:CO 1.28

Kontraktion nach Menge 4.3 %  
 " " N<sub>2</sub> 41.1 %  
 " " CO<sub>2</sub> %  
 Durchschnittliche Kontraktion 41.2 %

|               |      |                  |                     |
|---------------|------|------------------|---------------------|
| umgesetzt     | % CO | % H <sub>2</sub> | % CO+H <sub>2</sub> |
| verflüssigt   | 49.2 | 59.4             | 50.9                |
| Verfl.-Grad A | 38.6 |                  |                     |
| " " P         | 78.6 |                  |                     |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 4.9 CO<sub>2</sub> 16.4 bezogen auf CO-Umsatz

### Produkte

|                |                                  |        |
|----------------|----------------------------------|--------|
| Paraffingatsch | 2.40 kg                          | 27.4 % |
| Ol-Kondensat   | 4.25 "                           | 48.6 % |
| A.-K. Benzin   | 2.10 "                           | 24.0 % |
| Flüssige Prod. | 8.75 "                           | 100 %  |
| Sywasser       | 14.00 kg = 160 × flüss. Produkte |        |

### Gesamtprodukt

|              |        |    |
|--------------|--------|----|
| SB           | 45     | °C |
| - 200 °C     | 55.2   | %  |
| 200 - 320 °C | 20.5   | %  |
| > 320 °C     | 23.5   | %  |
| Olefine      | Vol. % |    |
| - 200°       | 2.2    |    |
| 200-320°     | 6.6    |    |

### Ausbeute

Flüssige Prod. 43.9 g/Nm<sup>3</sup> Sygas 48.8 g/Nm<sup>3</sup> Nutzgas (16.0 + 4.2) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

### Bemerkungen:

Ofen wurde 1755 wegen erhöhter Feindruck = flüssig abgestellt.  
 Wiederaufnahmen 15<sup>50</sup> h.  
 Gegenüberstellung auf 9 Nm<sup>3</sup>/h

000116

# Druckversuchsanlage

Versuchsbericht vom 21./22. 12. 1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt — kg

Betriebsstunden 20/5211  
 Gasdruck 30,0 atü  
 Temperatur 17,0 atü 306,2 °C

Sy-W-Gas 190 Nm<sup>3</sup>  
 " " " "  
 " " " "  
 " 0,5 Nm<sup>3</sup>/h

Restgas 132 Nm<sup>3</sup>  
 " " " "  
 Kreislaufgas 607 Nm<sup>3</sup>  
 Kreislauf 1:320

Belastung Nm<sup>3</sup>/kg,h Nm<sup>3</sup>/Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO          | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C <sub>2</sub> | N <sub>2</sub> -F | Lifergewicht |
|-----------|-----------------|-------------------------------|----------------|-------------|----------------|-----------------|----------------|----------------|-------------------|--------------|
| Sygas     | <u>6,1</u>      | —                             | <u>0,1</u>     | <u>38,7</u> | <u>49,2</u>    | <u>0,3</u>      | <u>5,6</u>     | —              | <u>5,60</u>       |              |
| Restgas   | <u>15,3</u>     | <u>0,3</u>                    | <u>0,1</u>     | <u>33,4</u> | <u>41,0</u>    | <u>1,7</u>      | <u>8,2</u>     | <u>1,00</u>    | <u>8,05</u>       |              |
| Kref.     |                 |                               |                | <u>34,7</u> | <u>48,8</u>    |                 |                |                |                   |              |

Gesamt-Inerte (Idealgas) 13,1 %  
 H<sub>2</sub>:CO im Sygas 1,27  
 H<sub>2</sub>:CO im Restgas 1,23  
 Verbrauch von H<sub>2</sub>:CO 1,34

Kontraktion nach Menge 30,0 %  
 " " N<sub>2</sub> 30,5 %  
 " " CO<sub>2</sub> — %  
 Durchschnittliche Kontraktion 30,3 %

umgesetzt 40,1 % CO  
 verflüssigt 26,0  
 Verfl.-Grad A 65,0  
 " " P

% H<sub>2</sub> 42,1  
 % CO + H<sub>2</sub> 41,1

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 5,7 CO<sub>2</sub> 29,2 bezogen auf CO-Umsatz

**Produkte**

|                |   |               |
|----------------|---|---------------|
| Paraffingasch  | <u>1,90</u> kg                                  | <u>25,3</u> % |
| Ol-Kondensat   | <u>7,50</u> "                                   | <u>46,7</u> % |
| A.-K. Benzin   | <u>2,10</u> "                                   | <u>28,0</u> % |
| Flüssige Prod. | <u>7,50</u>                                     | 100 %         |
| Sywasser       | <u>12,04</u> kg = <u>1,60</u> × flüss. Produkte |               |

**Gesamtprodukt**

|                                       |               |
|---------------------------------------|---------------|
| SB                                    | <u>45</u> °C  |
| — 200 °C                              | <u>54,5</u> % |
| 200 — 320 °C                          | <u>21,6</u> % |
| > 320 °C                              | <u>23,5</u> % |
| Olefine                               | Vol. %        |
| — 200° <u>25</u> ; 200-320° <u>68</u> |               |

**Ausbeute**

|                |                                     |                                       |  |
|----------------|-------------------------------------|---------------------------------------|--|
| Flüssige Prod. | <u>39,5</u> g/Nm <sup>3</sup> Sygas | <u>45,1</u> g/Nm <sup>3</sup> Nutzgas | <u>(20+112)</u> g/Nm <sup>3</sup> Idealgas |
| Gasol          | " "                                 | " "                                   | " "  |
| Gesamt-Produkt | " "                                 | " "                                   | " "  |
| Sywasser       | " "                                 | " "                                   | " "  |

**Bemerkungen:**  
 Ölstand von 1315 l - 1640 l wegen  
 Gasausfall.  
 Spindelmenge mit 9 Nm<sup>3</sup>/h

000117



|   |                 |                               |                   |                           |   |                            |                |             |                   |              |  |
|---|-----------------|-------------------------------|-------------------|---------------------------|---|----------------------------|----------------|-------------|-------------------|--------------|--|
| <b>Druckversuchsanlage</b>                                  |                 |                               |                   |                           | Versuchsbericht vom <u>19./20. 12. 1943</u>       |                            |                |             |                   |              |  |
| Ofen-Nr. <u>11</u>  |                 |                               |                   |                           | Betriebsstunden <u>24/5156</u>                    |                            |                |             |                   |              |  |
| Füllung: <u>11</u>  |                 |                               |                   |                           | Gasdruck <u>20.0</u> atü                          |                            |                |             |                   |              |  |
| Co-Fe-Inhalt <u>-</u> kg                                    |                 |                               |                   |                           | Temperatur <u>25.0</u> atü <u>225</u> °C          |                            |                |             |                   |              |  |
| W-Gas <u>307</u> Nm <sup>3</sup>                            |                 |                               |                   |                           | Restgas <u>187</u> Nm <sup>3</sup>                |                            |                |             |                   |              |  |
| " " " "   |                 |                               |                   |                           | " " " " Nm <sup>3</sup> /h                        |                            |                |             |                   |              |  |
| " " " " <u>12.8</u> Nm <sup>3</sup> /h                      |                 |                               |                   |                           | Kreislaufgas <u>758</u> Nm <sup>3</sup>           |                            |                |             |                   |              |  |
| " " " " " "   |                 |                               |                   |                           | Kreislauf <u>1.247</u>                            |                            |                |             |                   |              |  |
| Belastung   |                 |                               |                   |                           | Nm <sup>3</sup> /kg,h                             |                            |                |             |                   |              |  |
| Analysen:   |                 |                               |                   |                           |   |                            |                |             |                   |              |  |
|   | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub>    | CO                        | H <sub>2</sub>                                    | CH <sub>4</sub>            | N <sub>2</sub> | C-Z         | N <sub>2</sub> -F | Litergewicht |  |
| Sygas   | <u>6.4</u>      | <u>-</u>                      | <u>0.1</u>        | <u>38.8</u>               | <u>50.3</u>                                       | <u>0.3</u>                 | <u>4.1</u>     | <u>-</u>    | <u>4.03</u>       |              |  |
| Restgas   | <u>28.8</u>     | <u>0.5</u>                    | <u>0.1</u>        | <u>21.1</u>               | <u>36.6</u>                                       | <u>5.6</u>                 | <u>7.3</u>     | <u>1.10</u> | <u>7.30</u>       |              |  |
|   |                 |                               |                   | <u>25.2</u>               | <u>40.4</u>                                       |                            |                |             |                   |              |  |
|   |                 |                               |                   | <u>1.60</u>               |   |                            |                |             |                   |              |  |
| Gesamt-Inerte (Idealgas) <u>10.9</u> %                      |                 |                               |                   |                           | Kontraktion nach Menge <u>39.1</u> %              |                            |                |             |                   |              |  |
| H <sub>2</sub> :CO im Sygas <u>1.30</u>                     |                 |                               |                   |                           | " " N <sub>2</sub> <u>44.6</u> %                  |                            |                |             |                   |              |  |
| H <sub>2</sub> :CO im Restgas <u>1.74</u>                   |                 |                               |                   |                           | " " CO <sub>2</sub> <u>-</u> %                    |                            |                |             |                   |              |  |
| Verbrauch von H <sub>2</sub> :CO <u>1.11</u>                |                 |                               |                   |                           | Durchschnittliche Kontraktion <u>54.6</u> %       |                            |                |             |                   |              |  |
| umgesetzt <u>70.0</u> % CO                                  |                 |                               |                   |                           | % H <sub>2</sub> <u>59.8</u>                      |                            |                |             |                   |              |  |
| verflüssigt <u>38.2</u>                                     |                 |                               |                   |                           | % CO + H <sub>2</sub> <u>65.0</u>                 |                            |                |             |                   |              |  |
| Verfl.-Grad A <u>54.6</u>                                   |                 |                               |                   |                           |   |                            |                |             |                   |              |  |
| " " P   |                 |                               |                   |                           |   |                            |                |             |                   |              |  |
| CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub> <u>10.3</u> |                 |                               |                   |                           | CO <sub>2</sub> <u>35.1</u> bezogen auf CO-Umsatz |                            |                |             |                   |              |  |
| <b>Produkte</b>   |                 |                               |                   |                           | <b>Gesamtprodukt</b>                              |                            |                |             |                   |              |  |
| Paraffingas   | <u>3.00</u>     | kg                            | <u>14.6</u>       | %                         | SB  | <u>33</u>                  | °C             |             |                   |              |  |
| Ol-Kondensat  | <u>5.30</u>     | "                             | <u>34.6</u>       | %                         | - 200 °C  | <u>65.8</u>                | %              |             |                   |              |  |
| A.-K. Benzin  | <u>7.00</u>     | "                             | <u>45.8</u>       | %                         | 200 - 320 °C                                      | <u>18.8</u>                | %              |             |                   |              |  |
| Flüssige Prod.  | <u>15.30</u>    | "                             |                   | 100 %                     | > 320 °C  | <u>18.8</u>                | %              |             |                   |              |  |
| Sywasser  | <u>18.90</u>    | kg = <u>1.23</u>              | × flüss. Produkte |                           | Olefine   | Vol. %                     |                |             |                   |              |  |
|   |                 |                               |                   |                           | - 200° <u>6.8</u> ; 200-320° <u>6.1</u>           |                            |                |             |                   |              |  |
| <b>Ausbeute</b>   |                 |                               |                   |                           |   |                            |                |             |                   |              |  |
| Flüssige Prod.  | <u>49.9</u>     | g/Nm <sup>3</sup> Sygas       | <u>56.9</u>       | g/Nm <sup>3</sup> Nutzgas | <u>180.1</u>                                      | g/Nm <sup>3</sup> Idealgas |                |             |                   |              |  |
| Gasol   | "               | "                             | "                 | "                         | "   | "                          |                |             |                   |              |  |
| Gesamt-Produkt  | "               | "                             | "                 | "                         | "   | "                          |                |             |                   |              |  |
| Sywasser  | "               | "                             | "                 | "                         | "   | "                          |                |             |                   |              |  |
| <b>Bemerkungen:</b>   |                 |                               |                   |                           |   |                            |                |             |                   |              |  |

000119

# Druckversuchsanlage

Versuchsbericht vom 18.11.12 1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt — kg

Betriebsstunden 24/5/32  
 Gasdruck 20.0 atü  
 Temperatur 25.0 atü 225 °C

Sy-W-Gas 311 Nm<sup>3</sup>  
 " " " "  
 " 10.0 Nm<sup>3</sup>/h

Restgas 220 Nm<sup>3</sup>  
 " " " "  
 Kreislaufgas 8.11 Nm<sup>3</sup>/h  
 Kreislauf 1.261 Nm<sup>3</sup>

### Belastung

Nm<sup>3</sup> / kg, h

Nm<sup>3</sup> / Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas     | 5.9             | -                             | 0.1            | 39.3 | 50.0           | 0.3             | 4.4            | -    | 4.34              |              |
| Restgas   | 16.0            | 0.2                           | 0.1            | 32.6 | 42.3           | 2.6             | 6.2            | 1.00 | 6.17              |              |
|           |                 |                               |                | 34.4 | 44.4           |                 |                |      |                   |              |
|           |                 |                               |                | 1.   | 12.9           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 10 %  
 H<sub>2</sub>:CO im Sygas 1.27  
 H<sub>2</sub>:CO im Restgas 1.30  
 Verbrauch von H<sub>2</sub>:CO 1.23

Kontraktion nach Menge 29.3 %  
 " " N<sub>2</sub> 29.5 %  
 " " CO<sub>2</sub> — %  
 Durchschnittliche Kontraktion 29.4 %

umgesetzt 41.6 % CO  
 verflüssigt 24.0 % H<sub>2</sub>  
 Verfl.-Grad A 57.1 % CO + H<sub>2</sub>  
 " " P

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 9.4 CO<sub>2</sub> 32.8 bezogen auf CO-Umsatz

### Produkte

Paraffingatsch 1.70 kg 16.5 %  
 Öl-Kondensat 4.80 " 46.6 %  
 A.-K. Benzin 3.80 " 36.9 %  
 Flüssige Prod. 10.30 " 100 %  
 Sywasser 18.70 kg = 1.51 × flüss. Produkte

### Gesamtprodukt

SB 38 °C  
 — 200 °C 63.7 %  
 200 — 320 °C 18.6 %  
 > 320 °C 16.3 %  
 Olefine Vol. %  
 — 200 °C 71; 200-320 °C 6.2

### Ausbeute

Flüssige Prod. 33.1 g/Nm<sup>3</sup> Sygas 37.1 g/Nm<sup>3</sup> Nutzgas (80+12) g/Nm<sup>3</sup> Idealgas  
 Gasöl " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

### Bemerkungen:

000120





# Druckversuchsanlage

Produktionsbericht vom 16/12. 12 1942

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt: ✓ kg

Betriebsstunden 24/50 V.H.  
 Gasdruck 20 atü  
 Temperatur 16.5/250 atü 20.18-225

Sy-W-Gas 310 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
 " 12.9 Nm<sup>3</sup>/h

Restgas 103 Nm<sup>3</sup>  
 " " " " " " " "  
 Kreislaufgas 814 Nm<sup>3</sup>  
 Kreislauf 2.63

Belastung Nm<sup>3</sup>/kg.h Nm<sup>3</sup>/Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas     | 6.3             | ✓    | 0.1            | 39.0 | 49.9           | 0.3             | 4.4            | ✓    | 42.9              |              |
| Restgas   | 26.2            | 0.2  | 0.1            | 23.2 | 37.3           | 5.1             | 7.7            | 10.4 | 7.67              |              |
|           |                 |      |                | 27.6 | 40.6           |                 |                |      |                   |              |
|           |                 |      |                | 11.4 | 4.7            |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 11.1 %  
 H<sub>2</sub>:CO im Sygas 1.28  
 H<sub>2</sub>:CO im Restgas 1.61  
 Verbrauch von H<sub>2</sub>:CO 1.12

Kontraktion nach Menge 41.0 %  
 " " N<sub>2</sub> 44.6 %  
 " " CO<sub>2</sub> %  
 Durchschnittliche Kontraktion 49.8 %

umgesetzt %CO 67.1 %H<sub>2</sub> 58.6 %CO+H<sub>2</sub> 25.9  
 verflüssigt 39.2  
 Verfl.-Grad A 58.6  
 " " P

CH<sub>4</sub> + CmHn 9.7 CO<sub>2</sub> 31.7 bezogen auf CO-Umsatz

**Produkte**

|                |       |           |      |                   |
|----------------|-------|-----------|------|-------------------|
| Paraffingatsch | 4.35  | kg        | 25.0 | %                 |
| Ol-Kondensat   | 7.20  | "         | 44.4 | %                 |
| A.-K. Benzin   | 5.85  | "         | 35.6 | %                 |
| Flüssige Prod. | 17.40 |           |      | 100%              |
| Sywasser       | 153.0 | kg = 9.77 |      | × flüss. Produkte |

**Gesamtprodukt**

|         |      |             |
|---------|------|-------------|
| SB      | 34   | °C          |
| - 100°  |      | % = 22.4    |
| - 200°  | 54.2 | %           |
| - 320°  | 27.3 | %           |
| Olefine |      | Vol. %      |
| - 200°  |      | 200-320° 69 |

**Ausbeute**

|                |      |                         |      |                           |       |                            |
|----------------|------|-------------------------|------|---------------------------|-------|----------------------------|
| Flüssige Prod. | 56.2 | g Nm <sup>3</sup> Sygas | 62.2 | g Nm <sup>3</sup> Nützgas | 166.4 | g Nm <sup>3</sup> Idealgas |
| Gasol          |      | "                       | "    | "                         | "     | "                          |
| Gesamt-Produkt |      | "                       | "    | "                         | "     | "                          |
| Sywasser       |      | "                       | "    | "                         | "     | "                          |

**Bemerkungen:**  
 Ofen temperatur vom 16.0 atü auf 25.0 atü erhöht  
 Feinschwammmenge nicht normal 12.8 m<sup>3</sup>/h

000122



# Druckversuchsanlage

Versuchsbericht vom 14/15. 12. 1943

Ofen-Nr. 11  
 Füllung: 13.  
 C-Fe-Inhalt - kg

Betriebsstunden 24/5036  
 Gasdruck 20,0 atü  
 Temperatur 16,0 atü 203,4 °C

W-Gas 212 Nm<sup>3</sup>  
 " " "  
 " 1,8 Nm<sup>3</sup>/h

Restgas 159 Nm<sup>3</sup>  
 " " Nm<sup>3</sup>/h  
 Kreislaufgas 634 Nm<sup>3</sup>  
 Kreislauf 2,98

Belastung Nm<sup>3</sup> / kg, h

| Analysen: | Nm <sup>3</sup> /Norm.-Vol., h |                               |                |      |                |                 |                |     |                   |              |
|-----------|--------------------------------|-------------------------------|----------------|------|----------------|-----------------|----------------|-----|-------------------|--------------|
|           | CO <sub>2</sub>                | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht |
| Sygas     | 5.9                            | -                             | 0.1            | 39.1 | 49.2           | 0.3             | 5.4            | -   | 5.38              |              |
| Restgas   | 12.1                           | 0.1                           | 0.1            | 36.3 | 42.7           | 1.5             | 2.3            | 100 | 7.20              |              |
|           |                                |                               |                | 36.8 | 44.3           |                 |                |     |                   |              |
|           |                                |                               |                |      | 12.0           |                 |                |     |                   |              |

Gesamt-Inerte (Idealgas) 11.5%  
 H<sub>2</sub>:CO im Sygas 12.6  
 H<sub>2</sub>:CO im Restgas 1.18  
 Verbrauch von H<sub>2</sub>:CO 1.42

Kontraktion nach Menge 24.9 %  
 " " N<sub>2</sub> 25.9 %  
 " " CO<sub>2</sub> %  
 Durchschnittliche Kontraktion 25.4 %

% CO  
 umgesetzt 31.5  
 verflüssigt 21.6  
 Verfl.-Grad A 68.7  
 " " P

% H<sub>2</sub> 35.7  
 % CO+H<sub>2</sub> 37.6

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 6.6 CO<sub>2</sub> 24.7

bezogen auf CO-Umsatz

| Produkte       |                                  | %    |       |
|----------------|----------------------------------|------|-------|
| Paraffingatsch | 2.80 kg                          | 32.4 | %     |
| Ol-Kondensat   | 2.10 "                           | 24.0 | %     |
| A.-K. Benzin   | 2.60 "                           | 34.6 | %     |
| Flüssige Prod. | 7.50 "                           |      | 100 % |
| Sywasser       | 1.70 kg = 1.23 × flüss. Produkte |      |       |

| Gesamtprodukt |        |
|---------------|--------|
| SB            | 32 °C  |
| = 200 °C      | 47.4 % |
| 200 - 320 °C  | 23.6 % |
| > 320 °C      | 32.1 % |

Olefine Vol. %  
 - 200 °C 27.7; 200-320 °C 2.5

## Ausbeute

Flüssige Prod. 35.4 g/Nm<sup>3</sup> Sygas 40.1 g/Nm<sup>3</sup> Nutzgas (100-112) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

000124



# Druckversuchsanlage

Versuchsbericht vom 12./13. 12. 1943

Ofen-Nr. 11  
 Füllung: 13.  
 C<sub>6</sub>-Fe-Inhalt - kg

Betriebsstunden 24/4988  
 Gasdruck 20.0 atü  
 Temperatur 15.0 atü 200.4 °C

W-Gas 308 Nm<sup>3</sup>  
 " " " "  
 " " " "  
 " 4.7 Nm<sup>3</sup>/h

Restgas 189 Nm<sup>3</sup>  
 " " " "  
 Kreislaufgas 203 Nm<sup>3</sup>  
 Kreislauf 1. 337

Belastung Nm<sup>3</sup> / kg, h

Nm<sup>3</sup> / Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|-----|-------------------|--------------|
| Sygas     | 6.3             | -                             | 0.1            | 37.9 | 48.7           | 0.3             | 6.7            | -   | 6.63              |              |
| Restgas   | 9.2             | 0.1                           | 0.1            | 37.0 | 45.8           | 1.2             | 6.6            | -   | 6.50              |              |
|           |                 |                               |                | 37.3 | 41.6           |                 |                |     |                   |              |
|           |                 |                               |                | 71   | 125            |                 |                |     |                   |              |

Gesamt-Inerte (Idealgas) 13.4 %

H<sub>2</sub>:CO im Sygas 1.28

H<sub>2</sub>:CO im Restgas 1.22

Verbrauch von H<sub>2</sub>:CO

Kontraktion nach Menge %

" " N<sub>2</sub> %

" " CO<sub>2</sub> %

Durchschnittliche Kontraktion %

% CO

% H<sub>2</sub>

% CO + H<sub>2</sub>

umgesetzt

verflüssigt

Verfl.-Grad A

" " P

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> ..... CO<sub>2</sub> ..... bezogen auf CO-Umsatz

## Produkte

Gesamtprodukt 10-30.5

|                |             |      |             |                   |
|----------------|-------------|------|-------------|-------------------|
| Paraffingasch  | <u>1.00</u> | kg   | <u>31.8</u> | %                 |
| Öl-Kondensat   | <u>0.80</u> | "    | <u>25.3</u> | %                 |
| A.-K. Benzin   | <u>1.35</u> | "    | <u>42.9</u> | %                 |
| Flüssige Prod. | <u>3.15</u> | "    |             | 100 %             |
| Sywasser       | <u>4.20</u> | kg = |             | × flüss. Produkte |

|              |              |    |
|--------------|--------------|----|
| SB           | <u>48</u>    | °C |
| - 200 °C     | <u>116.2</u> | %  |
| 200 - 320 °C | <u>21.9</u>  | %  |
| > 320 °C     |              | %  |

Olefine Vol. %  
 - 200° 50.0; 200-320° 17.9

## Ausbeute

Flüssige Prod. g/Nm<sup>3</sup> Sygas g/Nm<sup>3</sup> Nutzgas g/Nm<sup>3</sup> Idealgas

Gasol " " " " " "

Gesamt-Produkt " " " " " "

Sywasser " " " " " "

Bemerkungen:

000126



# Druckversuchsanlage

Versuchsbericht vom 10.11.12, 1943

Ofen-Nr. 11  
 Füllung: 13.  
 Fe-Inhalt - kg

Betriebsstunden 2414940  
 Gasdruck atü  
 Temperatur 175-114 atü 267,5-197,4 °C

Sy-W-Gas 220 Nm<sup>3</sup>  
 " " " "  
 " 1/2 Nm<sup>3</sup>/h

Restgas 165 Nm<sup>3</sup>  
 " " " "  
 Kreislaufgas 654 Nm<sup>3</sup>  
 Kreislauf 1.297

| Analysen: | Nm <sup>3</sup> / kg,h |                               |                |      |                |                 |                |      | Nm <sup>3</sup> / Norm.-Vol., h |              |  |
|-----------|------------------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|---------------------------------|--------------|--|
|           | CO <sub>2</sub>        | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F               | Litergewicht |  |
| Sygas     | 6.2                    | -                             | 0.1            | 38.7 | 48.1           | 0.3             | 6.6            | -    | 6.46                            |              |  |
| Restgas   | 13.2                   | 0.2                           | 0.1            | 34.7 | 40.5           | 1.7             | 8.6            | 1.02 | 8.53                            |              |  |
|           |                        |                               |                | 35.6 | 43.9           |                 |                |      |                                 |              |  |
|           |                        |                               |                | 11   | 16.1           |                 |                |      |                                 |              |  |

Gesamt-Inerte (Idealgas) 13.2 %  
 H<sub>2</sub>:CO im Sygas 1.24  
 H<sub>2</sub>:CO im Restgas 1.20  
 Verbrauch von H<sub>2</sub>:CO 1.34

Kontraktion nach Menge 25.0 %  
 " " N<sub>2</sub> 24.1 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 24.55 %

umgesetzt 32.3 % CO  
 verflüssigt 19.9  
 Verfl.-Grad A 61.7  
 " " P -

% H<sub>2</sub> 34.8  
 % CO+H<sub>2</sub> 33.55

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 1.9 CO<sub>2</sub> 30.1 bezogen auf CO-Umsatz

### Produkte

Paraffingatsch 2.48 kg 39.5 %  
 Öl-Kondensat 1.65 " 26.1 %  
 A.-K. Benzin 2.70 " 42.5 %  
 Flüssige Prod. 6.35 " 100 %  
 Sywasser 7.70 kg = 1.91 × flüss. Produkte

### Gesamtprodukt

SB 36 °C  
 - 200 °C 19.3 %  
 200 - 320 °C 24.5 %  
 > 320 °C 22.5 %  
 Olefine Vol. %  
 - 200° 22; 200-320° 22

### Ausbeute

Flüssige Prod. 28.7 g/Nm<sup>3</sup> Sygas 33.4 g/Nm<sup>3</sup> Nutzgas - g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

### Bemerkungen:

000128







# Druckversuchsanlage

Versuchsbericht vom 7. 8. 12 1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt / kg

Betriebsstunden 24/4868  
 Gasdruck 20.0 atü  
 Temperatur 25.0 - 15.0 atü 25 °C

Sy-W-Gas 295 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
 " 12.3 Nm<sup>3</sup>/h

Restgas 247 Nm<sup>3</sup>  
 " " " " " " " "  
 Kreislaufgas 818 Nm<sup>3</sup>  
 Kreislauf 1122 Nm<sup>3</sup>

Belastung Nm<sup>3</sup> / kg, h

| Analysen: | Nm <sup>3</sup> /Norm.-Vol., h |                               |                |      |                |                 |                |   | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------|--------------------------------|-------------------------------|----------------|------|----------------|-----------------|----------------|---|------|-------------------|--------------|
|           | CO <sub>2</sub>                | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> |   |      |                   |              |
| Sygas     | 6.0                            | -                             | 0.1            | 39.2 | 47.6           | 0.3             | 6.8            | - | 6.07 |                   |              |
| Restgas   |                                |                               |                |      |                |                 |                |   |      |                   |              |

Gesamt-Inerte (Idealgas) %

H<sub>2</sub>:CO im Sygas

H<sub>2</sub>:CO im Restgas

Verbrauch von H<sub>2</sub>:CO

Kontraktion nach Menge

" " N<sub>2</sub> %

" " CO<sub>2</sub> %

Durchschnittliche Kontraktion %

% CO

% H<sub>2</sub>

% CO + H<sub>2</sub>

umgesetzt

verflüssigt

Verfl.-Grad A

" " P

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> CO<sub>2</sub> bezogen auf CO-Umsatz

### Produkte

|                |      |      |      |                   |
|----------------|------|------|------|-------------------|
| Paraffingatsch | 1,30 | kg   | 241  | %                 |
| Öl-Kondensat   | 1,20 | "    | 22,2 | %                 |
| A.-K. Benzin   | 2,90 | "    | 53,7 | %                 |
| Flüssige Prod. | 5,40 | "    |      | 100 %             |
| Sywasser       | 5,80 | kg = |      | × flüss. Produkte |

### Gesamtprodukt

|              |      |    |
|--------------|------|----|
| SB           | 12   | °C |
| - 200 °C     | 56,8 | %  |
| 200 - 320 °C | 19,6 | %  |
| > 320 °C     | 23,9 | %  |

Olefine Vol. %  
 - 200° 44; 200-320° 11

### Ausbeute

|                | g/Nm <sup>3</sup> Sygas | g/Nm <sup>3</sup> Nutzgas | g/Nm <sup>3</sup> Idealgas |
|----------------|-------------------------|---------------------------|----------------------------|
| Gasol          | "                       | "                         | "                          |
| Gesamt-Produkt | "                       | "                         | "                          |
| Sywasser       | "                       | "                         | "                          |

### Bemerkungen:

20<sup>20</sup> - 22<sup>30</sup> Stromausfall Temp. des Ofens  
 um 10<sup>00</sup> auf 16.0 abgefallen

000131



**Druckversuchsanlage**

**Produktionsbericht vom** 5-6.12.1943

Ofen-Nr. 11

Betriebsstunden 15/4824

Füllung: 15

Gasdruck 20.0 atü

Co-Fe-Inhalt: 14.1 kg

Temperatur 250 atü 215 °C

Sy-W-Gas: 186 Nm<sup>3</sup>

Restgas: 10.6 Nm<sup>3</sup>

" " " " " "

" " " " " " Nm<sup>3</sup>/h

" " " " " "

Kreislaufgas: 482 Nm<sup>3</sup>

" " " " " "

Kreislauf: 1.213

Belastung: 13.4 Nm<sup>3</sup>/kg,h 13.4 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | C <sub>n</sub> H <sub>n</sub> | O <sub>2</sub> | CO | H <sub>2</sub> <sup>o</sup> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|-------------------------------|----------------|----|-----------------------------|-----------------|----------------|-----|-------------------|--------------|
| Sygas     |                 |                               |                |    |                             |                 |                |     |                   |              |
| Restgas   |                 |                               |                |    |                             |                 |                |     |                   |              |

Gesamt-Inerte (Idealgas) 43.0 %

Kontraktion nach Menge 43.0 %

H<sub>2</sub>: CO im Sygas

" " N<sub>2</sub> %

H<sub>2</sub>: CO im Restgas

" " CO<sub>2</sub> %

Verbrauch von H<sub>2</sub>: CO

Durchschnittliche Kontraktion %

|               | %CO | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|---------------|-----|-----------------|--------------------|
| umgesetzt     |     |                 |                    |
| verflüssigt   |     |                 |                    |
| Verfl.-Grad A |     |                 |                    |
| " " P         |     |                 |                    |

CH<sub>4</sub> + C<sub>n</sub>H<sub>n</sub> 3.1 CO<sub>2</sub> 3.1 bezogen auf CO-Umsatz

**Produkte**

**Gesamtprodukt**

|                |                 |                   |
|----------------|-----------------|-------------------|
| Paraffingatsch | <u>1.0</u> kg   | <u>1.0</u> %      |
| Ol-Kondensat   | <u>5.0</u> "    | <u>5.0</u> %      |
| A.-K. Benzin   | <u>3.1</u> "    | <u>3.1</u> %      |
| Flüssige Prod. | "               | 100 %             |
| Sywasser       | <u>1.0</u> kg = | X flüss. Produkte |

|         |                       |
|---------|-----------------------|
| SB      | <u>120</u> °C         |
| - 100°  | <u>1.0</u> %          |
| - 200°  | <u>1.0</u> %          |
| - 320°  | <u>1.0</u> %          |
| Olefine | Vol. %                |
| - 200°  | <u>1.0</u> ; 200-320° |

**Ausbeute**

| Flüssige Prod. | g Nm <sup>3</sup> Sygas | g Nm <sup>3</sup> Nutzgas | g/Nm <sup>3</sup> Idealgas |
|----------------|-------------------------|---------------------------|----------------------------|
| Gasol          | "                       | "                         | "                          |
| Gesamt-Produkt | "                       | "                         | "                          |
| Sywasser       | "                       | "                         | "                          |

**Bemerkungen:**

*Die Ausbeute an Paraffin ist im Vergleich zu den anderen Produkten geringfügig.*

000133





# Druckversuchsanlage

Produktionsbericht vom 2-3. 19 1943

Ofen-Nr. 11

Betriebsstunden 24/4761

Füllung: 13

Gasdruck 200 atü

Co-Fe-Inhalt: / kg

Temperatur 250 atü 225 °C

Sy-W-Gas 315 Nm³

Restgas 181 Nm³

" " " " " "

" " " " " "

" " " " " "

Kreislaufgas 492 Nm³

" " " " " "

Kreislauf 9231

Belastung: / Nm³/kg,h / Nm³/Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas     | 6.7             | 0.1                           | 0.1            | 28.0 | 2.8            | 0.3             | 6.1            | -    | 5.96              |              |
| Restgas   | 25.4            | 0.1                           | 0.1            | 27.9 | 39.8           | 4.8             | 9.7            | 16.5 | 9.84              |              |
|           |                 |                               |                | 11   | 146            |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 22 %  
 H<sub>2</sub> CO im Sygas 22 %  
 H<sub>2</sub> CO im Restgas 22 %  
 Verbrauch von H<sub>2</sub>: CO 22 %  
 Kontraktion nach Menge 22 %  
 " " N<sub>2</sub> 22 %  
 " " CO<sub>2</sub> 22 %  
 Durchschnittliche Kontraktion 22 %

umgesetzt, %CO = %H<sub>2</sub> = %CO+H<sub>2</sub>  
 verfügbar  
 Verfl.-Grad A  
 " " P

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> / CO<sub>2</sub> bezogen auf CO-Umsatz

## Produkte

Paraffingatsch 2.77 kg  
 Öl-Kondensat 4.95  
 A.-K. Benzin 4.91  
 Flüssige Prod. 15.55  
 Sywasser 2.77 kg = 100 % flüss. Produkte

## Gesamtprodukt

SB / °C  
 - 100°  
 - 200°  
 - 320°  
 Olefine Vol. %  
 - 200° ; 200 - 320°

## Ausbeute

Flüssige Prod. 199 g Nm³ Sygas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

000136



# Druckversuchsanlage

Produktionsbericht vom 1.2.12 1943

Ofen-Nr. 11

Betriebsstunden 24/4737

Füllung: 13

Gasdruck 20.0 atü

Co-Fe-Inhalt: kg

Temperatur 25.0 atü 25 °C

Sy-W-Gas 30.5 Nm³

Restgas 2.73 Nm³

" " " " Nm³/h

Kreislaufgas 7.83 Nm³/h

" " " " Nm³/h

Kreislauf 1.25

Belastung: Nm³/kg, h Nm³/Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas     | 6.5             | 1                             | 0.1            | 28.3 | 2.81           | 0.3             | 6.2            | 1    | 1.14              |              |
| Restgas   | 25.7            | 0.3                           | 0.1            | 22.4 | 36.0           | 4.9             | 10.6           | 10.4 | 2.50              |              |
|           |                 |                               |                | 24.6 | 36.0           |                 |                |      |                   |              |
|           |                 |                               |                | 11   | 14.6           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 1.11 %  
 H<sub>2</sub> CO im Sygas 1.32  
 H<sub>2</sub> CO im Restgas 2.11  
 Verbrauch von H<sub>2</sub>: CO 1.11

Kontraktion nach Menge 13.0 %  
 " " N<sub>2</sub> 7.6 %  
 " " CO<sub>2</sub> 7.0 %  
 Durchschnittliche Kontraktion 43.3 %

|               | %CO  | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|---------------|------|-----------------|--------------------|
| umgesetzt     | 28.2 | 14.6            | 42.8               |
| verflüssigt   | 28.2 | 14.6            | 42.8               |
| Verfl.-Grad A | 52.8 |                 |                    |
| " " P         |      |                 |                    |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 2.60 CO<sub>2</sub> 3.11 berogen auf CO-Umsatz

## Produkte

Paraffingatsch 2.60 kg  
 O-Kondensat 8.60 "  
 A-K. Benzin 7.60 "  
 Flüssige Prod. 15.20 "  
 Sywasser 21.50 kg = 1.11 X flüss. Produkte

## Gesamtprodukt

SB 1.11 °C  
 - 100° 1.11 %  
 - 200° 1.11 %  
 - 320° 1.11 %  
 Olefine Vol. %  
 - 200° 1.11 ; 200-320° 1.11

## Ausbeute

Flüssige Prod. 29.1 g Nm³ Sygas  
 Gasol " " " g Nm³ Nutzgas  
 Gesamt-Produkt " " " g Nm³ Idealgas  
 Sywasser " " " " " "

## Bemerkungen:

000137





# Druckversuchsanlage

Produktionsbericht vom 28/29 11 1943

Ofen-Nr. 11

Betriebsstunden 23/4665

Füllung: 13

Gasdruck 2000 atü

Co-Fe-Inhalt / kg

Temperatur 250 atü 225 °C

Sy-W-Gas 3.09 Nm<sup>3</sup>

Restgas 173 Nm<sup>3</sup>

" " " " " "

" " " " " "

" " " " " "

Kreislaufgas 755 Nm<sup>3</sup>/h

" " " " " "

Kreislauf " " " " " "

Belastung 105 Nm<sup>3</sup>/kg.h Nm<sup>3</sup>/Norm.-Vol., h

| Analysen | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|----------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas    | 5.8             | /                             | 0.1            | 39.2 | 48.0           | 0.3             | 6.6            | /    | 6.46              |              |
| Restgas  | 23.8            | 0.2                           | 0.1            | 24.5 | 36.1           | 4.4             | 10.9           | 1.05 | 10.8              |              |
|          |                 |                               |                | 22.8 | 39.5           |                 |                |      |                   |              |
|          |                 |                               |                | 1.1  | 14.2           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) %

Kontraktion nach Menge 44.0 %

H<sub>2</sub>: CO im Sygas %

" " N<sub>2</sub> 40.3 %

H<sub>2</sub>: CO im Restgas %

" " CO<sub>2</sub> %

Verbrauch von H<sub>2</sub>: CO %

Durchschnittliche Kontraktion %

|               | %CO | %H <sub>2</sub> | %CO + H <sub>2</sub> |
|---------------|-----|-----------------|----------------------|
| umgesetzt     |     |                 |                      |
| verflüssigt   |     |                 |                      |
| Verfl.-Grad A |     |                 |                      |
| " " P         |     |                 |                      |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> CO<sub>2</sub> bezogen auf CO-Umsatz

## Produkte

|                |       |      |                   |
|----------------|-------|------|-------------------|
| Paraffingatsch | 3.15  | kg   | %                 |
| Ol-Kondensat   | 9.20  | "    | %                 |
| A.-K. Benzin   | 4.90  | "    | %                 |
| Flüssige Prod. | 17.25 | "    | 100%              |
| Sywasser       | 21.20 | kg = | × flüss. Produkte |

## Gesamtprodukt

|         |            |
|---------|------------|
| SB      | °C         |
| - 100°  | %          |
| - 200°  | %          |
| - 320°  | %          |
| Olefine | Vol. %     |
| - 200°  | 200 - 320° |

## Ausbeute

|                |                         |                           |                            |
|----------------|-------------------------|---------------------------|----------------------------|
| Flüssige Prod. | g/Nm <sup>3</sup> Sygas | g/Nm <sup>3</sup> Nutzgas | g/Nm <sup>3</sup> Idealgas |
| Gasol          | "                       | "                         | "                          |
| Gesamt-Produkt | "                       | "                         | "                          |
| Sywasser       | "                       | "                         | "                          |

## Bemerkungen:

Fluss wurde 750 manometer angefahren

000140

# Druckversuchsanlage

Produktionsbericht vom 27/28. 11. 1943

Ofen-Nr. 11

Betriebsstunden 31/ 4640

Füllung: 13

Gasdruck 20.0 atü

Co-Fe-Inhalt: ..... kg

Temperatur: 25.0 atü 225 °C

Sy-W-Gas 8.76 Nm<sup>3</sup>

Restgas 159 Nm<sup>3</sup>

" " " " " "

" " " " " "

" " " " " "

Kreislaufgas 584 Nm<sup>3</sup>

" " " " " "

Kreislauf 1.221 Nm<sup>3</sup>

Belastung: 105 Nm<sup>3</sup>/kg,h

| Analysen: | Nm <sup>3</sup> /Norm.-Vol., h |                               |                |      |                |                 |                | C-Z | N <sub>2</sub> -F | Liegewicht |
|-----------|--------------------------------|-------------------------------|----------------|------|----------------|-----------------|----------------|-----|-------------------|------------|
|           | CO <sub>2</sub>                | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> |     |                   |            |
| Sygas     | 5.8                            | /                             | 0.1            | 39.4 | 48.2           | 0.3             | 6.2            | /   | 0.13              |            |
| Restgas   | 2.44                           | 0.3                           | 0.1            | 24.3 | 39.2           | 4.6             | 10.1           | /   | 10.0              |            |
|           |                                |                               |                | 29.1 | 40.2           |                 |                |     |                   |            |
|           |                                |                               |                | 1    | 138            |                 |                |     |                   |            |

Gesamt-Inerte (Idealgas) 2.4 %

Kontraktion nach Menge 43.4 %

H<sub>2</sub>:CO im Sygas 1.3

" " N<sub>2</sub> 38.7 %

H<sub>2</sub>:CO im Restgas 4.7

" " CO<sub>2</sub> 10.1 %

Verbrauch von H<sub>2</sub>:CO 1.16

Durchschnittliche Kontraktion 40.55 %

|               | %CO         | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|---------------|-------------|-----------------|--------------------|
| umgesetzt     | <u>6.5</u>  | <u>48.2</u>     | <u>54.7</u>        |
| verflüssigt   | <u>1.1</u>  | <u>1.1</u>      | <u>2.2</u>         |
| Verfl.-Grad A | <u>17</u>   |                 |                    |
| " " P         | <u>68.0</u> |                 |                    |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> ..... CO<sub>2</sub> ..... bezogen auf CO-Umsatz

## Produkte

|                |              |      |                   |
|----------------|--------------|------|-------------------|
| Paraffingas    | <u>3.30</u>  | kg   |                   |
| Ol-Kondensat   | <u>7.90</u>  | "    |                   |
| A.-K. Benzin   | <u>4.40</u>  | "    |                   |
| Flüssige Prod. | <u>15.60</u> | "    | 100 %             |
| Sywasser       | <u>17.80</u> | kg = | X flüss. Produkte |

## Gesamtprodukt

|         |            |
|---------|------------|
| SB      | °C         |
| - 100°  | %          |
| - 200°  | %          |
| - 320°  | %          |
| Olefine | Vol. %     |
| - 200°  | 200 - 320° |

## Ausbeute

|                |              |                         |              |                           |              |                            |
|----------------|--------------|-------------------------|--------------|---------------------------|--------------|----------------------------|
| Flüssige Prod. | <u>16.12</u> | g Nm <sup>3</sup> Sygas | <u>11.9</u>  | g Nm <sup>3</sup> Nutzgas | <u>11.9</u>  | g/Nm <sup>3</sup> Idealgas |
| Gasol          | <u>16.12</u> | "                       | <u>11.9</u>  | "                         | <u>11.9</u>  | "                          |
| Gesamt-Produkt | <u>17.32</u> | "                       | <u>13.5</u>  | "                         | <u>13.5</u>  | "                          |
| Sywasser       | <u>17.80</u> | "                       | <u>17.80</u> | "                         | <u>17.80</u> | "                          |

## Bemerkungen:

*Offen 5:30 abgestellt wegen Stromausfall*

000141











# Druckversuchsanlage

Versuchsbericht vom 22/23 11 4 1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt \_\_\_\_\_ kg

Betriebsstunden 24/4523  
 Gasdruck 20,0 atü  
 Temperatur 25,0 atü 235 °C

Sy-W-Gas 326 Nm<sup>3</sup>  
 " " "  
 " " "  
 " 136 Nm<sup>3</sup>/h

Restgas 195 Nm<sup>3</sup>  
 " " "  
 Kreislaufgas 779 Nm<sup>3</sup>  
 Kreislauf 1: 2,29

Belastung 117 Nm<sup>3</sup>/kg,h Nm<sup>3</sup>/Norm-Vol., h

| Analysen: | Nm <sup>3</sup> /kg,h |                               |                |      |                | Nm <sup>3</sup> /Norm-Vol., h |                |      |                   |              |
|-----------|-----------------------|-------------------------------|----------------|------|----------------|-------------------------------|----------------|------|-------------------|--------------|
|           | CO <sub>2</sub>       | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub>               | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
| Sygas     | 6,0                   | ✓                             | 0,1            | 39,3 | 48,0           | 0,3                           | 6,3            | ✓    | 6,15              |              |
| Restgas   | 25,4                  | 0,3                           | 0,1            | 23,0 | 35,7           | 4,6                           | 10,9           | 10,3 | 10,2              |              |
|           |                       |                               |                | 22,9 | 39,5           |                               |                |      |                   |              |
|           |                       |                               |                | 11   | 141            |                               |                |      |                   |              |

Gesamt-Inerte (Idealgas) 12,2 %  
 H<sub>2</sub>:CO im Sygas 1,4  
 H<sub>2</sub>:CO im Restgas 1,5  
 Verbrauch von H<sub>2</sub>:CO 1,05

Kontraktion nach Menge 40,1 %  
 " " N<sub>2</sub> 42,1 %  
 " " CO<sub>2</sub> \_\_\_\_\_ %  
 Durchschnittliche Kontraktion 41,6 %

|               |      |                  |                       |
|---------------|------|------------------|-----------------------|
|               | % CO | % H <sub>2</sub> | % CO + H <sub>2</sub> |
| umgesetzt     | 66,8 | 57,7             | 62,25                 |
| verflüssigt   | 39,3 |                  |                       |
| Verfl.-Grad A | 58,8 |                  |                       |
| " " P         |      |                  |                       |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 8,8 CO<sub>2</sub> 32,3 bezogen auf CO-Umsatz

### Produkte

|                |             |                                   |             |       |
|----------------|-------------|-----------------------------------|-------------|-------|
| Paraffingasch  | <u>3,00</u> | kg                                | <u>17,4</u> | %     |
| Ol-Kondensat   | <u>8,50</u> | "                                 | <u>49,1</u> | %     |
| A.-K. Benzin   | <u>5,80</u> | "                                 | <u>33,5</u> | %     |
| Flüssige Prod. | <u>17,3</u> | "                                 |             | 100 % |
| Sywasser       | <u>21,0</u> | kg = <u>141</u> × flüss. Produkte |             |       |

### Gesamtprodukt

|              |             |                |
|--------------|-------------|----------------|
| SB           | <u>40</u>   | °C             |
| - 200 °C     | <u>62,9</u> | % <u>0,67</u>  |
| 200 - 320 °C | <u>17,3</u> | % <u>0,714</u> |
| > 320 °C     | <u>12,1</u> | %              |
| Olefine      |             | Vol. %         |
| - 200°       | <u>68</u>   |                |
| 200-320°     | <u>53</u>   |                |

### Ausbeute

|                |             |                         |             |                           |                |                            |
|----------------|-------------|-------------------------|-------------|---------------------------|----------------|----------------------------|
| Flüssige Prod. | <u>58,7</u> | g/Nm <sup>3</sup> Sygas | <u>69,8</u> | g/Nm <sup>3</sup> Nutzgas | <u>(201,6)</u> | g/Nm <sup>3</sup> Idealgas |
| Gasöl          | <u>17,7</u> | "                       | <u>18,2</u> | "                         | "              | "                          |
| Gesamt-Produkt | <u>66,8</u> | "                       | <u>26,0</u> | "                         | "              | "                          |
| Sywasser       |             | "                       |             | "                         | "              | "                          |

### Bemerkungen:

*gesamt: 48% Olefine*

000146



**Druckversuchsanlage** Produktionsbericht vom 20./21. 11. 1949

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt: - kg

Betriebsstunden: 24/4475  
 Gasdruck: 20,0 atü  
 Temperatur: 250 atü 225 °C

W-Gas: 315 Nm³  
 Restgas: 180 Nm³  
 Kreislaufgas: 740 Nm³  
 Kreislauf: 1: 275

Belastung: Nm³/kg.h Nm³/Norm-Vol., h

| Analysen: | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO    | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|------|----------------|-------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas     | 6.0             | -    | 0.1            | 79.1  | 48.7           | 0.3             | 5.8            | -    | 5.72              |              |
| Restgas   | 26.0            | 0.3  | 0.1            | 22.5  | 25.6           | 4.9             | 10.6           | 1.04 | 10.55             |              |
|           |                 |      |                | 27.4  | 39.4           |                 |                |      |                   |              |
|           |                 |      |                | 1.143 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas): 10.9 %  
 H<sub>2</sub>: CO im Sygas: 19.5 %  
 H<sub>2</sub>: CO im Restgas: 5.5 %  
 Verbrauch von H<sub>2</sub>: CO: 10.4 %

Kontraktion nach Menge: 42.8 %  
 " " N<sub>2</sub>: 45.6 %  
 " " CO<sub>2</sub>: - %  
 Durchschnittliche Kontraktion: 44.2 %

|               | %CO  | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|---------------|------|-----------------|--------------------|
| umgesetzt     | 68.7 | 13.3            | 82.0               |
| verflüssigt   | 49.3 |                 |                    |
| Verfl.-Grad A | 1.15 |                 |                    |
| " " P         |      |                 |                    |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub>: 8.4 CO<sub>2</sub>: 29.9 bezogen auf CO-Umsatz

| Produkte       |                                   |        | Gesamtprodukt |          |
|----------------|-----------------------------------|--------|---------------|----------|
| Paraffingatsch | 3.40 kg                           | 18.6 % | SB            | °C       |
| Ol-Kondensat   | 8.90 "                            | 48.6 % | - 100°        | %        |
| A-K. Benzin    | 6.00 "                            | 32.8 % | - 200°        | %        |
| Flüssige Prod. | 18.30 "                           | 100 %  | - 320°        | %        |
| Sywasser       | 23.80 kg = 1.25 x flüss. Produkte |        | Olefine       | Vol. %   |
|                |                                   |        | - 200°        | 200-320° |

**Ausbeute**

Flüssige Prod.: 581 g Nm³ Sygas g Nm³ Nutzgas g Nm³ Idealgas  
 Gasol: " " " " " "  
 Gesamt-Produkt: " " " " " "  
 Sywasser: " " " " " "

**Bemerkungen:**

000148







**Druckversuchsanlage**

Produktionsbericht vom 16/17.11.1947

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt: - kg

Betriebsstunden 24/4385  
 Gasdruck: 20.4 atü  
 Temperatur: 25.5 atü 225 °C

Sy-W-Gas 311 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
 " 12.9 Nm<sup>3</sup>/h

Restgas 177 Nm<sup>3</sup>  
 " " " " " " " "  
 Kreislaufgas 763 Nm<sup>3</sup>  
 Kreislauf 1: 2.46

Belastung: 1.01 Nm<sup>3</sup>/kg,h Nm<sup>3</sup>/Norm.-Vol., h

| Analysenp. | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas      | 6.5             | -    | 0.1            | 38.5 | 48.5           | 0.3             | 6.1            | -    | 6.03              | -            |
| Restgas    | 25.6            | 0.3  | 0.1            | 22.5 | 36.0           | 4.7             | 10.8           | 10.5 | 10.70             | -            |
|            |                 |      |                | 27.1 | 39.2           |                 |                |      |                   |              |
|            |                 |      |                | 1.   | 1.46           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 130 %  
 H<sub>2</sub> CO im Sygas 126  
 H<sub>2</sub> CO im Restgas 122  
 Verbrauch von H<sub>2</sub>: CO 128

Kontraktion nach Menge 49.3 %  
 " " N<sub>2</sub> 43.7 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 49.5 %

|               |             |                 |                    |
|---------------|-------------|-----------------|--------------------|
| umgesetzt     | %CO         | %H <sub>2</sub> | %CO+H <sub>2</sub> |
| verflüssigt   | <u>67</u>   | <u>26</u>       | <u>93</u>          |
| Verfl.-Grad A | <u>46.5</u> |                 |                    |
| " " P         |             |                 |                    |

CH<sub>4</sub> + CmHn 9.1 CO<sub>2</sub> 20.7 bezogen auf CO-Umsatz

**Produkte**

Paraffingatsch 3.00 kg 11.6 %  
 Cl-Kondensat 7.60 " 42.4 %  
 A.-K. Benzin 5.50 " 20.2 %  
 Flüssige Prod. 16.10 100 %  
 Sywasser 22.40 kg = 132 x flüss. Produkte

**Gesamtprodukt**

SB 37 °C  
 - 100° 0.161 %  
 - 200° 12.2 %  
 - 320° 12.2 %  
 Olefine Vol. %  
 - 200° 11 ; 200-320° 70

**Ausbeute**

|                |                                   |                                     |                                      |
|----------------|-----------------------------------|-------------------------------------|--------------------------------------|
| Flüssige Prod. | <u>17</u> g/Nm <sup>3</sup> Sygas | <u>88</u> g/Nm <sup>3</sup> Nutzgas | <u>20</u> g/Nm <sup>3</sup> Idealgas |
| Gasöl          | <u>13</u> " " "                   | <u>17.4</u> " " "                   | " " "                                |
| Gesamt-Produkt | <u>6.53</u> " " "                 | <u>26.3</u> " " "                   | " " "                                |
| Sywasser       | <u>20.8</u> " " "                 | <u>117</u> " " "                    | " " "                                |

**Bemerkungen:**

*Gasöl mit 45% Olef.*

000152



# Druckversuchsanlage

Produktionsbericht vom 15./16. II 1943

Ofen-Nr. M

Füllung: 13

Gf-Fa-Inhalt: \_\_\_\_\_ kg

Betriebsstunden 21/4361

Gasdruck 20.0 atü

Temperatur 25.0 atü 225 °C

Sy-W-Gas 285 Nm<sup>3</sup>

Restgas 147 Nm<sup>3</sup>

Kreislaufgas 206 Nm<sup>3</sup>/h

Kreislauf 1: 2,48 Nm<sup>3</sup>

Belastung: 100 Nm<sup>3</sup>/kg,h

| Analysen: | Nm <sup>3</sup> /Norm.-Vol., h |      |                |      |                |                 |                |      |                   |              |
|-----------|--------------------------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
|           | CO <sub>2</sub>                | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
| Sygas     | 6.4                            | -    | 0.1            | 38.5 | 18.3           | 0.3             | 6.4            | -    | 6.35              |              |
| Restgas   | 24.3                           | 0.3  | 0.1            | 23.9 | 37.3           | 2.7             | 10.0           | 1.04 | 9.95              |              |
|           |                                |      |                | 28.7 | 40.5           |                 |                |      |                   |              |
|           |                                |      |                | 1    | 1.44           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 28.2 %

H<sub>2</sub> CO im Sygas 1.1 %

H<sub>2</sub> CO im Restgas 1.2 %

Verbrauch von H<sub>2</sub> CO 1.2 %

Kontraktion nach Menge 48.5 %

N<sub>2</sub> 36.1 %

CO<sub>2</sub> \_\_\_\_\_ %

Durchschnittliche Kontraktion \_\_\_\_\_ %

|               | %CO         | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|---------------|-------------|-----------------|--------------------|
| umgesetzt     | <u>100</u>  | <u>56.6</u>     | <u>54.9</u>        |
| verflüssigt   | <u>25.3</u> |                 |                    |
| Verfl.-Grad A | <u>25.3</u> |                 |                    |
| " " P         |             |                 |                    |

CH<sub>4</sub> + CmHn 10.5 CO<sub>2</sub> 22.2 bezogen auf CO-Umsatz

## Produkte

|                |                                 |               |
|----------------|---------------------------------|---------------|
| Paraffingatsch | <u>2.84</u> kg                  | <u>11.6</u> % |
| Cl-Kondensat   | <u>7.84</u> "                   | <u>31.6</u> % |
| A.-K. Benzin   | <u>6.54</u> "                   | <u>25.6</u> % |
| Flüssige Prod. | <u>15.10</u> "                  | <u>58.8</u> % |
| Sywasser       | <u>19.20</u> kg = <u>74.3</u> % | <u>100</u> %  |

## Gesamtprodukt

|            |               |
|------------|---------------|
| SB         | <u>37</u> °C  |
| - 100°     | <u>5.8</u> %  |
| - 200°     | <u>58.8</u> % |
| - 320°     | <u>20.4</u> % |
| Olefine    | Vol. %        |
| - 200°     | <u>68</u> %   |
| - 200-320° | <u>58</u> %   |

## Ausbeute

|                |                                      |                                       |  |
|----------------|--------------------------------------|---------------------------------------|--|
| Flüssige Prod. | <u>15.10</u> g Nm <sup>3</sup> Sygas | <u>11.0</u> g Nm <sup>3</sup> Nutzgas | <u>60.7</u> g/Nm <sup>3</sup> Idealgas |
| Gasol          |                                      |                                       |  |
| Gesamt-Produkt |                                      |                                       |  |
| Sywasser       | <u>67.3</u> "                        | <u>77.6</u> "                         |  |

## Bemerkungen:

Stillstand von 22<sup>10</sup> - 22<sup>15</sup> C wegen Strom in Gasfall.

000153





| <b>Druckversuchsanlage</b>   |                      |                               |                       | Versuchsbericht vom 12. 12. 11 1943                                       |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
|--|----------------------|-------------------------------|-----------------------|---|----------------------|-----------------|----------------|------|-------------------|--|----------------------|-------------------------------|-----------------------|-----------|----------------|-----------------|----------------|-------------|-------------------|-----------------|-------|---------------|------|-----|----------------------|-------|-----|-----|--|------------------------|--------|---------|------|-----|-----|------|------|-----|------|---------------------|--------|----------|------|---|--|--|------|------|--|---------------------|--------|--------------|------|---|--|--|--|-------|--|------------------------|-------|----------|--|---|--|--|--|--|--|---|--|---------|--|--------|--|--|--|--|--|--|--|-------------------|-----|--|--|--|--|--|--|
| Ofen-Nr. 11<br>Füllung: 13<br>Co-Fe-Inhalt kg  |                      |                               |                       | Betriebsstunden 24/4292<br>Gasdruck 20 atü<br>Temperatur 250 atü °C       |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Sy-W-Gas 3.08 Nm³<br>" " " " " "<br>" " " " " "<br>" " " " " " 12.8 Nm³/h  |                      |                               |                       | Restgas 182 Nm³<br>" " " " " "<br>Kreislaufgas 826 Nm³<br>Kreislauf 1.265 |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Belastung Nm³ / kg,h   |                      |                               |                       | Nm³ / Norm.-Vol., h   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th>Analysen:</th> <th>CO<sub>2</sub></th> <th>C<sub>m</sub>H<sub>n</sub></th> <th>O<sub>2</sub></th> <th>CO</th> <th>H<sub>2</sub></th> <th>CH<sub>4</sub></th> <th>N<sub>2</sub></th> <th>C-Z</th> <th>N<sub>2</sub>-F</th> <th>Litergewicht</th> </tr> </thead> <tbody> <tr> <td>Sygas</td> <td>6.6</td> <td>1.2</td> <td>0.1</td> <td>38.0</td> <td>48.6</td> <td>0.3</td> <td>6.4</td> <td></td> <td>6.3</td> <td></td> </tr> <tr> <td>Restgas</td> <td>2.50</td> <td>0.3</td> <td>0.1</td> <td>23.3</td> <td>36.7</td> <td>4.6</td> <td>10.0</td> <td>1.00</td> <td>9.90</td> <td></td> </tr> <tr> <td></td> <td></td> <td></td> <td></td> <td>26.5</td> <td>39.8</td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> <tr> <td></td> <td></td> <td></td> <td></td> <td>1.150</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> </tbody> </table>  |                      |                               |                       |   |                      |                 |                |      |                   | Analysen:  | CO <sub>2</sub>      | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub>        | CO        | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z         | N <sub>2</sub> -F | Litergewicht    | Sygas | 6.6           | 1.2  | 0.1 | 38.0                 | 48.6  | 0.3 | 6.4 |  | 6.3                    |        | Restgas | 2.50 | 0.3 | 0.1 | 23.3 | 36.7 | 4.6 | 10.0 | 1.00                | 9.90   |          |      |   |  |  | 26.5 | 39.8 |  |                     |        |              |      |   |  |  |  | 1.150 |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Analysen:  | CO <sub>2</sub>      | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub>        | CO  | H <sub>2</sub>       | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht   |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Sygas  | 6.6                  | 1.2                           | 0.1                   | 38.0  | 48.6                 | 0.3             | 6.4            |      | 6.3               |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Restgas  | 2.50                 | 0.3                           | 0.1                   | 23.3  | 36.7                 | 4.6             | 10.0           | 1.00 | 9.90              |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
|  |                      |                               |                       | 26.5  | 39.8                 |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
|  |                      |                               |                       | 1.150   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Gesamt-Inerte (Idealgas) 13.11 %   |                      |                               |                       | Kontraktion nach Menge 4.10 %   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| H <sub>2</sub> :CO im Sygas 1.42   |                      |                               |                       | " " " N <sub>2</sub> 36.5 %   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| H <sub>2</sub> :CO im Restgas  |                      |                               |                       | " " " CO <sub>2</sub> %   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Verbrauch von H <sub>2</sub> :CO 1.08  |                      |                               |                       | Durchschnittliche Kontraktion %   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| <table style="width:100%;"> <tr> <td></td> <td style="text-align: center;">% CO</td> <td style="text-align: center;">% H<sub>2</sub></td> <td style="text-align: center;">% CO + H<sub>2</sub></td> </tr> <tr> <td>umgesetzt</td> <td style="text-align: center;">6.11</td> <td style="text-align: center;">4.10</td> <td style="text-align: center;">10.21</td> </tr> <tr> <td>verflüssigt</td> <td style="text-align: center;">2.87</td> <td style="text-align: center;">1.15</td> <td style="text-align: center;">4.02</td> </tr> <tr> <td>Verfl.-Grad A</td> <td style="text-align: center;">45.7</td> <td></td> <td></td> </tr> <tr> <td>" " P</td> <td></td> <td></td> <td></td> </tr> </table>  |                      |                               |                       |   |                      |                 |                |      |                   |  | % CO                 | % H <sub>2</sub>              | % CO + H <sub>2</sub> | umgesetzt | 6.11           | 4.10            | 10.21          | verflüssigt | 2.87              | 1.15            | 4.02  | Verfl.-Grad A | 45.7 |     |                      | " " P |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
|  | % CO                 | % H <sub>2</sub>              | % CO + H <sub>2</sub> |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| umgesetzt  | 6.11                 | 4.10                          | 10.21                 |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| verflüssigt  | 2.87                 | 1.15                          | 4.02                  |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Verfl.-Grad A  | 45.7                 |                               |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| " " P  |                      |                               |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| <table style="width:100%;"> <tr> <td>CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 11.6</td> <td>CO<sub>2</sub> 3.97</td> <td colspan="8">bezogen auf CO-Umsatz</td> </tr> <tr> <td colspan="5"><b>Produkte</b></td> <td colspan="5"><b>Gesamtprodukt</b></td> </tr> <tr> <td>Paraffingatsch 2.42 kg</td> <td>16.4 %</td> <td>SB</td> <td>37</td> <td>°C</td> <td colspan="5"></td> </tr> <tr> <td>Öl-Kondensat 7.40 "</td> <td>49.8 %</td> <td>- 200 °C</td> <td>22.4</td> <td>%</td> <td colspan="5"></td> </tr> <tr> <td>A.-K. Benzin 5.00 "</td> <td>33.8 %</td> <td>200 - 320 °C</td> <td>19.6</td> <td>%</td> <td colspan="5"></td> </tr> <tr> <td>Flüssige Prod. 14.82 "</td> <td>100 %</td> <td>&gt; 320 °C</td> <td></td> <td>%</td> <td colspan="5"></td> </tr> <tr> <td>Sywasser 21.90 kg = 1.2 x flüss. Produkte</td> <td></td> <td>Olefine</td> <td></td> <td>Vol. %</td> <td colspan="5"></td> </tr> <tr> <td></td> <td></td> <td>- 200° ; 200-320°</td> <td>5.8</td> <td></td> <td colspan="5"></td> </tr> </table> |                      |                               |                       |   |                      |                 |                |      |                   | CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub> 11.6 | CO <sub>2</sub> 3.97 | bezogen auf CO-Umsatz         |                       |           |                |                 |                |             |                   | <b>Produkte</b> |       |               |      |     | <b>Gesamtprodukt</b> |       |     |     |  | Paraffingatsch 2.42 kg | 16.4 % | SB      | 37   | °C  |     |      |      |     |      | Öl-Kondensat 7.40 " | 49.8 % | - 200 °C | 22.4 | % |  |  |      |      |  | A.-K. Benzin 5.00 " | 33.8 % | 200 - 320 °C | 19.6 | % |  |  |  |       |  | Flüssige Prod. 14.82 " | 100 % | > 320 °C |  | % |  |  |  |  |  | Sywasser 21.90 kg = 1.2 x flüss. Produkte |  | Olefine |  | Vol. % |  |  |  |  |  |  |  | - 200° ; 200-320° | 5.8 |  |  |  |  |  |  |
| CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub> 11.6   | CO <sub>2</sub> 3.97 | bezogen auf CO-Umsatz         |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| <b>Produkte</b>  |                      |                               |                       |   | <b>Gesamtprodukt</b> |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Paraffingatsch 2.42 kg   | 16.4 %               | SB                            | 37                    | °C  |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Öl-Kondensat 7.40 "  | 49.8 %               | - 200 °C                      | 22.4                  | %   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| A.-K. Benzin 5.00 "  | 33.8 %               | 200 - 320 °C                  | 19.6                  | %   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Flüssige Prod. 14.82 "   | 100 %                | > 320 °C                      |                       | %   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Sywasser 21.90 kg = 1.2 x flüss. Produkte  |                      | Olefine                       |                       | Vol. %  |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
|  |                      | - 200° ; 200-320°             | 5.8                   |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| <b>Ausbeule</b>  |                      |                               |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Flüssige Prod. 48.1 g/Nm³ Sygas 7.5 g/Nm³ Nützgas 7.5 g/Nm³ Idealgas   |                      |                               |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Gasöl " " " " " "  |                      |                               |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Gesamt-Produkt " " " " " "   |                      |                               |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| Sywasser 71.2 " " 82.3 " " " "   |                      |                               |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |
| <b>Bemerkungen:</b>  |                      |                               |                       |   |                      |                 |                |      |                   |  |                      |                               |                       |           |                |                 |                |             |                   |                 |       |               |      |     |                      |       |     |     |  |                        |        |         |      |     |     |      |      |     |      |                     |        |          |      |   |  |  |      |      |  |                     |        |              |      |   |  |  |  |       |  |                        |       |          |  |   |  |  |  |  |  |   |  |         |  |        |  |  |  |  |  |  |  |                   |     |  |  |  |  |  |  |

000156































**Druckversuchsanlage**

**Produktionsbericht vom** 29/30.10. 1943

Ofen-Nr. 11  
 Füllung: 13  
 Fe-Fe-Inhalt: - kg

Betriebsstunden 20/39.40  
 Gasdruck 25.0 atü  
 Temperatur 25.0 atü 225 °C

W-Gas 354 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
 " 12.4 Nm<sup>3</sup>/h

Restgas 149 Nm<sup>3</sup>  
 " 4.15 Nm<sup>3</sup>/h  
 Kreislaufgas 665 Nm<sup>3</sup>  
 Kreislauf 8.62

Belastung - Nm<sup>3</sup>/kg.h 1.00 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                      | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|--------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas                          | 6.5             | -    | 0.1            | 38.7 | 49.0           | 0.3             | 5.4            | -    | 5.30              |              |
| Restgas                        | 26.8            | 0.3  | 0.1            | 22.2 | 36.4           | 4.8             | 9.4            | 1.09 | 9.30              |              |
| Amalgam                        |                 |      |                | 26.8 | 39.9           |                 |                |      |                   |              |
| H <sub>2</sub> im Kreislaufgas |                 |      |                |      | 1.49           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 12.3 %  
 H<sub>2</sub>:CO im Sygas 1.27  
 H<sub>2</sub>:CO im Restgas 1.64  
 Verbrauch von H<sub>2</sub>:CO 1.07

Kontraktion nach Menge 0.4 %  
 " " N<sub>2</sub> 0.5 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 0.9 %

|               | %CO         | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|---------------|-------------|-----------------|--------------------|
| umgesetzt     | <u>66.1</u> | <u>56.1</u>     | <u>60.5</u>        |
| verflüssigt   |             |                 |                    |
| Verfl.-Grad A |             |                 |                    |
| " " P         |             |                 | <u>36.2</u>        |

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 9.9 CO<sub>2</sub> 36.5 bezogen auf CO-Umsatz

**Produkte**

|                |   |               |
|----------------|---|---------------|
| Paraffingatsch | <u>3.70</u> kg                                  | <u>15.3</u> % |
| Ol-Kondensat   | <u>7.00</u> "                                   | <u>51.1</u> % |
| A.-K. Benzin   | <u>4.60</u> "                                   | <u>33.6</u> % |
| Flüssige Prod. | <u>15.70</u> "                                  | 100 %         |
| Sywasser       | <u>19.00</u> kg = <u>1.39</u> x flüss. Produkte |               |

**Gesamtprodukt**

|         |              |
|---------|--------------|
| SB      | °C           |
| - 100°  | %            |
| - 200°  | %            |
| - 320°  | %            |
| Olefine | Vol. %       |
| - 200°  | ; 200 - 320° |

**Ausbeute**

|                |                                     |  |                            |
|----------------|-------------------------------------|--|----------------------------|
| Flüssige Prod. | <u>54.0</u> g Nm <sup>3</sup> Sygas | <u>61.6</u> g Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) | g/Nm <sup>3</sup> Idealgas |
| Gasol          | "                                   | "  | "                          |
| Gesamt-Produkt | "                                   | "  | "                          |
| Sywasser       | "                                   | "  | "                          |

**Bemerkungen:**  
 Die U 30 h Stillstand wegen Strom- u. Gasanfall  
 000170

# Druckversuchsanlage

Produktionsbericht vom 28./29.10. 1943

Ofen-Nr. 11  
 Füllung: 13.  
 Co-Fe-Inhalt: - kg

Betriebsstunden 24/3950  
 Gasdruck 20.2 atü  
 Temperatur 25.0 atü 225°C

Sy-W-Gas 293 Nm<sup>3</sup>  
 " " " " " "  
 " " " " " "  
 " 18.2 Nm<sup>3</sup>/h

Restgas 176 Nm<sup>3</sup>  
 " 7.3 Nm<sup>3</sup>/h  
 Kreislaufgas 714 Nm<sup>3</sup>  
 Kreislauf 2.44

Belastung - Nm<sup>3</sup>/kg.h 0.96 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                   | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht |
|-----------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|-----|-------------------|--------------|
| Sygas                       | 6.7             | -    | 0.1            | 37.9 | 49.4           | 0.7             | 5.6            | -   | 5.51              |              |
| Restgas                     | 25.1            | 0.3  | 0.1            | 22.2 | 38.8           | 4.8             | 9.5            | 109 | 9.44              |              |
| <i>Gasanalyse</i>           |                 |      |                | 26.8 | 41.3           |                 |                |     |                   |              |
| <i>H<sub>2</sub> 160 mm</i> |                 |      |                | 1.54 |                |                 |                |     |                   |              |

Gesamt-Inerte (Idealgas) 22.8 %  
 H<sub>2</sub>:CO im Sygas 1.30  
 H<sub>2</sub>:CO im Restgas 1.71  
 Verbrauch von H<sub>2</sub>:CO 1.07

Kontraktion nach Menge 40.1 %  
 " " N<sub>2</sub> 41.5 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 40.8 %

umgesetzt 66.8 %CO  
 verflüssigt 54.7 %H<sub>2</sub>  
 Verfl.-Grad A 1.00 %CO+H<sub>2</sub>  
 " " P 28.8

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 10.0 CO 32.3 bezogen auf CO-Umsatz

## Produkte

Paraffingösch 2.70 kg 19.3 %  
 Öl-Kondensat 6.60 " 47.1 %  
 A.-K. Benzin 4.70 " 33.6 %  
 Flüssige Prod. 14.00 100%  
 Sywasser 19.70 kg = 1.41 x flüss. Produkte

## Gesamtprodukt

S<sub>B</sub> - °C  
 - 100° - %  
 - 200° - %  
 - 320° - %  
 Olefine Vol. %  
 - 200° - , 200-320° -

## Ausbeute

Flüssige Prod. 44.8 g Nm<sup>3</sup> Sygas 54.7 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

000171



**Druckversuchsanlage** **Produktionsbericht vom 26./27. 10 1942**

Ofen-Nr. 11  
 Füllung: 13  
 Go-Fe-Inhalt: — kg

Betriebsstunden 24/3902  
 Gasdruck 20,0 atü  
 Temperatur 25,0 atü 225 °C

Sy-W-Gas 317 Nm<sup>3</sup>  
 Restgas 19,3 Nm<sup>3</sup>  
 " 8,1 Nm<sup>3</sup>/h  
 Kreislaufgas 794 Nm<sup>3</sup>  
 " 13,2 Nm<sup>3</sup>/h  
 Kreislauf 9,50

Belastung — Nm<sup>3</sup>/kg,h 1,04 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                      | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|--------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas                          | 6,6             | —                             | 0,1            | 38,3 | 48,8           | 0,3             | 5,9            | —    | 5,82              |              |
| Restgas                        | 26,1            | 0,4                           | 0,1            | 22,1 | 36,4           | 4,7             | 10,2           | 1,09 | 10,07             |              |
| Kreislaufgas                   |                 |                               |                | 26,8 | 40,0           |                 |                |      |                   |              |
| H <sub>2</sub> im Kreislaufgas |                 |                               |                | 1,49 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 12,9 %  
 H<sub>2</sub>, CO im Sygas 1,28  
 H<sub>2</sub>, CO im Restgas 1,65  
 Verbrauch von H<sub>2</sub>: CO 1,08

Kontraktion nach Menge 39,4 %  
 " " N<sub>2</sub> 42,4 %  
 " " CO<sub>2</sub> — %  
 Durchschnittliche Kontraktion 40,7 %

umgesetzt 65,8 %CO  
 verflüssigt —  
 Verfl.-Grad A —  
 " " P 29,2

9,9 CH<sub>4</sub> + 35,3 CO<sub>2</sub> bezogen auf CO-Umsatz

| Produkte       |   |               | Gesamtprodukt |            |
|----------------|---|---------------|---------------|------------|
| Paraffingatsch | <u>3,30</u> kg                                  | <u>20,8</u> % | SB            | °C         |
| Ol-Kondensat   | <u>7,70</u> "                                   | <u>50,4</u> % | — 100°        | %          |
| A.-K. Benzin   | <u>4,40</u> "                                   | <u>28,8</u> % | — 200°        | %          |
| Flüssige Prod. | <u>15,30</u>                                    | 100%          | — 320°        | %          |
| Sywasser       | <u>20,30</u> kg = <u>1,33</u> x flüss. Produkte |               | Olefine       | Vol. %     |
|                |   |               | — 200°        | 200 - 320° |

**Ausbeute**

Flüssige Prod. 48,2 g Nm<sup>3</sup> Sygas 55,3 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " " " " " " " "  
 Gesamt-Produkt " " " " " " " " " " " "  
 Sywasser " " " " " " " " " " " "

**Bemerkungen:**

**000173**



**Druckversuchsanlage**

**Produktionsbericht vom** 24/25.10. 1949

Ofen-Nr. 11  
 Füllung: 13  
 G-Fe-Inhalt: \_\_\_\_\_ kg

Betriebsstunden 24/3854  
 Gasdruck 25.0 atü  
 Temperatur 25.0 atü 225 °C

S-W-Gas 333 Nm<sup>3</sup>  
 " " " " " "  
 " " " " " "  
 " " " " " "  
13.9 Nm<sup>3</sup>/h

Restgas 18.2 Nm<sup>3</sup>  
 " " " " " "  
 " " " " " "  
 Kreislaufgas 805 Nm<sup>3</sup>  
 Kreislauf 2.42

Belastung: \_\_\_\_\_ Nm<sup>3</sup> / kg, h 1.09 Nm<sup>3</sup> / Norm.-Vol., h

| Analysen:                     | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas                         | 5.9             | -                             | 0.1            | 39.1 | 48.9           | 0.3             | 5.7            | -    | 5.63              |              |
| Restgas                       | 25.4            | 0.4                           | 0.1            | 23.4 | 36.6           | 4.6             | 9.5            | 1.08 | 9.32              |              |
| <i>Restgas</i>                |                 |                               |                | 28.0 | 40.2           |                 |                |      |                   |              |
| <i>H<sub>2</sub> 1.60 min</i> |                 |                               |                |      |                |                 |                |      |                   |              |
| <i>Andris 1.60 min</i>        |                 |                               |                |      |                |                 |                |      |                   |              |
|                               |                 |                               |                | 1.44 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 12.0 %  
 H<sub>2</sub>: CO im Sygas 1.25  
 H<sub>2</sub>: CO im Restgas 1.56  
 Verbrauch von H<sub>2</sub>: CO 1.04

Kontraktion nach Menge 39.7 %  
 " " N<sub>2</sub> 39.5 %  
 " " CO<sub>2</sub> \_\_\_\_\_ %  
 Durchschnittliche Kontraktion 34.6 %

|               |             |                 |                    |
|---------------|-------------|-----------------|--------------------|
| umgesetzt     | %CO         | %H <sub>2</sub> | %CO+H <sub>2</sub> |
| verflüssigt   | <u>63.9</u> | <u>54.8</u>     | <u>58.9</u>        |
| Verfl.-Grad A | _____       | _____           | _____              |
| " " P         | _____       | _____           | <u>30.4</u>        |

CH<sub>4</sub> + C<sub>2</sub>H<sub>4</sub> 9.9 CO<sub>2</sub> 34.6 bezogen auf CO-Umsatz

**Produkte**

|                |              |                  |             |                   |
|----------------|--------------|------------------|-------------|-------------------|
| Paraffingatsch | <u>3.30</u>  | kg               | <u>19.9</u> | %                 |
| Ol-Kondensat   | <u>7.42</u>  | "                | <u>44.6</u> | %                 |
| A-K. Benzin    | <u>5.90</u>  | "                | <u>35.5</u> | %                 |
| Flüssige Prod. | <u>16.62</u> |                  |             | 100%              |
| Sywasser       | <u>24.00</u> | kg = <u>1.27</u> |             | × flüss. Produkte |

**Gesamtprodukt**

|         |            |
|---------|------------|
| SB      | °C         |
| - 100°  | %          |
| - 200°  | %          |
| - 320°  | %          |
| Olefine | Vol. %     |
| - 200°  | 200 - 320° |

**Ausbeute**

Flüssige Prod. 49.8 g Nm<sup>3</sup> Sygas 56.6 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g Nm<sup>3</sup> Idealgas  
 Gasol \_\_\_\_\_  
 Gesamt-Produkt \_\_\_\_\_  
 Sywasser \_\_\_\_\_

**Bemerkungen:**

000175









**Druckversuchsanlage**

**Produktionsbericht vom** 25.12.10.1949

Ofen-Nr. 10  
 Füllung: 13  
 Co-Fe-Inhalt: - kg

Betriebsstunden 24/3762  
 Gasdruck 20,6 atü  
 Temperatur 25,4 atü 225 °C

W-Gas 241 Nm<sup>3</sup>  
 " " " " " "  
 " " " " " "  
 " 12,5 Nm<sup>3</sup>/h

Restgas - Nm<sup>3</sup>  
 " " " " " "  
 Kreislaufgas 791 Nm<sup>3</sup>  
 Kreislauf 2,62

Belastung: - Nm<sup>3</sup>/kg,h 0,99 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                         | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litorgewicht |
|-----------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|-----|-------------------|--------------|
| Sygas                             | 6.2             | -                             | 0.1            | 38.8 | 48.9           | 0.3             | 5.7            | -   | 5.18              |              |
| Restgas                           | 28.7            | 0.4                           | 0.1            | 20.2 | 25.2           | 6.0             | 9.4            | 115 | 9.32              |              |
| H <sub>2</sub> CO im Kreislaufgas |                 |                               |                | 15.4 | 29.0           |                 |                |     |                   |              |
|                                   |                 |                               |                | 1.1  | 5.3            |                 |                |     |                   |              |

Gesamt-Inerte (Idealgas) 12,3 %  
 H<sub>2</sub>, CO im Sygas 1,26  
 H<sub>2</sub>, CO im Restgas 1,74  
 Verbrauch von H<sub>2</sub>, CO 1,04

Kontraktion nach Menge - %  
 " " N<sub>2</sub> 29,5 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 29,5 %

umgesetzt 68,6 %CO 56,5 %H<sub>2</sub> 1,8 %CO+H<sub>2</sub>  
 verflüssigt -  
 Verfl.-Grad A -  
 " " P 30,8

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 12,5 CO<sub>2</sub> 48,0 bezogen auf CO-Umsatz

**Produkte**

Paraffingatsch 2,85 kg 18,0 %  
 Öl-Kondensat 7,40 " 46,7 %  
 A.-K. Benzin 5,50 " 35,3 %  
 Flüssige Prod. 15,85 " 100 %  
 Sywasser 20,0 kg = 1,26 × flüss. Produkte

**Gesamtprodukt**

SB - °C  
 - 100° - %  
 - 200° - %  
 - 320° - %  
 Olefine Vol. %  
 - 200° - ; 200 - 320° -

**Ausbeute**

Flüssige Prod. 52,7 g Nm<sup>3</sup> Sygas 60,0 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) - g Nm<sup>3</sup> Idealgas  
 Gasöl - " " " " " "  
 Gesamt-Produkt - " " " " " "  
 Sywasser - " " " " " "

**Bemerkungen:**

000179



# Druckversuchsanlage

Produktionsbericht vom 18/09. 10. 1943

Ofen-Nr. 11

Betriebsstunden 24/3715

Füllung: 13.

Gasdruck 30 atü

Co-Fe-Inhalt: — kg

Temperatur 25.8 atü 225 °C

Sp-W-Gas 309 Nm³

Restgas 168 Nm³

— Nm³/h

— Nm³/h

16.9 Nm³/h

Kreislaufgas 757 Nm³

Kreislauf 2.42

Belastung: — Nm³/kg.h 1.01 Nm³/Norm.-Vol., h

| Analysen:                 | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|---------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas                     | 6.2             | —    | 0.1            | 39.3 | 49.4           | 0.3             | 4.7            | —    | 4.60              |              |
| Restgas                   | 29.1            | 0.4  | 0.1            | 20.2 | 15.6           | 6.0             | 8.5            | 1.09 | 8.40              |              |
| Amalgam                   |                 |      |                | 25.8 | 29.1.6         |                 |                |      |                   |              |
| H <sub>2</sub> 1.60 mm Hg |                 |      |                |      | 1.53           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 11.3 %  
 H<sub>2</sub>, CO im Sygas 1.26  
 H<sub>2</sub>, CO im Restgas 1.75  
 Verbrauch von H<sub>2</sub>: CO 1.05

Kontraktion nach Menge 44.2 %  
 " " N<sub>2</sub> 45.2 %  
 " " CO<sub>2</sub> — %  
 Durchschnittliche Kontraktion 44.2 %

umgesetzt  $\frac{\%CO}{41.5}$   $\frac{\%H_2}{60.0}$   $\frac{\%CO+H_2}{65.0}$   
 verflüssigt \_\_\_\_\_  
 Verfl.-Grad A \_\_\_\_\_  
 " " P \_\_\_\_\_ 29.4

CH<sub>4</sub> + ~~CO~~ 10.8 CO<sub>2</sub> 35.2 bezogen auf CO-Umsatz

## Produkte

## Gesamtprodukt

Paraffingasch 2.79 kg 16.8 %  
 Öl-Kondensat 8.40 " 50.6 %  
 A.-K. Benzin 5.40 " 32.6 %  
 Flüssige Prod. 16.59 " 100 %  
 Sywasser 21.40 kg = 1.27 × flüss. Produkte

SB \_\_\_\_\_ °C  
 — 100° \_\_\_\_\_ %  
 — 200° \_\_\_\_\_ %  
 — 320° \_\_\_\_\_ %  
 Olefine Vol. %  
 — 200° \_\_\_\_\_ ; 200-320° \_\_\_\_\_

## Ausbeute

Flüssige Prod. 53.6 g Nm³ Sygas 60.5 g Nm³ Nutzgas (CO+H<sub>2</sub>) g Nm³ Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

000181

# Druckversuchsanlage

Versuchsbericht vom 17/11 10 1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt / kg

Betriebsstunden 24/3691  
 Gasdruck 20,0 atü  
 Temperatur 25,0 atü 225 °C

Sy-W-Gas 309 Nm<sup>3</sup>  
 " " " "  
 " " " "  
 " 12,9 Nm<sup>3</sup>/h

Restgas 172 Nm<sup>3</sup>  
 " 4,2 Nm<sup>3</sup>/h  
 Kreislaufgas 727 Nm<sup>3</sup>  
 Kreislauf 2,35 Nm<sup>3</sup>

## Belastung

Nm<sup>3</sup>/kg,h 1,02

Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:        | Nm <sup>3</sup> /kg,h |                               |                |      |                |                 |                |      | Nm <sup>3</sup> /Norm.-Vol., h |              |  |
|------------------|-----------------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|--------------------------------|--------------|--|
|                  | CO <sub>2</sub>       | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F              | Litergewicht |  |
| Sygas            | 6,1                   | /                             | 0,1            | 39,1 | 49,9           | 0,3             | 4,5            | /    | 4,43                           |              |  |
| Restgas          | 29,6                  | 0,4                           | 0,1            | 19,9 | 36,0           | 6,1             | 7,9            | 1,13 | 7,87                           |              |  |
| <i>Spurengas</i> |                       |                               |                | 25,6 | 40,2           |                 |                |      |                                |              |  |
| <i>Halbes</i>    |                       |                               |                |      | 1,57           |                 |                |      |                                |              |  |

Gesamt-Inerte (Idealgas) 11,0 %  
 H<sub>2</sub>:CO im Sygas 1,28  
 H<sub>2</sub>:CO im Restgas 1,81  
 Verbrauch von H<sub>2</sub>:CO 1,06

Kontraktion nach Menge 44,4 %  
 " " N<sub>2</sub> 44,0 %  
 " " CO<sub>2</sub> / %  
 Durchschnittliche Kontraktion 44,0 %

umgesetzt 71,6 % CO  
 verflüssigt 59,7 % H<sub>2</sub>  
 Verfl.-Grad A 65,0 % CO + H<sub>2</sub>  
 " " P 27,6

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 11,1 CO<sub>2</sub> 34,3 bezogen auf CO-Umsatz

## Produkte

Paraffingasch 2,80 kg 14,9 %  
 Öl-Kondensat 7,70 " 40,3 %  
 A.-K. Benzin 5,10 " 26,8 %  
 Flüssige Prod. 15,60 " 100 %  
 Sywasser 20,20 kg = 1,30 × flüss. Produkte

## Gesamtprodukt

SB °C  
 - 200 °C %  
 200 - 320 °C %  
 > 320 °C %  
 Olefine Vol. %  
 - 200° ; 200-320°

## Ausbeute:

Flüssige Prod. 50,5 g/Nm<sup>3</sup> Sygas 56,8 g/Nm<sup>3</sup> Nutzgas (CO + H<sub>2</sub>)  
 Gasol " " " " g/Nm<sup>3</sup> Idealgas  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

000182

|  |       |             |                   |                       |                                      |        |     |      |     |              |
|--|-------|-------------|-------------------|-----------------------|--------------------------------------|--------|-----|------|-----|--------------|
| <b>Druckversuchsanlage</b>                     |       |             |                   |                       | Versuchsbericht vom 16./17. 10. 1943 |        |     |      |     |              |
| Ofen-Nr. 11                                    |       |             |                   |                       | Betriebsstunden 24/3664              |        |     |      |     |              |
| Füllung: 13                                    |       |             |                   |                       | Gasdruck 20 atü                      |        |     |      |     |              |
| Co-Fe-Inhalt / kg                              |       |             |                   |                       | Temperatur 25 atü 225 °C             |        |     |      |     |              |
| Sy-W-Gas 305 Nm³                               |       |             |                   |                       | Restgas — Nm³                        |        |     |      |     |              |
| " " " "  |       |             |                   |                       | " " " " Nm³/h                        |        |     |      |     |              |
| " " " " 18,7 Nm³/h                             |       |             |                   |                       | Kreislaufgas 772 Nm³                 |        |     |      |     |              |
|  |       |             |                   |                       | Kreislauf 8,53                       |        |     |      |     |              |
| Belastung                                      |       |             |                   |                       | Nm³ / kg, h 1,00                     |        |     |      |     |              |
| Analysen:                                      |       |             |                   |                       |                                      |        |     |      |     |              |
|  | CO₂   | CmHn        | O₂                | CO                    | H₂                                   | CH₄    | N₂  | C-Z  | N-F | Litergewicht |
| W Sygas  | 5,8   | —           | 0,1               | 39,6                  | 49,2                                 | 0,3    | 5,0 | —    | 4,9 |              |
| Restgas  | 29,6  | 0,4         | 0,1               | 20,0                  | 35,0                                 | 6,1    | 8,8 | 1,13 | 8,7 |              |
| Arbeitsgas                                     |       |             |                   | 25,6                  | 39,0                                 |        |     |      |     |              |
| H₂ 160 mm                                      |       |             |                   | 1,52                  |                                      |        |     |      |     |              |
| Gesamt-Inerte (Idealgas) 11,2 %                |       |             |                   |                       |                                      |        |     |      |     |              |
| H₂:CO im Sygas 1,24                            |       |             |                   |                       | Kontraktion nach Menge — %           |        |     |      |     |              |
| H₂:CO im Restgas 1,75                          |       |             |                   |                       | " " N₂ 43,7 %                        |        |     |      |     |              |
| Verbrauch von H₂:CO 1,04                       |       |             |                   |                       | " " CO₂ — %                          |        |     |      |     |              |
|  |       |             |                   |                       | Durchschnittliche Kontraktion 43,7 % |        |     |      |     |              |
| umgesetzt % CO 71,5 % H₂ 60,0 % CO+H₂ 65,1     |       |             |                   |                       |                                      |        |     |      |     |              |
| verflüssigt —                                  |       |             |                   |                       |                                      |        |     |      |     |              |
| Verfl.-Grad A                                  |       |             |                   |                       |                                      |        |     |      |     |              |
| " " P 30,8                                     |       |             |                   |                       |                                      |        |     |      |     |              |
| CH₄ + C₂H₆ 11,1 CO₂ 38,4 bezogen auf CO-Umsatz |       |             |                   |                       |                                      |        |     |      |     |              |
| <b>Produkte</b>                                |       |             |                   |                       | <b>Gesamtprodukt</b>                 |        |     |      |     |              |
| Paraffingasch                                  | 2,95  | kg          | 14,2              | %                     | SB                                   | °C     |     |      |     |              |
| Ol-Kondensat                                   | 8,00  | "           | 46,0              | %                     | — 200 °C                             | %      |     |      |     |              |
| A.-K. Benzin                                   | 6,20  | "           | 36,2              | %                     | 200 — 320 °C                         | %      |     |      |     |              |
| Flüssige Prod.                                 | 17,15 | "           |                   | 100 %                 | > 320 °C                             | %      |     |      |     |              |
| Sywasser                                       | 20,50 | kg = 1,20   | × flüss. Produkte |                       | Olefine                              | Vol. % |     |      |     |              |
|  |       |             |                   |                       | — 200° ; 200-320°                    |        |     |      |     |              |
| <b>Ausbeute</b>                                |       |             |                   |                       |                                      |        |     |      |     |              |
| Flüssige Prod.                                 | 56,2  | g/Nm³ Sygas | 63,3              | g/Nm³ Nutzgas (CO+H₂) | g/Nm³ Idealgas                       |        |     |      |     |              |
| Gasol  | "     | "           | "                 | "                     | "                                    |        |     |      |     |              |
| Gesamt-Produkt                                 | "     | "           | "                 | "                     | "                                    |        |     |      |     |              |
| Sywasser                                       | "     | "           | "                 | "                     | "                                    |        |     |      |     |              |
| <b>Bemerkungen:</b>                            |       |             |                   |                       |                                      |        |     |      |     |              |

000183

**Druckversuchsanlage** Produktionsbericht vom 15.11.10 1943

Ofen-Nr. 11  
 Füllung: 12  
 CO-Fe-Inhalt: - kg  
 Betriebsstunden: 24/3643  
 Gasdruck: 20 atü  
 Temperatur: 25.0 atü 235 °C

Sy-W-Gas: 303 Nm<sup>3</sup>  
 Restgas: - Nm<sup>3</sup>  
 Kreislaufgas: 274 Nm<sup>3</sup>  
 Kreislauf: 2,55  
 " " " " 12,6 Nm<sup>3</sup>/h

Belastung: 0,99 Nm<sup>3</sup>/kg.h

| Analysen:                         | Nm <sup>3</sup> /Nörm.-Vol., h |      |                |      |                |                 |                |      |                   |              |
|-----------------------------------|--------------------------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
|                                   | CO <sub>2</sub>                | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
| Sygas                             | 5,8                            | -    | 0,1            | 39,5 | 49,4           | 0,3             | 4,9            | -    | 4,81              |              |
| Restgas                           | 29,2                           | 0,4  | 0,1            | 20,3 | 35,4           | 6,1             | 8,5            | 1,15 | 8,45              |              |
| Analysen                          |                                |      |                | 25,8 | 39,4           |                 |                |      |                   |              |
| H <sub>2</sub> CO im Kreislaufgas |                                |      |                | 1,53 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 11,1 %  
 H<sub>2</sub>:CO im Sygas 1,25  
 H<sub>2</sub>:CO im Restgas 1,44  
 Verbrauch von H<sub>2</sub>:CO 1,05  
 Kontraktion nach Menge - %  
 " " N<sub>2</sub> 43,3 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 43,3 %

umgesetzt 40,9 %CO  
 verflüssigt 59,6 %H<sub>2</sub>  
 Verfl.-Grad A 64,6 %CO+H<sub>2</sub>  
 " " P 35,2

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 11,1 CO<sub>2</sub> 38,4 bezogen auf CO-Umsatz

| Produkte       |   | Gesamtprodukt |          |
|----------------|---|---------------|----------|
| Paraffingatsch | <u>4,75</u> kg                                  | <u>24,6</u>   | %        |
| Ol-Kondensat   | <u>8,40</u> "                                   | <u>43,4</u>   | %        |
| A.-K. Benzin   | <u>6,30</u> "                                   | <u>38,0</u>   | %        |
| Flüssige Prod. | <u>19,35</u> "                                  |               | 100%     |
| Sywasser       | <u>22,10</u> kg = <u>1,14</u> × flüss. Produkte |               |          |
|                |   | SB            | °C       |
|                |   | - 100°        | %        |
|                |   | - 200°        | %        |
|                |   | - 320°        | %        |
|                |   | Olefine       | Vol. %   |
|                |   | - 200°        | 200-320° |

**Ausbeute**  
 Flüssige Prod. 63,9 g Nm<sup>3</sup> Sygas 41,9 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>)  
 Gasol " " " " " " " " " " " "  
 Gesamt-Produkt " " " " " " " " " " " "  
 Sywasser " " " " " " " " " " " "

**Bemerkungen:**

000184



|  |  |                               |                             |             |  |                 |                |             |                   |              |  |
|--|--|-------------------------------|-----------------------------|-------------|--|-----------------|----------------|-------------|-------------------|--------------|--|
| <b>Druckversuchsanlage</b>   |  |                               |                             |             | <b>Produktionsbericht vom 14./15. 10. 1942</b> |                 |                |             |                   |              |  |
| Ofen-Nr. <u>11</u>   |  |                               |                             |             | Betriebsstunden <u>24/3619</u>                 |                 |                |             |                   |              |  |
| Füllung: <u>13</u>   |  |                               |                             |             | Gasdruck <u>20</u> atü                         |                 |                |             |                   |              |  |
| Co-Fe-Inhalt: _____ kg   |  |                               |                             |             | Temperatur <u>250</u> atü <u>325</u> °C        |                 |                |             |                   |              |  |
| Sy-W-Gas <u>333</u> Nm <sup>3</sup>                                    |  |                               |                             |             | Restgas <u>194</u> Nm <sup>3</sup>             |                 |                |             |                   |              |  |
| " " " " " "  |  |                               |                             |             | " " " " " " <u>13,9</u> Nm <sup>3</sup> /h     |                 |                |             |                   |              |  |
| " " " " " " <u>13,5</u> Nm <sup>3</sup> /h                             |  |                               |                             |             | Kreislaufgas <u>746</u> Nm <sup>3</sup>        |                 |                |             |                   |              |  |
| " " " " " " " "  |  |                               |                             |             | Kreislauf <u>2,31</u>                          |                 |                |             |                   |              |  |
| Belastung _____ Nm <sup>3</sup> /kg,h                                  |  |                               |                             |             | <u>1,00</u> Nm <sup>3</sup> /Norm.-Vol., h     |                 |                |             |                   |              |  |
| Analysen:  | CO <sub>2</sub>  | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub>              | CO          | H <sub>2</sub>                                 | CH <sub>4</sub> | N <sub>2</sub> | C-Z         | N <sub>2</sub> -F | Litorgewicht |  |
| Sygas  | <u>5,7</u>   | -                             | <u>0,1</u>                  | <u>39,6</u> | <u>49,5</u>                                    | <u>0,3</u>      | <u>4,8</u>     | -           | <u>11,74</u>      |              |  |
| Restgas  | <u>33,9</u>  | <u>0,4</u>                    | <u>0,1</u>                  | <u>25,3</u> | <u>37,7</u>                                    | <u>4,3</u>      | <u>8,8</u>     | <u>1,13</u> | <u>8,23</u>       |              |  |
| Phylgas  |  |                               |                             | <u>0,6</u>  | <u>41,3</u>                                    |                 |                |             |                   |              |  |
| H <sub>2</sub> O im Sygas  |  |                               |                             | <u>1,40</u> |  |                 |                |             |                   |              |  |
| Gesamt-Inerte (Idealgas)   | <u>10,9</u> %  |                               |                             |             | Kontraktion nach Menge <u>41,1</u> %           |                 |                |             |                   |              |  |
| H <sub>2</sub> CO im Sygas   | <u>1,25</u>  |                               |                             |             | " " N <sub>2</sub> <u>42,4</u> %               |                 |                |             |                   |              |  |
| H <sub>2</sub> CO im Restgas   | <u>1,49</u>  |                               |                             |             | " " CO <sub>2</sub> _____ %                    |                 |                |             |                   |              |  |
| Verbrauch von H <sub>2</sub> CO  | <u>1,10</u>  |                               |                             |             | Durchschnittliche Kontraktion <u>41,8</u> %    |                 |                |             |                   |              |  |
| umgesetzt  | %CO <u>63,0</u>  |                               | %H <sub>2</sub> <u>55,6</u> |             | %CO+H <sub>2</sub> <u>58,8</u>                 |                 |                |             |                   |              |  |
| verflüssigt  | _____  |                               | _____                       |             | _____  |                 |                |             |                   |              |  |
| Verfl.-Grad A  | _____  |                               | _____                       |             | _____  |                 |                |             |                   |              |  |
| " " P  | _____  |                               | _____                       |             | _____ <u>39,4</u>                              |                 |                |             |                   |              |  |
| CH <sub>4</sub> + C <sub>2</sub> H <sub>6</sub> <u>8,9</u>             | CO <sub>2</sub> <u>33,0</u>                                |                               |                             |             | bezogen auf CO-Umsatz                          |                 |                |             |                   |              |  |
| <b>Produkte</b>  |  |                               |                             |             | <b>Gesamtprodukt</b>                           |                 |                |             |                   |              |  |
| Paraffingatsch <u>3,20</u> kg  | <u>19,6</u> %  |                               |                             |             | SB _____ °C                                    |                 |                |             |                   |              |  |
| Ol-Kondensat <u>1,30</u> "   | <u>4,4</u> %   |                               |                             |             | - 100° _____ %                                 |                 |                |             |                   |              |  |
| A.-K. Benzin <u>5,70</u> "   | <u>33,0</u> %  |                               |                             |             | - 200° _____ %                                 |                 |                |             |                   |              |  |
| Flüssige Prod. <u>17,30</u> "  | 100 %  |                               |                             |             | - 320° _____ %                                 |                 |                |             |                   |              |  |
| Sywasser <u>33,00</u> kg = <u>1,27</u> x flüss. Produkte               |  |                               |                             |             | Olefine Vol. %                                 |                 |                |             |                   |              |  |
|  |  |                               |                             |             | - 200° _____ , 200-320° _____                  |                 |                |             |                   |              |  |
| <b>Ausbeute</b>  |  |                               |                             |             |  |                 |                |             |                   |              |  |
| Flüssige Prod. <u>53,6</u> g Nm <sup>3</sup> Sygas                     | <u>60,1</u> g Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) |                               |                             |             |  |                 |                |             |                   |              |  |
| Gasol _____ " " "  | " " "  |                               |                             |             |  |                 |                |             |                   |              |  |
| Gesamt-Produkt _____ " " "   | " " "  |                               |                             |             |  |                 |                |             |                   |              |  |
| Sywasser _____ " " "   | " " "  |                               |                             |             |  |                 |                |             |                   |              |  |
| <b>Bemerkungen:</b>  |  |                               |                             |             |  |                 |                |             |                   |              |  |
| <u>Stillstand von 9<sup>50</sup> - 10<sup>00</sup> wegen zu Feinm.</u> |  |                               |                             |             |  |                 |                |             |                   |              |  |
| <u>an Knappe. L (Kaminabfall)</u>                                      |  |                               |                             |             |  |                 |                |             |                   |              |  |
|  |  |                               |                             |             | <b>000185</b>                                  |                 |                |             |                   |              |  |

# Druckversuchsanlage

Produktionsbericht vom 13./14.10.1949

Ofen-Nr. 11

Füllung: 12.

Co-Fa-Inhalt: - kg

Betriebsstunden 24/3595

Gasdruck 20 atü

Temperatur 250 atü 225°C

Sp-W-Gas 213 Nm³

13.0 Nm³/h

Restgas 184 Nm³

7.5 Nm³/h

Kreislaufgas 846 Nm³

2.58 Nm³

Belastung: - Nm³/kg,h

| Analysen:            | Nm³ / Norm.-Vol., h |      |     |      |      |     |     |      |      |  | Litergewicht |
|----------------------|---------------------|------|-----|------|------|-----|-----|------|------|--|--------------|
|                      | CO₂                 | CmHn | O₂  | CO   | H₂   | CH₄ | N₂  | C-Z  | N₂-F |  |              |
| Sygas                | 6.1                 | -    | 0.1 | 39.0 | 49.8 | 0.3 | 4.7 | -    | 4.61 |  |              |
| Restgas              | 27.7                | 0.4  | 0.1 | 21.8 | 26.1 | 5.4 | 8.5 | 1.19 | 8.36 |  |              |
| Abfallgas            |                     |      |     | 26.0 | 40.0 |     |     |      |      |  |              |
| H₂CO im Kreislaufgas |                     |      |     | 1.50 |      |     |     |      |      |  |              |

Gesamt-Inerte (Idealgas) 11.2 %

H₂CO im Sygas 1.28

H₂CO im Restgas 1.66

Verbrauch von H₂CO 1.10

Kontraktion nach Menge 42.2 %

" " N₂ 44.9 %

" " CO₂ - %

Durchschnittliche Kontraktion 41.6 %

umgesetzt: %CO 68.5, %H₂ 59.0, %CO+H₂ 63.1

verflüssigt: -

Verfl.-Grad A: -

" " P: 32.0

CH₄ + CmHn 10.3, CO₂ 35.6 bezogen auf CO-Umsatz

## Produkte

|                |                                   |        |
|----------------|-----------------------------------|--------|
| Paraffingatsch | 3.45 kg                           | 19.4 % |
| Ol-Kondensat   | 8.60 "                            | 48.5 % |
| A.-K. Benzin   | 5.70 "                            | 33.1 % |
| Flüssige Prod. | 17.75 "                           | 100 %  |
| Sywasser       | 22.40 kg = 1.26 x flüss. Produkte |        |

## Gesamtprodukt

|         |            |
|---------|------------|
| - SB    | °C         |
| - 100°  | %          |
| - 200°  | %          |
| - 320°  | %          |
| Olefine | Vol. %     |
| - 200°  | ; 200-320° |

## Ausbeute

|                |                  |                            |                |
|----------------|------------------|----------------------------|----------------|
| Flüssige Prod. | 56.7 g Nm³ Sygas | 63.8 g Nm³ Nutzgas (CO+H₂) | g/Nm³ Idealgas |
| Gasol          | " "              | " "                        | " "            |
| Gesamt-Produkt | " "              | " "                        | " "            |
| Sywasser       | " "              | " "                        | " "            |

## Bemerkungen:

000186





|   |                 |                                    |                             |  |   |                      |                |            |                   |              |
|---|-----------------|------------------------------------|-----------------------------|--|---|----------------------|----------------|------------|-------------------|--------------|
| <b>Druckversuchsanlage</b>                      |                 |                                    |                             | Versuchsbericht vom <u>10/11 10</u> 19 <u>43</u> |   |                      |                |            |                   |              |
| Ofen-Nr. <u>11</u>                              |                 |                                    |                             | Betriebsstunden <u>24/35 83</u>                  |   |                      |                |            |                   |              |
| Füllung: <u>13</u>                              |                 |                                    |                             | Gasdruck <u>20</u> atü                           |   |                      |                |            |                   |              |
| Co-Fe-Inhalt <u>-</u> kg                        |                 |                                    |                             | Temperatur <u>25</u> atü <u>25</u> °C            |   |                      |                |            |                   |              |
| Sy-W-Gas <u>324</u> Nm <sup>3</sup>             |                 |                                    |                             | Restgas <u>180</u> Nm <sup>3</sup>               |   |                      |                |            |                   |              |
| " " " "   |                 |                                    |                             | " <u>4,5</u> Nm <sup>3</sup> /h                  |   |                      |                |            |                   |              |
| " " " "   |                 |                                    |                             | Kreislaufgas <u>742</u> Nm <sup>3</sup>          |   |                      |                |            |                   |              |
| " <u>13,5</u> Nm <sup>3</sup> /h                |                 |                                    |                             | Kreislauf <u>2,29</u>                            |   |                      |                |            |                   |              |
| Belastung <u>-</u> Nm <sup>3</sup> /kg,h        |                 |                                    |                             | <u>1,06</u> Nm <sup>3</sup> /Norm.-Vol., h       |   |                      |                |            |                   |              |
| Analysen:                                       | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub>      | O <sub>2</sub>              | CO   | H <sub>2</sub>                                  | CH <sub>4</sub>      | N <sub>2</sub> | C-Z        | N <sub>2</sub> -F | Litergewicht |
| W Sygas   | <u>27,6</u>     | <u>0,4</u>                         | <u>0,1</u>                  | <u>38,8</u>                                      | <u>48,9</u>                                     | <u>0,3</u>           | <u>5,9</u>     | <u>✓</u>   | <u>58,5</u>       |              |
| Restgas   | <u>27,6</u>     | <u>0,4</u>                         | <u>0,1</u>                  | <u>20,7</u>                                      | <u>35,1</u>                                     | <u>5,7</u>           | <u>10,4</u>    | <u>115</u> | <u>102,6</u>      |              |
| <i>Handwritten note: 26,2 39,4 1,50</i>         |                 |                                    |                             |  |   |                      |                |            |                   |              |
| Gesamt-Inerte (Idealgas) <u>10,3</u> %          |                 |                                    |                             | Kontraktion nach Menge <u>44,5</u> %             |   |                      |                |            |                   |              |
| H <sub>2</sub> :CO im Sygas <u>1,26</u>         |                 |                                    |                             | " " N <sub>2</sub> <u>43,0</u> %                 |   |                      |                |            |                   |              |
| H <sub>2</sub> :CO im Restgas <u>1,40</u>       |                 |                                    |                             | " " CO <sub>2</sub> <u>✓</u> %                   |   |                      |                |            |                   |              |
| Verbrauch von H <sub>2</sub> :CO <u>1,04</u>    |                 |                                    |                             | Durchschnittliche Kontraktion <u>43,8</u> %      |   |                      |                |            |                   |              |
| umgesetzt                                       |                 | % CO                               | % H <sub>2</sub>            |  | % CO+H <sub>2</sub>                             |                      |                |            |                   |              |
| verflüssigt                                     |                 | <u>40,1</u>                        | <u>59,7</u>                 |  | <u>64,3</u>                                     |                      |                |            |                   |              |
| Verfl.-Grad A                                   |                 |                                    |                             |  |   |                      |                |            |                   |              |
| " " P   |                 |                                    |                             |  | <u>31,0</u>                                     |                      |                |            |                   |              |
| CH <sub>4</sub> + C <sub>2</sub> H <sub>6</sub> |                 | <u>10,4</u>                        | CO <sub>2</sub> <u>34,9</u> |  | bezogen auf CO-Umsatz                           |                      |                |            |                   |              |
| <b>Produkte</b>                                 |                 |                                    |                             |  |   | <b>Gesamtprodukt</b> |                |            |                   |              |
| Paraffingatsch                                  | <u>3,20</u>     | kg                                 | <u>14,9</u>                 | %  | SB  | °C                   |                |            |                   |              |
| Öl-Kondensat                                    | <u>3,70</u>     | "                                  | <u>48,6</u>                 | %  | <u>- 200 °C</u>                                 | %                    |                |            |                   |              |
| A.-K. Benzin                                    | <u>6,00</u>     | "                                  | <u>38,5</u>                 | %  | <u>200 - 320 °C</u>                             | %                    |                |            |                   |              |
| Flüssige Prod.                                  | <u>7,90</u>     | "                                  |                             | 100 %  | <u>&gt; 320 °C</u>                              | %                    |                |            |                   |              |
| Sywasser  | <u>20,70</u>    | kg = <u>1,16</u> × flüss. Produkte |                             |  | Olefine   | Vol. %               |                |            |                   |              |
|   |                 |                                    |                             |  | <u>- 200°</u>                                   | <u>; 200-320°</u>    |                |            |                   |              |
| <b>Ausbeute</b>                                 |                 |                                    |                             |  |   |                      |                |            |                   |              |
| Flüssige Prod.                                  | <u>55,3</u>     | g/Nm <sup>3</sup> Sygas            | <u>63,0</u>                 | g/Nm <sup>3</sup> Nutzgas                        | (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> Idealgas |                      |                |            |                   |              |
| Gasol   | "               | "                                  | "                           | "  | " "   |                      |                |            |                   |              |
| Gesamt-Produkt                                  | "               | "                                  | "                           | "  | " "   |                      |                |            |                   |              |
| Sywasser  | "               | "                                  | "                           | "  | " "   |                      |                |            |                   |              |
| <b>Bemerkungen:</b>                             |                 |                                    |                             |  |   |                      |                |            |                   |              |

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|   |                 |                               |                   |                                    |   |                 |                |             |                   |              |
|---|-----------------|-------------------------------|-------------------|------------------------------------|---|-----------------|----------------|-------------|-------------------|--------------|
| <b>Druckversuchsanlage</b>  |                 |                               |                   |                                    | Versuchsbericht vom <u>9/10 10</u> 194 <u>3</u> |                 |                |             |                   |              |
| Ofen-Nr. <u>11</u>  |                 |                               |                   |                                    | Betriebsstunden <u>24/3449</u>                  |                 |                |             |                   |              |
| Füllung: <u>13</u>  |                 |                               |                   |                                    | Gasdruck <u>20</u> atü                          |                 |                |             |                   |              |
| Co-Fe-Inhalt _____ kg   |                 |                               |                   |                                    | Temperatur <u>25</u> atü <u>225</u> °C          |                 |                |             |                   |              |
| Sy-W-Gas <u>1315</u> Nm³  |                 |                               |                   |                                    | Restgas <u>191</u> Nm³                          |                 |                |             |                   |              |
| " " " "   |                 |                               |                   |                                    | " <u>8,0</u> Nm³/h                              |                 |                |             |                   |              |
| " <u>13,1</u> Nm³/h   |                 |                               |                   |                                    | Kreislaufgas <u>804</u> Nm³                     |                 |                |             |                   |              |
| " " " "   |                 |                               |                   |                                    | Kreislauf <u>2,55</u>                           |                 |                |             |                   |              |
| Belastung _____   |                 |                               |                   |                                    | Nm³/kg.h <u>1,03</u>                            |                 |                |             |                   |              |
| Analysen:   |                 |                               |                   |                                    | Nm³/Norm.-Vol., h                               |                 |                |             |                   |              |
|   | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub>    | CO                                 | H <sub>2</sub>                                  | CH <sub>4</sub> | N <sub>2</sub> | C-Z         | N <sub>2</sub> -F | Litergewicht |
| W Sygas   | <u>6,1</u>      | ✓                             | <u>0,1</u>        | <u>38,8</u>                        | <u>49,0</u>                                     | <u>0,3</u>      | <u>5,7</u>     | ✓           | <u>5,56</u>       |              |
| Restgas   | <u>26,5</u>     | <u>0,4</u>                    | <u>0,1</u>        | <u>22,3</u>                        | <u>36,0</u>                                     | <u>5,3</u>      | <u>9,4</u>     | <u>1,15</u> | <u>9,34</u>       |              |
| <i>Restgas</i>  |                 |                               |                   | <u>26,9</u>                        | <u>39,6</u>                                     |                 |                |             |                   |              |
| <i>H<sub>2</sub> 1,68 in Sygas</i>                                  |                 |                               |                   | <u>1,44</u>                        |   |                 |                |             |                   |              |
| Gesamt-Inerte (Idealgas) <u>12,1</u> %                              |                 |                               |                   |                                    | Kontraktion nach Menge <u>39,3</u> %            |                 |                |             |                   |              |
| H <sub>2</sub> :CO im Sygas <u>1,26</u>                             |                 |                               |                   |                                    | " " N <sub>2</sub> <u>40,5</u> %                |                 |                |             |                   |              |
| H <sub>2</sub> :CO im Restgas <u>1,62</u>                           |                 |                               |                   |                                    | " " CO <sub>2</sub> _____ %                     |                 |                |             |                   |              |
| Verbrauch von H <sub>2</sub> :CO <u>1,08</u>                        |                 |                               |                   |                                    | Durchschnittliche Kontraktion <u>39,9</u> %     |                 |                |             |                   |              |
| % CO  |                 |                               |                   |                                    | % H <sub>2</sub>                                |                 |                |             |                   |              |
| umgesetzt <u>65,5</u>   |                 |                               |                   |                                    | <u>56,0</u>                                     |                 |                |             |                   |              |
| verflüssigt   |                 |                               |                   |                                    | % CO+H <sub>2</sub> <u>60,2</u>                 |                 |                |             |                   |              |
| Verfl.-Grad A   |                 |                               |                   |                                    |   |                 |                |             |                   |              |
| " " P   |                 |                               |                   |                                    | <u>32,0</u>                                     |                 |                |             |                   |              |
| CH <sub>4</sub> + <u>24</u> <u>11,4</u> CO <sub>2</sub> <u>38,6</u> |                 |                               |                   |                                    | bezogen auf CO-Umsatz                           |                 |                |             |                   |              |
| <b>Produkte</b>   |                 |                               |                   |                                    | <b>Gesamprodukt</b>                             |                 |                |             |                   |              |
| Paraffingasch   | <u>2,50</u>     | kg                            | <u>14,9</u>       | %                                  | SB  | °C              |                |             |                   |              |
| Ol-Kondensat  | <u>9,10</u>     | "                             | <u>54,2</u>       | %                                  | — 200 °C  | %               |                |             |                   |              |
| A.-K. Benzin  | <u>5,20</u>     | "                             | <u>30,9</u>       | %                                  | 200 — 320 °C                                    | %               |                |             |                   |              |
| Flüssige Prod.  | <u>16,80</u>    | "                             |                   | 100 %                              | > 320 °C  | %               |                |             |                   |              |
| Sywasser  | <u>23,20</u>    | kg = <u>1,38</u>              | × flüss. Produkte |                                    | Olefine   | Vol. %          |                |             |                   |              |
|   |                 |                               |                   |                                    | — 200°  | ; 200-320°      |                |             |                   |              |
| <b>Ausbeute</b>   |                 |                               |                   |                                    |   |                 |                |             |                   |              |
| Flüssige Prod.  | <u>53,4</u>     | g/Nm³ Sygas                   | <u>60,8</u>       | g/Nm³ Nutzgas (CO+H <sub>2</sub> ) | g/Nm³ Idealgas                                  |                 |                |             |                   |              |
| Gasol   |                 | "                             |                   | "                                  | "   |                 |                |             |                   |              |
| Gesamt-Produkt  |                 | "                             |                   | "                                  | "   |                 |                |             |                   |              |
| Sywasser  |                 | "                             |                   | "                                  | "   |                 |                |             |                   |              |
| Bemerkungen:  |                 |                               |                   |                                    |   |                 |                |             |                   |              |

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# Druckversuchsanlage

Produktionsbericht vom 8/9/10 1933

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt: \_\_\_\_\_ kg

Betriebsstunden 24/3475  
 Gasdruck 20 atü  
 Temperatur 25.8 atü 325 °C

Sy-W-Gas 30.3 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
12.6 Nm<sup>3</sup>/h

Restgas 169 Nm<sup>3</sup>  
 " 4.1 Nm<sup>3</sup>/h  
 Kreislaufgas 29.3 Nm<sup>3</sup>  
 Kreislauf 2.62

Belastung \_\_\_\_\_ Nm<sup>3</sup>/kg.h 0.99 Nm<sup>3</sup>/Norm-Vol., h

| Analysen:                         | CO <sub>2</sub> | CmHn       | O <sub>2</sub> | CO          | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z         | N <sub>2</sub> -F | Litergewicht |
|-----------------------------------|-----------------|------------|----------------|-------------|----------------|-----------------|----------------|-------------|-------------------|--------------|
| Sygas                             | <u>6.4</u>      | -          | <u>0.1</u>     | <u>38.6</u> | <u>49.0</u>    | <u>0.3</u>      | <u>5.6</u>     | -           | <u>5.49</u>       |              |
| Restgas                           | <u>25.9</u>     | <u>0.6</u> | <u>0.1</u>     | <u>20.6</u> | <u>25.5</u>    | <u>5.4</u>      | <u>9.2</u>     | <u>1.22</u> | <u>9.61</u>       |              |
| Analysen                          |                 |            |                | <u>25.6</u> | <u>39.2</u>    |                 |                |             |                   |              |
| H <sub>2</sub> CO im Kreislaufgas |                 |            |                | <u>1.53</u> |                |                 |                |             |                   |              |

Gesamt-Inerte (Idealgas) 10.4 %  
 H<sub>2</sub>: CO im Sygas 1.27 %  
 H<sub>2</sub>: CO im Restgas 1.72 %  
 Verbrauch von H<sub>2</sub>: CO 1.07 %  
 Kontraktion nach Menge 44.2 %  
 " " N<sub>2</sub> 43.0 %  
 " " CO<sub>2</sub> \_\_\_\_\_ %  
 Durchschnittliche Kontraktion 43.6 %

umgesetzt 10.0 % CO  
 verflüssigt \_\_\_\_\_ % H<sub>2</sub> 59.2 % CO+H<sub>2</sub> 64.0 %  
 Verfl.-Grad A \_\_\_\_\_  
 " " P \_\_\_\_\_  
31.1

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 10.1 CO<sub>2</sub> 36.6 bezogen auf CO-Umsatz

## Produkte

Paraffingatsch 2.35 kg 19.5 %  
 Öl-Kondensat 8.20 " 49.3 %  
 A.-K. Benzin 5.20 " 31.2 %  
 Flüssige Prod. 16.65 " 100 %  
 Sywasser 23.50 kg = 1.41 x flüss. Produkte

## Gesamtprodukt

SB \_\_\_\_\_ °C  
 - 100° \_\_\_\_\_ %  
 - 200° \_\_\_\_\_ %  
 - 320° \_\_\_\_\_ %  
 Olefine Vol. %  
 - 200° \_\_\_\_\_ 200-320° \_\_\_\_\_

## Ausbeute

Flüssige Prod. 54.0 g Nm<sup>3</sup> Sygas 62.8 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasol \_\_\_\_\_ " " " " " "  
 Gesamt-Produkt \_\_\_\_\_ " " " " " "  
 Sywasser \_\_\_\_\_ " " " " " "

## Bemerkungen:

000191

**Druckversuchsanlage**

**Produktionsbericht vom 7/8. 10. 1943**

Ofen-Nr. 11  
 Füllung: 13  
 Fe-Inhalt: — kg

Betriebsstunden 24/451  
 Gasdruck 30 atü  
 Temperatur 350 atü 335 °C

W-Gas 321 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
 " " 13,4 Nm<sup>3</sup>/h

Restgas 178 Nm<sup>3</sup>  
 " " 4,4 Nm<sup>3</sup>/h  
 Kreislaufgas 757 Nm<sup>3</sup>  
 Kreislauf 2,34

Belastung — Nm<sup>3</sup>/kg.h 1,00 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:              | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Lüfergewicht |
|------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas                  | 6,4             | —                             | 0,1            | 28,4 | 49,7           | 0,3             | 5,6            | —    | 5,49              |              |
| Restgas                | 28,3            | 0,5                           | 0,1            | 20,5 | 35,7           | 5,3             | 9,6            | 1,96 | 9,34              |              |
| Phalgen                |                 |                               |                | 25,8 | 40,0           |                 |                |      |                   |              |
| Ha 100 im Kreislaufgas |                 |                               |                | 1,55 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 11,9 %  
 H<sub>2</sub>: CO im Sygas 1,39  
 H<sub>2</sub>: CO im Restgas 1,74  
 Verbrauch von H<sub>2</sub>: CO 1,10

Kontraktion nach Menge 44,5 %  
 " " N<sub>2</sub> 42,5 %  
 " " CO<sub>2</sub> — %  
 Durchschnittliche Kontraktion 43,5 %

umgesetzt 69,8 % CO  
 verflüssigt —  
 Verfl.-Grad A —  
 " " P —  
 " " " " 28,4

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 10,0 CO<sub>2</sub> 35,8 bezogen auf CO-Umsatz

**Produkte**

Paraffingasöl 2,84 kg 14,5 %  
 Öl-Kondensat 4,10 " 49,8 %  
 A.-K. Benzin 5,20 " 32,4 %  
 Flüssige Prod. 16,24 " 100 %  
 Sywasser 29,34 kg = 1,44 x flüss. Produkte

**Gesamtprodukt**

SB — °C  
 — 100° — %  
 — 200° — %  
 — 320° — %  
 Olefine Vol. %  
 — 200° — 200-320°

**Ausbeute**

Flüssige Prod. 50,0 g Nm<sup>3</sup> Sygas 57,5 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g Nm<sup>3</sup> Idealgas  
 Gasöl " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

**Bemerkungen:**

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|  |        |  |     |                            |      |                      |      |      |       |             |  |
|--|--------|--|-----|----------------------------|------|----------------------|------|------|-------|-------------|--|
| <b>Druckversuchsanlage</b>                 |        | <b>Produktionsbericht vom</b> 6.7.10. 1942 |     |                            |      |                      |      |      |       |             |  |
| Ofen-Nr. 11                                |        | Betriebsstunden 24/2427                    |     |                            |      |                      |      |      |       |             |  |
| Füllung: 13                                |        | Gasdruck 20,0 atü                          |     |                            |      |                      |      |      |       |             |  |
| Co-Fe-Inhalt — kg                          |        | Temperatur 350 atü 325 °C                  |     |                            |      |                      |      |      |       |             |  |
| Sy-W-Gas 296 Nm³                           |        | Restgas 156 Nm³                            |     |                            |      |                      |      |      |       |             |  |
| " " " " " "                                |        | " " " " " " 6,5 Nm³/h                      |     |                            |      |                      |      |      |       |             |  |
| " " " " " " 12,3 Nm³/h                     |        | Kreislaufgas 221 Nm³                       |     |                            |      |                      |      |      |       |             |  |
|  |        | Kreislauf 2,60                             |     |                            |      |                      |      |      |       |             |  |
| Belastung: — Nm³/kg.h                      |        | 0,97                                       |     |                            |      |                      |      |      |       |             |  |
| Analysen:                                  |        | Nm³/Norm.-Vol., h                          |     |                            |      |                      |      |      |       |             |  |
|  | CO₂    | CmHn                                       | O₂  | CO                         | H₂   | CH₄                  | N₂   | C-Z  | N₂-F  | Utergewicht |  |
| Sygas                                      | 6,1    | —  | 0,1 | 39,0                       | 48,9 | 0,3                  | 5,6  | —    | 5,42  |             |  |
| Restgas                                    | 30,0   | 0,4  | 0,1 | 19,3                       | 22,8 | 5,9                  | 10,5 | 1,11 | 10,44 |             |  |
| Ameisensäure                               |        |  |     | 24,8                       | 38,0 |                      |      |      |       |             |  |
| H₂O im Kreislaufgas                        |        |  |     | 1,53                       |      |                      |      |      |       |             |  |
| Gesamt-Inerte (Idealgas) 12,1 %            |        | Kontraktion nach Menge 47,2 %              |     |                            |      |                      |      |      |       |             |  |
| H₂: CO im Sygas 1,26                       |        | " " N₂ 47,6 %                              |     |                            |      |                      |      |      |       |             |  |
| H₂: CO im Restgas 1,75                     |        | " " CO₂ — %                                |     |                            |      |                      |      |      |       |             |  |
| Verbrauch von H₂: CO 1,08                  |        | Durchschnittliche Kontraktion 47,4 %       |     |                            |      |                      |      |      |       |             |  |
| umgesetzt %CO 43,9                         |        | %H₂ 63,5                                   |     | %CO+H₂ 68,1                |      |                      |      |      |       |             |  |
| verfügig                                   |        |  |     |                            |      |                      |      |      |       |             |  |
| Verf.-Grad A                               |        |  |     |                            |      |                      |      |      |       |             |  |
| " " P                                      |        |  |     |                            |      |                      |      |      |       | 29,3        |  |
| CH₄ + CmHn 9,8                             |        | CO₂ 33,6                                   |     | bezogen auf CO-Umsatz      |      |                      |      |      |       |             |  |
| <b>Produkte</b>                            |        |  |     |                            |      | <b>Gesamtprodukt</b> |      |      |       |             |  |
| Paraffingatsch 3,40 kg                     | 20,8 % |  |     | SB — 100° °C               |      |                      |      |      |       |             |  |
| Ol-Kondensat 7,60 "                        | 46,3 % |  |     | — 200° °C                  |      |                      |      |      |       |             |  |
| A.-K. Benzin 5,40 "                        | 33,9 % |  |     | — 320° °C                  |      |                      |      |      |       |             |  |
| Flüssige Prod. 16,40 "                     | 100 %  |  |     | Olefine Vol. %             |      |                      |      |      |       |             |  |
| Sywasser 22,10 kg = 1,35 x flüss. Produkte |        |  |     | — 200° 200-320°            |      |                      |      |      |       |             |  |
| <b>Ausbeute</b>                            |        | Flüssige Prod. 55,4 g/Nm³ Sygas            |     | 62,0 g/Nm³ Nutzgas (CO+H₂) |      | g/Nm³ Idealgas       |      |      |       |             |  |
| Gasol                                      |        | " " " "                                    |     | " " " "                    |      | " " " "              |      |      |       |             |  |
| Gesamt-Produkt                             |        | " " " "                                    |     | " " " "                    |      | " " " "              |      |      |       |             |  |
| Sywasser                                   |        | " " " "                                    |     | " " " "                    |      | " " " "              |      |      |       |             |  |
| <b>Bemerkungen:</b>                        |        |  |     |                            |      |                      |      |      |       |             |  |

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# Druckversuchsanlage

Produktionsbericht vom 25./26.9.1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt: kg

Betriebsstunden 24 / 3167  
 Gasdruck 20 atü  
 Temperatur 25 atü 225 °C

W-Gas 288 Nm<sup>3</sup>  
 " " " " " "  
 " 12,0 Nm<sup>3</sup>/h

Restgas 151 Nm<sup>3</sup>  
 " 6,3 Nm<sup>3</sup>/h  
 Kreislaufgas 146,5 Nm<sup>3</sup>  
 Kreislauf 2,66

Belastung Nm<sup>3</sup>/kg,h 0,95

| Analysen:                                 | Nm <sup>3</sup> /Norm.-Vol., h |      |                |       |                |                 |                |      |                   |  | Litergewicht |
|---|--------------------------------|------|----------------|-------|----------------|-----------------|----------------|------|-------------------|--|--------------|
|   | CO <sub>2</sub>                | CmHn | O <sub>2</sub> | CO    | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F |  |              |
| W Sygas                                   | 6,8                            | -    | 0,1            | 38,1  | 48,6           | 0,3             | 6,1            | -    | 5,98              |  |              |
| Restgas                                   | 31,0                           | 0,4  | 0,1            | 17,2  | 33,0           | 6,3             | 12,0           | 1,18 | 11,90             |  |              |
| <i>Maßgaben</i>                           |                                |      |                | 22,9  | 37,3           |                 |                |      |                   |  |              |
| <i>H<sub>2</sub> 1,00 im Kreislaufgas</i> |                                |      |                | 11,63 |                |                 |                |      |                   |  |              |

Gesamt-Inerte (Idealgas) 13,3 %  
 H<sub>2</sub>:CO im Sygas 1,27  
 H<sub>2</sub>:CO im Restgas 1,92  
 Verbrauch von H<sub>2</sub>:CO 1,08

Kontraktion nach Menge 47,6 %  
 " " N<sub>2</sub> 49,8 %  
 " " CO<sub>2</sub> %  
 Durchschnittliche Kontraktion 48,7 %

umgesetzt %CO 77,0 %H<sub>2</sub> 65,0 %CO+H<sub>2</sub> 70,2  
 verfügbar \_\_\_\_\_  
 Verfl.-Grad A \_\_\_\_\_  
 " " P \_\_\_\_\_  
 27,6

CH<sub>4</sub> + *andere* 10,0 CO<sub>2</sub> 31,0 bezogen auf CO-Umsatz

| Produkte       |                 |                   |
|----------------|-----------------|-------------------|
| Paraffingasch  | 3,10 kg         | 20,2 %            |
| Ol-Kondensat   | 7,10 "          | 46,4 %            |
| A.-K. Benzin   | 5,10 "          | 33,4 %            |
| Flüssige Prod. | 15,30           | 100 %             |
| Sywasser       | 20,40 kg = 1,32 | x flüss. Produkte |

| Gesamtprodukt |            |
|---------------|------------|
| SB            | °C         |
| - 100°        | %          |
| - 200°        | %          |
| - 320°        | %          |
| Olefine       | Vol. %     |
| - 200°        | 200 - 320° |

**Ausbeute**  
 Flüssige Prod. 53,2 g Nm<sup>3</sup> Sygas 61,4 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

**Bemerkungen:**

000204

# Druckversuchsanlage

Produktionsbericht vom 24./25. 9. 1943

Ofen-Nr. 11  
 Füllung: 13  
 Fe-Inhalt: - kg

Betriebsstunden: 24/3143  
 Gasdruck: 20 atü  
 Temperatur: 25 atü 225 °C

W-Gas: 308 Nm<sup>3</sup>  
 " " " " " "  
 " " " " " "  
 " " " " " " 12,8 Nm<sup>3</sup>/h

Restgas: 153 Nm<sup>3</sup>  
 " " " " " " 6,4 Nm<sup>3</sup>/h  
 Kreislaufgas: 46,4 Nm<sup>3</sup>  
 Kreislauf: 2,48

Belastung: - Nm<sup>3</sup>/kg.h  
 Analysen: - Nm<sup>3</sup>/Norm.-Vol., h

|  | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Liegewicht |
|--|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|------------|
| W-Gas  | 6,6             | -    | 0,1            | 38,5 | 49,2           | 0,3             | 5,3            | -    | 5,19              |            |
| Restgas  | 31,4            | 0,4  | 0,1            | 17,1 | 34,5           | 6,4             | 10,1           | 1,12 | 10,03             |            |
| Analysen                                       |                 |      |                | 33,2 | 38,8           |                 |                |      |                   |            |
| H <sub>2</sub> 110 m <sup>3</sup> Kreislaufgas |                 |      |                |      |                |                 |                |      |                   |            |
|  |                 |      |                |      | 116,7          |                 |                |      |                   |            |

Gesamt-Inerte (Idealgas) 12,3 %  
 H<sub>2</sub>-CO im Sygas 4,8  
 H<sub>2</sub>-CO im Restgas 2,02  
 Verbrauch von H<sub>2</sub>: CO 1,04

Kontraktion nach Menge: 50,3 %  
 " " N<sub>2</sub>: 49,7 %  
 " " CO: - %  
 Durchschnittliche Kontraktion: 50,0 %

umgesetzt: %CO 44,7 %H<sub>2</sub> 64,9 %CO+H<sub>2</sub> 70,5  
 verflüssigt: -  
 Verfl.-Grad A: -  
 " " " " " " 26,1

CH<sub>4</sub> + ~~CO~~ 4,7 CO<sub>2</sub> 30,4 bezogen auf CO-Umsatz

## Produkte

Paraffingasch 3,20 kg 20,4 %  
 Öl-Kondensat 7,20 " 45,8 %  
 A.-K. Benzin 5,30 " 33,8 %  
 Flüssige Prod. 15,70 " 100 %  
 Sywasser 20,70 kg = 1,32 x flüss. Produkte

## Gesamtprodukt

SB: °C  
 - 100° %  
 - 200° %  
 + 320° %  
 Olefine Vol. %  
 - 200° ; 200-320°

## Ausbeute

Flüssige Prod. 51,0 g/Nm<sup>3</sup> Sygas 58,1 g/Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

000205





















**Druckversuchsanlage**

Produktionsbericht vom 14./15.9.1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt: — kg

Betriebsstunden 24/3905  
 Gasdruck 30 atü  
 Temperatur 250 atü 225 °C

sy-W-Gas 316 Nm<sup>3</sup>  
 13.2 Nm<sup>3</sup>/h

Restgas 169 Nm<sup>3</sup>  
 7.1 Nm<sup>3</sup>/h  
 Kreislaufgas 7.24 Nm<sup>3</sup>  
 Kreislauf 2.44

Belastung: — Nm<sup>3</sup>/kg.h 1.04 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                         | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| sy-Gas                            | 6.9             | —                             | 0.1            | 32.9 | 48.2           | 0.3             | 6.6            | —    | 6.48              |              |
| Restgas                           | 29.4            | 0.5                           | 0.1            | 19.0 | 32.5           | 5.2             | 11.8           | 1.00 | 11.65             |              |
| H <sub>2</sub> CO im Kreislaufgas |                 |                               |                | 24.5 | 24.8           |                 |                |      |                   |              |
|                                   |                 |                               |                | 1.54 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 13.67 %  
 H<sub>2</sub>: CO im Sygas 1.27  
 H<sub>2</sub>: CO im Restgas 1.76  
 Verbrauch von H<sub>2</sub>: CO 1.09

Kontraktion nach Menge 42.5 %  
 " " N<sub>2</sub> 44.4 %  
 " " CO<sub>2</sub> 45.5 %  
 Durchschnittliche Kontraktion 45.5 %

umgesetzt %CO 12.5 %H<sub>2</sub> 62.3 %CO+H<sub>2</sub> 66.7  
 verflüssigt \_\_\_\_\_  
 Verfl.-Grad A \_\_\_\_\_  
 " " P \_\_\_\_\_ 28.4

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 10.2 CO<sub>2</sub> 33.1 bezogen auf CO-Umsatz

**Produkte**

Paraffingatsch 3.62 kg 22.4 %  
 Öl-Kondensat 8.52 " 52.3 %  
 A.-K. Benzin 4.10 " 25.3 %  
 Flüssige Prod. 16.24 " 100 %  
 Sywasser 19.60 kg = 1.21 " X flüss. Produkte

**Gesamtprodukt**

SB \_\_\_\_\_ °C  
 — 100° \_\_\_\_\_ %  
 — 200° \_\_\_\_\_ %  
 — 320° \_\_\_\_\_ %  
 Olefine Vol. %  
 — 200° \_\_\_\_\_ 200-320° \_\_\_\_\_

**Ausbeute**

Flüssige Prod. 51.5 g/Nm<sup>3</sup> Sygas 59.8 g/Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasöl " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

**Bemerkungen:**

Ofen wird mit Wassergas im Kreislauf gefahren.

000215

**Druckversuchsanlage** **Produktionsbericht vom** 13.11.9. 1943

Ofen-Nr. 11 Betriebsstunden 24/2551  
 Füllung: 13 Gasdruck 20 atü  
 G.-Fe.-Inhalt - kg Temperatur 250 atü 225 C

W-Gas 295 Nm<sup>3</sup> Restgas - Nm<sup>3</sup>  
 " " " " " " Nm<sup>3</sup>/h  
 " " " " " " Nm<sup>3</sup>  
 " 12,3 Nm<sup>3</sup>/h Kreislaufgas 772 Nm<sup>3</sup>  
 Kreislauf 2,62

Belastung 0,97 Nm<sup>3</sup>/kg.h 0,97 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen                      | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas                         | 6,5             | -    | 0,1            | 38,7 | 42,1           | 0,1             | 7,3            | -    | 7,23              |              |
| Restgas                       | 30,7            | 0,4  | 0,1            | 18,3 | 32,8           | 6,0             | 12,1           | 1,10 | 12,07             |              |
| Amalgam                       |                 |      |                | 24,0 | 36,8           |                 |                |      |                   |              |
| H <sub>2</sub> CO von Amalgam |                 |      |                | 1,53 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 14,2 %  
 H<sub>2</sub>, CO im Sygas 1,22 %  
 H<sub>2</sub>, CO im Restgas 1,79 %  
 Kontraktion nach Menge - %  
 " " N<sub>2</sub> 40,0 %  
 " " CO<sub>2</sub> - %  
 Verbrauch von H<sub>2</sub>, CO - %  
 Durchschnittliche Kontraktion 40,0 %

umgesetzt 71,5 %CO  
 verflüssigt 58,2 %H<sub>2</sub>  
 Verfl.-Grad 64,1 %CO+H<sub>2</sub>  
 " " P 26,9

CH<sub>4</sub> + ~~Amalg~~ 11,9 CO<sub>2</sub> 42,3 bezogen auf CO-Umsatz

| Produkte       |              |                  |                   | Gesamtprodukt |          |
|----------------|--------------|------------------|-------------------|---------------|----------|
| Paraffingasch  | <u>2,73</u>  | kg               | <u>19,4</u>       | SB            | °C       |
| Ol-Kondensat   | <u>7,60</u>  | "                | <u>54,4</u>       | - 100°        | %        |
| A.-K. Benzin   | <u>3,50</u>  | "                | <u>25,4</u>       | - 200°        | %        |
| Flüssige Prod. | <u>13,82</u> | "                | 100%              | - 320°        | %        |
| Sywasser       | <u>18,70</u> | kg = <u>1,35</u> | x flüss. Produkte | Olefine       | Vol. %   |
|                |              |                  |                   | - 200°        | 200-320° |

**Ausbeute**  
 Flüssige Prod. 46,9 g/Nm<sup>3</sup> Sygas 55,3 g.Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " " " " " " " "  
 Gesamt-Produkt " " " " " " " " " " " "  
 Sywasser " " " " " " " " " " " "

**Bemerkungen:**

**000216**







| <b>Druckversuchsanlage</b>   |   |                                       |                |             | <b>Produktionsbericht vom</b> <i>11. / 11. 9. 1943</i> |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
|--|---|---------------------------------------|----------------|-------------|--|-----------------|----------------|-------------|-------------------|--------------|---|-----------------|-----------------------|----------------|----|----------------|-----------------|----------------|-----|-------------------|--------------|------------|-------------|---|------------|-------------|-------------|------------|------------|---|-------------|--|---------|-------------|------------|------------|-------------|-------------|------------|-------------|-------------|-------------|--|--------------|--|--|--|-------------|-------------|--|--|--|--|--|---------------------------|--|--|--|--|-------------|--|--|--|--|--|
| Ofen-Nr. <i>11</i>   |   |                                       |                |             | Betriebsstunden <i>22/2809</i>                         |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Füllung: <i>12</i>   |   |                                       |                |             | Gasdruck <i>20</i> atü                                 |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Co-Fe-Inhalt: _____ kg   |   |                                       |                |             | Temperatur <i>25.0</i> atü <i>225</i> °C               |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Sy-W-Gas: <i>302</i> Nm <sup>3</sup>   |   |                                       |                |             | Restgas: <i>12.1</i> Nm <sup>3</sup>                   |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| " " " " " "  |   |                                       |                |             | " " " " " " <i>2.6</i> Nm <sup>3</sup> /h              |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| " " " " " " <i>13.4</i> Nm <sup>3</sup> /h   |   |                                       |                |             | Kreislaufgas: <i>40.4</i> Nm <sup>3</sup>              |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| " " " " " " " "  |   |                                       |                |             | Kreislauf: <i>2.33</i>                                 |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Belastung: _____ Nm <sup>3</sup> /kg.h   |   |                                       |                |             | _____ <i>1.05</i> Nm <sup>3</sup> /Norm.-Vol. h        |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th>Analysen:</th> <th>CO<sub>2</sub></th> <th>CmHn</th> <th>O<sub>2</sub></th> <th>CO</th> <th>H<sub>2</sub></th> <th>CH<sub>4</sub></th> <th>N<sub>2</sub></th> <th>C-Z</th> <th>N<sub>2</sub>-F</th> <th>Litergewicht</th> </tr> </thead> <tbody> <tr> <td>Sygas</td> <td><i>6.3</i></td> <td>-</td> <td><i>0.1</i></td> <td><i>39.8</i></td> <td><i>48.8</i></td> <td><i>0.3</i></td> <td><i>6.3</i></td> <td>-</td> <td><i>6.20</i></td> <td></td> </tr> <tr> <td>Restgas</td> <td><i>25.2</i></td> <td><i>0.4</i></td> <td><i>0.1</i></td> <td><i>23.9</i></td> <td><i>36.2</i></td> <td><i>4.8</i></td> <td><i>11.1</i></td> <td><i>1.15</i></td> <td><i>11.0</i></td> <td></td> </tr> <tr> <td>Kreislaufgas</td> <td></td> <td></td> <td></td> <td><i>22.8</i></td> <td><i>39.6</i></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> <tr> <td><i>12</i> CO im Kreislauf</td> <td></td> <td></td> <td></td> <td></td> <td><i>1.42</i></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> </tbody> </table> |   |                                       |                |             |  |                 |                |             |                   |              | Analysen:                                       | CO <sub>2</sub> | CmHn                  | O <sub>2</sub> | CO | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht | Sygas      | <i>6.3</i>  | - | <i>0.1</i> | <i>39.8</i> | <i>48.8</i> | <i>0.3</i> | <i>6.3</i> | - | <i>6.20</i> |  | Restgas | <i>25.2</i> | <i>0.4</i> | <i>0.1</i> | <i>23.9</i> | <i>36.2</i> | <i>4.8</i> | <i>11.1</i> | <i>1.15</i> | <i>11.0</i> |  | Kreislaufgas |  |  |  | <i>22.8</i> | <i>39.6</i> |  |  |  |  |  | <i>12</i> CO im Kreislauf |  |  |  |  | <i>1.42</i> |  |  |  |  |  |
| Analysen:  | CO <sub>2</sub>                                 | CmHn                                  | O <sub>2</sub> | CO          | H <sub>2</sub>   | CH <sub>4</sub> | N <sub>2</sub> | C-Z         | N <sub>2</sub> -F | Litergewicht |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Sygas  | <i>6.3</i>                                      | -                                     | <i>0.1</i>     | <i>39.8</i> | <i>48.8</i>  | <i>0.3</i>      | <i>6.3</i>     | -           | <i>6.20</i>       |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Restgas  | <i>25.2</i>                                     | <i>0.4</i>                            | <i>0.1</i>     | <i>23.9</i> | <i>36.2</i>  | <i>4.8</i>      | <i>11.1</i>    | <i>1.15</i> | <i>11.0</i>       |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Kreislaufgas   |   |                                       |                | <i>22.8</i> | <i>39.6</i>  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| <i>12</i> CO im Kreislauf  |   |                                       |                |             | <i>1.42</i>  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Gesamt-Inerte (Idealgas) <i>13.0</i> %   |   |                                       |                |             | Kontraktion nach Menge <i>43.4</i> %                   |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| H <sub>2</sub> CO im Sygas <i>1.23</i>   |   |                                       |                |             | " " N <sub>2</sub> <i>43.6</i> %                       |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| H <sub>2</sub> CO im Restgas <i>1.58</i>   |   |                                       |                |             | " " CO <sub>2</sub> _____ %                            |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Verbrauch von H <sub>2</sub> : CO <i>1.06</i>  |   |                                       |                |             | Durchschnittliche Kontraktion <i>43.5</i> %            |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| umgesetzt <i>66.4</i> % CO   |   |                                       |                |             | % H <sub>2</sub> <i>54.4</i>                           |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| verflüssigt _____  |   |                                       |                |             | % CO + H <sub>2</sub> <i>67.5</i>                      |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Verfl.-Grad A _____  |   |                                       |                |             | _____ <i>37.8</i>                                      |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| " " P _____  |   |                                       |                |             | _____  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th>CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub></th> <th>CO<sub>2</sub></th> <th colspan="9">bezogen auf CO-Umsatz</th> </tr> </thead> <tbody> <tr> <td><i>9.1</i></td> <td><i>30.5</i></td> <td colspan="9"></td> </tr> </tbody> </table>  |   |                                       |                |             |  |                 |                |             |                   |              | CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub> | CO <sub>2</sub> | bezogen auf CO-Umsatz |                |    |                |                 |                |     |                   |              | <i>9.1</i> | <i>30.5</i> |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub>  | CO <sub>2</sub>                                 | bezogen auf CO-Umsatz                 |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| <i>9.1</i>   | <i>30.5</i>                                     |                                       |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| <b>Produkte</b>  |   |                                       |                |             | <b>Gesamtprodukt</b>                                   |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Paraffingatsch   | <i>4.50</i> kg                                  | <i>87.4</i> %                         |                |             |  | SB              | °C             |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Ol-Kondensat   | <i>7.75</i> "                                   | <i>44.4</i> %                         |                |             |  | - 100°          | %              |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| A.-K. Benzin   | <i>4.00</i> "                                   | <i>34.6</i> %                         |                |             |  | - 200°          | %              |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Flüssige Prod.   | <i>16.25</i>                                    |                                       | 100 %          |             |  | - 320°          | %              |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Sywasser   | <i>20.30</i> kg = <i>1.25</i> x flüss. Produkte |                                       |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
|  |   |                                       |                |             | Olefine Vol. %   |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
|  |   |                                       |                |             | - 200° ..... , 200 - 320° .....                        |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| <b>Ausbeute</b>  |   |                                       |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Flüssige Prod.   | <i>53.8</i> g Nm <sup>3</sup> Sygas             | <i>61.9</i> g Nm <sup>3</sup> Nutzgas |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Gasol  | " "   | " "                                   |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Gesamt-Produkt   | " "   | " "                                   |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| Sywasser   | " "   | " "                                   |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |
| <b>Bemerkungen:</b> <i>Skizzenbuch von 10.2.43 - 11.11.43 keine Proben</i>   |   |                                       |                |             |  |                 |                |             |                   |              |   |                 |                       |                |    |                |                 |                |     |                   |              |            |             |   |            |             |             |            |            |   |             |  |         |             |            |            |             |             |            |             |             |             |  |              |  |  |  |             |             |  |  |  |  |  |                           |  |  |  |  |             |  |  |  |  |  |

000219









# Druckversuchsanlage

Produktionsbericht vom 5./6. 9. 1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt: kg

Betriebsstunden 24 / 2691  
 Gasdruck 20 atü  
 Temperatur 22,5 atü °C

W-Gas 298 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
 " 12,4 Nm<sup>3</sup>/h

Restgas 168 Nm<sup>3</sup>  
 " 4,0 Nm<sup>3</sup>/h  
 " " " " " " " "  
 Kreislaufgas 484 Nm<sup>3</sup>  
 Kreislauf 263

Belastung: Nm<sup>3</sup> / kg, h 0,98 Nm<sup>3</sup> / Norm.-Vol., h

| Analysen:                           | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | litergewicht |
|-------------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|-----|-------------------|--------------|
| W Sygas                             | 7,2             | -    | 0,1            | 34,4 | 47,9           | 0,3             | 4,1            | -   | 6,97              |              |
| Restgas                             | 26,5            | 0,5  | 0,1            | 21,4 | 34,8           | 4,7             | 12,0           | 118 | 11,90             |              |
| Kreislaufgas                        |                 |      |                | 25,8 | 38,4           |                 |                |     |                   |              |
| H <sub>2</sub> 11,6 im Kreislaufgas |                 |      |                |      | 1,49           |                 |                |     |                   |              |

Gesamt-Inerte (Idealgas) 14,4 %  
 H<sub>2</sub>: CO im Sygas 12,8  
 H<sub>2</sub>: CO im Restgas 1,63  
 Verbrauch von H<sub>2</sub>: CO 1,11

Kontraktion nach Menge 43,6 %  
 " " " " N<sub>2</sub> 41,5 %  
 " " " " CO<sub>2</sub> %  
 Durchschnittliche Kontraktion 42,6 %

umgesetzt: %CO 67,1 %H<sub>2</sub> 58,3 %CO+H<sub>2</sub> 62,1  
 verfügbar: " " " " " "  
 Verfl.-Grad A " " " " " "  
 " " P " " " " " "

CH<sub>4</sub> + CmHn 9,5 CO<sub>2</sub> 22,0 bezogen auf CO-Umsatz

## Produkte

Paraffingatsch 4,00 kg 25,2 %  
 Öl-Kondensat 7,85 " 49,6 %  
 A.-K. Benzin 4,00 " 25,2 %  
 Flüssige Prod. 15,85 " 100 %  
 Sywasser 20,10 kg = 1,27 x flüss. Produkte

## Gesamtprodukt

SB °C  
 - 100° %  
 - 200° %  
 - 320° %  
 Olefine Vol. %  
 - 200° , 200 - 320°

## Ausbeute

Flüssige Prod. 53,9 g Nm<sup>3</sup> Sygas 69,3 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

000224







# Druckversuchsanlage

Produktionsbericht vom 2.3.9/ 1943

Ofen-Nr. 71

Füllung: 13

Co-Fe-Inhalt: kg

Betriebsstunden 24/26.19

Gasdruck 20 atü

Temperatur 225 atü 219 °C

Sy-W-Gas 297 Nm³

" " " " " "

" " " " " "

" 12.4 Nm³/h

Restgas 166 Nm³

" 16.9 Nm³/h

Kreislaufgas 12.1 Nm³

Kreislauf 2.143

Belastung Nm³/kg,h 0.48

| Analysen: | Nm³/Norm.-Vol., h |      |     |      |      |     |      |     |      |  | Lifergewicht |
|-----------|-------------------|------|-----|------|------|-----|------|-----|------|--|--------------|
|           | CO₂               | CmHn | O₂  | CO   | H₂   | CH₄ | N₂   | C-Z | N₂-F |  |              |
| Sygas     | 6.1               |      | 0.1 | 28.8 | 44.9 | 0.2 | 4.5  |     |      |  |              |
| Restgas   | 26.2              | 0.2  | 0.1 | 26.8 | 22.1 | 0.5 | 19.3 | 0.8 |      |  |              |
| Wasser    |                   |      |     |      |      |     |      |     |      |  |              |

Gesamt-Inerte (Idealgas) 24.0 %

H₂CO im Sygas

H₂CO im Restgas

Verbrauch von H₂: CO

Kontraktion nach Menge 43.0 %

" " N₂ 95.2 %

" " CO₂

Durchschnittliche Kontraktion 28.4 %

|               | %CO  | %H₂  | %CO+H₂ |
|---------------|------|------|--------|
| umgesetzt     | 28.4 | 64.5 |        |
| verflüssigt   |      |      |        |
| Verfl.-Grad A | 7    |      |        |
| " " P         |      |      |        |

CH₄ + CmHn CO₂ bezogen auf CO-Umsatz

## Produkte

|                |                   |        |
|----------------|-------------------|--------|
| Paraffingas    | 4.25 kg           | 1.25 % |
| Ol-Kondensat   | 2.00 "            | 0.6 %  |
| A.-K. Benzin   | 4.50 "            | 1.3 %  |
| Flüssige Prod. | 11.75 "           | 3.4 %  |
| Sywasser       | 20.25 kg = 12.1 % | 100 %  |

## Gesamtprodukt

|         |          |
|---------|----------|
| SB      | °C       |
| - 100°  | %        |
| - 200°  | %        |
| - 320°  | %        |
| Olefine | Vol. %   |
| - 200°  | 200-320° |

## Ausbeute

|                |                  |                    |                     |
|----------------|------------------|--------------------|---------------------|
| Flüssige Prod. | 66.7 g Nm³ Sygas | 65.2 g Nm³ Nutzgas | 62.4 g Nm³ Idealgas |
| Gasol          | " " "            | " " "              | " " "               |
| Gesamt-Produkt | " " "            | " " "              | " " "               |
| Sywasser       | " " "            | " " "              | " " "               |

## Bemerkungen:

000227









# Druckversuchsanlage

Produktionsbericht vom 28. | 29. 8. 1943

Ofen-Nr. 11

Betriebsstunden 241 249

Füllung: 13

Gasdruck 20 atü

Ka-Fe-Inhalt: - kg

Temperatur 225 atü 219 °C

Sy-W-Gas 32.1 Nm³

Restgas 186 Nm³

" " " " " "

" " " " " "

" " " " 13.4 Nm³/h

Kreislaufgas 46.4 Nm³

Kreislauf 2.38

Belastung Nm³/kg,h 1.05 Nm³/Norm.-Vol., h

| Analysen:                           | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-------------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                           | 7.6             | -    | 0.1            | 36.8 | 49.0           | 0.3             | 6.2            | -    | 6.09              |              |
| Sygas                               | 26.4            | 0.5  | 0.1            | 21.3 | 36.4           | 1.3             | 10.7           | 1.11 | 10.57             |              |
| Restgas                             |                 |      |                | 25.8 | 40.3           |                 |                |      |                   |              |
| H <sub>2</sub> 16.0 im Kreislaufgas |                 |      |                |      |                |                 |                |      |                   |              |

|                                 |      |   |                               |      |   |
|---------------------------------|------|---|-------------------------------|------|---|
| Gesamt-Inertie (Idealgas)       | 14.8 | % | Kontraktion nach Menge        | 42.0 | % |
| H <sub>2</sub> CO im Sygas      | 1.33 |   | " " N <sub>2</sub>            | 42.7 | % |
| H <sub>2</sub> CO im Restgas    | 1.42 |   | " " CO <sub>2</sub>           | -    | % |
| Verbrauch von H <sub>2</sub> CO | 1.13 |   | Durchschnittliche Kontraktion | 42.2 | % |

|               |     |      |                 |      |                    |      |
|---------------|-----|------|-----------------|------|--------------------|------|
| umgesetzt     | %CO | 66.5 | %H <sub>2</sub> | 56.7 | %CO+H <sub>2</sub> | 61.0 |
| verflüssigt   |     |      |                 |      |                    |      |
| Verfl.-Grad A |     |      |                 |      |                    |      |
| " " P         |     |      |                 |      |                    | 31.7 |

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 8.9 CO<sub>2</sub> 31.4 bezogen auf CO-Umsatz

| Produkte                                   | Gesamtprodukt       |
|--|---------------------|
| Paraffingatsch 4.45 kg 26.4 %              | SB °C               |
| Öl-Kondensat 8.50 " 50.4 %                 | - 100° %            |
| A.-K.-Benzin 3.90 " 83.2 %                 | - 200° %            |
| Flüssige Prod. 16.85 " 100%                | - 320° %            |
| Sywasser 24.50 kg = 1.45 x flüss. Produkte | Olefine Vol. %      |
|  | - 200° ; 200 - 320° |

| Ausbeute                        |  |
|---------------------------------|--|
| Flüssige Prod. 52.5 g Nm³ Sygas | 61.2 g Nm³ Nutzgas (CO+H <sub>2</sub> ) g Nm³ Idealgas |
| Gasol                           | " " " " " "  |
| Gesamt-Produkt                  | " " " " " "  |
| Sywasser                        | " " " " " "  |

Bemerkungen:

000232







# Druckversuchsanlage

Produktionsbericht vom 25./26. 1943

Ofen-Nr. 11  
 Füllung: 12  
 Co-Fe-Inhalt: - kg

Betriebsstunden 24/2430  
 Gasdruck 25 atü  
 Temperatur 225 atü 219 °C

Sy-W-Gas 316 Nm<sup>3</sup>  
 " " " " " " " "  
 " 13,2 Nm<sup>3</sup>/h

Restgas 189 Nm<sup>3</sup>  
 " 4,6 Nm<sup>3</sup>/h  
 Kreislaufgas 291 Nm<sup>3</sup>  
 Kreislauf 2,82

Belastung - Nm<sup>3</sup>/kg, h 1,04

| Analysen:                               | Nm <sup>3</sup> /kg, h |      |                |      |                |                 | Nm <sup>3</sup> /Norm.-Vol., h |      |                   |  | Litergewicht |
|---|------------------------|------|----------------|------|----------------|-----------------|--------------------------------|------|-------------------|--|--------------|
|   | CO <sub>2</sub>        | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub>                 | C-Z  | N <sub>2</sub> -F |  |              |
| Sygas                                   | 8,3                    | -    | 0,1            | 35,8 | 49,0           | 0,3             | 6,5                            | -    | 6,40              |  |              |
| Restgas                                 | 29,8                   | 0,4  | 0,1            | 12,8 | 35,2           | 5,3             | 11,4                           | 1,18 | 11,33             |  |              |
| <i>Druckgas</i>                         |                        |      |                | 22,5 | 38,8           |                 |                                |      |                   |  |              |
| <i>H<sub>2</sub> CO im Kreislaufgas</i> |                        |      |                |      | 1,72           |                 |                                |      |                   |  |              |

Gesamt-Inerte (Idealgas) 15,2 %  
 H<sub>2</sub>:CO im Sygas 1,37 %  
 H<sub>2</sub>:CO im Restgas 1,98 %  
 Verbrauch von H<sub>2</sub>:CO 1,13 %  
 Kontraktion nach Menge 42,7 %  
 " " N<sub>2</sub> 43,5 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 43,1 %

umgesetzt 71,9 %CO  
 verflüssigt 59,1 %H<sub>2</sub>  
 Verfl.-Grad A 164,5 %CO+H<sub>2</sub>  
 " " P 26,7

CH<sub>4</sub> 10,5 CO<sub>2</sub> 33,6 bezogen auf CO-Umsatz

**Produkte**

|                |   |               |
|----------------|---|---------------|
| Paraffingasch  | <u>3,90</u> kg                                  | <u>20,4</u> % |
| Ol-Kondensat   | <u>2,20</u> "                                   | <u>49,3</u> % |
| A.-K. Benzin   | <u>3,50</u> "                                   | <u>34,0</u> % |
| Flüssige Prod. | <u>14,60</u> "                                  | 100 %         |
| Sywasser       | <u>22,90</u> kg = <u>1,57</u> X flüss. Produkte |               |

**Gesamtprodukt**

|         |            |
|---------|------------|
| SB      | °C         |
| - 100°  | %          |
| - 200°  | %          |
| - 320°  | %          |
| Olefine | Vol. %     |
| - 200°  | 200 - 320° |

**Ausbeute**  
 Flüssige Prod. 46,6 g Nm<sup>3</sup> Sygas 54,5 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

Bemerkungen:

000235



# Druckversuchsanlage

Produktionsbericht vom 23.12.8. 1943

Ofen-Nr. 11

Betriebsstunden 24 / 2382

Füllung: 13

Gasdruck 20 atü

Gas-Fe-Inhalt - kg

Temperatur 22,5 atü 219 °C

W-Gas 313 Nm³

Restgas 164 Nm³

" " " "

" 6,8 Nm³/h

" " " "

Kreislaufgas 869 Nm³

" 13,0 Nm³/h

Kreislauf 2,48

Belastung - Nm³/kg,h 1,03 Nm³/Norm.-Vol., h

Analysen: CO<sub>2</sub> C<sub>m</sub>H<sub>n</sub> O<sub>2</sub> CO H<sub>2</sub> CH<sub>4</sub> N<sub>2</sub> C-Z N<sub>2</sub>-F Litergewicht

|                                   |      |     |     |      |      |     |      |      |       |  |
|-----------------------------------|------|-----|-----|------|------|-----|------|------|-------|--|
| Sygas                             | 8,0  | -   | 0,1 | 36,1 | 48,5 | 0,3 | 4,0  | -    | 6,93  |  |
| Restgas                           | 18,8 | 0,5 | 0,1 | 18,4 | 35,1 | 4,7 | 12,4 | 1,08 | 12,34 |  |
| Kreislaufgas                      |      |     |     | 23,0 | 38,7 |     |      |      |       |  |
| H <sub>2</sub> CO im Kreislaufgas |      |     |     | 1    | 68   |     |      |      |       |  |

Gesamt-Inerte (Idealgas) 15,4 %

Kontraktion nach Menge 47,6 %

H<sub>2</sub> CO im Sygas 1,34

" " N<sub>2</sub> - %

H<sub>2</sub> CO im Restgas 1,91

" " CO<sub>2</sub> - %

Verbrauch von H<sub>2</sub>: CO 1,14

Durchschnittliche Kontraktion 47,6 %

umgesetzt %CO 73,5 %H<sub>2</sub> 62,1 %CO+H<sub>2</sub> 67,0

verflüssigt

Verfl.-Grad A

" " P 27,4

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 8,2 CO<sub>2</sub> 93,7 bezogen auf CO-Umsatz

## Produkte

|                |       |           |                   |      |
|----------------|-------|-----------|-------------------|------|
| Paraffingatsch | 3,75  | kg        | 24,4              | %    |
| Ol-Kondensat   | 1,70  | "         | 50,2              | %    |
| A.-K. Benzin   | 3,90  | "         | 25,4              | %    |
| Flüssige Prod. | 15,35 | "         |                   | 100% |
| Sywasser       | 22,90 | kg = 1,49 | x flüss. Produkte |      |

## Gesamtprodukt

|         |            |
|---------|------------|
| SB      | °C         |
| - 100°  | %          |
| - 200°  | %          |
| - 320°  | %          |
| Olefine | Vol. %     |
| - 200°  | 200 - 320° |

## Ausbeute

|                |      |             |      |                                    |                |
|----------------|------|-------------|------|------------------------------------|----------------|
| Flüssige Prod. | 29,0 | g Nm³ Sygas | 54,9 | g Nm³ Nutzgas (CO+H <sub>2</sub> ) | g Nm³ Idealgas |
| Gasol          |      | "           | "    | "                                  | "              |
| Gesamt-Produkt |      | "           | "    | "                                  | "              |
| Sywasser       |      | "           | "    | "                                  | "              |

## Bemerkungen:

000237

**Druckversuchsanlage** **Produktionsbericht vom 22./23. 8 1943**

Ofen-Nr. 11 Betriebsstunden 19 / 23,58  
 Füllung: 13 Gasdruck 20 atü  
 CO-Fe-Inhalt - kg Temperatur 221,5 atü 219 °C

Sp. W-Gas 289 Nm³  
 Restgas - Nm³  
 " " " " Nm³/h  
 " 15,2 Nm³/h  
 Kreislaufgas 525 Nm³  
 Kreislauf 1,82

Belastung 1,20 Nm³/kg.h Nm³/Norm.-Vol., h

| Analysen:                  | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>c</sub> -F | Litergewicht |
|----------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas                      | 4,1             | -    | 0,1            | 37,3 | 44,9           | 0,3             | 7,3            | =    | 7,17              |              |
| Restgas                    | 22,8            | 0,4  | 0,1            | 18,5 | 34,6           | 5,1             | 12,5           | 1,08 | 12,37             |              |
| <i>ammoniak</i>            |                 |      |                | 25,2 | 39,3           |                 |                |      |                   |              |
| <i>H<sub>2</sub> 69 an</i> |                 |      |                |      | 1,56           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 14,8 %  
 H<sub>2</sub>: CO im Sygas 1,29  
 H<sub>2</sub>: CO im Restgas 1,87  
 Verbrauch von H<sub>2</sub>: CO 0,79  
 Kontraktion nach Menge - %  
 " " N<sub>2</sub> 42,0 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 42,0 %

umgesetzt 41,3 %CO 43,7 %H<sub>2</sub> 55,8 %CO+H<sub>2</sub>  
 verflüssigt \_\_\_\_\_  
 Verfl.-Grad A \_\_\_\_\_  
 " " P 100 - 630,4 abgestellt wegen Strom - in Gesamtsfall 27,8

CH<sub>4</sub> + 2CmHn 10,0 CO<sub>2</sub> 36,0 bezogen auf CO-Umsatz

| Produkte       |   |               | Gesamtprodukt |              |
|----------------|---|---------------|---------------|--------------|
| Paraffingatsch | <u>3,36</u> kg                                  | <u>27,8</u> % | SB            | °C           |
| Ol-Kondensat   | <u>5,72</u> "                                   | <u>47,4</u> % | - 100°        | %            |
| A.-K. Benzin   | <u>3,00</u> "                                   | <u>24,8</u> % | - 200°        | %            |
| Flüssige Prod. | <u>12,02</u> "                                  | 100%          | - 320°        | %            |
| Sywasser       | <u>15,30</u> kg = <u>12,7</u> x flüss. Produkte |               | Olefine       | Vol. %       |
|                |   |               | - 200°        | , 200 - 320° |

**Ausbeute**  
 Flüssige Prod. 41,8 g Nm³ Sygas 49,0 g Nm³ Nutzgas (CO+H<sub>2</sub>) g/Nm³ Idealgas  
 Gasol " " " " " " " "  
 Gesamt-Produkt " " " " " " " "  
 Sywasser " " " " " " " "

**Bemerkungen:**

**000238**



| <b>Druckversuchsanlage</b>   |                 |                 |                    | <b>Produktionsbericht vom 20.12.8. 1943</b> |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
|--|-----------------|-----------------|--------------------|---|----------------|----------------------|----------------|------|-------------------|-------------|-----------|-----------------|-----------------|--------------------|-----------|----------------|-----------------|----------------|-------------|-------------------|-------------|-------|---------------|---|-----|------|-------|-----|-----|------|------|--|---------|------|-----|-----|------|------|-----|------|------|-------|--|----------|--|--|--|------|------|--|--|--|--|--|------------------------------|--|--|--|------|--|--|--|--|--|--|
| Ofen-Nr. 11  |                 |                 |                    | Betriebsstunden 24/2315                     |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Füllung: 13  |                 |                 |                    | Gasdruck 80 atü                             |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| O <sub>2</sub> -Fe-Inhalt: F kg  |                 |                 |                    | Temperatur 22,5 atü 219 °C                  |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| W-Gas 292 Nm <sup>3</sup>  |                 |                 |                    | Restgas 151 Nm <sup>3</sup>                 |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| " " " " "  |                 |                 |                    | " 6,3 Nm <sup>3</sup> /h                    |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| " " " " "  |                 |                 |                    | Kreislaufgas 684 Nm <sup>3</sup>            |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| " " " " " 13,2 Nm <sup>3</sup> /h  |                 |                 |                    | Kreislauf 2134                              |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Belastung: Nm <sup>3</sup> /kg.h 0,90  |                 |                 |                    | Nm <sup>3</sup> /Norm-Vol., h               |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th>Analysen:</th> <th>CO<sub>2</sub></th> <th>CmHn</th> <th>O<sub>2</sub></th> <th>CO</th> <th>H<sub>2</sub></th> <th>CH<sub>4</sub></th> <th>N<sub>2</sub></th> <th>C-Z</th> <th>N<sub>2</sub>-F</th> <th>Utergewicht</th> </tr> </thead> <tbody> <tr> <td>W Gas</td> <td>6,7</td> <td>-</td> <td>0,1</td> <td>37,9</td> <td>48,3</td> <td>0,3</td> <td>6,7</td> <td>-</td> <td>6,63</td> <td></td> </tr> <tr> <td>Restgas</td> <td>30,3</td> <td>0,6</td> <td>0,1</td> <td>17,5</td> <td>33,7</td> <td>5,4</td> <td>12,4</td> <td>1,17</td> <td>12,28</td> <td></td> </tr> <tr> <td>Spaltgas</td> <td></td> <td></td> <td></td> <td>23,6</td> <td>32,1</td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> <tr> <td>H<sub>2</sub>CO im Restgas</td> <td></td> <td></td> <td></td> <td>1,62</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> </tbody> </table> |                 |                 |                    |   |                |                      |                |      |                   |             | Analysen: | CO <sub>2</sub> | CmHn            | O <sub>2</sub>     | CO        | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z         | N <sub>2</sub> -F | Utergewicht | W Gas | 6,7           | - | 0,1 | 37,9 | 48,3  | 0,3 | 6,7 | -    | 6,63 |  | Restgas | 30,3 | 0,6 | 0,1 | 17,5 | 33,7 | 5,4 | 12,4 | 1,17 | 12,28 |  | Spaltgas |  |  |  | 23,6 | 32,1 |  |  |  |  |  | H <sub>2</sub> CO im Restgas |  |  |  | 1,62 |  |  |  |  |  |  |
| Analysen:  | CO <sub>2</sub> | CmHn            | O <sub>2</sub>     | CO  | H <sub>2</sub> | CH <sub>4</sub>      | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Utergewicht |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| W Gas  | 6,7             | -               | 0,1                | 37,9  | 48,3           | 0,3                  | 6,7            | -    | 6,63              |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Restgas  | 30,3            | 0,6             | 0,1                | 17,5  | 33,7           | 5,4                  | 12,4           | 1,17 | 12,28             |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Spaltgas   |                 |                 |                    | 23,6  | 32,1           |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| H <sub>2</sub> CO im Restgas   |                 |                 |                    | 1,62  |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Gesamt-Inerte (Idealgas) 13,8 %  |                 |                 |                    | Kontraktion nach Menge 48,3 %               |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| H <sub>2</sub> :CO im Sygas 1,28   |                 |                 |                    | " " N <sub>2</sub> 46,0 %                   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| H <sub>2</sub> :CO im Restgas 1,93   |                 |                 |                    | " " CO <sub>2</sub> - %                     |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Verbrauch von H <sub>2</sub> :CO 1,07  |                 |                 |                    | Durchschnittliche Kontraktion 47,2 %        |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th></th> <th>%CO</th> <th>%H<sub>2</sub></th> <th>%CO+H<sub>2</sub></th> </tr> </thead> <tbody> <tr> <td>umgesetzt</td> <td>75,5</td> <td>63,1</td> <td>68,6</td> </tr> <tr> <td>verflüssigt</td> <td></td> <td></td> <td></td> </tr> <tr> <td>Verfl.-Grad A</td> <td></td> <td></td> <td></td> </tr> <tr> <td>" " P</td> <td></td> <td></td> <td>26,0</td> </tr> </tbody> </table>  |                 |                 |                    |   |                |                      |                |      |                   |             |           | %CO             | %H <sub>2</sub> | %CO+H <sub>2</sub> | umgesetzt | 75,5           | 63,1            | 68,6           | verflüssigt |                   |             |       | Verfl.-Grad A |   |     |      | " " P |     |     | 26,0 |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
|  | %CO             | %H <sub>2</sub> | %CO+H <sub>2</sub> |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| umgesetzt  | 75,5            | 63,1            | 68,6               |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| verflüssigt  |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Verfl.-Grad A  |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| " " P  |                 |                 | 26,0               |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| CH <sub>4</sub> 8,9 CO <sub>2</sub> 38,4 bezogen auf CO-Umsatz   |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| <b>Produkte</b>  |                 |                 |                    |   |                | <b>Gesamtprodukt</b> |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Paraffingatsch 4,10 kg 28,8 %  |                 |                 |                    |   |                | SB °C                |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Ol-Kondensat 6,60 " 46,5 %   |                 |                 |                    |   |                | - 100° °C            |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| A.-K. Benzin 3,50 " 24,7 %   |                 |                 |                    |   |                | - 200° °C            |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Flüssige Prod. 14,20 " 100 %   |                 |                 |                    |   |                | - 320° °C            |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Sywasser 18,50 kg = 1,30 x flüss. Produkte   |                 |                 |                    |   |                | Olefine Vol. %       |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
|  |                 |                 |                    |   |                | - 200° , 200-320°    |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| <b>Ausbeute</b>  |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Flüssige Prod. 48,6 g-Nm <sup>3</sup> -Sygas 56,3 g-Nm <sup>3</sup> -Nutzgas (CO+H <sub>2</sub> ) 6,9 Nm <sup>3</sup> -Idealgas  |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Gasol " " " " " " " " " " " "  |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Gesamt-Produkt " " " " " " " " " " " "   |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| Sywasser " " " " " " " " " " " "   |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |
| <b>Bemerkungen:</b>  |                 |                 |                    |   |                |                      |                |      |                   |             |           |                 |                 |                    |           |                |                 |                |             |                   |             |       |               |   |     |      |       |     |     |      |      |  |         |      |     |     |      |      |     |      |      |       |  |          |  |  |  |      |      |  |  |  |  |  |                              |  |  |  |      |  |  |  |  |  |  |

000240



**Druckversuchsanlage**

Produktionsbericht vom 19./20. 8. 1943

Ofen-Nr. M  
 Füllung: 13  
 Fe-Inhalt: - kg

Betriebsstunden 24/22.91  
 Gasdruck 2.0 atü  
 Temperatur 22.5 atü 219 °C

W-Gas 30.1 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
18.5 " Nm<sup>3</sup>/h

Restgas 15.3 Nm<sup>3</sup>  
 " 6.4 " Nm<sup>3</sup>/h  
 Kreislaufgas 7.54 " Nm<sup>3</sup>  
 Kreislauf 8.50

Belastung - Nm<sup>3</sup>/kg,h 0.99 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                               | Nm <sup>3</sup> /kg,h |                               |                |       |                |                 |                |      | Nm <sup>3</sup> /Norm.-Vol., h |  | Litergewicht |
|---|-----------------------|-------------------------------|----------------|-------|----------------|-----------------|----------------|------|--------------------------------|--|--------------|
|   | CO <sub>2</sub>       | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO    | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F              |  |              |
| W-Gas                                   | 6.8                   | -                             | 0.1            | 34.7  | 48.2           | 0.3             | 6.9            | -    | 6.78                           |  |              |
| Restgas                                 | 30.1                  | 0.5                           | 0.1            | 14.9  | 133.4          | 5.3             | 12.7           | 1.17 | 12.57                          |  |              |
| <i>Handwritten: Halbes Kreislaufgas</i> |                       |                               |                | 83.6  | 37.6           |                 |                |      |                                |  |              |
|   |                       |                               |                | 11.59 |                |                 |                |      |                                |  |              |

Gesamt-Inerte (Idealgas) 14.1 %  
 H<sub>2</sub>, CO im Sygas 1.28  
 H<sub>2</sub>, CO im Restgas 1.27  
 Verbrauch von H<sub>2</sub>, CO 1.09

Kontraktion nach Menge 49.1 %  
 " " N<sub>2</sub> - %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 49.1 %

umgesetzt 15.9 %CO  
 verfügbar 64.7 %H<sub>2</sub>  
 Verfl.-Grad A 89.6 %CO+H<sub>2</sub>  
 " " P 29.4

CH<sub>4</sub> 2.9 bezogen auf CO-Umsatz  
 CO<sub>2</sub> 29.6

**Produkte**

Paraffingas 4.50 kg 26.8 %  
 Öl-Kondensat 7.95 " 44.5 %  
 A.-K. Benzin 4.30 " 25.4 %  
 Flüssige Prod. 16.45 " 100 %  
 Sywasser 1.10 kg = 1.26 x flüss. Produkte

**Gesamtprodukt**

SB - °C  
 - 100° - %  
 - 200° - %  
 - 320° - %  
 Olefine Vol. %  
 - 200° - ; 200-320° -

**Ausbeute**

Flüssige Prod. 55.6 g/Nm<sup>3</sup> Sygas 64.8 g/Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasöl " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

**Bemerkungen:**

000241





|   |                                     |                                     |  |  |                |                            |                                |             |                   |              |  |
|---|-------------------------------------|-------------------------------------|--|--|----------------|----------------------------|--------------------------------|-------------|-------------------|--------------|--|
| <b>Druckversuchsanlage</b>                    |                                     |                                     |  | <b>Produktionsbericht vom 16./17.8. 1943</b> |                |                            |                                |             |                   |              |  |
| Ofen-Nr. <u>11</u>                            |                                     |                                     |  | Betriebsstunden <u>24/23.19</u>              |                |                            |                                |             |                   |              |  |
| Füllung: <u>13</u>                            |                                     |                                     |  | Gasdruck <u>20</u> atü                       |                |                            |                                |             |                   |              |  |
| Co-Fe-Inhalt: <u>-</u> kg                     |                                     |                                     |  | Temperatur <u>22,5</u> atü <u>219</u> °C     |                |                            |                                |             |                   |              |  |
| Sy-W-Gas <u>303</u> Nm <sup>3</sup>           |                                     |                                     |  | Restgas <u>162</u> Nm <sup>3</sup>           |                |                            |                                |             |                   |              |  |
| " " " " " "                                   |                                     |                                     |  | " " " " " " <u>6.8</u> Nm <sup>3</sup> /h    |                |                            |                                |             |                   |              |  |
| " " " " " " <u>11.6</u> Nm <sup>3</sup> /h    |                                     |                                     |  | Kreislaufgas <u>75</u> Nm <sup>3</sup>       |                |                            |                                |             |                   |              |  |
| " " " " " " " "                               |                                     |                                     |  | Kreislauf <u>142.42</u>                      |                |                            |                                |             |                   |              |  |
| Belastung: <u>0.199</u> Nm <sup>3</sup> /kg,h |                                     |                                     |  | Nm <sup>3</sup> /Norm.-Vol., h               |                |                            |                                |             |                   |              |  |
| Analysen:                                     | CO <sub>2</sub>                     | CmHn                                | O <sub>2</sub>                         | CO   | H <sub>2</sub> | CH <sub>4</sub>            | N <sub>2</sub>                 | C-Z         | N <sub>2</sub> -F | Litergewicht |  |
| Sygas   | <u>6.9</u>                          | <u>-</u>                            | <u>0.1</u>                             | <u>37.2</u>                                  | <u>4.3</u>     | <u>0.3</u>                 | <u>6.7</u>                     | <u>-</u>    | <u>6.58</u>       |              |  |
| Restgas                                       | <u>29.4</u>                         | <u>0.4</u>                          | <u>0.1</u>                             | <u>16.5</u>                                  | <u>34.9</u>    | <u>4.7</u>                 | <u>12.0</u>                    | <u>1.89</u> | <u>11.58</u>      |              |  |
| O-Gas   |                                     |                                     |  | <u>24.0</u>                                  | <u>36.7</u>    |                            |                                |             |                   |              |  |
| Bildungswärme                                 |                                     |                                     |  | <u>161</u>                                   |                |                            |                                |             |                   |              |  |
| Gesamt-Inerte (Idealgas) <u>14.0</u> %        |                                     |                                     |  | Kontraktion nach Menge <u>46</u> %           |                |                            |                                |             |                   |              |  |
| H <sub>2</sub> +CO im Sygas <u>7.22</u>       |                                     |                                     |  | " " N <sub>2</sub> <u>44</u> %               |                |                            |                                |             |                   |              |  |
| H <sub>2</sub> +CO im Restgas <u>1.29</u>     |                                     |                                     |  | " " CO <sub>2</sub> <u>-</u> %               |                |                            |                                |             |                   |              |  |
| Verbrauch von H <sub>2</sub> : CO <u>10.5</u> |                                     |                                     |  | Durchschnittliche Kontraktion <u>0.75</u> %  |                |                            |                                |             |                   |              |  |
| umgesetzt                                     | %CO <u>76.2</u>                     |                                     |  | %H <sub>2</sub> <u>59.1</u>                  |                |                            | %CO+H <sub>2</sub> <u>0.21</u> |             |                   |              |  |
| verflüssigt                                   | _____                               |                                     |  | _____  |                |                            | _____                          |             |                   |              |  |
| Verfl.-Grad A                                 | _____                               |                                     |  | _____  |                |                            | _____                          |             |                   |              |  |
| " " P   | _____                               |                                     |  | _____  |                |                            | _____                          |             |                   |              |  |
| CH <sub>4</sub>                               | CmHn                                | CO <sub>2</sub>                     | bezogen auf CO-Umsatz                  |  |                |                            |                                |             |                   |              |  |
| <u>8.3</u>                                    | <u>33.3</u>                         |                                     |  |  |                |                            |                                |             |                   |              |  |
| <b>Produkte</b>                               |                                     |                                     |  |  |                | <b>Gesamtprodukt</b>       |                                |             |                   |              |  |
| Paraffingatsch                                | <u>5.00</u> kg                      | <u>2.8</u> %                        | t                                      |  |                | SB _____ °C                |                                |             |                   |              |  |
| Ol-Kondensat                                  | <u>1.25</u> "                       | <u>0.6</u> %                        | -                                      |  |                | 100° _____ %               |                                |             |                   |              |  |
| A.-K. Benzin                                  | <u>4.60</u> "                       | <u>2.6</u> %                        | -                                      |  |                | 200° _____ %               |                                |             |                   |              |  |
| Flüssige Prod.                                | <u>17.85</u> "                      | 100 %                               | -                                      |  |                | 320° _____ %               |                                |             |                   |              |  |
| Sywasser                                      | <u>20.40</u> kg = _____             | X flüss. Produkte                   | -                                      |  |                | Olefine Vol. %             |                                |             |                   |              |  |
|   |                                     |                                     | -                                      |  |                | 200° _____, 200-320° _____ |                                |             |                   |              |  |
| <b>Ausbeute</b>                               |                                     |                                     |  |  |                |                            |                                |             |                   |              |  |
| Flüssige Prod.                                | <u>58.8</u> g Nm <sup>3</sup> Sygas | <u>62</u> g Nm <sup>3</sup> Nutzgas | <u>60.1</u> g Nm <sup>3</sup> Idealgas |  |                |                            |                                |             |                   |              |  |
| Gasol   | " "                                 | " "                                 | " "                                    |  |                |                            |                                |             |                   |              |  |
| Gesamt-Produkt                                | " "                                 | " "                                 | " "                                    |  |                |                            |                                |             |                   |              |  |
| Sywasser                                      | " "                                 | " "                                 | " "                                    |  |                |                            |                                |             |                   |              |  |
| <b>Bemerkungen:</b>                           |                                     |                                     |  |  |                |                            |                                |             |                   |              |  |

000244



|                                       |      |  |     |                       |      |  |      |      |       |              |  |
|---------------------------------------|------|--|-----|-----------------------|------|--|------|------|-------|--------------|--|
| <b>Druckversuchsanlage</b>            |      | <b>Produktionsbericht vom</b> 14./15.8. 1943 |     |                       |      |  |      |      |       |              |  |
| Ofen-Nr. 11                           |      | Betriebsstunden 24/2471                      |     |                       |      |  |      |      |       |              |  |
| Füllung: 13.                          |      | Gasdruck: 12 atü                             |     |                       |      |  |      |      |       |              |  |
| Co-Fe-Inhalt: — kg                    |      | Temperatur: 32,5 atü 219°C                   |     |                       |      |  |      |      |       |              |  |
| Sy-W-Gas: 311 Nm³                     |      | Restgas: 205 Nm³                             |     |                       |      |  |      |      |       |              |  |
| " " " " " "                           |      | " " " " " " 8,6 Nm³/h                        |     |                       |      |  |      |      |       |              |  |
| " " " " " " 12,9 Nm³/h                |      | Kreislaufgas: 715 Nm³                        |     |                       |      |  |      |      |       |              |  |
| " " " " " " " "                       |      | Kreislauf: 1+2,46                            |     |                       |      |  |      |      |       |              |  |
| Belastung: 1                          |      | Nm³ / kg, h 1,02                             |     |                       |      |  |      |      |       |              |  |
| Nm³ / Norm.-Vol., h                   |      |  |     |                       |      |  |      |      |       |              |  |
| Analysen:                             | CO₂  | CmHn   | O₂  | CO                    | H₂   | CH₄  | N₂   | C-Z  | N₂-F  | Litergewicht |  |
| Sygas                                 | 6,3  | —  | 0,1 | 18,7                  | 47,7 | 0,3  | 6,9  | —    | 6,78  |              |  |
| Restgas                               | 21,0 | 0,4  | 0,1 | 25,3                  | 39,7 | 2,9  | 10,6 | 1,08 | 10,46 |              |  |
| O-Gas                                 |      |  |     | 29,3                  | 46,0 |  |      |      |       |              |  |
| H <sub>2</sub> O                      |      |  |     | 1,44                  |      |  |      |      |       |              |  |
| Gesamt-Inerte (Idealgas) 13,6 %       |      | Kontraktion nach Menge 34,0 %                |     |                       |      |  |      |      |       |              |  |
| H₂, CO im Sygas 1,75                  |      | " " N₂ 35,0 %                                |     |                       |      |  |      |      |       |              |  |
| H₂, CO im Restgas 1,57                |      | " " CO₂ — %                                  |     |                       |      |  |      |      |       |              |  |
| Verbrauch von H₂, CO 0,98             |      | Durchschnittliche Kontraktion 34,5 %         |     |                       |      |  |      |      |       |              |  |
| %CO                                   |      | %H₂  |     | %CO+H₂                |      |  |      |      |       |              |  |
| umgesetzt 57,2                        |      | 45,6   |     | 50,7                  |      |  |      |      |       |              |  |
| verflüssigt                           |      |  |     |                       |      |  |      |      |       |              |  |
| Verfl.-Grad A                         |      |  |     | 30,3                  |      |  |      |      |       |              |  |
| P                                     |      |  |     |                       |      |  |      |      |       |              |  |
| CH <sub>4</sub> , H <sub>2</sub> 17,2 |      | CO <sub>2</sub> 33,8                         |     | bezogen auf CO-Umsatz |      |  |      |      |       |              |  |
| <b>Produkte</b>                       |      |  |     |                       |      | <b>Gesamtprodukt</b>                                   |      |      |       |              |  |
| Paraffingatsch 2,50 kg 19 %           |      |  |     |                       |      | SB — °C  |      |      |       |              |  |
| Ol-Kondensat 6,15 " 47 %              |      |  |     |                       |      | — 100° %   |      |      |       |              |  |
| A.-K. Benzin 4,40 " 34 %              |      |  |     |                       |      | — 200° %   |      |      |       |              |  |
| Flüssige Prod. 13,05 " 100°           |      |  |     |                       |      | — 320° %   |      |      |       |              |  |
| Sywasser 12,57 kg = x flüss. Produkte |      |  |     |                       |      | Olefine Vol. %   |      |      |       |              |  |
|                                       |      |  |     |                       |      | — 200° , 200-320°                                      |      |      |       |              |  |
| <b>Ausbeute</b>                       |      |  |     |                       |      |  |      |      |       |              |  |
| Flüssige Prod. 46,0 g Nm³ Sygas       |      |  |     |                       |      | 48,6 g Nm³ Nutzgas (CO+H <sub>2</sub> ) g Nm³ Idealgas |      |      |       |              |  |
| Gasol " " " " " "                     |      |  |     |                       |      |  |      |      |       |              |  |
| Gesamt-Produkt " " " " " "            |      |  |     |                       |      |  |      |      |       |              |  |
| Sywasser " " " " " "                  |      |  |     |                       |      |  |      |      |       |              |  |
| <b>Bemerkungen:</b>                   |      |  |     |                       |      |  |      |      |       |              |  |

000246



# Druckversuchsanlage

Produktionsbericht vom 12.11.1943

Ofen-Nr. 11  
 Füllung: 13  
 Gb-Fe-Inhalt: — kg

Betriebsstunden 24/2125  
 Gasdruck 10 atü  
 Temperatur 22,5 atü 219 °C

Sy-W-Gas 302 Nm³  
 " " 12,6 Nm³/h

Restgas 195 Nm³  
 " " 8,1 Nm³/h  
 Kreislaufgas 285 Nm³  
 Kreislauf 1+2,6

Belastung: — Nm³/kg,h 0,98 Nm³/Norm-Vol., h

| Analysen:                   | Nm³/kg,h |      |     |      |      |     |      | Nm³/Norm-Vol., h |      |   | Litergewicht |
|-----------------------------|----------|------|-----|------|------|-----|------|------------------|------|---|--------------|
|                             | CO₂      | CmHn | O₂  | CO   | H₂   | CH₄ | N₂   | C-Z              | N₂-F |   |              |
| Sygas                       | 5,9      | —    | 0,1 | 39,0 | 48,0 | 0,3 | 6,7  | —                | 6,63 | — |              |
| Restgas                     | 23,3     | 0,4  | 0,1 | 24,9 | 28,8 | 3,2 | 10,1 | 1,10             | 12,7 | — |              |
| 0-Gas                       |          |      |     | 28,8 | 41,4 |     |      |                  |      |   |              |
| H <sub>2</sub> leb im 0-Gas |          |      |     |      | 14,4 |     |      |                  |      |   |              |

Gesamt-Inerte (Idealgas) 13 %  
 H₂, CO im Sygas 1,23  
 H₂, CO im Restgas 1,56  
 Verbrauch von H₂, CO 1,00

Kontraktion nach Menge 35,2 %  
 " " N₂ — %  
 " " CO₂ — %  
 Durchschnittliche Kontraktion 35,6 %

umgesetzt %CO 59,0 %H₂ 48,0 %CO+H₂ 53,0  
 verflüssigt — — —  
 Verfl.-Grad A — — —  
 " " P — — —

CH₄ + C<sub>m</sub>H<sub>n</sub> 7,6 CO₂ — bezogen auf CO-Umsatz

**Produkte**

|                |       |          |    |                   |
|----------------|-------|----------|----|-------------------|
| Paraffingatsch | 2,75  | kg       | 24 | %                 |
| Ol-Kondensat   | 6,9   | "        | 44 | %                 |
| A.-K. Benzin   | 5,10  | "        | 32 | %                 |
| Flüssige Prod. | 15,75 | "        |    | 100 %             |
| Sywasser       | 12,80 | kg = 0,4 |    | X flüss. Produkte |

**Gesamtprodukt**

|         |        |            |
|---------|--------|------------|
| SB      | —      | °C         |
| — 100°  | —      | %          |
| — 200°  | —      | %          |
| — 320°  | —      | %          |
| Olefine | Vol. % |            |
| — 200°  | —      | 200 - 320° |

**Ausbeute**

Flüssige Prod. 52,7 g Nm³ Sygas 62,0 g Nm³ Nutzgas (CO+H₂) g/Nm³ Idealgas  
 Gasol — " " " " " "  
 Gesamt-Produkt — " " " " " "  
 Sywasser — " " " " " "

**Bemerkungen:**

000248



| <b>Druckversuchsanlage</b>                               |                                       | <b>Produktionsbericht vom</b> 17./12.6. 1943  |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
|--|---------------------------------------|---|---|-------------|-----------------|-------------------------------|----------------|-------------|-------------------|-----------------|----------------|-----|-------------------|--------------|-----------|------------|----------|------------|-------------|-------------|------------|------------|----------|-------------|--|-------|-------------|------------|------------|-------------|-------------|------------|-------------|-------------|--------------|----------|---------|------------|------------|------------|-------------|-------------|------------|--|--|--|--|
| Ofen-Nr. <u>11</u>                                       | Betriebsstunden <u>24/2101</u>        | Gasdruck <u>10</u> atü  | Temperatur <u>22,5</u> atü <u>219.C</u> |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Füllung: <u>13</u>                                       | kg                                    | Restgas <u>193</u> Nm <sup>3</sup>  | " <u>8,1</u> Nm <sup>3</sup> /h         |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Ge-Fe-Inhalt: <u>-</u>                                   | kg                                    | Kreislaufgas <u>246</u> Nm <sup>3</sup>   | Kreislauf <u>1+2,5</u>                  |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| St-W-Gas: <u>297</u> Nm <sup>3</sup>                     |                                       | Belastung <u>0,98</u> Nm <sup>3</sup> /kg.h   | Nm <sup>3</sup> /Norm.-Vol., h          |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| <u>12,4</u> Nm <sup>3</sup> /h                           |                                       | <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th>Analysen:</th> <th>CO<sub>2</sub></th> <th>C<sub>m</sub>H<sub>n</sub></th> <th>O<sub>2</sub></th> <th>CO</th> <th>H<sub>2</sub></th> <th>CH<sub>4</sub></th> <th>N<sub>2</sub></th> <th>C-Z</th> <th>N<sub>2</sub>-F</th> <th>litergewicht</th> </tr> <tr> <td><u>11</u></td> <td><u>6,5</u></td> <td><u>-</u></td> <td><u>0,1</u></td> <td><u>38,3</u></td> <td><u>47,5</u></td> <td><u>0,3</u></td> <td><u>7,3</u></td> <td><u>-</u></td> <td><u>7,20</u></td> <td></td> </tr> <tr> <td>Sygas</td> <td><u>21,6</u></td> <td><u>0,3</u></td> <td><u>0,1</u></td> <td><u>24,5</u></td> <td><u>39,0</u></td> <td><u>2,3</u></td> <td><u>11,2</u></td> <td><u>1,15</u></td> <td><u>11,13</u></td> <td><u>-</u></td> </tr> <tr> <td>Restgas</td> <td><u>0,2</u></td> <td><u>0,1</u></td> <td><u>0,1</u></td> <td><u>28,4</u></td> <td><u>41,4</u></td> <td><u>1,4</u></td> <td></td> <td></td> <td></td> <td></td> </tr> </table> |   | Analysen:   | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO          | H <sub>2</sub>    | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | litergewicht | <u>11</u> | <u>6,5</u> | <u>-</u> | <u>0,1</u> | <u>38,3</u> | <u>47,5</u> | <u>0,3</u> | <u>7,3</u> | <u>-</u> | <u>7,20</u> |  | Sygas | <u>21,6</u> | <u>0,3</u> | <u>0,1</u> | <u>24,5</u> | <u>39,0</u> | <u>2,3</u> | <u>11,2</u> | <u>1,15</u> | <u>11,13</u> | <u>-</u> | Restgas | <u>0,2</u> | <u>0,1</u> | <u>0,1</u> | <u>28,4</u> | <u>41,4</u> | <u>1,4</u> |  |  |  |  |
| Analysen:  | CO <sub>2</sub>                       | C <sub>m</sub> H <sub>n</sub>   | O <sub>2</sub>                          | CO          | H <sub>2</sub>  | CH <sub>4</sub>               | N <sub>2</sub> | C-Z         | N <sub>2</sub> -F | litergewicht    |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| <u>11</u>  | <u>6,5</u>                            | <u>-</u>  | <u>0,1</u>                              | <u>38,3</u> | <u>47,5</u>     | <u>0,3</u>                    | <u>7,3</u>     | <u>-</u>    | <u>7,20</u>       |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Sygas  | <u>21,6</u>                           | <u>0,3</u>  | <u>0,1</u>                              | <u>24,5</u> | <u>39,0</u>     | <u>2,3</u>                    | <u>11,2</u>    | <u>1,15</u> | <u>11,13</u>      | <u>-</u>        |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Restgas  | <u>0,2</u>                            | <u>0,1</u>  | <u>0,1</u>                              | <u>28,4</u> | <u>41,4</u>     | <u>1,4</u>                    |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Gesamt-Inerte (Idealgas) <u>11,1</u> %                   |                                       | Kontraktion nach Menge <u>35,0</u> %  |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| H <sub>2</sub> : CO im Sygas <u>12,4</u>                 |                                       | " " N <sub>2</sub> <u>35,3</u> %  |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| H <sub>2</sub> : CO im Restgas <u>1,59</u>               |                                       | " " CO <sub>2</sub> <u>-</u> %  |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Verbrauch von H <sub>2</sub> : CO <u>0,99</u>            |                                       | Durchschnittliche Kontraktion <u>35,2</u> %   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| umgesetzt <u>57,0</u> % CO                               | <u>46,7</u> % H <sub>2</sub>          | <u>52,0</u> % CO+H <sub>2</sub>   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| verflüssigt  |                                       |   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Verfl.-Grad A  |                                       |   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| CH <sub>4</sub> <u>8,1</u> Nm <sup>3</sup>               | CO <sub>2</sub> <u>33,4</u>           | bezogen auf CO-Umsatz   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| <b>Produkte</b>  |                                       | <b>Gesamtprodukt</b>  |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Paraffingatsch. <u>2,45</u> kg                           | <u>12</u> %                           | SB <u>-</u> °C  |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Öl-Kondensat <u>6,90</u> "                               | <u>49</u> %                           | - 100° <u>-</u> %   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| A.-K. Benzin <u>4,90</u> "                               | <u>34</u> %                           | - 200° <u>-</u> %   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Flüssige Prod. <u>14,25</u>                              | 100 %                                 | - 320° <u>-</u> %   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Sywasser <u>12,80</u> kg = <u>0,90</u> x flüss. Produkte |                                       | Olefine Vol. %  |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
|  |                                       | - 200° <u>-</u> , 200-320° <u>-</u>   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| <b>Ausbeute</b>  |                                       |   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Flüssige Prod. <u>42,0</u> g Nm <sup>3</sup> Sygas       | <u>52,0</u> g Nm <sup>3</sup> Nutzgaz | <u>(Loth)</u> g/Nm <sup>3</sup> Idealgas  |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Gasol  |                                       |   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Gesamt-Produkt   |                                       |   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| Sywasser   |                                       |   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |
| <b>Bemerkungen:</b>                                      |                                       |   |   |             |                 |                               |                |             |                   |                 |                |     |                   |              |           |            |          |            |             |             |            |            |          |             |  |       |             |            |            |             |             |            |             |             |              |          |         |            |            |            |             |             |            |  |  |  |  |

000249

# Druckversuchsanlage

Produktionsbericht vom 10./11. 8. 1942

Ofen-Nr. 11  
 Füllung: 13.  
 Co-Fe-Inhalt: kg

Betriebsstunden 24/2022  
 Gasdruck 10 atü  
 Temperatur 22,5 atü 219°C

Sy-W-Gas 319 Nm<sup>3</sup>  
 " " " " " "  
 " 13.3 Nm<sup>3</sup>/h

Restgas 205 Nm<sup>3</sup>  
 " 8.5 Nm<sup>3</sup>/h  
 Kreislaufgas 806 Nm<sup>3</sup>  
 Kreislauf 1+2.53

Belastung Nm<sup>3</sup>/kg.h 1.05 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen: | Nm <sup>3</sup> /kg.h |      |                |      |                |                 |                |      |                   | Litergewicht |
|-----------|-----------------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
|           | CO <sub>2</sub>       | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F |              |
| Sygas     | 7.0                   | -    | 0.1            | 37.6 | 48.1           | 0.3             | 6.9            | -    | 6.77              |              |
| Restgas   | 22.1                  | 0.3  | 0.1            | 23.5 | 39.6           | 3.2             | 10.4           | 1.08 | 11.57             |              |
| O-Gas     | 16/100 im O-Gas       |      |                | 27.7 | 42.0           |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 1.22 %  
 H<sub>2</sub>:CO im Sygas 1.67  
 H<sub>2</sub>:CO im Restgas 1.01  
 Verbrauch von H<sub>2</sub>:CO 1.01

Kontraktion nach Menge 25.6 %  
 " " N<sub>2</sub> - %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 25.6 %

umgesetzt %CO 59.3 %H<sub>2</sub> 47.0 %CO+H<sub>2</sub> 52.4  
 verflüssigt  
 Verfl.-Grad A  
 " " P 29.6

CH<sub>4</sub> + CmHn 17.8 CO<sub>2</sub> 33.8 bezogen auf CO-Umsatz

## Produkte

Paraffingatsch 2.40 kg 18 %  
 Öl-Kondensat 6.30 " 47 %  
 A.-K. Benzin 4.70 " 35 %  
 Flüssige Prod. 13.40 100 %  
 Sywasser 13.00 kg = 0.97 x flüss. Produkte

## Gesamtprodukt

SB °C  
 - 100° %  
 - 200° %  
 - 320° %  
 Olefine Vol. %  
 - 200° ; 200-320°

## Ausbeute

Flüssige Prod. 42.0 g Nm<sup>3</sup> Sygas 49.0 g Nm<sup>3</sup> Nutzgas  
 Gasöl " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

000250



|  |   |   |  |         |                |                      |                |      |                   |              |
|--|---|---|--|---------|----------------|----------------------|----------------|------|-------------------|--------------|
| <b>Druckversuchsanlage</b>                   |   | <b>Produktionsbericht vom</b> 8. / 9. 1943  |  |         |                |                      |                |      |                   |              |
| Ofen-Nr. <u>M</u>                            |   | Betriebsstunden <u>24/2029</u>              |  |         |                |                      |                |      |                   |              |
| Füllung: <u>M</u>                            |   | Gasdruck <u>11</u> atü                      |  |         |                |                      |                |      |                   |              |
| Co-Fe-Inhalt _____ kg                        |   | Temperatur <u>22,5</u> atü <u>219.c</u>     |  |         |                |                      |                |      |                   |              |
| Sy-W-Gas <u>2,98</u> Nm <sup>3</sup>         |   | Restgas <u>18,1</u> Nm <sup>3</sup>         |  |         |                |                      |                |      |                   |              |
| " " " " _____ Nm <sup>3</sup>                |   | " " " " <u>9,5</u> Nm <sup>3</sup> /h       |  |         |                |                      |                |      |                   |              |
| " " " " <u>10,4</u> Nm <sup>3</sup> /h       |   | Kreislaufgas <u>17,55</u> Nm <sup>3</sup>   |  |         |                |                      |                |      |                   |              |
| " " " " _____ Nm <sup>3</sup>                |   | Kreislauf <u>17,53</u>                      |  |         |                |                      |                |      |                   |              |
| Belastung _____ Nm <sup>3</sup> /kg,h        |   | _____ Nm <sup>3</sup> /Norm.-Vol., h        |  |         |                |                      |                |      |                   |              |
| <b>Analysen:</b>                             | CO <sub>2</sub>                                 | CmHn  | O <sub>2</sub>                                       | CO      | H <sub>2</sub> | CH <sub>4</sub>      | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
| W  | 6,5   | -   | 0,1  | 37,5    | 42,6           | 0,3                  | 7,0            | -    | 2,33              | -            |
| Sygas  | 2,8   | 0,4   | 0,1  | 24,0    | 29,2           | 3,2                  | 11,4           | 1,10 | 11,31             | -            |
| Restgas                                      |   |   |  |         |                |                      |                |      |                   |              |
| O-Gas  |   |   |  | 22,9    | 4,7            |                      |                |      |                   |              |
| H <sub>2</sub> CO im O-Gas                   |   |   |  | 1,50    |                |                      |                |      |                   |              |
| Gesamt-Inerte (Idealgas) <u>14,6</u> %       |   | Kontraktion nach Menge <u>39,3</u> %        |  |         |                |                      |                |      |                   |              |
| H <sub>2</sub> :CO im Sygas <u>1,26</u>      |   | " " N <sub>2</sub> <u>36,2</u> %            |  |         |                |                      |                |      |                   |              |
| H <sub>2</sub> :CO im Restgas <u>1,63</u>    |   | " " CO <sub>2</sub> _____ %                 |  |         |                |                      |                |      |                   |              |
| Verbrauch von H <sub>2</sub> :CO <u>1,02</u> |   | Durchschnittliche Kontraktion <u>37,7</u> % |  |         |                |                      |                |      |                   |              |
| umgesetzt                                    | <u>60,3</u> %CO                                 | <u>48,8</u> %H <sub>2</sub>                 | <u>53,8</u> %CO+H <sub>2</sub>                       |         |                |                      |                |      |                   |              |
| verflüssigt                                  |   |   |  |         |                |                      |                |      |                   |              |
| Verfl.-Grad A                                |   |   |  |         |                |                      |                |      |                   |              |
| " " P  |   |   | <u>32,1</u>  |         |                |                      |                |      |                   |              |
| CH <sub>4</sub> +CmHn                        | <u>17,4</u>                                     | CO <sub>2</sub>                             | <u>29,8</u> bezogen auf CO-Umsatz                    |         |                |                      |                |      |                   |              |
| <b>Produkte</b>                              |   |   |  |         |                | <b>Gesamtprodukt</b> |                |      |                   |              |
| Paraffingatsch                               | <u>2,80</u> kg                                  | <u>2,0</u>                                  | %  | SB      | °C             |                      |                |      |                   |              |
| Ol-Kondensat                                 | <u>6,30</u> "                                   | <u>4,5</u>                                  | %  | - 100°  | %              |                      |                |      |                   |              |
| A.-K. Benzin                                 | <u>4,80</u> "                                   | <u>3,5</u>                                  | %  | - 200°  | %              |                      |                |      |                   |              |
| Flüssige Prod.                               | <u>13,90</u>                                    |   | 100%   | - 320°  | %              |                      |                |      |                   |              |
| Sywasser                                     | <u>13,10</u> kg = <u>0,94</u> x flüss. Produkte |   |  | Olefine | Vol. %         |                      |                |      |                   |              |
|  |   |   |  | - 200°  | 200 - 320°     |                      |                |      |                   |              |
| <b>Ausbeute</b>                              |   |   |  |         |                |                      |                |      |                   |              |
| Flüssige Prod.                               | <u>46,6</u> g Nm <sup>3</sup> Sygas             | <u>54</u> g Nm <sup>3</sup> Nutzgas         | <u>(CO+H<sub>2</sub>)</u> g Nm <sup>3</sup> Idealgas |         |                |                      |                |      |                   |              |
| Gasol  | " "   | " "   | " "  |         |                |                      |                |      |                   |              |
| Gesamt-Produkt                               | " "   | " "   | " "  |         |                |                      |                |      |                   |              |
| Sywasser                                     | " "   | " "   | " "  |         |                |                      |                |      |                   |              |
| <b>Bemerkungen:</b>                          |   |   |  |         |                |                      |                |      |                   |              |

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**Druckversuchsanlage**

**Produktionsbericht vom** 4/5 8. 1943

Ofen-Nr. M  
 Füllung: 13  
 Fe-Inhalt: - kg

Betriebsstunden 24 / 1933  
 Gasdruck 10 atü  
 Temperatur 82,5 atü 219 °C

W-Gas 304 Nm<sup>3</sup>  
 " " " " " " " "  
 " " " " " " " "  
 " 12,4 Nm<sup>3</sup>/h

Restgas 186 Nm<sup>3</sup>  
 " 4,8 Nm<sup>3</sup>/h  
 Kreislaufgas 683 Nm<sup>3</sup>  
 Kreislauf - 3,24

Belastung 1,00 Nm<sup>3</sup> / kg, h Nm<sup>3</sup> / Norm.-Vol., h

| Analysen:               | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Sygas                   | 8,0             | -                             | 0,1            | 36,3 | 42,3           | 0,3             | 7,0            | -    | 6,84              |              |
| Restgas                 | 24,1            | 0,4                           | 0,1            | 21,3 | 39,5           | 3,5             | 11,1           | 1,11 | 11,03             |              |
| Wasserdampf             |                 |                               |                | 26,0 | 42,2           |                 |                |      |                   |              |
| H <sub>2</sub> im Sygas |                 |                               |                |      | 6,8            |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 15,4 %  
 H<sub>2</sub>CO im Sygas 1,33  
 H<sub>2</sub>CO im Restgas 1,35  
 Verbrauch von H<sub>2</sub>: CO 1,03

Kontraktion nach Menge 38,8 %  
 " " N<sub>2</sub> 37,4 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 38,3 %

|               | %CO         | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|---------------|-------------|-----------------|--------------------|
| umgesetzt     | <u>67,0</u> | <u>49,5</u>     | <u>55,7</u>        |
| verflüssigt   |             |                 |                    |
| Verfl.-Grad A |             |                 |                    |
| " " P         |             |                 | <u>37,0</u>        |

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 2,0 CO<sub>2</sub> 24,8 bezogen auf CO-Umsatz

**Produkte**

Paraffingatsch 2,21 kg 23,0 %  
 Öl-Kondensat 4,90 " 52,2 %  
 A.-K. Benzin 4,50 " 47,0 %  
 Flüssige Prod. 12,21 " 100 %  
 Sywasser 13,00 kg = 1,06 x flüss. Produkte

**Gesamtprodukt**

SB - °C  
 - 100° - %  
 - 200° - %  
 - 320° - %  
 Olefine 7 Vol. %  
 - 200° - ; 200 - 320° -

**Ausbeute**

Flüssige Prod. 40,2 g Nm<sup>3</sup> Sygas 44,5 g Nm<sup>3</sup> Nutzas (60-70) g/Nm<sup>3</sup> Idealgas  
 Gasol " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

**Bemerkungen:**

000256











**Druckversuchsanlage**

Produktionsbericht vom 30.1.31/4 1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt: kg

Betriebsstunden 20/1813  
 Gasdruck 10 atü  
 Temperatur 82,5 atü 819 °C

Sy-W-Gas 849 Nm<sup>3</sup>  
 12,5 Nm<sup>3</sup>/h

Restgas 182 Nm<sup>3</sup>  
 Kreislaufgas 590 Nm<sup>3</sup>  
 Kreislauf 2,37

Belastung Nm<sup>3</sup>/kg.h 0,99 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:              | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| W <sub>Sygas</sub>     | 6,9             | -                             | 0,1            | 34,6 | 47,4           | 0,3             | 7,4            | -    | 7,88              | -            |
| Restgas                | 81,9            | 0,4                           | 0,1            | 83,6 | 39,5           | 0,1             | 11,4           | 1,07 | 11,35             | -            |
| Amalgam                |                 |                               |                | 87,8 | 42,0           |                 |                |      |                   |              |
| Na 100 mm Kreislaufgas |                 |                               |                | 1,51 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 1,44 %  
 H<sub>2</sub>:CO im Sygas 1,24  
 H<sub>2</sub>:CO im Restgas 1,67  
 Kontraktion nach Menge  
 N<sub>2</sub>  
 CO<sub>2</sub>  
 Verbrauch von H<sub>2</sub>:CO  
 Durchschnittliche Kontraktion

umgesetzt %CO %H<sub>2</sub> %CO+H<sub>2</sub>  
 verflüssigt  
 Verfl.-Grad A

Stilbestand von 115 - 500 g wegen Strom- u. Gasausfall

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> bezogen auf CO-Umsatz

**Produkte**

Paraffingatsch 2,31 kg 2,42 %  
 Öl-Kondensat 3,70 " 3,90 %  
 A-K. Benzin 3,50 " 3,68 %  
 Flüssige Prod. 9,51 100 %  
 Sywasser 10,00 kg = 1,05 x flüss. Produkte

**Gesamtprodukt**

SB °C  
 - 100° %  
 - 200° %  
 - 320° %  
 Olefine Vol. %  
 - 200° ; 200 - 320°

**Ausbeute**

Flüssige Prod. g/Nm<sup>3</sup> Sygas g/Nm<sup>3</sup> Nutzgas g/Nm<sup>3</sup> Idealgas  
 Gasöl  
 Gesamt-Produkt  
 Sywasser

**Bemerkungen:**

000261





**Druckversuchsanlage** **Produktionsbericht vom 26./27.7. 1943**

|                   |                            |
|-------------------|----------------------------|
| Ofen-Nr. 11       | Betriebsstunden 24/ 1762   |
| Füllung: 13       | Gasdruck 10 atü            |
| Co-Fe-Inhalt - kg | Temperatur 22,5 atü 219 °C |

|                              |                                  |
|------------------------------|----------------------------------|
| Sy-W-Gas 301 Nm <sup>3</sup> | Restgas 187 Nm <sup>3</sup>      |
| " " " " "                    | " 7,8 Nm <sup>3</sup> /h         |
| " " " " "                    | Kreislaufgas 706 Nm <sup>3</sup> |
| 12,6 Nm <sup>3</sup> /h      | Kreislauf 2,34                   |

Belastung - Nm<sup>3</sup>/kg.h 0,99 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                          | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                          | 7,1             | -                             | 0,1            | 37,3 | 48,6           | 0,3             | 6,7            | -    | 6,53              |              |
| Restgas                            | 23,6            | 0,3                           | 0,1            | 22,1 | 39,4           | 3,7             | 10,8           | 1,15 | 10,67             |              |
| Kreislaufgas                       |                 |                               |                | 26,6 | 42,2           |                 |                |      |                   |              |
| H <sub>2</sub> /CO im Kreislaufgas |                 |                               |                | 1,59 |                |                 |                |      |                   |              |

|  |                                      |
|--|--------------------------------------|
| Gesamt-Inerte (Idealgas) 14,1 %        | Kontraktion nach Menge 37,9 %        |
| H <sub>2</sub> : CO im Sygas 1,30      | " N <sub>2</sub> 38,7 %              |
| H <sub>2</sub> : CO im Restgas 1,78    | " CO - %                             |
| Verbrauch von H <sub>2</sub> : CO 1,05 | Durchschnittliche Kontraktion 38,3 % |

|                     |                       |                          |
|---------------------|-----------------------|--------------------------|
| umgesetzt 63,5 % CO | 50,0 % H <sub>2</sub> | 56,0 % CO+H <sub>2</sub> |
| verflüssigt         |                       |                          |
| Verfl.-Grad A       |                       |                          |
| " " P               |                       | 32,2                     |

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 8,4 CO<sub>2</sub> 31,5 bezogen auf CO-Umsatz

| Produkte       |                 |                   |  | Gesamtprodukt |            |
|----------------|-----------------|-------------------|--|---------------|------------|
| Paraffingatsch | 3,30 kg         | 22,4 %            |  | SB            | °C         |
| Cl-Kondensat   | 6,10 "          | 41,5 %            |  | - 100°        | %          |
| A.-K. Benzin   | 5,30 "          | 36,1 %            |  | - 200°        | %          |
| Flüssige Prod. | 14,70 "         | 100%              |  | - 320°        | %          |
| Sywasser       | 12,90 kg = 0,88 | x flüss. Produkte |  | Olefine       | Vol. %     |
|                |                 |                   |  | - 200°        | , 200-320° |

**Ausbeute**

|                |                              |   |                            |
|----------------|------------------------------|---|----------------------------|
| Flüssige Prod. | 48,9 g Nm <sup>3</sup> Sygas | 57,0 g Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) | g Nm <sup>3</sup> Idealgas |
| Gasol          | " "                          | " "   | " "                        |
| Gesamt-Produkt | " "                          | " "   | " "                        |
| Sywasser       | " "                          | " "   | " "                        |

**Bemerkungen:**

000264

Ofen wird mit Wassergas im Kreislauf gefahren.



| Druckversuchsanlage                                 |                 | Produktionsbericht vom 25./26.7. 1943                                |                   |                           |   |                      |                    |      |                   |               |  |
|---|-----------------|--|-------------------|---------------------------|---|----------------------|--------------------|------|-------------------|---------------|--|
| Ofen-Nr. 11   |                 | Betriebsstunden 21/1738  |                   |                           |   |                      |                    |      |                   |               |  |
| Füllung 13  |                 | Gasdruck 10 atü  |                   |                           |   |                      |                    |      |                   |               |  |
| C <sub>2</sub> -Fe-Inhalt — kg                      |                 | Temperatur 21,5 atü 217 °C   |                   |                           |   |                      |                    |      |                   |               |  |
| Sy-W-Gas 305 Nm <sup>3</sup>                        |                 | Restgas 202 Nm <sup>3</sup>  |                   |                           |   |                      |                    |      |                   |               |  |
| " " " "   |                 | " 9,6 Nm <sup>3</sup> /h   |                   |                           |   |                      |                    |      |                   |               |  |
| " " " "   |                 | Kreislaufgas 661 Nm <sup>3</sup>                                     |                   |                           |   |                      |                    |      |                   |               |  |
| " 14,5 Nm <sup>3</sup> /h                           |                 | Kreislauf 2,16   |                   |                           |   |                      |                    |      |                   |               |  |
| Belastung — Nm <sup>3</sup> /kg.h                   |                 | 1,14 Nm <sup>3</sup> /Norm-Vol., h                                   |                   |                           |   |                      |                    |      |                   |               |  |
| Analysen:   | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub>  | O <sub>2</sub>    | CO                        | H <sub>2</sub>                                  | CH <sub>4</sub>      | N <sub>2</sub>     | C-Z  | N <sub>2</sub> -F | Liegengewicht |  |
| Wassergas   | 6,3             | —  | 0,1               | 38,4                      | 47,7  | 0,3                  | 7,2                | —    | 7,13              |               |  |
| Restgas   | 23,0            | 0,2  | 0,1               | 23,3                      | 38,5  | 3,6                  | 11,3               | 1,08 | 11,22             |               |  |
| Kreislaufgas  |                 |  |                   | 28,0                      | 41,4  |                      |                    |      |                   |               |  |
| H <sub>2</sub> /CO im Kreislaufgas                  |                 | 1,48   |                   |                           |   |                      |                    |      |                   |               |  |
| Gesamt-Inerte (Idealgas) 13,9 %                     |                 | Kontraktion nach Menge 33,8 %  |                   |                           |   |                      |                    |      |                   |               |  |
| H <sub>2</sub> /CO im Sygas 1,24                    |                 | " " N <sub>2</sub> 36,5 %  |                   |                           |   |                      |                    |      |                   |               |  |
| H <sub>2</sub> /CO im Restgas 1,65                  |                 | " " CO <sub>2</sub> — %  |                   |                           |   |                      |                    |      |                   |               |  |
| Verbrauch von H <sub>2</sub> : CO 0,98              |                 | Durchschnittliche Kontraktion 35,2 %                                 |                   |                           |   |                      |                    |      |                   |               |  |
|   | %CO             |  |                   |                           |   | %H <sub>2</sub>      | %CO+H <sub>2</sub> |      |                   |               |  |
| umgesetzt   | 60,6            |  |                   |                           |   | 47,5                 | 52,3               |      |                   |               |  |
| verflüssigt   |                 |  |                   |                           |   |                      |                    |      |                   |               |  |
| Verf.-Grad A  |                 | Stillstand wegen Stromausfall von 0 <sup>30</sup> -3 <sup>15</sup> h |                   |                           |   |                      |                    |      |                   |               |  |
| " " P   |                 |  |                   |                           |   |                      |                    |      |                   |               |  |
| CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub> 8,7 |                 | CO <sub>2</sub> 37,0   |                   | bezogen auf CO-Umsatz     |   |                      |                    |      |                   |               |  |
| <b>Produkte</b>                                     |                 |  |                   |                           |   | <b>Gesamtprodukt</b> |                    |      |                   |               |  |
| Paraffingatsch                                      | 3,60            | kg   | 27,0              | %                         | SB  | °C                   |                    |      |                   |               |  |
| Ol-Kondensat  | 5,75            | "  | 43,0              | %                         | — 100°  | %                    |                    |      |                   |               |  |
| A.-K. Benzin  | 4,00            | "  | 30,0              | %                         | — 200°  | %                    |                    |      |                   |               |  |
| Flüssige Prod.                                      | 13,35           | "  | 100%              |                           | — 320°  | %                    |                    |      |                   |               |  |
| Sywasser  | 11,50           | kg =   | X flüss. Produkte |                           |   | Olefine              | Vol. %             |      |                   |               |  |
|   |                 |  |                   |                           | — 200°  | ; 200-320°           |                    |      |                   |               |  |
| <b>Ausbeute</b>                                     |                 |  |                   |                           |   |                      |                    |      |                   |               |  |
| Flüssige Prod.                                      | 43,8            | g Nm <sup>3</sup> Sygas  | 50,9              | g Nm <sup>3</sup> Nutzgas | (CO+H <sub>2</sub> ) g Nm <sup>3</sup> Idealgas |                      |                    |      |                   |               |  |
| Gasol   |                 | "  | "                 | "                         | " "   |                      |                    |      |                   |               |  |
| Gesamt-Produkt                                      |                 | "  | "                 | "                         | " "   |                      |                    |      |                   |               |  |
| Sywasser  |                 | "  | "                 | "                         | " "   |                      |                    |      |                   |               |  |
| <b>Bemerkungen:</b>                                 |                 |  |                   |                           |   |                      |                    |      |                   |               |  |
| 000265  |                 |  |                   |                           |   |                      |                    |      |                   |               |  |
| Ofen wird mit Wassergas im Kreislauf gefahren.      |                 |  |                   |                           |   |                      |                    |      |                   |               |  |





| Druckversuchsanlage                            |                                   | Produktionsbericht vom 22./23.7. 1943 |                        |                       |      |                      |      |      |       |              |  |
|--|-----------------------------------|---------------------------------------|------------------------|-----------------------|------|----------------------|------|------|-------|--------------|--|
| Ofen-Nr. 11                                    | Betriebsstunden 24/1669           |                                       |                        |                       |      |                      |      |      |       |              |  |
| Füllung: 13                                    | Gasdruck 10 atü                   |                                       |                        |                       |      |                      |      |      |       |              |  |
| Co-Fe-Inhalt: - kg                             | Temperatur 22,5 atü 219 °C        |                                       |                        |                       |      |                      |      |      |       |              |  |
| W-Gas 295 Nm³                                  | Restgas 181 Nm³                   |                                       |                        |                       |      |                      |      |      |       |              |  |
| " " " " "                                      | " 7,5 Nm³/h                       |                                       |                        |                       |      |                      |      |      |       |              |  |
| " " " " "                                      | Kreislaufgas 758 Nm³              |                                       |                        |                       |      |                      |      |      |       |              |  |
| 12,3 Nm³/h                                     | Kreislauf 2,57                    |                                       |                        |                       |      |                      |      |      |       |              |  |
| Belastung - Nm³/kg, h 0,97 Nm³/Norm.-Vol., h   |                                   |                                       |                        |                       |      |                      |      |      |       |              |  |
| Analysen:                                      | CO₂                               | CmHn                                  | O₂                     | CO                    | H₂   | CH₄                  | N₂   | C-Z  | N₂-F  | Litergewicht |  |
| Wassergas                                      | 6,7                               | -                                     | 0,1                    | 37,7                  | 48,5 | 0,3                  | 6,7  | -    | 6,57  |              |  |
| Restgas  | 22,8                              | 0,3                                   | 0,1                    | 22,7                  | 39,6 | 3,7                  | 10,6 | 1,15 | 10,53 |              |  |
| Kreislaufgas                                   |                                   |                                       |                        | 26,9                  | 42,1 |                      |      |      |       |              |  |
| H₂/CO im Kreislaufgas                          |                                   |                                       |                        | 1,57                  |      |                      |      |      |       |              |  |
| Gesamt-Inerte (Idealgas)                       | 13,8 %                            | Kontraktion nach Menge                |                        |                       |      | 38,6 %               |      |      |       |              |  |
| H₂:CO im Sygas                                 | 1,29                              | " " N₂                                |                        |                       |      | 37,6 %               |      |      |       |              |  |
| H₂:CO im Restgas                               | 1,74                              | " " CO₂                               |                        |                       |      | - %                  |      |      |       |              |  |
| Verbrauch von H₂:CO                            | 1,02                              | Durchschnittliche Kontraktion         |                        |                       |      | 38,1 %               |      |      |       |              |  |
| umgesetzt                                      | %CO 62,6                          | %H₂ 49,5                              | %CO+H₂ 55,2            |                       |      |                      |      |      |       |              |  |
| verflüchtigt                                   |                                   |                                       |                        |                       |      |                      |      |      |       |              |  |
| Verfl.-Grad A                                  |                                   |                                       |                        |                       |      |                      |      |      |       |              |  |
| " " P  |                                   |                                       |                        |                       | 32,4 |                      |      |      |       |              |  |
| CH₄ + CnHn                                     | 8,4                               | CO₂                                   | 26,2                   | bezogen auf CO-Umsatz |      |                      |      |      |       |              |  |
| <b>Produkte</b>                                |                                   |                                       |                        |                       |      | <b>Gesamtprodukt</b> |      |      |       |              |  |
| Paraffingatsch                                 | 3,80 kg                           | 26,4 %                                | SB                     |                       |      | °C                   |      |      |       |              |  |
| Cl-Kondensat                                   | 6,00 "                            | 41,7 %                                | - 100°                 |                       |      | %°                   |      |      |       |              |  |
| A.-K. Benzin                                   | 4,60 "                            | 31,9 %                                | - 200°                 |                       |      | %°                   |      |      |       |              |  |
| Flüssige Prod.                                 | 14,40                             | 100 %                                 | - 320°                 |                       |      | %°                   |      |      |       |              |  |
| Sywasser                                       | 12,60 kg = 0,88 X flüss. Produkte |                                       | Olefine                |                       |      | Vol. %               |      |      |       |              |  |
|  |                                   |                                       | - 200°                 |                       |      | , 200-320°           |      |      |       |              |  |
| <b>Ausbeute</b>                                |                                   |                                       |                        |                       |      |                      |      |      |       |              |  |
| Flüssige Prod.                                 | 48,8 g Nm³ Sygas                  | 56,6 g Nm³ Nutzgas                    | (CO+H₂) g/Nm³ Idealgas |                       |      |                      |      |      |       |              |  |
| Gasol  | " " "                             | " " "                                 | " " "                  |                       |      |                      |      |      |       |              |  |
| Gesamt-Produkt                                 | " " "                             | " " "                                 | " " "                  |                       |      |                      |      |      |       |              |  |
| Sywasser                                       | " " "                             | " " "                                 | " " "                  |                       |      |                      |      |      |       |              |  |
| <b>Bemerkungen:</b>                            |                                   |                                       |                        |                       |      |                      |      |      |       |              |  |
| 000268   |                                   |                                       |                        |                       |      |                      |      |      |       |              |  |
| Ofen wird mit Wassergas im Kreislauf gefahren. |                                   |                                       |                        |                       |      |                      |      |      |       |              |  |



**Druckversuchsanlage** **Produktionsbericht vom** 20./21.7. 1943

|                    |                          |
|--------------------|--------------------------|
| Ofen-Nr. 11        | Betriebsstunden 24/1621  |
| Füllung: 13        | Gasdruck 10 atü          |
| Co-Fe-Inhalt: - kg | Temperatur 20 atü 214 °C |

|                  |                      |
|------------------|----------------------|
| Sy-W-Gas 302 Nm³ | Restgas 193 Nm³      |
| " " " " " "      | " 8,0 Nm³/h          |
| " " " " " "      | Kreislaufgas 776 Nm³ |
| " 12,6 Nm³/h     | Kreislauf 2,56       |

Belastung: - Nm³/kg,h 1,00 Nm³/Norm.-Vol.,h

| Analysen:                          | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C <sub>2</sub> -Z | N <sub>2</sub> -F | Litergewicht |
|------------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|-------------------|-------------------|--------------|
| Wassergas                          | 7,1             | -    | 0,1            | 37,5 | 49,0           | 0,3             | 6,0            | -                 | 5,97              |              |
| Sygas                              | 20,8            | 0,3  | 0,1            | 25,6 | 41,7           | 2,5             | 9,0            | 1,09              | 8,93              |              |
| Restgas                            |                 |      |                | 29,0 | 43,7           |                 |                |                   |                   |              |
| Kreislaufgas                       |                 |      |                |      |                |                 |                |                   |                   |              |
| H <sub>2</sub> /CO im Kreislaufgas |                 |      |                | 1,50 |                |                 |                |                   |                   |              |

|  |                                      |
|--|--------------------------------------|
| Gesamt-Inerte (Idealgas) 13,5 %        | Kontraktion nach Menge 36,0 %        |
| H <sub>2</sub> :CO im Sygas 1,31       | " " N <sub>2</sub> 33,3 %            |
| H <sub>2</sub> :CO im Restgas 1,63     | " " CO <sub>2</sub> - %              |
| Verbrauch von H <sub>2</sub> : CO 0,99 | Durchschnittliche Kontraktion 34,7 % |

|               |             |                         |                            |
|---------------|-------------|-------------------------|----------------------------|
| umgesetzt     | %CO<br>55,5 | %H <sub>2</sub><br>41,8 | %CO+H <sub>2</sub><br>47,8 |
| verflüsig     | -----       | -----                   | -----                      |
| Verfl.-Grad A | -----       | -----                   | -----                      |
| " " P         | -----       | -----                   | 39,0                       |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 6,4 CO<sub>2</sub> 31,0 bezogen auf CO-Umsatz

| Produkte                                   | Gesamtprodukt                 |
|--|-------------------------------|
| Paraffingatsch 3,30 kg 21,4 %              | SB ----- °C                   |
| Ol-Kondensat 6,90 " 44,8 %                 | - 100° ----- %                |
| A.-K. Benzin 5,20 " 33,8 %                 | - 200° ----- %                |
| Flüssige Prod. 15,40 100 %                 | - 320° ----- %                |
| Sywasser 13,20 kg = 0,86 × flüss. Produkte | Olefine Vol. %                |
|  | - 200° ----- ; 200-320° ----- |

**Ausbeute**

|                                 |   |                |
|---------------------------------|---|----------------|
| Flüssige Prod. 51,0 g Nm³ Sygas | 59,0 g Nm³ Nutzgas (CO+H <sub>2</sub> ) | g/Nm³ Idealgas |
| Gasol                           | " " "                                   | " " "          |
| Gesamt-Produkt                  | " " "                                   | " " "          |
| Sywasser                        | " " "                                   | " " "          |

**Bemerkungen:**

000270

Ofen wird mit Wassergas im Kreislauf gefahren.













NO. 0000276

BLANK

**Druckversuchsanlage**

**Produktionsbericht vom** 14./15.7. 1943

|                  |                          |
|------------------|--------------------------|
| Ofen-Nr. 11      | Betriebsstunden 24/1477  |
| Füllung: 13      | Gasdruck 10 atü          |
| Co-Fe-Inhalt: kg | Temperatur 20 atü 214 °C |

|                    |                      |
|--------------------|----------------------|
| Sy-W-Gas 288 Nm³   | Restgas 187 Nm³      |
| " " " " "          | " " " " 7,8 Nm³/h    |
| " " " " 12,0 Nm³/h | Kreislaufgas 832 Nm³ |
|                    | Kreislauf 2,89       |

Belastung: Nm³/kg,h 0,95      Nm³/Norm.-Vol.,h

| Analysen:                          | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                          | 6,0             | -    | 0,1            | 39,2 | 47,9           | 0,3             | 6,5            | -    | 6,43              |              |
| Restgas                            | 20,5            | 0,3  | 0,1            | 26,0 | 40,0           | 3,2             | 9,9            | 1,05 | 9,78              |              |
| Kreislaufgas                       |                 |      |                | 29,4 | 42,1           |                 |                |      |                   |              |
| H <sub>2</sub> /CO im Kreislaufgas |                 |      |                | 1,43 |                |                 |                |      |                   |              |

|  |                                      |
|--|--------------------------------------|
| Gesamt-Inerte (Idealgas) 12,9 %        | Kontraktion nach Menge 35,0 %        |
| H <sub>2</sub> , CO im Sygas 1,22      | " " N <sub>2</sub> 34,2 %            |
| H <sub>2</sub> , CO im Restgas 1,54    | " " CO <sub>2</sub> - %              |
| Verbrauch von H <sub>2</sub> : CO 0,98 | Durchschnittliche Kontraktion 34,6 % |

|               |          |                      |                         |
|---------------|----------|----------------------|-------------------------|
| umgesetzt     | %CO 56,6 | %H <sub>2</sub> 45,3 | %CO+H <sub>2</sub> 50,4 |
| verflüssigt   |          |                      |                         |
| Verfl.-Grad A |          |                      |                         |
| " " P         |          |                      | 38,1                    |

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 8,1      CO<sub>2</sub> 33,3      bezogen auf CO-Umsatz

| Produkte                 |                   |         | Gesamtprodukt |  |
|--------------------------|-------------------|---------|---------------|--|
| Paraffingatsch 4,60 kg   | 30,2 %            | SB      | °C            |  |
| Ol-Kondensat 6,30 "      | 41,5 %            | - 100°  | %             |  |
| A.-K. Benzin 8,20 "      | 28,3 %            | - 200°  | %             |  |
| Flüssige Prod. 15,20     | 100 %             | - 320°  | %             |  |
| Sywasser 14,00 kg = 0,92 | × flüss. Produkte | Olefine | Vol. %        |  |
|                          |                   | - 200°  | , 200-320°    |  |

| Ausbeute            |             |      |                                     |
|---------------------|-------------|------|-------------------------------------|
| Flüssige Prod. 52,8 | g/Nm³ Sygas | 60,7 | (CO+H <sub>2</sub> ) g/Nm³ Idealgas |
| Gasol               | "           | "    | "                                   |
| Gesamt-Produkt      | "           | "    | "                                   |
| Sywasser            | "           | "    | "                                   |

**Bemerkungen:**  
 Ofen wird mit Wassergas im Kreislauf gefahren.  
 000277

# Druckversuchsanlage

Produktionsbericht vom 13./14.7. 1943

Ofen-Nr. 11  
 Füllung: 13  
 C<sub>2</sub>-Fe-Inhalt: - kg

Betriebsstunden 24/1453  
 Gasdruck 10 atü  
 Temperatur 20 atü 214 °C

Sy-W-Gas 329 Nm<sup>3</sup>  
 " " " " " "  
 " " " " " "  
 " 13,7 Nm<sup>3</sup>/h

Restgas 223 Nm<sup>3</sup>  
 " 9,3 Nm<sup>3</sup>/h  
 Kreislaufgas 727 Nm<sup>3</sup>  
 Kreislauf 2,21

Belastung: - Nm<sup>3</sup>/kg,h 1,08 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                          | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Utergewicht |
|------------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|-------------|
| Wassergas                          | 5,9             | -                             | 0,1            | 39,1 | 47,7           | 0,3             | 6,9            | -    | 6,77              |             |
| Restgas                            | 18,7            | 0,2                           | 0,1            | 28,0 | 40,5           | 2,4             | 10,1           | 1,06 | 9,98              |             |
| Kreislaufgas                       |                 |                               |                | 31,4 | 42,8           |                 |                |      |                   |             |
| H <sub>2</sub> /CO im Kreislaufgas |                 |                               |                | 1,36 |                |                 |                |      |                   |             |

|                                       |                                      |
|---------------------------------------|--------------------------------------|
| Gesamt-Inerte (Idealgas) 13,2 %       | Kontraktion nach Menge 32,2 %        |
| H <sub>2</sub> :CO im Sygas 1,22      | " " N <sub>2</sub> 32,2 %            |
| H <sub>2</sub> :CO im Restgas 1,45    | " " CO <sub>2</sub> - %              |
| Verbrauch von H <sub>2</sub> :CO 1,00 | Durchschnittliche Kontraktion 32,2 % |

|               |          |                      |                         |
|---------------|----------|----------------------|-------------------------|
| umgesetzt     | %CO 51,5 | %H <sub>2</sub> 42,3 | %CO+H <sub>2</sub> 46,5 |
| verflüssigt   |          |                      |                         |
| Verfl.-Grad A |          |                      |                         |
| " " P         |          |                      | 35,8                    |

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 9,7 CO<sub>2</sub> 33,8 bezogen auf CO-Umsatz

## Produkte

|  |        |
|--|--------|
| Paraffingätsch 3,80 kg                     | 25,3 % |
| Ol-Kondensat 6,50 "                        | 43,3 % |
| A.-K. Benzin 4,70 "                        | 31,4 % |
| Flüssige Prod. 15,00                       | 100 %  |
| Sywasser 14,50 kg = 0,97 x flüss. Produkte |        |

## Gesamtprodukt

|         |            |
|---------|------------|
| SB      | °C         |
| - 100°  | %          |
| - 200°  | %          |
| - 320°  | %          |
| Olefine | Vol. %     |
| - 200°  | , 200-320° |

## Ausbeute

|   |   |   |                              |
|---|---|---|------------------------------|
| Flüssige Prod. 45,6 g Nm <sup>3</sup> Sygas | 52,5 g Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) |   |                              |
| Gasol                                       | "   | " | " g/Nm <sup>3</sup> Idealgas |
| Gesamt-Produkt                              | "   | " | "                            |
| Sywasser                                    | "   | " | "                            |

## Bemerkungen:

Ofen wird mit Wassergas im Kreislauf gefahren.

000278















**Druckversuchsanlage** **Produktionsbericht** vom 6./7.7. 1943

|                   |                          |
|-------------------|--------------------------|
| Ofen-Nr. 11       | Betriebsstunden 16/1285  |
| Füllung: 13       | Gasdruck 10 atü          |
| Ca-Fe-Inhalt - kg | Temperatur 11 atü 187 °C |

|                                   |                                  |
|-----------------------------------|----------------------------------|
| W-Gas 197 Nm <sup>3</sup>         | Restgas 150 Nm <sup>3</sup>      |
| " " " " "                         | " " " " 9,4 Nm <sup>3</sup> /h   |
| " " " " " 12,3 Nm <sup>3</sup> /h | Kreislaufgas 511 Nm <sup>3</sup> |
|                                   | Kreislauf 2,60                   |

Belastung  $\frac{\text{Nm}^3}{\text{kg} \cdot \text{h}}$  0,97  $\frac{\text{Nm}^3}{\text{Norm.-Vol., h}}$

| Analysen: | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|-------------------------------|----------------|----|----------------|-----------------|----------------|-----|-------------------|--------------|
| Sygas     |                 |                               |                |    |                |                 |                |     |                   |              |
| Restgas   |                 |                               |                |    |                |                 |                |     |                   |              |

|                                     |                                   |
|-------------------------------------|-----------------------------------|
| Gesamt-Inerte (Idealgas) - %        | Kontraktion nach Menge 24,0 %     |
| H <sub>2</sub> CO im Sygas -        | " " N <sub>2</sub> - %            |
| H <sub>2</sub> CO im Restgas -      | " " CO <sub>2</sub> - %           |
| Verbrauch von H <sub>2</sub> : CO - | Durchschnittliche Kontraktion - % |

umgesetzt  $\frac{\% \text{CO}}$   $\frac{\% \text{H}_2}$   $\frac{\% \text{CO} + \text{H}_2}$

verflüssigt

Verfl.-Grad A Stillstand von 8<sup>00h</sup> - 16<sup>20h</sup> wegen Gasausfall.

" " P

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> - CO<sub>2</sub> - bezogen auf CO-Umsatz

| Produkte       |                                  |        | Gesamtprodukt |            |
|----------------|----------------------------------|--------|---------------|------------|
| Paraffingatsch | 2,25 kg                          | 45,5 % | SB            | °C         |
| Ol-Kondensat   | 1,50 "                           | 30,3 % | - 100°        | %          |
| A.-K. Benzin   | 1,20 "                           | 24,2 % | - 200°        | %          |
| Flüssige Prod. | 4,95 "                           | 100%   | - 320°        | %          |
| Sywasser       | 6,40 kg = 1,29 x flüss. Produkte |        | Olefine       | Val. %     |
|                |                                  |        | - 200°        | 200 - 320° |

**Ausbeute**

Flüssige Prod.  $\frac{\text{g}}{\text{Nm}^3}$  Sygas  $\frac{\text{g}}{\text{Nm}^3}$  Nutzgas  $\frac{\text{g}}{\text{Nm}^3}$  Idealgas

Gasol " " " " " " " "

Gesamt-Produkt " " " " " " " "

Sywasser " " " " " " " "

**Bemerkungen:**

000285

Ofen wird mit Wassergas im Kreislauf gefahren.





**Druckversuchsanlage** **Produktionsbericht vom 3./4.7. 1943**

|                   |                          |
|-------------------|--------------------------|
| Ofen-Nr. 11       | Betriebsstunden 24/1221  |
| Füllung: 13       | Gasdruck 1,0 atü         |
| Co-Fe-Inhalt - kg | Temperatur 20 atü 214 °C |

|                                 |                                  |
|---------------------------------|----------------------------------|
| S/W-Gas 31,6 Nm <sup>3</sup>    | Restgas 202 Nm <sup>3</sup>      |
| " " " " "                       | " " " " 8,4 Nm <sup>3</sup> /h   |
| " " " " "                       | Kreislaufgas 756 Nm <sup>3</sup> |
| " " " " 13,2 Nm <sup>3</sup> /h | Kreislauf 1 + 2,4                |

Belastung - Nm<sup>3</sup>/kg.h 1,04 Nm<sup>3</sup>/Norm-Vol., h

| Analysen:                          | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                          | 5,2             | -    | 0,1            | 40,1 | 47,5           | 0,3             | 6,8            | -    | 6,67              |              |
| Restgas                            | 20,6            | 0,2  | 0,1            | 26,7 | 39,1           | 2,9             | 10,4           | 1,02 | 10,37             |              |
| Kreislaufgas                       |                 |      |                | 30,7 | 41,7           |                 |                |      |                   |              |
| H <sub>2</sub> /CO im Kreislaufgas |                 |      |                | 1,36 |                |                 |                |      |                   |              |

|                                       |                                      |
|---------------------------------------|--------------------------------------|
| Gesamt-Inerte (Idealgas) 12,4 %       | Kontraktion nach Menge 36,2 %        |
| H <sub>2</sub> :CO im Sygas 1,19      | " " N <sub>2</sub> 35,6 %            |
| H <sub>2</sub> :CO im Restgas 1,46    | " " CO <sub>2</sub> - %              |
| Verbrauch von H <sub>2</sub> :CO 0,97 | Durchschnittliche Kontraktion 35,9 % |

|                 | %CO  | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|-----------------|------|-----------------|--------------------|
| umgesetzt       | 57,5 | 47,3            | 51,9               |
| verflüssigt     |      |                 |                    |
| Verfl.-Grad / A |      |                 | 30,2               |
| " " P           |      |                 |                    |

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 6,7 CO<sub>2</sub> 34,8 bezogen auf CO-Umsatz

| Produkte                                   | Gesamtprodukt     |
|--|-------------------|
| Paraffingatsch 4,15 kg 30 %                | SB °C             |
| Ol-Kondensat 5,20 " 38 %                   | - 100° %          |
| A.-K. Benzin 4,40 " 32 %                   | - 200° %          |
| Flüssige Prod. 13,75 " 100 %               | - 320° %          |
| Sywasser 12,90 kg = 0,94 × flüss. Produkte | Olefine Vol. %    |
|  | - 200° , 200-320° |

| Ausbeute                                    |  |
|---|--|
| Flüssige Prod. 43,5 g/Nm <sup>3</sup> Sygas | 49,6 g/Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> Idealgas |
| Gasol                                       | " " " " " " " "  |
| Gesamt-Produkt                              | " " " " " " " "  |
| Sywasser                                    | " " " " " " " "  |

**Bemerkungen:** 000288

Ofen wird mit Wassergas im Kreislaufgas gefahren.









**Druckversuchsanlage** **Produktionsbericht vom 29./30.6. 1943**

|                          |  |
|--------------------------|--|
| Ofen-Nr. <u>11</u>       | Betriebsstunden <u>24/1125</u>         |
| Füllung: <u>13</u>       | Gasdruck <u>10</u> atü                 |
| Co-Fe-Inhalt <u>-</u> kg | Temperatur <u>20</u> atü <u>214</u> °C |

|                                  |   |
|----------------------------------|---|
| W-Gas <u>294</u> Nm <sup>3</sup> | Restgas <u>179</u> Nm <sup>3</sup>      |
| " " " "                          | " <u>7,5</u> Nm <sup>3</sup> /h         |
| " " " "                          | Kreislaufgas <u>780</u> Nm <sup>3</sup> |
| " <u>12,2</u> Nm <sup>3</sup> /h | Kreislauf <u>2,65</u>                   |

Belastung - Nm<sup>3</sup>/kg,h 0,96 Nm<sup>3</sup>/Norm-Vol., h

| Analysen:                          | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                          | 6,2             | -                             | 0,1            | 38,5 | 49,1           | 0,3             | 5,8            | -    | 5,75              |              |
| Syngas                             | 22,2            | 10,2                          | 0,1            | 24,9 | 39,8           | 3,2             | 9,6            | 1,03 | 9,52              |              |
| Restgas                            |                 |                               |                |      |                |                 |                |      |                   |              |
| Kraftgas                           |                 |                               |                | 28,6 | 39,8           |                 |                |      |                   |              |
| H <sub>2</sub> /CO im Kreislaufgas |                 |                               |                | 1,39 |                |                 |                |      |                   |              |

|  |   |
|--|---|
| Gesamt-Inerte (Idealgas) <u>12,4</u> %       | Kontraktion nach Menge <u>39,1</u> %        |
| H <sub>2</sub> :CO im Syngas <u>1,28</u>     | " " N <sub>2</sub> <u>39,7</u> %            |
| H <sub>2</sub> :CO im Restgas <u>1,60</u>    | " " CO <sub>2</sub> <u>-</u> %              |
| Verbrauch von H <sub>2</sub> :CO <u>1,07</u> | Durchschnittliche Kontraktion <u>39,4</u> % |

|                           |                                       |  |
|---------------------------|---------------------------------------|--|
| umgesetzt <u>60,8</u> %CO | umgesetzt <u>51,0</u> %H <sub>2</sub> | umgesetzt <u>55,2</u> %CO+H <sub>2</sub> |
| verflüssigt _____         | verflüssigt _____                     | verflüssigt _____                        |
| Verfl.-Grad A _____       | Verfl.-Grad A _____                   | Verfl.-Grad A <u>32,9</u>                |
| " " P _____               | " " P _____                           | " " P _____                              |

CH<sub>4</sub> + C<sub>2</sub>H<sub>4</sub> 7,0 CO<sub>2</sub> 31,1 bezogen auf CO-Umsatz

| Produkte   | Gesamtprodukt               |
|--|-----------------------------|
| Paraffingatsch <u>4,20</u> kg <u>28,4</u> %              | SB _____ °C                 |
| Ol-Kondensat <u>6,50</u> " <u>43,9</u> %                 | - 100° _____ %              |
| A.-K. Benzin <u>4,10</u> " <u>27,7</u> %                 | - 200° _____ %              |
| Flüssige Prod. <u>14,80</u> " <u>100</u> %               | - 320° _____ %              |
| Sywasser <u>13,80</u> kg = <u>0,93</u> x flüss. Produkte | Olefine Vol. %              |
|  | - 200° _____ 200-320° _____ |

| Ausbeute  |  |                            |           |
|---|--|----------------------------|-----------|
| Flüssige Prod. <u>50,4</u> g/Nm <sup>3</sup> Syngas | <u>57,5</u> g/Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) | g/Nm <sup>3</sup> Idealgas |           |
| Gasol _____   | " " _____  | " " _____                  | " " _____ |
| Gesamt-Produkt _____                                | " " _____  | " " _____                  | " " _____ |
| Sywasser _____                                      | " " _____  | " " _____                  | " " _____ |

**Bemerkungen:** **000292**

Ofen wird mit Wassergas im Kreislauf gefahren.





**Druckversuchsanlage** **Produktionsbericht vom 26./27.6. 1943**

|                          |  |
|--------------------------|--|
| Ofen-Nr. <u>11</u>       | Betriebsstunden <u>24/1053</u>         |
| Füllung: <u>13</u>       | Gasdruck <u>10</u> atü                 |
| Co-Fe-Inhalt <u>-</u> kg | Temperatur <u>20</u> atü <u>214</u> °C |

|  |   |
|--|---|
| Sy-W-Gas <u>300</u> Nm <sup>3</sup>    | Restgas <u>184</u> Nm <sup>3</sup>      |
| " " " " " "                            | " " " " <u>7,7</u> Nm <sup>3</sup> /h   |
| " " " " <u>12,5</u> Nm <sup>3</sup> /h | Kreislaufgas <u>805</u> Nm <sup>3</sup> |
|  | Kreislauf <u>2,68</u>                   |

Belastung 0,99 Nm<sup>3</sup>/kg,h Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                          | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                          | 6,5             | -    | 0,1            | 38,3 | 48,4           | 0,3             | 6,4            | -    | 6,27              |              |
| Restgas                            | 22,5            | 0,2  | 0,1            | 24,3 | 39,8           | 3,2             | 9,9            | 1,09 | 9,79              |              |
| Kreislaufgas                       |                 |      |                | 28,2 | 42,2           |                 |                |      |                   |              |
| H <sub>2</sub> /CO im Kreislaufgas |                 |      |                | 1,49 |                |                 |                |      |                   |              |

|  |   |
|--|---|
| Gesamt-Inerte (Idealgas) <u>13,3</u> %       | Kontraktion nach Menge <u>38,6</u> %        |
| H <sub>2</sub> :CO im Sygas <u>1,26</u>      | " " N <sub>2</sub> <u>35,9</u> %            |
| H <sub>2</sub> :CO im Restgas <u>1,64</u>    | " " CO <sub>2</sub> <u>-</u> %              |
| Verbrauch von H <sub>2</sub> :CO <u>1,01</u> | Durchschnittliche Kontraktion <u>37,3</u> % |

|                           |                             |                                |
|---------------------------|-----------------------------|--------------------------------|
| umgesetzt <u>60,3</u> %CO | %H <sub>2</sub> <u>48,4</u> | %CO+H <sub>2</sub> <u>53,7</u> |
| verflüssigt               |                             |                                |
| Verfl.-Grad A             |                             |                                |
| " " P                     |                             | <u>35,2</u>                    |

CH<sub>4</sub> + C<sub>2</sub>H<sub>6</sub> 7,4 CO<sub>2</sub> 32,8 bezogen auf CO-Umsatz

| Produkte       |  |               |       | Gesamtprodukt |          |
|----------------|--|---------------|-------|---------------|----------|
| Paraffingatsch | <u>4,10</u> kg                                 | <u>26,4</u> % |       | SB            | °C       |
| Ol-Kondensat   | <u>6,10</u> "                                  | <u>39,4</u> % |       | - 100°        | %        |
| A.-K. Benzin   | <u>5,30</u> "                                  | <u>34,2</u> % |       | - 200°        | %        |
| Flüssige Prod. | <u>15,50</u> "                                 |               | 100 % | - 320°        | %        |
| Sywasser       | <u>9,50</u> kg = <u>0,61</u> X flüss. Produkte |               |       | Olefine       | Vol. %   |
|                |  |               |       | - 200°        | 200-320° |

**Ausbeute**

|                |                                     |  |                                     |
|----------------|-------------------------------------|--|-------------------------------------|
| Flüssige Prod. | <u>51,7</u> g/Nm <sup>3</sup> Sygas | <u>59,5</u> g/Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) | <u>2</u> g/Nm <sup>3</sup> Idealgas |
| Gasol          | " "                                 | " "  | " "                                 |
| Gesamt-Produkt | " "                                 | " "  | " "                                 |
| Sywasser       | " "                                 | " "  | " "                                 |

**Bemerkungen:**

**000295**

Ofen wird mit Wassergas im Kreislauf gefahren.







**Druckversuchsanlage** **Produktionsbericht vom 22/23.6. 1943**

|                           |  |
|---------------------------|--|
| Ofen-Nr. <u>11</u>        | Betriebsstunden <u>17/988</u>          |
| Füllung: <u>13</u>        | Gasdruck <u>10</u> atü                 |
| Cp-Fe-Inhalt: <u>—</u> kg | Temperatur <u>20</u> atü <u>214</u> °C |

|  |  |
|--|--|
| Sy-W-Gas: <u>—</u> Nm <sup>3</sup>         | Restgas: <u>—</u> Nm <sup>3</sup>      |
| " " " " " "                                | " " " " " " Nm <sup>3</sup> /h         |
| " " " " " " <u>12,7</u> Nm <sup>3</sup> /h | Kreislaufgas: <u>—</u> Nm <sup>3</sup> |
|  | Kreislauf: <u>1 + 2,5</u>              |

Belastung: — Nm<sup>3</sup>/kg,h 1,00 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen: | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|-----------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas | 6,1             | —    | 0,1            | 38,6 | 48,4           | 0,3             | 6,5            | —    | —                 |              |
| Restgas   | 21,7            | 0,2  | 0,1            | 24,8 | 40,4           | 3,1             | 9,7            | 1,02 | —                 |              |

|   |   |
|---|---|
| Gesamt-Inerte (Idealgas) <u>13,0</u> %      | Kontraktion nach Menge: <u>—</u> %        |
| H <sub>2</sub> : CO im Sygas <u>1,25</u>    | " " N <sub>2</sub> : <u>—</u> %           |
| H <sub>2</sub> : CO im Restgas <u>1,63</u>  | " " CO <sub>2</sub> : <u>—</u> %          |
| Verbrauch von H <sub>2</sub> : CO: <u>—</u> | Durchschnittliche Kontraktion: <u>—</u> % |

|                         |   |  |
|-------------------------|---|--|
| umgesetzt: <u>—</u> %CO | umgesetzt: <u>—</u> %H <sub>2</sub>                         | umgesetzt: <u>—</u> %CO+H <sub>2</sub> |
| verflüssigt: <u>—</u>   |   |  |
| Verfl.-Grad A           | Stillstand ab 1 <sup>20h</sup> wegen Fliegerschaden bei den |  |
| " " P                   | KW-Betrieben.   |  |

CH<sub>4</sub> + CmHn — CO<sub>2</sub> — bezogen auf CO-Umsatz

| Produkte   | Gesamtprodukt                         |
|--|---------------------------------------|
| Paraffingatsch: <u>—</u> kg                        | SB: <u>—</u> °C                       |
| Ol-Kondensat: <u>—</u> "                           | — 100°: <u>—</u> %                    |
| A.-K. Benzin: <u>—</u> "                           | — 200°: <u>—</u> %                    |
| Flüssige Prod.: <u>—</u> "                         | — 320°: <u>—</u> %                    |
| Sywasser: <u>—</u> kg = <u>—</u> × flüss. Produkte | Olefine: Vol. %                       |
|  | — 200°: <u>—</u> ; 200-320°: <u>—</u> |

**Ausbeute**

|                 |                                  |                                    |                                     |
|-----------------|----------------------------------|------------------------------------|-------------------------------------|
| Flüssige Prod.: | <u>—</u> g/Nm <sup>3</sup> Sygas | <u>—</u> g/Nm <sup>3</sup> Nutzgas | <u>—</u> g/Nm <sup>3</sup> Idealgas |
| Gasöl:          | <u>—</u> " "                     | <u>—</u> " "                       | <u>—</u> " "                        |
| Gesamt-Produkt: | <u>—</u> " "                     | <u>—</u> " "                       | <u>—</u> " "                        |
| Sywasser:       | <u>—</u> " "                     | <u>—</u> " "                       | <u>—</u> " "                        |

**Bemerkungen:**

000298

Ofen wird mit Wassergas im Kreislauf gefahren.





# Druckversuchsanlage

Versuchsbericht vom 19./20. 6. 1943

Ofen-Nr. 11  
 Füllung: 13.  
 C<sub>6</sub>-Fe-Inhalt -- kg

Betriebsstunden 24/927  
 Gasdruck 10 atü  
 Temperatur 20 atü 214 °C

S<sub>4</sub>-W-Gas 293 Nm<sup>3</sup>  
 " " " "  
 " 12,2 Nm<sup>3</sup>/h

Restgas 183 Nm<sup>3</sup>  
 " 7,2 Nm<sup>3</sup>/h  
 Kreislaufgas 741 Nm<sup>3</sup>  
 Kreislauf 1 + 2,53

| Analysen:                      | Nm <sup>3</sup> / kg,h 0,96 |                               |                |      |                |                 |                | Nm <sup>3</sup> /Norm.-Vol., h |                   |              |  |
|--------------------------------|-----------------------------|-------------------------------|----------------|------|----------------|-----------------|----------------|--------------------------------|-------------------|--------------|--|
|                                | CO <sub>2</sub>             | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z                            | N <sub>2</sub> -F | Litergewicht |  |
| Wassergas Syngas               | 5,6                         | --                            | 0,1            | 39,3 | 47,8           | 0,3             | 6,9            | --                             | 6,73              |              |  |
| Restgas                        | 21,5                        | 0,2                           | 0,1            | 24,8 | 39,4           | 3,1             | 10,9           | 1,09                           | 10,88             |              |  |
| Kreisgas                       |                             |                               |                | 28,9 | 41,7           |                 |                |                                |                   |              |  |
| H <sub>2</sub> /CO im Kreisgas |                             |                               |                |      | 1,44           |                 |                |                                |                   |              |  |

|                                  |        |                               |        |
|----------------------------------|--------|-------------------------------|--------|
| Gesamt-Inerte (Idealgas)         | 12,9 % | Kontraktion nach Menge        | 37,5 % |
| H <sub>2</sub> :CO im-Syngas     | 1,22   | " " N <sub>2</sub>            | 38,0 % |
| H <sub>2</sub> :CO im Restgas    | 1,59   | " " CO <sub>2</sub>           | -- %   |
| Verbrauch von H <sub>2</sub> :CO | 0,98   | Durchschnittliche Kontraktion | 37,8 % |

|               |  |                       |                          |
|---------------|--|-----------------------|--------------------------|
| umgesetzt     | % CO 60,8  | % H <sub>2</sub> 48,7 | % CO+H <sub>2</sub> 54,1 |
| verflüssigt   |  |                       |                          |
| Verll.-Grad A | Stillstand von 23 <sup>20</sup> - 23 <sup>30</sup> Uhr |                       |                          |
| " " P         | wegen Stromausfall.                                    |                       |                          |
|               |  |                       | 33,2                     |

CH<sub>4</sub> + C<sub>2</sub>H<sub>4</sub> 6,8 CO<sub>2</sub> 32,6 bezogen auf CO-Umsatz

| Produkte       |                                   | Gesamtprodukt     |        |
|----------------|-----------------------------------|-------------------|--------|
| Paraffingasch  | 3,90 kg 27 %                      | SB                | °C     |
| Ol-Kondensat   | 6,50 " 45 %                       | - 200 °C          | %      |
| A.-K. Benzin   | 4,10 " 28 %                       | 200 - 320 °C      | %      |
| Flüssige Prod. | 14,50 " 100 %                     | > 320 °C          | %      |
| Sywasser       | 12,70 kg = 0,88 × flüss. Produkte | Olefine           | Vol. % |
|                |                                   | - 200° ; 200-320° |        |

## Ausbeute

|                |                              |                               |  |                            |
|----------------|------------------------------|-------------------------------|--|----------------------------|
| Flüssige Prod. | 49,5 g/Nm <sup>3</sup> W-gas | 56,9 g/Nm <sup>3</sup> Syngas | g/Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) | g/Nm <sup>3</sup> Idealgas |
| Gasol          | " "                          | " "                           | " "  | " "                        |
| Gesamt-Produkt | " "                          | " "                           | " "  | " "                        |
| Sywasser       | " "                          | " "                           | " "  | " "                        |

## Bemerkungen:

Ofen wird mit Wassergas im Kreislauf gefahren.

000301

# Druckversuchsanlage

Versuchsbericht vom 18./19. 6. 1943

Ofen-Nr. 11  
 Füllung: 13.  
 O<sub>2</sub>-Fe-Inhalt -- kg

Betriebsstunden 24/903  
 Gasdruck 10 atü  
 Temperatur 20 atü 214 °C

W-Gas 309 Nm<sup>3</sup>  
 " " "  
 " " "  
 " 12,9 Nm<sup>3</sup>/h

Restgas 198 Nm<sup>3</sup>  
 " 8,25 Nm<sup>3</sup>/h  
 Kreislaufgas 750 Nm<sup>3</sup>  
 Kreislauf 1 + 2,43

Belastung -- Nm<sup>3</sup> / kg,h 1,01 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                      | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|--------------------------------|-----------------|------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                      | 5,7             | -    | 0,1            | 39,2 | 48,3           | 0,3             | 6,4            | -    | 6,26              |              |
| Restgas                        | 20,9            | 0,3  | 0,1            | 25,4 | 40,9           | 2,9             | 10,0           | 1,11 | 9,90              |              |
| Kreisgas                       |                 |      |                | 29,6 | 42,9           |                 |                |      |                   |              |
| H <sub>2</sub> /CO im Kreisgas |                 |      |                | 1,45 |                |                 |                |      |                   |              |

|                                  |        |                               |        |
|----------------------------------|--------|-------------------------------|--------|
| Gesamt-Inerte (Idealgas)         | 12,5 % | Kontraktion nach Menge        | 36 %   |
| H <sub>2</sub> :CO im Sygas      | 1,23   | " " N <sub>2</sub>            | 37 %   |
| H <sub>2</sub> :CO im Restgas    | 1,59   | " " CO <sub>2</sub>           | - %    |
| Verbrauch von H <sub>2</sub> :CO | 0,98   | Durchschnittliche Kontraktion | 36,5 % |

|               |           |                       |                          |
|---------------|-----------|-----------------------|--------------------------|
| umgesetzt     | % CO 58,8 | % H <sub>2</sub> 46,9 | % CO+H <sub>2</sub> 52,4 |
| verflüssigt   |           |                       |                          |
| Verfl.-Grad A |           |                       |                          |
| " " P         |           |                       | 33,6                     |

CH<sub>4</sub> + C<sub>2</sub>H<sub>4</sub> 5,0 CO<sub>2</sub> 32,7 bezogen auf CO-Umsatz

| Produkte       | Gesamtprodukt                     |                   |
|----------------|-----------------------------------|-------------------|
| Paraffingasch  | 4,70 kg                           | 31,3 %            |
| Ol-Kondensat   | 6,65 "                            | 44,2 %            |
| A.-K. Benzin   | 3,70 "                            | 24,5 %            |
| Flüssige Prod. | 15,05 "                           | 100 %             |
| Sywasser       | 12,20 kg = 0,81 × flüss. Produkte |                   |
|                |                                   | SB °C             |
|                |                                   | - 200 °C %        |
|                |                                   | 200 - 320 °C %    |
|                |                                   | > 320 °C %        |
|                |                                   | Olefine Vol.-%    |
|                |                                   | - 200° - 200-320° |

## Ausbeute

|                |                              |                              |  |          |
|----------------|------------------------------|------------------------------|--|----------|
| Flüssige Prod. | 48,7 g/Nm <sup>3</sup> W-gas | 55,7 g/Nm <sup>3</sup> Sygas | Nutzgas (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> | Idealgas |
| Gasol          | "                            | "                            | "  | "        |
| Gesamt-Produkt | "                            | "                            | "  | "        |
| Sywasser       | "                            | "                            | "  | "        |
| Bemerkungen:   | "                            | "                            | "  | "        |

000302

Ofen wird mit Wassergas im Kreislauf gefahren.

| Druckversuchsanlage                             |                                   | Versuchsbericht vom 17./18. 6. 1943 |   |                      |                |                 |                                |      |                   |              |  |
|---|-----------------------------------|-------------------------------------|---|----------------------|----------------|-----------------|--------------------------------|------|-------------------|--------------|--|
| Ofen-Nr. 11                                     |                                   | Betriebsstunden 24/879              |   |                      |                |                 |                                |      |                   |              |  |
| Füllung: 13.                                    |                                   | Gasdruck 10 atü                     |   |                      |                |                 |                                |      |                   |              |  |
| Fe-Inhalt -- kg                                 |                                   | Temperatur 20 atü 214 °C            |   |                      |                |                 |                                |      |                   |              |  |
| W-Gas 304 Nm <sup>3</sup>                       |                                   | Restgas 183 Nm <sup>3</sup>         |   |                      |                |                 |                                |      |                   |              |  |
| " " "   |                                   | " 7,6 Nm <sup>3</sup> /h            |   |                      |                |                 |                                |      |                   |              |  |
| " " "   |                                   | Kreislaufgas 847 Nm <sup>3</sup>    |   |                      |                |                 |                                |      |                   |              |  |
| " 12,7 Nm <sup>3</sup> /h                       |                                   | Kreislauf 1 + 2,8                   |   |                      |                |                 |                                |      |                   |              |  |
| Belastung --                                    |                                   | Nm <sup>3</sup> /kg,h 1,00          |   |                      |                |                 | Nm <sup>3</sup> /Norm.-Vol., h |      |                   |              |  |
| Analysen:                                       | CO <sub>2</sub>                   | C <sub>m</sub> H <sub>n</sub>       | O <sub>2</sub>  | CO                   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub>                 | C-Z  | N <sub>2</sub> -F | Litergewicht |  |
| Wassergas                                       | 5,5                               | -                                   | 0,1   | 40,0                 | 48,7           | 0,3             | 5,4                            | --   | 5,33              |              |  |
| Restgas   | 21,2                              | 0,3                                 | 0,1   | 26,0                 | 40,0           | 3,0             | 9,4                            | 1,07 | 9,34              |              |  |
| Kreisgas  |                                   |                                     |   | 29,7                 | 42,2           |                 |                                |      |                   |              |  |
| H <sub>2</sub> /CO im Kreisgas                  |                                   |                                     |   | 1,42                 |                |                 |                                |      |                   |              |  |
| Gesamt-Inerte (Idealgas) 11,3 %                 |                                   | Kondensation nach Menge             |   | -- %                 |                |                 |                                |      |                   |              |  |
| H <sub>2</sub> :CO im Sygas 1,22                |                                   | " " N <sub>2</sub>                  |   | 43 %                 |                |                 |                                |      |                   |              |  |
| H <sub>2</sub> :CO im Restgas 1,54              |                                   | " " CO <sub>2</sub>                 |   | -- %                 |                |                 |                                |      |                   |              |  |
| Verbrauch von H <sub>2</sub> :CO 1,03           |                                   | Durchschnittliche Kontraktion       |   | 43                   |                |                 |                                |      |                   |              |  |
| umgesetzt                                       | % CO 63,0                         | % H <sub>2</sub> 53,2               | % CO+H <sub>2</sub> 57,7                                |                      |                |                 |                                |      |                   |              |  |
| verflüssigt                                     |                                   |                                     |   |                      |                |                 |                                |      |                   |              |  |
| Verfl.-Grad A                                   |                                   |                                     |   |                      |                |                 |                                |      |                   |              |  |
| " " P   | 28,5                              |                                     |   |                      |                |                 |                                |      |                   |              |  |
| CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub> | 5,7                               | CO <sub>2</sub> 26,3                | bezogen auf CO-Umsatz                                   |                      |                |                 |                                |      |                   |              |  |
| <b>Produkte</b>                                 |                                   |                                     |   | <b>Gesamtprodukt</b> |                |                 |                                |      |                   |              |  |
| Paraffingasch                                   | 4,00 kg                           | 29 %                                | SB  | °C                   |                |                 |                                |      |                   |              |  |
| Öl-Kondensat                                    | 5,90 "                            | 42 %                                | - 200 °C  | %                    |                |                 |                                |      |                   |              |  |
| A.-K. Benzin                                    | 4,00 "                            | 29 %                                | 200 - 320 °C  | %                    |                |                 |                                |      |                   |              |  |
| Flüssige Prod.                                  | 13,90 "                           | 100 %                               | > 320 °C  | %                    |                |                 |                                |      |                   |              |  |
| Sywasser  | 13,00 kg = 0,94 × flüss. Produkte |                                     | Olefine   | Vol. %               |                |                 |                                |      |                   |              |  |
|   |                                   |                                     | - 200°  | ; 200-320°           |                |                 |                                |      |                   |              |  |
| <b>Ausbeute</b>                                 |                                   |                                     |   |                      |                |                 |                                |      |                   |              |  |
| Flüssige Prod.                                  | 45,7 g/Nm <sup>3</sup> W-gas      | 51,6 g/Nm <sup>3</sup> Sygas        | Nutzgas (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> Idealgas |                      |                |                 |                                |      |                   |              |  |
| Gasol   | " "                               | " "                                 | " "   | " "                  | " "            | " "             |                                |      |                   |              |  |
| Gesamt-Produkt                                  | " "                               | " "                                 | " "   | " "                  | " "            | " "             |                                |      |                   |              |  |
| Sywasser  | " "                               | " "                                 | " "   | " "                  | " "            | " "             |                                |      |                   |              |  |
| <b>Bemerkungen:</b>                             |                                   |                                     |   |                      |                |                 |                                |      |                   |              |  |
| Ofen wird mit Wassergas im Kreislauf gefahren.  |                                   |                                     |   |                      |                |                 |                                |      |                   |              |  |
| 000303  |                                   |                                     |   |                      |                |                 |                                |      |                   |              |  |

| <b>Druckversuchsanlage</b>  |                 | Versuchsbericht vom <b>16./17. 6.</b> 194 <b>3</b>          |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
|---|-----------------|---|----------------|---|----------------|--|----------------|--------------------------------------|-------------------|---|-----------------|------|----------------|----|----------------|-----------------|----------------|-----|-------------------|--------------|-----------|------------|-----------|------------|-------------|-------------|------------|------------|-----------|-------------|--|---------|-------------|------------|------------|-------------|-------------|------------|-------------|-------------|--------------|--|------------|--|--|--|-------------|-------------|--|--|--|--|--|----------------------------------|--|--|--|-------------|--|--|--|--|--|--|
| Ofen-Nr. <b>11</b>  |                 | Betriebsstunden <b>23/855</b>                               |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Füllung: <b>13.</b>   |                 | Gasdruck <b>10</b> atü                                      |                | Temperatur <b>20</b> atü <b>214</b> °C    |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| C6-Fe-Inhalt <b>--</b> kg   |                 | Restgas <b>192</b> Nm <sup>3</sup>                          |                | " <b>8,4</b> Nm <sup>3</sup> /h           |                | Kreislaufgas <b>789</b> Nm <sup>3</sup>      |                | Kreislauf <b>1 + 2,66</b>            |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| W-Gas <b>297</b> Nm <sup>3</sup>  |                 | " " " "   |                | " " " "                                   |                | " " " "                                      |                | " " " "                              |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| " <b>12,9</b> Nm <sup>3</sup> /h  |                 |   |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Belastung <b>--</b> Nm <sup>3</sup> /kg,h   |                 | <b>1,02</b> Nm <sup>3</sup> /Norm.-Vol., h                  |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| <table border="1"> <thead> <tr> <th>Analysen:</th> <th>CO<sub>2</sub></th> <th>CmHn</th> <th>O<sub>2</sub></th> <th>CO</th> <th>H<sub>2</sub></th> <th>CH<sub>4</sub></th> <th>N<sub>2</sub></th> <th>C-Z</th> <th>N<sub>2</sub>-F</th> <th>Litergewicht</th> </tr> </thead> <tbody> <tr> <td>Wassergas</td> <td><b>5,5</b></td> <td><b>--</b></td> <td><b>0,1</b></td> <td><b>39,7</b></td> <td><b>48,1</b></td> <td><b>0,3</b></td> <td><b>6,3</b></td> <td><b>--</b></td> <td><b>6,25</b></td> <td></td> </tr> <tr> <td>Restgas</td> <td><b>21,1</b></td> <td><b>0,2</b></td> <td><b>0,1</b></td> <td><b>26,2</b></td> <td><b>39,3</b></td> <td><b>2,8</b></td> <td><b>10,3</b></td> <td><b>1,13</b></td> <td><b>10,12</b></td> <td></td> </tr> <tr> <td>Kreislsgas</td> <td></td> <td></td> <td></td> <td><b>29,9</b></td> <td><b>41,7</b></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> <tr> <td>H<sub>2</sub>/CO im Kreislsgas</td> <td></td> <td></td> <td></td> <td><b>1,39</b></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> </tbody> </table> |                 |   |                |   |                |  |                |                                      |                   | Analysen:                                   | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht | Wassergas | <b>5,5</b> | <b>--</b> | <b>0,1</b> | <b>39,7</b> | <b>48,1</b> | <b>0,3</b> | <b>6,3</b> | <b>--</b> | <b>6,25</b> |  | Restgas | <b>21,1</b> | <b>0,2</b> | <b>0,1</b> | <b>26,2</b> | <b>39,3</b> | <b>2,8</b> | <b>10,3</b> | <b>1,13</b> | <b>10,12</b> |  | Kreislsgas |  |  |  | <b>29,9</b> | <b>41,7</b> |  |  |  |  |  | H <sub>2</sub> /CO im Kreislsgas |  |  |  | <b>1,39</b> |  |  |  |  |  |  |
| Analysen:   | CO <sub>2</sub> | CmHn  | O <sub>2</sub> | CO  | H <sub>2</sub> | CH <sub>4</sub>                              | N <sub>2</sub> | C-Z                                  | N <sub>2</sub> -F | Litergewicht                                |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Wassergas   | <b>5,5</b>      | <b>--</b>   | <b>0,1</b>     | <b>39,7</b>                               | <b>48,1</b>    | <b>0,3</b>                                   | <b>6,3</b>     | <b>--</b>                            | <b>6,25</b>       |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Restgas   | <b>21,1</b>     | <b>0,2</b>  | <b>0,1</b>     | <b>26,2</b>                               | <b>39,3</b>    | <b>2,8</b>                                   | <b>10,3</b>    | <b>1,13</b>                          | <b>10,12</b>      |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Kreislsgas  |                 |   |                | <b>29,9</b>                               | <b>41,7</b>    |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| H <sub>2</sub> /CO im Kreislsgas  |                 |   |                | <b>1,39</b>                               |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Gesamt-Inerte (Idealgas) <b>12,2</b> %  |                 | H <sub>2</sub> :CO im Sygas <b>1,21</b>                     |                | H <sub>2</sub> :CO im Restgas <b>1,50</b> |                | Verbrauch von H <sub>2</sub> :CO <b>1,00</b> |                | Kontraktion nach Menge <b>35,5</b> % |                   | " " N <sub>2</sub> <b>38,0</b> %            |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
|   |                 |   |                |   |                |  |                | " " CO <sub>2</sub> <b>--</b> %      |                   | Durchschnittliche Kontraktion <b>36,3</b> % |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| umgesetzt <b>58,0</b> % CO  |                 |   |                | <b>48,0</b> % H <sub>2</sub>              |                |  |                | <b>52,5</b> % CO + H <sub>2</sub>    |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| verflüssigt   |                 | <b>Stillstand von 18<sup>05</sup> - 19<sup>00</sup> Uhr</b> |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Verfl.-Grad A   |                 | <b>wegen Stromausfall.</b>                                  |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| " " P   |                 |   |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| CH <sub>4</sub> <b>6,4</b>  |                 | CO <sub>2</sub> <b>35,7</b>                                 |                | bezogen auf CO-Umsatz                     |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| <b>Produkte</b>   |                 |   |                |   |                | <b>Gesamprodukt</b>                          |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Paraffingesch <b>4,80</b> kg  |                 | <b>31,4</b> %   |                | SB  |                | <b>200</b> °C                                |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Öl-Kondensat <b>6,50</b> "  |                 | <b>42,5</b> %   |                | 200 - 320 °C                              |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| A.-K. Benzin <b>4,00</b> "  |                 | <b>26,1</b> %   |                | > 320 °C                                  |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Flüssige Prod. <b>15,30</b> "   |                 | <b>100</b> %  |                | Olefine                                   |                | Vol. %                                       |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Sywasser <b>12,60</b> kg = <b>0,82</b> × flüss. Produkte  |                 |   |                | - 200°                                    |                | ; 200-320°                                   |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| <b>Ausbeute</b>   |                 |   |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Flüssige Prod. <b>51,5</b> g/Nm <sup>3</sup> <b>W-gas</b>   |                 | <b>58,6</b> g/Nm <sup>3</sup> <b>Sygas</b>                  |                | Nutzgas (CO+H <sub>2</sub> )              |                | g/Nm <sup>3</sup> Idealgas                   |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Gasol   |                 | " "   |                | " "                                       |                | " "  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Gesamt-Produkt  |                 | " "   |                | " "                                       |                | " "  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| Sywasser  |                 | " "   |                | " "                                       |                | " "  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| <b>Bemerkungen:</b>   |                 |   |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| <b>Ofen wird mit Wassergas im Kreislauf gefahren.</b>   |                 |   |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |
| <b>000304</b>   |                 |   |                |   |                |  |                |                                      |                   |   |                 |      |                |    |                |                 |                |     |                   |              |           |            |           |            |             |             |            |            |           |             |  |         |             |            |            |             |             |            |             |             |              |  |            |  |  |  |             |             |  |  |  |  |  |                                  |  |  |  |             |  |  |  |  |  |  |



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|  |  |  |  |                                     |  |  |  |  |  |  |
|--|--|--|--|-------------------------------------|--|--|--|--|--|--|
| <b>Druckversuchsanlage</b>   |  |  |  | Versuchsbericht vom 15./16. 6. 194  |  |  |  |  |  |  |
| Ofen-Nr. 11  |  |  |  | Betriebsstunden 23/832              |  |  |  |  |  |  |
| Füllung: 13.   |  |  |  | Gasdruck 10 atü                     |  |  |  |  |  |  |
| Co-Fe-Inhalt -- kg   |  |  |  | Temperatur 20 atü 214 °C            |  |  |  |  |  |  |
| W-Gas 295 Nm <sup>3</sup>  |  |  |  | Restgas 161 Nm <sup>3</sup>         |  |  |  |  |  |  |
| " " "  |  |  |  | " 7,0 Nm <sup>3</sup> /h            |  |  |  |  |  |  |
| " 12,8 Nm <sup>3</sup> /h  |  |  |  | Kreislaufgas 715 Nm <sup>3</sup>    |  |  |  |  |  |  |
| " " "  |  |  |  | Kreislauf 1 + 2,42                  |  |  |  |  |  |  |
| Belastung -- Nm <sup>3</sup> / kg.h  |  |  |  | 1,01 Nm <sup>3</sup> /Norm.-Vol., h |  |  |  |  |  |  |
| Analysen: CO <sub>2</sub> C <sub>m</sub> H <sub>n</sub> O <sub>2</sub> CO H <sub>2</sub> CH <sub>4</sub> N <sub>2</sub> C-Z N <sub>2</sub> -F Litergewicht |  |  |  |                                     |  |  |  |  |  |  |
| <b>Wassergas</b>   |  |  |  |                                     |  |  |  |  |  |  |
| Restgas  |  |  |  |                                     |  |  |  |  |  |  |
| <b>Kreislaufgas</b>  |  |  |  |                                     |  |  |  |  |  |  |
| H <sub>2</sub> /CO im Kreislaufgas   |  |  |  |                                     |  |  |  |  |  |  |
| Gesamt-Inerte (Idealgas) 11,9 %  |  |  |  |                                     |  |  |  |  |  |  |
| H <sub>2</sub> :CO im Sygas 1,22   |  |  |  |                                     |  |  |  |  |  |  |
| H <sub>2</sub> :CO im Restgas 1,55   |  |  |  |                                     |  |  |  |  |  |  |
| Verbrauch von H <sub>2</sub> :CO 1,06  |  |  |  |                                     |  |  |  |  |  |  |
| Kontraktion nach Menge 45,4 %  |  |  |  |                                     |  |  |  |  |  |  |
| " " N <sub>2</sub> 46,8 %  |  |  |  |                                     |  |  |  |  |  |  |
| " " CO <sub>2</sub> -- %   |  |  |  |                                     |  |  |  |  |  |  |
| Durchschnittliche Kontraktion 46,1 %   |  |  |  |                                     |  |  |  |  |  |  |
| umgesetzt % CO 66,2 % H <sub>2</sub> 57,2 % CO+H <sub>2</sub> 61,2   |  |  |  |                                     |  |  |  |  |  |  |
| verflüssigt  |  |  |  |                                     |  |  |  |  |  |  |
| Verfl.-Grad A Ofen wurde um 9 <sup>00</sup> Uhr wieder angefahren.   |  |  |  |                                     |  |  |  |  |  |  |
| " " P 28,2   |  |  |  |                                     |  |  |  |  |  |  |
| CH <sub>4</sub> 4,5 CO <sub>2</sub> 25,0 bezogen auf CO-Umsatz   |  |  |  |                                     |  |  |  |  |  |  |
| <b>Produkte</b>  |  |  |  |                                     |  |  |  |  |  |  |
| <b>Gesamtprodukt</b>   |  |  |  |                                     |  |  |  |  |  |  |
| Paraffingatsch 5,00 kg 35,4 %  |  |  |  |                                     |  |  |  |  |  |  |
| Ol-Kondensat 5,65 " 40,0 %   |  |  |  |                                     |  |  |  |  |  |  |
| A.-K. Benzin 3,50 " 24,6 %   |  |  |  |                                     |  |  |  |  |  |  |
| Flüssige Prod. 14,15 " 100 %   |  |  |  |                                     |  |  |  |  |  |  |
| Sywasser 13,20 kg = 0,93 × flüss. Produkte   |  |  |  |                                     |  |  |  |  |  |  |
| SB °C  |  |  |  |                                     |  |  |  |  |  |  |
| - 200 °C %   |  |  |  |                                     |  |  |  |  |  |  |
| 200 - 320 °C %   |  |  |  |                                     |  |  |  |  |  |  |
| > 320 °C %   |  |  |  |                                     |  |  |  |  |  |  |
| Olefine Vol. %   |  |  |  |                                     |  |  |  |  |  |  |
| - 200° ; 200-320°  |  |  |  |                                     |  |  |  |  |  |  |
| <b>Ausbeute</b>  |  |  |  |                                     |  |  |  |  |  |  |
| Flüssige Prod. 48,0 g/Nm <sup>3</sup> W-gas 54,5 g/Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> Idealgas                                 |  |  |  |                                     |  |  |  |  |  |  |
| Gasol " " " " " "  |  |  |  |                                     |  |  |  |  |  |  |
| Gesamt-Produkt " " " " " "   |  |  |  |                                     |  |  |  |  |  |  |
| Sywasser " " " " " "   |  |  |  |                                     |  |  |  |  |  |  |
| <b>Bemerkungen:</b>  |  |  |  |                                     |  |  |  |  |  |  |
| Ofen wird mit Wassergas im Kreislauf gefahren.   |  |  |  |                                     |  |  |  |  |  |  |
| 000305   |  |  |  |                                     |  |  |  |  |  |  |

| Druckversuchsanlage                             |  | Versuchsbericht vom 14./15. 6. 1943 |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
|---|--|-------------------------------------|-----------------|-------------------------------|-----------------------|--------------|---------------------|----------|------|------|-----------------|-------------------------------|----------------|----|----------------|-----------------|----------------|-----|-------------------|--------------|
| Ofen-Nr. 11                                     |  | Betriebsstunden 17/809              |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Füllung: 13.                                    |  | Gasdruck 10 atü                     |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| 66-Fe-Inhalt - kg                               |  | Temperatur 20 atü 214 °C            |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Sy-W-Gas 225 Nm³                                |  | Restgas 143 Nm³                     |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| " " " "   |  | " 8,4 Nm³/h                         |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| " " " "   |  | Kreislaufgas 543 Nm³                |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| " 13,2 Nm³/h                                    |  | Kreislauf 1 + 2,42                  |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Belastung -                                     |  | Nm³ / kg,h 1,04                     |                 |                               |                       |              | Nm³/Norm.-Vol., h   |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Analysen:                                       |  |                                     |                 |                               |                       |              |                     |          |      |      | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht |
| Wassergas                                       |  | 6,2                                 | -               | 0,1                           | 38,8                  | 48,9         | 0,3                 | 5,7      | --   | 5,55 |                 |                               |                |    |                |                 |                |     |                   |              |
| Restgas   |  | 22,6                                | 0,2             | 0,1                           | 24,4                  | 40,6         | 3,0                 | 9,1      | 1,09 | 8,96 |                 |                               |                |    |                |                 |                |     |                   |              |
| Kralfgas  |  |                                     |                 |                               | 28,6                  | 43,0         |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| H <sub>2</sub> /CO im Kralfgas                  |  |                                     |                 |                               | 1,50                  |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Gesamt-Inerte (Idealgas)                        |  | 12,3                                | %               | Kontraktion nach Menge        |                       |              |                     |          |      |      | 36,5            | %                             |                |    |                |                 |                |     |                   |              |
| H <sub>2</sub> :CO im Sygas                     |  | 1,26                                |                 | " " N <sub>2</sub>            |                       |              |                     |          |      |      | 38,0            | %                             |                |    |                |                 |                |     |                   |              |
| H <sub>2</sub> :CO im Restgas                   |  | 1,66                                |                 | " " CO <sub>2</sub>           |                       |              |                     |          |      |      | --              | %                             |                |    |                |                 |                |     |                   |              |
| Verbrauch von H <sub>2</sub> :CO                |  | 1,00                                |                 | Durchschnittliche Kontraktion |                       |              |                     |          |      |      | 37,3            | %                             |                |    |                |                 |                |     |                   |              |
| umgesetzt                                       |  | 60,6                                | % CO            | 48,0                          | % H <sub>2</sub>      | 53,6         | % CO+H <sub>2</sub> |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| verflüssigt                                     |  | Ofen wurde infolge Stromausfall     |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Verfl.-Grad A                                   |  | um 15 Uhr stillgesetzt.             |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| " " P   |  |                                     |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| CH <sub>4</sub> + C <sub>2</sub> H <sub>6</sub> |  | 6,7                                 | CO <sub>2</sub> | 34,6                          | bezogen auf CO-Umsatz |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| <b>Produkte</b>                                 |  | <b>Gesamtprodukt</b>                |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Paraffingatsch                                  |  | 0,80                                | kg              | --                            | %                     | SB           | --                  | °C       |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Ol-Kondensat                                    |  | 4,80                                | "               | --                            | %                     | -- 200 °C    | --                  | %        |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| A.-K. Benzin                                    |  | 3,30                                | "               | --                            | %                     | 200 - 320 °C | --                  | %        |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Flüssige Prod.                                  |  | 8,90                                | "               | --                            | 100 %                 | > 320 °C     | --                  | %        |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Sywasser  |  | 9,20                                | kg =            | -                             | × flüss. Produkte     | Olefine      | Vol. %              |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
|   |  |                                     |                 |                               |                       | -- 200°      | --                  | 200-320° |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| <b>Ausbeute</b>                                 |  |                                     |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Flüssige Prod.                                  |  | --                                  | g/Nm³ Sygas     | --                            | g/Nm³ Nutzgas         | --           | g/Nm³ Idealgas      |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Gasol   |  | "                                   | "               | "                             | "                     | "            | "                   |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Gesamt-Produkt                                  |  | "                                   | "               | "                             | "                     | "            | "                   |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Sywasser  |  | "                                   | "               | "                             | "                     | "            | "                   |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| <b>Bemerkungen:</b>                             |  |                                     |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |
| Ofen wird mit Wassergas im Kreislauf gefahren.  |  |                                     |                 |                               |                       |              |                     |          |      |      |                 |                               |                |    |                |                 |                |     |                   |              |

000306

# Druckversuchsanlage

Versuchsbericht vom 13./14. 6. 1943

Ofen-Nr. 11  
 Füllung: 13.  
 O-Fe-Inhalt -- kg

Betriebsstunden 24/792  
 Gasdruck 10 alü  
 Temperatur 20 alü 214 °C

Sy-W-Gas 307 Nm<sup>3</sup>  
 " " "  
 " " "  
 " 12,8 Nm<sup>3</sup>/h

Restgas 187 Nm<sup>3</sup>  
 " 7,8 Nm<sup>3</sup>/h  
 Kreislaufgas 782 Nm<sup>3</sup>  
 Kreislauf 1 + 2,55

| Belastung                          |                  | Nm <sup>3</sup> / kg,h        |                |      |                |                 |                |      | Nm <sup>3</sup> /Norm.-Vol., h |              |  |
|------------------------------------|------------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|--------------------------------|--------------|--|
| Analysen:                          | -CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F              | Litergewicht |  |
| Wassergas Sygas                    | 7,0              | -                             | 0,1            | 37,6 | 49,5           | 0,3             | 5,5            | --   | 5,35                           |              |  |
| Restgas                            | 24,0             | 0,2                           | 0,1            | 22,9 | 40,8           | 3,1             | 8,9            | 1,18 | 8,85                           |              |  |
| Kreislaufgas                       |                  |                               |                | 27,0 | 43,3           |                 |                |      |                                |              |  |
| H <sub>2</sub> /CO im Kreislaufgas |                  |                               |                | 1,60 |                |                 |                |      |                                |              |  |

|                                  |        |                               |        |
|----------------------------------|--------|-------------------------------|--------|
| Gesamt-Inerte (Idealgas)         | 12,9 % | Kontraktion nach Menge        | 39,0 % |
| H <sub>2</sub> :CO im Sygas      | 1,32   | " " N <sub>2</sub>            | 39,5 % |
| H <sub>2</sub> :CO im Restgas    | 1,78   | " " CO <sub>2</sub>           | -- %   |
| Verbrauch von H <sub>2</sub> :CO | 1,04   | Durchschnittliche Kontraktion | 39,3 % |

|               |           |                       |                          |
|---------------|-----------|-----------------------|--------------------------|
| umgesetzt     | % CO 63,1 | % H <sub>2</sub> 49,9 | % CO+H <sub>2</sub> 55,6 |
| verflüssigt   |           |                       |                          |
| Verfl.-Grad A |           |                       |                          |
| " " P         |           |                       | 30,2                     |

CH<sub>4</sub> + A/G/M/ 6,7 CO<sub>2</sub> 31,6 bezogen auf CO-Umsatz

| Produkte       |                                   | Gesamtprodukt     |        |
|----------------|-----------------------------------|-------------------|--------|
| Paraffingasch  | 3,70 kg 26 %                      | SB                | °C     |
| Ol-Kondensat   | 5,50 " 39 %                       | - 200 °C          | %      |
| A.-K. Benzin   | 5,00 " 35 %                       | 200 - 320 °C      | %      |
| Flüssige Prod. | 14,20 " 100 %                     | > 320 °C          | %      |
| Sywasser       | 14,20 kg = 1,00 × flüss. Produkte | Olefine           | Vol. % |
|                |                                   | - 200° ; 200-320° |        |

| Ausbeute       |                        | W-gas Sygas            |  |
|----------------|------------------------|------------------------|--|
| Flüssige Prod. | 46,3 g/Nm <sup>3</sup> | 53,2 g/Nm <sup>3</sup> | Nutzgas (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> |
| Gasol          | " "                    | " "                    | Idealgas g/Nm <sup>3</sup>                     |
| Gesamt-Produkt | " "                    | " "                    | " "  |
| Sywasser       | " "                    | " "                    | " "  |

Bemerkungen:

Ofen wird mit Wassergas im Kreislauf gefahren

000307

|  |                 |                   |                |   |                |                 |  |                       |              |
|--|-----------------|-------------------|----------------|---|----------------|-----------------|--|-----------------------|--------------|
| <b>Druckversuchsanlage</b>                             |                 |                   |                | Versuchsbericht vom <b>12./13. 6. 1943</b>  |                |                 |  |                       |              |
| Ofen-Nr. <b>11</b>                                     |                 |                   |                | Betriebsstunden <b>24/768</b>               |                |                 |  |                       |              |
| Füllung: <b>13.</b>                                    |                 |                   |                | Gasdruck <b>10</b> atü                      |                |                 |  |                       |              |
| Co-Fe-Inhalt <b>..</b> kg                              |                 |                   |                | Temperatur <b>20</b> atü <b>214</b> °C      |                |                 |  |                       |              |
| W-Gas <b>306</b> Nm <sup>3</sup>                       |                 |                   |                | Restgas <b>194</b> Nm <sup>3</sup>          |                |                 |  |                       |              |
| " " " "  |                 |                   |                | " <b>8,1</b> Nm <sup>3</sup> /h             |                |                 |  |                       |              |
| " <b>12,8</b> Nm <sup>3</sup> /h                       |                 |                   |                | Kreislaufgas <b>787</b> Nm <sup>3</sup>     |                |                 |  |                       |              |
| " " " "  |                 |                   |                | Kreislauf <b>1 + 2,57</b>                   |                |                 |  |                       |              |
| Belastung <b>--</b>                                    |                 |                   |                | Nm <sup>3</sup> / kg, h <b>1,01</b>         |                |                 |  |                       |              |
| Analysen:  |                 |                   |                | Nm <sup>3</sup> /Norm.-Vol., h              |                |                 |  |                       |              |
|  | CO <sub>2</sub> | CmHn              | O <sub>2</sub> | CO  | H <sub>2</sub> | CH <sub>4</sub> | C-Z  | N <sub>2</sub> -F     | Litergewicht |
| Wassergas  | <b>6,9</b>      | <b>-</b>          | <b>0,1</b>     | <b>37,8</b>                                 | <b>49,2</b>    | <b>0,3</b>      | <b>5,7</b>                                     | <b>--</b>             | <b>5,64</b>  |
| Restgas  | <b>22,9</b>     | <b>0,1</b>        | <b>0,1</b>     | <b>23,8</b>                                 | <b>40,9</b>    | <b>3,2</b>      | <b>9,0</b>                                     | <b>1,03</b>           | <b>8,87</b>  |
| Kreislfgas   |                 |                   |                | <b>27,8</b>                                 | <b>43,2</b>    |                 |  |                       |              |
| H <sub>2</sub> /CO im Kreislfgas                       |                 |                   |                | <b>1,55</b>                                 |                |                 |  |                       |              |
| Gesamt-Inerte (Idealgas) <b>13,0</b> %                 |                 |                   |                | Kontraktion nach Menge <b>36,5</b> %        |                |                 |  |                       |              |
| H <sub>2</sub> :CO im Sygas <b>1,30</b>                |                 |                   |                | " " N <sub>2</sub> <b>36,5</b> %            |                |                 |  |                       |              |
| H <sub>2</sub> :CO im Restgas <b>1,72</b>              |                 |                   |                | " " CO <sub>2</sub> <b>--</b> %             |                |                 |  |                       |              |
| Verbrauch von H <sub>2</sub> :CO <b>1,02</b>           |                 |                   |                | Durchschnittliche Kontraktion <b>36,5</b> % |                |                 |  |                       |              |
| % CO   |                 |                   |                | % H <sub>2</sub>                            |                |                 |  | % CO + H <sub>2</sub> |              |
| umgesetzt <b>60,2</b>                                  |                 |                   |                | <b>47,2</b>                                 |                |                 |  | <b>52,8</b>           |              |
| verflüssigt  |                 |                   |                |   |                |                 |  |                       |              |
| Verfl.-Grad A  |                 |                   |                |   |                |                 |  |                       |              |
| " " P  |                 |                   |                |   |                |                 |  | <b>29,5</b>           |              |
| CH <sub>4</sub> : <b>7,5</b>                           |                 |                   |                | CO <sub>2</sub> : <b>33,5</b>               |                |                 |  | bezogen auf CO-Umsatz |              |
| <b>Produkte</b>  |                 |                   |                | <b>Gesamprodukt</b>                         |                |                 |  |                       |              |
| Paraffingätsch   | <b>3,60</b>     | kg                | <b>27,6</b>    | %   | SB             |                 | °C   |                       |              |
| Öl-Kondensat   | <b>5,40</b>     | "                 | <b>41,3</b>    | %   | — 200 °C       |                 | %  |                       |              |
| A.-K. Benzin   | <b>4,09</b>     | "                 | <b>31,1</b>    | %   | 200 — 320 °C   |                 | %  |                       |              |
| Flüssige Prod!   | <b>13,09</b>    | "                 |                | 100 %                                       | > 320 °C       |                 | %  |                       |              |
| Sywasser   | <b>11,90</b>    | kg =              | <b>0,91</b>    | × flüss. Produkte                           | Olefine        |                 | Vol. %   |                       |              |
|  |                 |                   |                |   |                |                 |  | — 200° ..... 200-320° |              |
| <b>Ausbeute</b>  |                 |                   |                |   |                |                 |  |                       |              |
| Flüssige Prod.   | <b>42,7</b>     | g/Nm <sup>3</sup> | <b>49,2</b>    | g/Nm <sup>3</sup>                           | W-gas Sygas    |                 | Nutzgas (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> |                       |              |
| Gasöl  | "               | "                 | "              | "   | " "            |                 | " "  |                       |              |
| Gesamt-Produkt   | "               | "                 | "              | "   | " "            |                 | " "  |                       |              |
| Sywasser   | "               | "                 | "              | "   | " "            |                 | " "  |                       |              |
| <b>Bemerkungen:</b>                                    |                 |                   |                |   |                |                 |  |                       |              |
| <b>Ofen wird mit Wassergas im Kreislauf betrieben.</b> |                 |                   |                |   |                |                 |  |                       |              |
| <b>000308</b>  |                 |                   |                |   |                |                 |  |                       |              |

| Druckversuchsanlage                            |                               | Versuchsbericht vom 11./12. 6. 1943  |                |      |        |               |     |      |      |              |
|--|-------------------------------|--------------------------------------|----------------|------|--------|---------------|-----|------|------|--------------|
| Ofen-Nr. 11                                    | Betriebsstunden 24/744        |                                      |                |      |        |               |     |      |      |              |
| Füllung: 13.                                   | Gasdruck 10 atü               |                                      |                |      |        |               |     |      |      |              |
| Co-Fe-Inhalt -- kg                             | Temperatur 20 atü 214 °C      |                                      |                |      |        |               |     |      |      |              |
| W-Gas 303 Nm³                                  | Restgas 192 Nm³               |                                      |                |      |        |               |     |      |      |              |
| " " "  | " 8 Nm³/h                     |                                      |                |      |        |               |     |      |      |              |
| " " "  | Kreislaufgas 734 Nm³          |                                      |                |      |        |               |     |      |      |              |
| " 12,6 Nm³/h                                   | Kreislauf: 1 + 2,42           |                                      |                |      |        |               |     |      |      |              |
| Belastung --                                   | Nm³ / kg,h 0,99               | Nm³/Norm.-Vol., h                    |                |      |        |               |     |      |      |              |
| Analysen:                                      | CO₂                           | CmHn                                 | O₂             | CO   | H₂     | CH₄           | N₂  | C-Z  | N-F  | Litergewicht |
| Wassergas                                      | 6,9                           | --                                   | 0,1            | 37,4 | 49,3   | 0,3           | 6,0 | --   | 5,82 |              |
| Restgas  | 24,1                          | 0,2                                  | 0,1            | 22,7 | 40,5   | 3,5           | 8,9 | 1,05 | 8,83 |              |
| Kreislaufgas                                   |                               |                                      |                | 27,0 | 43,1   |               |     |      |      |              |
| H₂/CO im Kreislaufgas                          |                               |                                      |                | 1,50 |        |               |     |      |      |              |
| Gesamt-Inerte (Idealgas) 13,3 %                | Kontraktion nach Menge        |                                      |                |      | 36,6 % |               |     |      |      |              |
| H₂:CO im Sygas 1,32                            | " " N₂                        |                                      |                |      | 34,2 % |               |     |      |      |              |
| H₂:CO im Restgas 1,78                          | " " CO₂                       |                                      |                |      | -- %   |               |     |      |      |              |
| Verbrauch von H₂:CO 1,01                       | Durchschnittliche Kontraktion |                                      |                |      | 35,4 % |               |     |      |      |              |
| umgesetzt                                      | % CO 60,2                     | % H₂ 46,0                            | % CO + H₂ 52,1 |      |        |               |     |      |      |              |
| verflüssigt                                    |                               |                                      |                |      |        |               |     |      |      |              |
| Verfl.-Grad A                                  |                               |                                      |                |      |        |               |     |      |      |              |
| " " P  | 28,7                          |                                      |                |      |        |               |     |      |      |              |
| CH₄ + H₂ + H₂O 9,7                             | CO₂ 32,4                      | bezogen auf CO-Umsatz                |                |      |        |               |     |      |      |              |
| Produkte                                       |                               |                                      |                |      |        | Gesamtprodukt |     |      |      |              |
| Paraffingasch 3,45 kg                          | 28 %                          | SB                                   | °C             |      |        |               |     |      |      |              |
| Ol-Kondensat 5,30 "                            | 43 %                          | - 200 °C                             | %              |      |        |               |     |      |      |              |
| A.-K. Benzin 3,60 "                            | 29 %                          | 200 - 320 °C                         | %              |      |        |               |     |      |      |              |
| Flüssige Prod. 12,35 "                         | 100 %                         | > 320 °C                             | %              |      |        |               |     |      |      |              |
| Sywasser 12,50 kg = 0,01 × flüss. Produkte     |                               | Olefine                              | Vol. %         |      |        |               |     |      |      |              |
|  |                               | - 200°                               | ; 200-320°     |      |        |               |     |      |      |              |
| Ausbeute                                       |                               |                                      |                |      |        |               |     |      |      |              |
| Flüssige Prod. 10,8                            | W-gas 47,2                    | g/Nm³ Nutzgas (CO+H₂) g/Nm³ Idealgas |                |      |        |               |     |      |      |              |
| Gasol  | " "                           |                                      |                |      |        |               |     |      |      |              |
| Gesamt-Produkt                                 | " "                           |                                      |                |      |        |               |     |      |      |              |
| Sywasser                                       | " "                           |                                      |                |      |        |               |     |      |      |              |
| Bemerkungen:                                   |                               |                                      |                |      |        |               |     |      |      |              |
| Ofen wird mit Wassergas im Kreislauf gefahren. |                               |                                      |                |      |        |               |     |      |      |              |
| 000309   |                               |                                      |                |      |        |               |     |      |      |              |



| Druckversuchsanlage                             |                                   |                               |                                      | Versuchsbericht vom 9./10. 6. 1943  |   |                      |                |      |                   |              |  |
|---|-----------------------------------|-------------------------------|--------------------------------------|-------------------------------------|---|----------------------|----------------|------|-------------------|--------------|--|
| Ofen-Nr. 11                                     |                                   |                               |                                      | Betriebsstunden 24/696              |   |                      |                |      |                   |              |  |
| Füllung: 13.                                    |                                   |                               |                                      | Gasdruck 10 atü                     |   |                      |                |      |                   |              |  |
| Zn-Fe-Inhalt -- kg                              |                                   |                               |                                      | Temperatur 20 atü 214 °C            |   |                      |                |      |                   |              |  |
| Sy-W-Gas 298 Nm <sup>3</sup>                    |                                   |                               |                                      | Restgas -- Nm <sup>3</sup>          |   |                      |                |      |                   |              |  |
| " " "   |                                   |                               |                                      | " -- Nm <sup>3</sup> /h             |   |                      |                |      |                   |              |  |
| " 12,4 Nm <sup>3</sup> /h                       |                                   |                               |                                      | Kreislaufgas 667 Nm <sup>3</sup>    |   |                      |                |      |                   |              |  |
| " " "   |                                   |                               |                                      | Kreislauf 2,44                      |   |                      |                |      |                   |              |  |
| Belastung -- Nm <sup>3</sup> /kg,h              |                                   |                               |                                      | 0,98 Nm <sup>3</sup> /Norm.-Vol., h |   |                      |                |      |                   |              |  |
| Analysen:                                       | CO <sub>2</sub>                   | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub>                       | CO                                  | H <sub>2</sub>  | CH <sub>4</sub>      | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |  |
| Wassergas Syngas                                | 8,7                               | -                             | 0,1                                  | 35,1                                | 49,5  | 0,3                  | 6,9            | --   | 6,15              |              |  |
| Restgas   | 25,2                              | 0,2                           | 0,1                                  | 20,4                                | 41,1  | 3,7                  | 9,3            | 1,12 | 9,22              |              |  |
| Kreislaufgas                                    |                                   |                               |                                      | 23,5                                | 43,5  |                      |                |      |                   |              |  |
| H <sub>2</sub> /CO im Kreislaufgas              |                                   |                               |                                      |                                     | 1,85  |                      |                |      |                   |              |  |
| Gesamt-Inerte (Idealgas)                        | 15,4 %                            |                               | Kontraktion nach Menge -- %          |                                     |   |                      |                |      |                   |              |  |
| H <sub>2</sub> :CO im Syngas                    | 1,41                              |                               | " " N <sub>2</sub> 33,3 %            |                                     |   |                      |                |      |                   |              |  |
| H <sub>2</sub> :CO im Restgas                   | 2,10                              |                               | " " CO <sub>2</sub> -- %             |                                     |   |                      |                |      |                   |              |  |
| Verbrauch von H <sub>2</sub> :CO                | 1,03                              |                               | Durchschnittliche Kontraktion 33,3 % |                                     |   |                      |                |      |                   |              |  |
| umgesetzt                                       | % CO 61,3                         |                               | % H <sub>2</sub> 44,7                |                                     | % CO + H <sub>2</sub> 51,5                              |                      |                |      |                   |              |  |
| verflüssigt                                     |                                   |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| Verfl.-Grad A                                   |                                   |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| " " P   | 33,0                              |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub> | 10,1                              |                               | CO <sub>2</sub> 37,5                 |                                     | bezogen auf CO-Umsatz                                   |                      |                |      |                   |              |  |
| <b>Produkte</b>                                 |                                   |                               |                                      |                                     |   | <b>Gesamtprodukt</b> |                |      |                   |              |  |
| Paraffingetsch                                  | 3,23 kg                           |                               | 23,8 %                               |                                     |   | SB                   | °C             |      |                   |              |  |
| Öl-Kondensat                                    | 5,40                              |                               | 39,8 %                               |                                     |   | - 200 °C             | %              |      |                   |              |  |
| A.-K. Benzin                                    | 4,90                              |                               | 36,4 %                               |                                     |   | 200 - 320 °C         | %              |      |                   |              |  |
| Flüssige Prod.                                  | 13,53                             |                               | 100 %                                |                                     |   | > 320 °C             | %              |      |                   |              |  |
| Sywasser  | 14,60 kg = 1,08 × flüss. Produkte |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| Olefine   |                                   |                               |                                      |                                     |   | Vol. %               |                |      |                   |              |  |
| - 200°  |                                   |                               |                                      |                                     |   | ; 200-320°           |                |      |                   |              |  |
| <b>Ausbeute</b>                                 |                                   |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| Flüssige Prod.                                  | 45,5 g/Nm <sup>3</sup>            |                               | W-gas Syngas 53,8 g/Nm <sup>3</sup>  |                                     | Nutzgas (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> Idealgas |                      |                |      |                   |              |  |
| Gasol   | " " " " " " " "                   |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| Gesamt-Produkt                                  | " " " " " " " "                   |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| Sywasser  | " " " " " " " "                   |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| <b>Bemerkungen:</b>                             |                                   |                               |                                      |                                     |   |                      |                |      |                   |              |  |
| Ofen wird mit Wassergas im Kreislauf gefahren.  |                                   |                               |                                      |                                     |   |                      |                |      |                   |              |  |

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|   |  |  |                               |   |      |                      |                 |                |      |                   |              |
|---|--|--|-------------------------------|---|------|----------------------|-----------------|----------------|------|-------------------|--------------|
| <b>Druckversuchsanlage</b>                          |  | <b>Produktionsbericht vom 8./9.6. 1943</b> |                               |   |      |                      |                 |                |      |                   |              |
| Ofen-Nr. 11   |  | 24/672                                     |                               |   |      |                      |                 |                |      |                   |              |
| Füllung: 13   |  | Betriebsstunden 10                         |                               |   |      |                      |                 |                |      |                   |              |
| Co-Fe-Inhalt - kg                                   |  | Gasdruck 10 atü                            |                               |   |      |                      |                 |                |      |                   |              |
|   |  | Temperatur 20 atü 214 °C                   |                               |   |      |                      |                 |                |      |                   |              |
| S <sub>2</sub> /W-Gas 295 Nm <sup>3</sup>           |  | Restgas - Nm <sup>3</sup>                  |                               |   |      |                      |                 |                |      |                   |              |
| " " " "   |  | " " " " Nm <sup>3</sup> /h                 |                               |   |      |                      |                 |                |      |                   |              |
| " " " "   |  | Kreislaufgas 794 Nm <sup>3</sup>           |                               |   |      |                      |                 |                |      |                   |              |
| " " " " 12,3 Nm <sup>3</sup> /h                     |  | Kreislauf 2,69                             |                               |   |      |                      |                 |                |      |                   |              |
| Belastung - Nm <sup>3</sup> /kg,h                   |  | 0,97                                       |                               |   |      |                      |                 |                |      |                   |              |
| Analysen:   |  | CO <sub>2</sub>                            | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub>                                  | CO   | H <sub>2</sub>       | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
| Wassergas   |  | 7,2  | -                             | 0,1   | 37,0 | 49,4                 | 0,3             | 6,0            | -    | 5,95              |              |
| Syngas  |  | 23,6                                       | 0,2                           | 0,1   | 22,3 | 40,9                 | 3,8             | 9,1            | 1,16 | 9,02              |              |
| Restgas   |  |  |                               |   | 26,3 | 43,2                 |                 |                |      |                   |              |
| Krsfgas   |  |  |                               |   |      |                      |                 |                |      |                   |              |
| H <sub>2</sub> /CO im Kreislaufgas                  |  |  |                               |   | 1,64 |                      |                 |                |      |                   |              |
| Gesamt-Inerte (Idealgas) 13,6 %                     |  | Kontraktion nach Menge 3 %                 |                               |   |      |                      |                 |                |      |                   |              |
| H <sub>2</sub> :CO im Sygas 1,34                    |  | " " N <sub>2</sub> 34,0 %                  |                               |   |      |                      |                 |                |      |                   |              |
| H <sub>2</sub> :CO im Restgas 1,83                  |  | " " CO <sub>2</sub> - %                    |                               |   |      |                      |                 |                |      |                   |              |
| Verbrauch von H <sub>2</sub> :CO 1,00               |  | Durchschnittliche Kontraktion 34,0 %       |                               |   |      |                      |                 |                |      |                   |              |
| umgesetzt %CO 60,3                                  |  | %H <sub>2</sub> 45,3                       |                               | %CO+H <sub>2</sub> 51,7                         |      |                      |                 |                |      |                   |              |
| verflüssigt   |  |  |                               |   |      |                      |                 |                |      |                   |              |
| Verfl.-Grad A                                       |  |  |                               |   |      |                      |                 |                |      |                   |              |
| " " P   |  | 36,2                                       |                               |   |      |                      |                 |                |      |                   |              |
| CH <sub>4</sub> + C <sub>m</sub> H <sub>n</sub> 9,9 |  | CO <sub>2</sub> 37,6                       |                               | bezogen auf CO-Umsatz                           |      |                      |                 |                |      |                   |              |
| <b>Produkte</b>                                     |  |  |                               |   |      | <b>Gesamtprodukt</b> |                 |                |      |                   |              |
| Paraffingatsch 3,75 kg                              |  | 25,0 %                                     |                               | SB ..... °C                                     |      |                      |                 |                |      |                   |              |
| Ol-Kondensat 6,00 "                                 |  | 40,0 %                                     |                               | - 100° %  |      |                      |                 |                |      |                   |              |
| A.-K. Benzin 5,32 "                                 |  | 35,0 %                                     |                               | - 200° %  |      |                      |                 |                |      |                   |              |
| Flüssige Prod. 15,07 "                              |  | 100 %                                      |                               | - 320° %  |      |                      |                 |                |      |                   |              |
| Sywasser 14,10 kg = 0,94 × flüss. Produkte          |  | Olefine Vol. %                             |                               |   |      |                      |                 |                |      |                   |              |
|   |  | - 200° ..... , 200-320° .....              |                               |   |      |                      |                 |                |      |                   |              |
| <b>Ausbeute</b>                                     |  |  |                               |   |      |                      |                 |                |      |                   |              |
| Flüssige Prod. 51,0 g Nm <sup>3</sup> Sygas         |  | 59,0 g Nm <sup>3</sup> Nutzgas             |                               | (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> Idealgas |      |                      |                 |                |      |                   |              |
| Gasol   |  |  |                               |   |      |                      |                 |                |      |                   |              |
| Gesamt-Produkt                                      |  |  |                               |   |      |                      |                 |                |      |                   |              |
| Sywasser  |  |  |                               |   |      |                      |                 |                |      |                   |              |
| <b>Bemerkungen:</b>                                 |  |  |                               |   |      |                      |                 |                |      |                   |              |
| Ofen wird mit Wassergas im Kreislauf gefahren.      |  |  |                               |   |      |                      |                 |                |      |                   |              |

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| <b>Druckversuchsanlage</b>   |                 |                               |                |      |                | <b>Produktionsbericht vom 6./7.6. 1943</b>  |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
|--|-----------------|-------------------------------|----------------|------|----------------|---|----------------|------|-------------------|--------------|--|-----------|-----------------|-------------------------------|----------------|----|----------------|-----------------|----------------|-----|-------------------|--------------|-----------|-----|---|-----|------|------|-----|-----|---|------|--|---------|------|-----|-----|------|------|-----|-----|------|------|--|-----------|--|--|--|------|------|--|--|--|--|--|------------------------------------|--|--|--|------|--|--|--|--|--|--|
| Ofen-Nr. 11  |                 |                               |                |      |                | Betriebsstunden 24/624                      |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Füllung: 13  |                 |                               |                |      |                | Gasdruck 10 atü                             |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| C <sub>2</sub> -Fe-Inhalt: .. kg   |                 |                               |                |      |                | Temperatur 20 atü 214 °C                    |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| W-Gas 309 Nm <sup>3</sup>  |                 |                               |                |      |                | Restgas 192 Nm <sup>3</sup>                 |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| " " " "  |                 |                               |                |      |                | " 8,0 Nm <sup>3</sup> /h                    |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| " " " "  |                 |                               |                |      |                | <b>XXI</b> Kreislaufgas 788 Nm <sup>3</sup> |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| " " " " 12,8 Nm <sup>3</sup> /h  |                 |                               |                |      |                | Kreislauf 2,55                              |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Belastung: - Nm <sup>3</sup> /kg.h 1,01  |                 |                               |                |      |                | Nm <sup>3</sup> /Norm.-Vol., h              |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th>Analysen:</th> <th>CO<sub>2</sub></th> <th>C<sub>m</sub>H<sub>n</sub></th> <th>O<sub>2</sub></th> <th>CO</th> <th>H<sub>2</sub></th> <th>CH<sub>4</sub></th> <th>N<sub>2</sub></th> <th>C-Z</th> <th>N<sub>2</sub>-F</th> <th>Litergewicht</th> </tr> </thead> <tbody> <tr> <td>Wassergas</td> <td>5,7</td> <td>-</td> <td>0,1</td> <td>39,6</td> <td>48,5</td> <td>0,3</td> <td>5,8</td> <td>-</td> <td>5,64</td> <td></td> </tr> <tr> <td>Restgas</td> <td>23,0</td> <td>0,2</td> <td>0,1</td> <td>25,0</td> <td>39,6</td> <td>3,2</td> <td>8,9</td> <td>1,06</td> <td>8,82</td> <td></td> </tr> <tr> <td>Krsrlfgas</td> <td></td> <td></td> <td></td> <td>29,2</td> <td>42,1</td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> <tr> <td>H<sub>2</sub>/CO im Kreislaufgas</td> <td></td> <td></td> <td></td> <td>1,44</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> </tbody> </table> |                 |                               |                |      |                |   |                |      |                   |              |  | Analysen: | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F | Litergewicht | Wassergas | 5,7 | - | 0,1 | 39,6 | 48,5 | 0,3 | 5,8 | - | 5,64 |  | Restgas | 23,0 | 0,2 | 0,1 | 25,0 | 39,6 | 3,2 | 8,9 | 1,06 | 8,82 |  | Krsrlfgas |  |  |  | 29,2 | 42,1 |  |  |  |  |  | H <sub>2</sub> /CO im Kreislaufgas |  |  |  | 1,44 |  |  |  |  |  |  |
| Analysen:  | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub>                             | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Wassergas  | 5,7             | -                             | 0,1            | 39,6 | 48,5           | 0,3   | 5,8            | -    | 5,64              |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Restgas  | 23,0            | 0,2                           | 0,1            | 25,0 | 39,6           | 3,2   | 8,9            | 1,06 | 8,82              |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Krsrlfgas  |                 |                               |                | 29,2 | 42,1           |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| H <sub>2</sub> /CO im Kreislaufgas   |                 |                               |                | 1,44 |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Gesamt-Inerte (Idealgas) 11,9 %  |                 |                               |                |      |                | Kontraktion nach Menge 37,9 %               |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| H <sub>2</sub> :CO im Sygas 1,22   |                 |                               |                |      |                | " " N <sub>2</sub> 36,0 %                   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| H <sub>2</sub> :CO im Restgas 1,58   |                 |                               |                |      |                | " " CO <sub>2</sub> - %                     |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Verbrauch von H <sub>2</sub> :CO 0,99  |                 |                               |                |      |                | Durchschnittliche Kontraktion 37,0 %        |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| umgesetzt %CO 60,1   |                 |                               |                |      |                | %H <sub>2</sub> 48,5                        |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| verflüssigt  |                 |                               |                |      |                | %CO+H <sub>2</sub> 53,8                     |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Verfl.-Grad A  |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| " " P  |                 |                               |                |      |                | 32,4  |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| CH <sub>4</sub> + C <sub>2</sub> H <sub>4</sub> 7,2 CO <sub>2</sub> 37,0 bezogen auf CO-Umsatz   |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| <b>Produkte</b>  |                 |                               |                |      |                | <b>Gesamtprodukt</b>                        |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Paraffingatsch 4,00 kg 26,8 %  |                 |                               |                |      |                | SB .. °C                                    |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Ol-Kondensat 6,00 " 40,1 %   |                 |                               |                |      |                | - 100° .. %                                 |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| A-K. Benzin 4,95 " 33,1 %  |                 |                               |                |      |                | - 200° .. %                                 |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Flüssige Prod. 14,95 100 %   |                 |                               |                |      |                | - 320° .. %                                 |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Sywasser 13,00 kg = 0,87 x flüss. Produkte   |                 |                               |                |      |                | Olefine Vol. %                              |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
|  |                 |                               |                |      |                | - 200° .., 200-320° ..                      |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| <b>Ausbeute</b>  |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Flüssige Prod. 48,4 g/Nm <sup>3</sup> Sygas 55,0 g/Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) g/Nm <sup>3</sup> Idealgas   |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Gasol " " " " " " " "  |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Gesamt-Produkt " " " " " " " "   |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Sywasser " " " " " " " "   |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| <b>Bemerkungen:</b>  |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| Ofen wird mit Wassergas im Kreislauf gefahren.   |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |
| <b>000314</b>  |                 |                               |                |      |                |   |                |      |                   |              |  |           |                 |                               |                |    |                |                 |                |     |                   |              |           |     |   |     |      |      |     |     |   |      |  |         |      |     |     |      |      |     |     |      |      |  |           |  |  |  |      |      |  |  |  |  |  |                                    |  |  |  |      |  |  |  |  |  |  |

























# Druckversuchsanlage

Produktionsbericht vom 25./26. 5. 1943

Ofen-Nr. 11

Füllung: 13

1/66 Co-Fe-Inhalt: - kg

Betriebsstunden 24/351

Gasdruck 10 atü

Temperatur 20 atü 214 °C

sy-W-Gas 304 Nm³

Restgas 156 Nm³

Kreislaufgas 846 Nm³/h

Kreislauf 278 Nm³

Belastung: - Nm³/kg.h 1,00

| Analysen:             | Nm³/kg.h |      |     |      |      | Nm³/Norm.-Vol., h |     |      |      |  | Litergewicht |
|-----------------------|----------|------|-----|------|------|-------------------|-----|------|------|--|--------------|
|                       | CO₂      | CmHn | O₂  | CO   | H₂   | CH₄               | N₂  | C-Z  | N₂-F |  |              |
| Wassergas             | 5,7      | -    | 0,1 | 39,3 | 49,1 | 0,3               | 5,5 | -    | -    |  |              |
| Restgas               | 23,3     | 0,3  | 0,1 | 24,4 | 38,9 | 3,6               | 9,4 | 1,12 |      |  |              |
| Kreislaufgas          |          |      |     | 28,4 | 41,6 |                   |     |      |      |  |              |
| H₂/CO im Kreislaufgas |          |      |     |      | 1,46 |                   |     |      |      |  |              |

Gesamt-Inerte (Idealgas) 11,6 %

H₂:CO im Sygas 1,25

H₂:CO im Restgas 1,59

Verbrauch von H₂:CO 1,07

Kontraktion nach Menge - %

" " N₂ - %

" " CO₂ - %

Durchschnittliche Kontraktion 45 %

umgesetzt %CO 66,0

verflüssigt

Verf.-Grad A

" " P

%H₂ 56,5

%CO+H₂ 60,7

CH₄ + CmHn 6,5 CO₂ 27,4 bezogen auf CO-Umsatz

## Produkte

|                |       |      |                             |
|----------------|-------|------|-----------------------------|
| Paraffingasch  | 2,60  | 10,7 | %                           |
| Ol-Kondensat   | 6,00  | 24,7 | %                           |
| A.-K. Benzin   | 15,65 | 64,6 | %                           |
| Flüssige Prod. | 24,25 | 100% | %                           |
| Sywasser       | 14,40 | 0,59 | kg = 0,59 x flüss. Produkte |

## Gesamtprodukt

|         |          |
|---------|----------|
| SB      | °C       |
| - 100°  | %        |
| - 200°  | %        |
| - 320°  | %        |
| Olefine | Vol. %   |
| - 200°  | 200-320° |

## Ausbeute

|                |             |                       |                |
|----------------|-------------|-----------------------|----------------|
| Flüssige Prod. | g/Nm³ Sygas | g/Nm³ Nutzgas (CO+H₂) | g/Nm³ Idealgas |
| Gasol          | "           | "                     | "              |
| Gesamt-Produkt | "           | "                     | "              |
| Sywasser       | "           | "                     | "              |

## Bemerkungen:

Ofen wird mit Wassergas im Kreislauf gefahren.

000326



|  |  |      |      |   |                   |                         |     |      |                |              |  |
|--|--|------|------|---|-------------------|-------------------------|-----|------|----------------|--------------|--|
| <b>Druckversuchsanlage</b>                     |  |      |      | <b>Produktionsbericht vom 23./24. 5. 1943</b> |                   |                         |     |      |                |              |  |
| Ofen-Nr. 11                                    |  |      |      | Betriebsstunden 23/303                        |                   |                         |     |      |                |              |  |
| Füllung: 13                                    |  |      |      | Gasdruck 10 atü                               |                   |                         |     |      |                |              |  |
| Co-Fe-Inhalt: .. kg                            |  |      |      | Temperatur 17,5 atü 207 °C                    |                   |                         |     |      |                |              |  |
| Sy-W-Gas 305 Nm³                               |  |      |      | Restgas .. Nm³                                |                   |                         |     |      |                |              |  |
| " " " " " "                                    |  |      |      | " " " " " " Nm³/h                             |                   |                         |     |      |                |              |  |
| " " " " " " 13,3 Nm³/h                         |  |      |      | Kreislaufgas 743 Nm³                          |                   |                         |     |      |                |              |  |
| " " " " " " " "                                |  |      |      | Kreislauf 2,44                                |                   |                         |     |      |                |              |  |
| Belastung .. Nm³ / kg.h                        |  |      |      | 1,04 Nm³ / Norm.-Vol., h                      |                   |                         |     |      |                |              |  |
| Analysen:                                      | CO₂  | CmHn | O₂   | CO  | H₂                | CH₄                     | N₂  | C-Z  | N₂-F           | Litergewicht |  |
| Wassergas                                      | 5,6  | -    | 0,1  | 39,7  | 49,0              | 0,3                     | 5,3 | -    | 5,23           |              |  |
| Sygas  | 17,2   | 0,4  | 0,1  | 30,1  | 41,4              | 2,3                     | 8,5 | 1,17 | 8,40           |              |  |
| Restgas  |  |      |      | 33,0  | 43,6              |                         |     |      |                |              |  |
| Krsflgas                                       |  |      |      |   |                   |                         |     |      |                |              |  |
| H/CO im Kreislaufgas                           |  |      |      | 1,32  |                   |                         |     |      |                |              |  |
| Gesamt-Inerte (Idealgas) 11,3 %                |  |      |      | Kontraktion nach Menge .. %                   |                   |                         |     |      |                |              |  |
| H₂:CO im Sygas 1,23                            |  |      |      | " " N₂ 37,7 %                                 |                   |                         |     |      |                |              |  |
| H₂:CO im Restgas 1,38                          |  |      |      | " " CO₂ .. %                                  |                   |                         |     |      |                |              |  |
| Verbrauch von H₂:CO 1,11                       |  |      |      | Durchschnittliche Kontraktion 37,7 %          |                   |                         |     |      |                |              |  |
| umgesetzt                                      | %CO  |      | %H₂  |   | %CO+H₂            |                         |     |      |                |              |  |
| verflüssigt                                    | 52,6   |      | 47,4 |   | 49,7              |                         |     |      |                |              |  |
| Verfl.-Grad A                                  |  |      |      |   |                   |                         |     |      |                |              |  |
| " " P  | Stromausfall von 3 <sup>05</sup> -4 <sup>10h</sup> |      |      |   |                   |                         |     |      |                |              |  |
| CH₄ + CₘHₙ 5,4                                 |  |      |      | CO₂ 24,4 bezogen auf CO-Umsatz                |                   |                         |     |      |                |              |  |
| <b>Produkte</b>                                |  |      |      |   |                   | <b>Gesamtprodukt</b>    |     |      |                |              |  |
| Paraffingatsch                                 | 1,40   | kg   | 8,6  | %   | SB .. °C          |                         |     |      |                |              |  |
| Ol-Kondensat                                   | 5,70   | "    | 35,0 | %   | - 100° .. %       |                         |     |      |                |              |  |
| A-K. Benzin                                    | 9,20   | "    | 56,4 | %   | - 200° .. %       |                         |     |      |                |              |  |
| Flüssige Prod.                                 | 16,30  | "    |      | 100%  | - 320° .. %       |                         |     |      |                |              |  |
| Sywasser                                       | 11,40  | kg = | 0,70 | flüss. Produkte                               | Olefine Vol. % .. |                         |     |      |                |              |  |
|  |  |      |      |   |                   | - 200° .. ; 200; 320° / |     |      |                |              |  |
| <b>Ausbeute</b>                                |  |      |      |   |                   |                         |     |      |                |              |  |
| Flüssige Prod.                                 | g Nm³ Sygas  |      |      |   | g Nm³ Nutzgas     |                         |     |      | g/Nm³ Idealgas |              |  |
| Gasol  | "  |      |      |   | "                 |                         |     |      | "              |              |  |
| Gesamt-Produkt                                 | "  |      |      |   | "                 |                         |     |      | "              |              |  |
| Sywasser                                       | "  |      |      |   | "                 |                         |     |      | "              |              |  |
| <b>Bemerkungen:</b>                            |  |      |      |   |                   |                         |     |      |                |              |  |
| Ofen wird mit Wassergas im Kreislauf gefahren. |  |      |      |   |                   |                         |     |      |                |              |  |
| 000328   |  |      |      |   |                   |                         |     |      |                |              |  |





**Druckversuchsanlage** **Produktionsbericht vom** 21./22.5. 1943

|                  |                            |
|------------------|----------------------------|
| Ofen-Nr. 11      | Betriebsstunden 24/256     |
| Füllung: 13      | Gasdruck 10 atü            |
| Co/Fe-Inhalt: kg | Temperatur 17,5 atü 207 °C |

|                                 |                                   |
|---------------------------------|-----------------------------------|
| Sy/W-Gas: 3,19 Nm <sup>3</sup>  | Restgas: Nm <sup>3</sup>          |
| " " " " "                       | " " " " Nm <sup>3</sup> /h        |
| " " " " 13,3 Nm <sup>3</sup> /h | Kreislaufgas: 840 Nm <sup>3</sup> |
|                                 | Kreislauf: 2,64                   |

Belastung: Nm<sup>3</sup>/kg, h 1,05 Nm<sup>3</sup>/Norm.-Vol., h

| Analysen:                          | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                          | 6,0             | -                             | 0,1            | 39,1 | 49,2           | 0,3             | 5,3            | -    | 5,16              |              |
| Sygas                              | 19,5            | 0,5                           | 0,1            | 27,8 | 41,3           | 2,6             | 8,1            | 1,12 | 8,05              |              |
| Restgas                            |                 |                               |                | 35,0 | 43,5           |                 |                |      |                   |              |
| Kreislaufgas                       |                 |                               |                |      |                |                 |                |      |                   |              |
| H <sub>2</sub> /CO in Kreislaufgas |                 |                               |                | 1,24 |                |                 |                |      |                   |              |

|                                       |                                    |
|---------------------------------------|------------------------------------|
| Gesamt-Inerte (Idealgas) 11,7 %       | Kontraktion nach Menge: %          |
| H <sub>2</sub> :CO im Sygas 1,26      | " " N <sub>2</sub> : %             |
| H <sub>2</sub> :CO im Restgas 1,49    | " " CO <sub>2</sub> : %            |
| Verbrauch von H <sub>2</sub> :CO 1,09 | Durchschnittliche Kontraktion 40 % |

|                |          |                      |                         |
|----------------|----------|----------------------|-------------------------|
| umgesetzt      | %CO 57,3 | %H <sub>2</sub> 49,6 | %CO+H <sub>2</sub> 53,0 |
| verflüssigt    |          |                      |                         |
| Verfl.-Grad A. |          |                      |                         |
| " " P          |          |                      |                         |

CH<sub>4</sub> + C<sub>m</sub>H<sub>n</sub> 5,6 CO<sub>2</sub> 26,8 bezogen auf CO-Umsatz

| Produkte   | Gesamtprodukt           |
|--|-------------------------|
| Paraffingatsch 2,30 kg 9,7 %                     | SB °C                   |
| Ol-Kondensat 21,45 " 90,3 %                      | - 100° °C               |
| A.-K. Benzin 23,75 " 100 %                       | - 200° °C               |
| Flüssige Prod. 15,70 kg = 0,66 x flüss. Produkte | - 320° °C               |
| Sywasser   | Olefine Vol. %          |
|  | - 200° ..... 200 - 320° |

**Ausbeute**

|                |                         |  |                            |
|----------------|-------------------------|--|----------------------------|
| Flüssige Prod. | g Nm <sup>3</sup> Sygas | g Nm <sup>3</sup> Nutzgas (CO+H <sub>2</sub> ) | g/Nm <sup>3</sup> Idealgas |
| Gasol          | " "                     | " "  | " "                        |
| Gesamt-Produkt | " "                     | " "  | " "                        |
| Sywasser       | " "                     | " "  | " "                        |

**Bemerkungen:**

Ofen wird mit Wassergas im Kreislauf gefahren.

000330

# Druckversuchsanlage

Produktionsbericht vom 20./21.5. 1943

Ofen-Nr. 11  
 Füllung: 13  
 G<sub>0</sub>-Fe-Inhalt: kg

Betriebsstunden 24/232  
 Gasdruck 10 atü  
 Temperatur 17,5 atü 207 °C

Sy-W-Gas 319 Nm<sup>3</sup>  
 " " " " " "  
 " 13,3 Nm<sup>3</sup>/h

Restgas 191 Nm<sup>3</sup>  
 " 8,0 Nm<sup>3</sup>/h  
 Kreislaufgas 798 Nm<sup>3</sup>  
 Kreislauf 2,50

Belastung Nm<sup>3</sup>/kg,h 1,05 Nm<sup>3</sup>/Norm.-Vol.,h

| Analysen:                          | CO <sub>2</sub> | C <sub>m</sub> H <sub>n</sub> | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z  | N <sub>2</sub> -F | Litergewicht |
|------------------------------------|-----------------|-------------------------------|----------------|------|----------------|-----------------|----------------|------|-------------------|--------------|
| Wassergas                          | 5,3             | -                             | 0,1            | 40,2 | 49,3           | 0,3             | 4,8            | -    | 4,71              |              |
| Restgas                            | 19,3            | 0,6                           | 0,1            | 29,1 | 40,7           | 2,5             | 7,7            | 1,07 | 7,63              |              |
| Kreislaufgas                       |                 |                               |                | 32,3 | 43,2           |                 |                |      |                   |              |
| H <sub>2</sub> /CO im Kreislaufgas |                 |                               |                | 1,34 |                |                 |                |      |                   |              |

Gesamt-Inerte (Idealgas) 10,5 %  
 H<sub>2</sub>, CO im Sygas 1,23  
 H<sub>2</sub>, CO im Restgas 1,40  
 Verbrauch von H<sub>2</sub>, CO 1,09

Kontraktion nach Menge 40,0 %  
 " " N<sub>2</sub> 38,4 %  
 " " CO<sub>2</sub> %  
 Durchschnittliche Kontraktion 39,2 %

|               | %CO  | %H <sub>2</sub> | %CO+H <sub>2</sub> |
|---------------|------|-----------------|--------------------|
| umgesetzt     | 56,0 | 49,6            | 52,5               |
| verflüssigt   |      |                 |                    |
| Verfl.-Grad A |      |                 |                    |
| " " P         |      |                 | 33,6               |

CH<sub>4</sub> + C<sub>2</sub>H<sub>4</sub> 5,4 CO<sub>2</sub> 28,6 bezogen auf CO-Umsatz

## Produkte

Paraffingasch 2,50 kg 15,7 %  
 Öl-Kondensat 6,55 " 41,0 %  
 A.-K. Benzin 6,90 " 43,3 %  
 Flüssige Prod. 15,95 " 100 %  
 Sywasser 18,20 kg = 1,14 x flüss. Produkte

## Gesamtprodukt

SB °C  
 - 100° %  
 - 200° %  
 - 320° %  
 Olefine Vol. %  
 - 200° , 200-320°

## Ausbeute

Flüssige Prod. 50,0 g Nm<sup>3</sup> Sygas 55,9 g Nm<sup>3</sup> Nutzgas (CO+H<sub>2</sub>) g/Nm<sup>3</sup> Idealgas  
 Gasöl " " " " " "  
 Gesamt-Produkt " " " " " "  
 Sywasser " " " " " "

## Bemerkungen:

Ofen wird mit Wassergas im Kreislauf gefahren.

000331



















**Druckversuchsanlage**

**Produktionsbericht vom** 10./11.5. 1943

Ofen-Nr. 11  
 Füllung: 13  
 Co-Fe-Inhalt - kg

Betriebsstunden 21/30  
 Gasdruck 10 atü  
 Temperatur 0,8-10,5 atü 96 - °C 185 °C

Sy-W-Gas 303 Nm<sup>3</sup>  
 " " " " " "  
 " " " " " " 14,4 Nm<sup>3</sup>/h

Restgas 242 Nm<sup>3</sup>  
 " " " " " " 11,5 Nm<sup>3</sup>/h  
 Kreislaufgas - Nm<sup>3</sup>  
 Kreislauf -

Belastung Nm<sup>3</sup>/kg,h 1,04 Nm<sup>3</sup>/Norm-Vol., h

| Analysen: | CO <sub>2</sub> | CmHn | O <sub>2</sub> | CO   | H <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | C-Z | N <sub>2</sub> -F <sub>2</sub> | Litergewicht |
|-----------|-----------------|------|----------------|------|----------------|-----------------|----------------|-----|--------------------------------|--------------|
| Wassergas | 6,6             | -    | 0,1            | 38,9 | 48,1           | 0,3             | 6,0            | -   | 5,92                           |              |
| Sygas     | 9,7             | 0,3  | 0,1            | 37,5 | 44,2           | 0,5             | 7,7            | -   | 7,57                           |              |
| Restgas   |                 |      |                |      |                |                 |                |     |                                |              |

Gesamt-Inerte (Idealgas) 13,0 %  
 H<sub>2</sub>, CO im Sygas 1,24  
 H<sub>2</sub>, CO im Restgas 1,18  
 Verbrauch von H<sub>2</sub>, CO 1,42

Kontraktion nach Menge 20,1 %  
 " " N<sub>2</sub> 21,9 %  
 " " CO<sub>2</sub> - %  
 Durchschnittliche Kontraktion 21,0 %

umgesetzt %CO 23,9 %H<sub>2</sub> 27,4 %CO+H<sub>2</sub> 25,8  
 verflüssigt  
 Verfl.-Grad A  
 " " P

CH<sub>4</sub> + CmHn - CO<sub>2</sub> - bezogen auf CO-Umsatz

| Produkte       |                             | Gesamtprodukt |          |
|----------------|-----------------------------|---------------|----------|
| Paraffingasch  | - kg                        | SB            | °C       |
| Ol-Kondensat   | 1,30                        | - 100°        | %        |
| A.-K. Benzin   | -                           | - 200°        | %        |
| Flüssige Prod. | 1,30                        | - 320°        | %        |
| Sywasser       | 9,00 kg = X flüss. Produkte | Olefine       | Vol. %   |
|                |                             | - 200°        | 200-320° |

**Ausbeute**

Flüssige Prod. g Nm<sup>3</sup> Sygas g Nm<sup>3</sup> Nutzgas g Nm<sup>3</sup> Idealgas  
 Gasol  
 Gesamt-Produkt  
 Sywasser

**Bemerkungen:**

Ofen wurde nach dem Stillstand (seit 26./27.3.) am 10.5 11<sup>00</sup>h wieder angefahren.

000340



Gasol ausbeute.

|  | Gasol | Gasol   | Gasol | Verf.: | Gasol   | Gasol | Gasol | Carbol |
|--|-------|---------|-------|--------|---------|-------|-------|--------|
| A.K.-Turm                              | 66    | 66      | 5a    |        | 69      | 69    | 56    |        |
| Datum                                  |       | 3/4. 6. | 43    |        | 4/5. 6. | 43    |       |        |
| Zeit                                   | 8-10  | 0-2     | 8-8   | 0-8    | 8-10    | 0-8   | 8-8   |        |
| Nm <sup>3</sup> /Sygas                 |       |         |       |        | 314     | 316   | 306   | 2,98   |
| l Restgas                              |       |         |       | 1003   | 103     | 103   |       | 1524   |
| % Kontr.                               |       |         |       |        |         |       |       | 1409   |
| l Gasolgem.                            | 1309  | 1345    | 623   | 47     | 1448    | 1346  | 749   | 35,3   |
| Analyse: CO <sub>2</sub>               | 25,6  | 22,4    | 23,6  | 64,0   | 28,0    | 29,9  | 20,8  | 64,5   |
| C <sub>3</sub> H <sub>6</sub>          | 12,0  | 10,4    | 11,6  | 2,5    | 27,2    | 20,5  | 10,5  | 2,0    |
| C <sub>2</sub> H <sub>4</sub>          | 0,7   | 0,5     | 0,5   | 0,6    | 0,6     | 0,5   | 0,3   | 0,7    |
| O <sub>2</sub>                         | 0,7   | 0,7     | 0,0   | 0,1    | 0,7     | 0,0   | 0,7   | 0,7    |
| CO                                     | 18,8  | 9,6     | 17,4  | 2,4    | 9,3     | 10,0  | 12,6  | 8,2    |
| H <sub>2</sub>                         | 12,7  | 17,4    | 26,7  | 4,4    | 16,9    | 16,7  | 30,7  | 3,5    |
| CH <sub>4</sub> +                      | 17,5  | 17,3    | 12,9  | 19,5   | 18,2    | 17,3  | 14,8  | 16,2   |
| N <sub>2</sub>                         | 5,2   | 6,3     | 6,5   | 4,5    | 5,7     | 5,7   | 17,0  | 4,8    |
| C-Zahl                                 | 3,16  | 3,42    | 3,29  | 2,58   | 3,05    | 3,32  | 3,42  | 3,77   |
| Litergew. entspr. d. C-Z. (Kurvenwert) |       |         |       |        | 1,47    | 2,13  | 2,14  | 2,37   |
| g Gasol/l Gasolgem                     |       |         |       |        | 0,78    | 0,87  | 0,55  | 0,63   |
| g Gasol                                |       |         |       |        | 1050    | 1020  | 383   | 74,4   |
| g Gasol/Nm <sup>3</sup> Sygas          |       |         |       |        | 10,0    | 9,70  | 1,21  | 8,4    |
| Bemerkungen:                           |       |         |       |        |         |       |       |        |

000342

g/Nm<sup>3</sup> Sygas

19,96

g/Nm<sup>3</sup> C<sub>3</sub>H<sub>6</sub>

22,70

% C<sub>3</sub>H<sub>6</sub>

48

Gasol ausbeute.

|                                       | Gasol        | Gasol        | Gasol      | Carbol       | Gasol      | Gasol        | Gasol      | Carbol       |
|---------------------------------------|--------------|--------------|------------|--------------|------------|--------------|------------|--------------|
| A.K.-Turm                             | 66           | 66           | 59         |              | 69         | 69           | 56         |              |
| Datum                                 | 2. 6. 43     |              |            |              | 2/3. 6. 43 |              |            |              |
| Zeit                                  | 8-16         | 0-8          | 8-8        | 8-8          | 8-16       | 0-8          | 8-8        | 8-8          |
| Nm <sup>3</sup> /Sygas                | 336<br>112   | 336<br>112   | 336        | 2138         | 284<br>95  | 284<br>95    | 227        | 2130         |
| l Restgas                             |              |              |            | 1491<br>1390 |            |              |            | 1566<br>1452 |
| % Kontr.                              |              |              |            | 39.9         |            |              |            | 34.5         |
| l Gasolgem.                           | 1205<br>7120 | 1295<br>7205 | 675<br>628 | 47<br>43.7   | 953<br>285 | 1144<br>1110 | 624<br>580 | 48<br>44.6   |
| Analyse: CO <sub>2</sub>              | 26.9         | 30.7         | 32.9       | 62.5         | 33.7       | 37.0         | 33.5       | 64.8         |
| O <sub>3</sub> H <sub>6</sub>         | 22.6         | 19.4         | 10.4       | 5.7          | 7.9        | 17.6         | 12.3       | 4.5          |
| O <sub>2</sub> H <sub>4</sub>         | 0.6          | 0.7          | 0.7        | 0.5          | 0.9        | 0.7          | 0.6        | 0.5          |
| O <sub>2</sub>                        | 0.7          | 0.7          | 0.7        | 0.7          | 0.7        | 0.7          | 0.7        | 0.7          |
| CO                                    | 9.5          | 10.9         | 14.9       | 7.8          | 15.5       | 12.0         | 14.8       | 7.7          |
| H <sub>2</sub>                        | 13.9         | 13.7         | 20.7       | 3.4          | 23.2       | 16.0         | 19.2       | 3.9          |
| CH <sub>4</sub> <sup>+</sup>          | 20.8         | 27.4         | 14.8       | 15.9         | 13.8       | 17.6         | 14.2       | 14.5         |
| N <sub>2</sub>                        | 6.2          | 4.3          | 5.5        | 4.7          | 5.5        | 5.0          | 5.3        | 4.0          |
| C-Zahl                                | 2.88         | 3.22         | 3.46       | 2.74         | 2.92       | 3.14         | 3.10       | 2.38         |
| Litergew. entspr. d.O-Z. (Kurvezwert) | 1.77         | 2.07         | 2.22       | 1.57         | 1.82       | 2.02         | 2.05       | 0.26         |
| g Gasol/l Gasolgem                    | 0.77         | 0.85         | 0.56       | 0.34         | 0.40       | 0.71         | 0.53       | 0.27         |
| g Gasol                               | 26.9         | 10.15        | 3.52       | 14.85        | 3.53       | 7.82         | 3.75       | 9.36         |
| g Gasol/Nm <sup>3</sup> Sygas         | 7.75         | 9.10         | 1.05       | 6.24         | 7.72       | 2.33         | 1.32       | 2.06         |
| Bemerkungen:                          |              |              |            |              |            |              |            |              |

g Nach Sygas  
g Nach Ca.  
g Nach H<sub>2</sub>

15.71  
18.58  
42

11.40  
13.00  
40

Druckversuchsanlage

Ofen ... 11

Füllung ... 13

Gasol ausbeute.

|   | Gasol                   | Gasol                   | Gasol                  | Carbol.               | Gasol                   | Gasol                   | Gasol                 | Carbol.               |
|---|-------------------------|-------------------------|------------------------|-----------------------|-------------------------|-------------------------|-----------------------|-----------------------|
| A.K.-Turm                                   | 6.6                     | 6.6                     | 5.9                    |                       | 6.9                     | 6.9                     | 5.6                   |                       |
| Datum                                       | 30/37.                  |                         | 51                     | 43                    | 37.5/1.6.               |                         | 43                    |                       |
| Zeit  | 8-16                    | 0-8                     | 8-8                    | 8-8                   | 8-16                    | 0-8                     | 8-8                   | 8-8                   |
| Nm <sup>3</sup> /Sygas                      | <del>295</del><br>295   | <del>295</del><br>295   | 295                    | 2.80                  | <del>309</del><br>309   | <del>309</del><br>309   | 309                   | 2.165                 |
| l Restgas                                   |                         |                         |                        | 1564                  |                         |                         |                       | 1638                  |
| % Kontr.                                    |                         |                         |                        | 46.5                  |                         |                         |                       | 46.9                  |
| l Gasolgem.                                 | <del>1398</del><br>1307 | <del>1445</del><br>1345 | <del>1402</del><br>853 | <del>48</del><br>44.6 | <del>1397</del><br>1225 | <del>1090</del><br>1090 | <del>744</del><br>691 | <del>57</del><br>47.5 |
| Analyse: CO <sub>2</sub>                    | 30.5                    | 29.5                    | 33.4                   | 64.7                  | 29.3                    | 29.0                    | 26.3                  | 58.4                  |
| C <sub>3</sub> H <sub>6</sub>               | 19.5                    | 16.2                    | 9.9                    | 4.6                   | 17.0                    | 16.0                    | 8.2                   | 8.0                   |
| C <sub>2</sub> H <sub>4</sub>               | 0.8                     | 0.6                     | 0.6                    | 0.5                   | 0.3                     | 0.6                     | 0.6                   | 0.5                   |
| O <sub>2</sub>                              | 0.0                     | 0.0                     | 0.1                    | 0.1                   | 0.7                     | 0.7                     | 0.7                   | 0.7                   |
| CO  | 10.9                    | 13.7                    | 15.0                   | 7.5                   | 12.7                    | 12.8                    | 19.7                  | 7.0                   |
| H <sub>2</sub>                              | 14.0                    | 15.7                    | 20.8                   | 3.7                   | 17.7                    | 17.8                    | 28.6                  | 3.8                   |
| CH <sub>4</sub> <sup>+</sup>                | 20.3                    | 20.0                    | 10.2                   | 14.9                  | 19.0                    | 19.0                    | 17.6                  | 18.2                  |
| N <sub>2</sub>                              | 4.0                     | 5.5                     | 6.0                    | 4.0                   | 4.5                     | 4.7                     | 5.5                   | 4.0                   |
| C-Zahl                                      | 3.96                    | 3.88                    | 3.77                   | 2.28                  | 3.96                    | 3.98                    | 3.43                  | 2.80                  |
| Litergew. entspr.<br>d. C-Z. (Kerosinbasis) | 2.03                    | 1.94                    | 1.92                   | 0.70                  | 2.03                    | 2.05                    | 2.20                  | 1.60                  |
| g Gasol/l Gasolgem                          | 0.87                    | 0.70                    | 0.47                   | 0.19                  | 0.73                    | 0.72                    | 0.44                  | 0.44                  |
| g Gasol                                     | 1058                    | 945                     | 340                    | 8.5                   | 895                     | 725                     | 301                   | 20.9                  |
| g Gasol/Nm <sup>3</sup> Sygas               | 10.40                   | 9.25                    | 1.03                   | 3.04                  | 8.7                     | 7.04                    | 0.97                  | 7.9                   |

Bemerkungen:

g/Nm<sup>3</sup> Ugas

13.89

16.74

g/Nm<sup>3</sup> Co + H<sub>2</sub>

15.9

18.95

% C<sub>2</sub>H<sub>2</sub>

44

49

000344



Druckversuchsanlage

Ofen M.....

Füllung..... 13

Gasolausbeute

|   | Gasol    | Gasol    | Gasol    | Gasol    | Gasol    | Gasol    | Gasol    |
|---|----------|----------|----------|----------|----------|----------|----------|
| A.K.-Turm                                 | 6a       | 6a       | 5a       |          | 6a       | 6a       | 5a       |
| Datum                                     | 29.10.29 | 29.10.29 | 29.10.29 | 29.10.29 | 29.10.29 | 29.10.29 | 29.10.29 |
| Zeit                                      | 11-16    | 11-16    | 11-16    | 11-16    | 11-16    | 11-16    | 11-16    |
| Nm <sup>3</sup> /Sygas                    | 303      | 303      | 303      | 303      | 303      | 303      | 303      |
| l Restgas                                 |          |          |          |          |          |          | 2.68     |
| % Kontr.                                  |          |          |          |          |          |          | 15.68    |
| l Gasolgem.                               |          |          |          |          |          |          | 44.2     |
| Analyse: CO <sub>2</sub>                  | 30.6     | 28.5     | 20.0     | 23.2     | 30.5     | 28.2     | 32.7     |
| C <sub>3</sub> H <sub>6</sub>             | 1.1      | 1.1      | 1.1      | 1.1      | 1.1      | 1.1      | 1.1      |
| O <sub>2</sub> H <sub>4</sub>             | 0.5      | 0.5      | 0.5      | 0.5      | 0.5      | 0.5      | 0.5      |
| O <sub>2</sub>                            | 0.1      | 0.1      | 0.1      | 0.1      | 0.1      | 0.1      | 0.1      |
| CO  | 0.0      | 0.0      | 0.0      | 0.0      | 0.0      | 0.0      | 0.0      |
| H <sub>2</sub>                            | 13.3     | 13.3     | 13.3     | 13.3     | 12.3     | 14.1     | 17.4     |
| CH <sub>4</sub> <sup>+</sup>              | 14.7     | 14.7     | 14.7     | 14.7     | 15.3     | 18.8     | 27.7     |
| N <sub>2</sub>                            | 14.7     | 14.7     | 14.7     | 14.7     | 14.0     | 15.2     | 12.0     |
| C-Zahl                                    | 3.24     | 3.24     | 3.24     | 3.24     | 3.24     | 3.26     | 3.27     |
| l.ergw. entspr. d.C-Z. (Korrekturentwert) | 1.93     | 1.93     | 1.93     | 1.93     | 2.02     | 2.09     | 2.10     |
| g Gasol/l Gasolgem                        | 0.74     | 0.74     | 0.74     | 0.74     | 0.74     | 0.66     | 0.43     |
| g Gasol                                   | 695      | 695      | 695      | 695      | 695      | 688      | 272      |
| g Gasol/Nm <sup>3</sup> Sygas             | 6.88     | 6.88     | 6.88     | 6.88     | 6.88     | 6.82     | 0.90     |

Bemerkungen:

1. 11.39  
 2. 13.9  
 3. 3.9  
 4. 11.58  
 5. 13.2  
 6. 4.5

000345



Druckversuchsanlage

Ofen ... 1 ...

Füllung ... 13 ...

Gasolausbeute.

000347

|  | 18/12.5 | 18/15.5 | 18/10.5 | 18/10.5 | 18/10.5 | 18/10.5 | 18/10.5 | 18/10.5 | 18/10.5 |
|--|---------|---------|---------|---------|---------|---------|---------|---------|---------|
| A.K.-Turm                              | 6a      |         | 6a      |         | 6a      |         | 6a      | 6a      | 6a      |
| Datum                                  | 18/12.5 | 18/15.5 | 18/10.5 |         | 18/10.5 |         | 18/10.5 | 18/10.5 | 18/10.5 |
| Zeit                                   | 8-8     | 8-8     | 8-8     | 8-8     | 8-8     | 8-8     | 8-16    | 0-8     | 8-8     |
| Nm <sup>3</sup> /Gas                   | 312     | 2,59    | 307     | 2,41    | 379     | 2,30    | 394/306 | 319/306 | 2,37    |
| l Restgas                              |         | 158     |         | 148     |         | 158     |         |         | 148     |
| % Kontr.                               |         | 41,6    |         | 43,5    |         | 39,2    |         |         | 40,0    |
| l Gasolgem.                            | 7,05    | 5,0     | 7,05    | 4,1     | 10,58   | 5,0     | 10,98   | 11,26   | 11,8    |
| Analyse: CO <sub>2</sub>               | 1,4     | 5,23    | 1,5     | 5,1     | 2,9     | 5,4     | 16,8    | 23,2    | 6,3     |
| C <sub>3</sub> H <sub>6</sub>          | 12,8    | 14,5    | 12,8    | 14,5    | 18,4    | 14,7    | 18,5    | 18,8    | 7,3     |
| O <sub>2</sub> H <sub>4</sub>          | 2,2     | 2,9     | 2,3     | 2,7     | 1,2     | 1,7     | 1,8     | 1,7     | 1,1     |
| O <sub>2</sub>                         | 0,0     | 0,1     | 0,0     | 0,1     | 0,1     | 0,1     | 0,1     | 0,0     | 0,0     |
| CO                                     | 18,4    | 2,9     | 16,9    | 16,3    | 13,7    | 10,0    | 14,6    | 16,7    | 9,8     |
| H <sub>2</sub>                         | 26,6    | 3,8     | 15,7    | 15,5    | 18,5    | 7,9     | 17,3    | 18,8    | 3,8     |
| CH <sub>4</sub> +                      | 8,4     | 13,5    | 15,1    | 15,0    | 16,3    | 11,4    | 16,4    | 13,9    | 11,1    |
| N <sub>2</sub>                         | 4,1     | 7,2     | 5,9     | 5,7     | 5,2     | 4,5     | 4,5     | 4,1     | 3,2     |
| C-Zahl                                 | 3,55    | 2,66    | 3,09    | 3,06    | 3,14    | 2,92    | 3,34    | 2,92    | 2,21    |
| Litergew. entspr. d.O-Z. (Kurvenwert)  | 1,24    | 1,38    | 1,00    | 1,02    | 2,02    | 1,46    | 2,14    | 1,80    | 0,57    |
| g Gasol/l Gasolgem                     | 0,52    | 0,45    | 0,91    | 0,50    | 0,65    | 0,36    | 0,75    | 0,60    | 0,20    |
| g Gasol                                | 346     | 20,9    | 5,55    | 10,5    | 6,35    | 16,9    | 76,2    | 6,28    | 9,0     |
| g Gasol/Nm <sup>3</sup> Gas            | 1,11    | 8,09    | 1,83    | 2,5     | 1,99    | 7,35    | 7,18    | 5,98    | 3,90    |
| Bemerkungen:                           |         |         |         |         |         |         |         |         |         |
| g/Nm <sup>3</sup> Wg.                  | 9,20    |         | 10,33   |         | 9,34    |         | 10,48   |         |         |
| g/Nm <sup>3</sup> Gas + H <sub>2</sub> | 10,78   |         | 11,38   |         | 10,44   |         | 11,87   |         |         |
| % l. d. n.                             | 52      |         | 52      |         | 49      |         | 57      |         |         |

Druckversuchsanlage

Ofen .....

Füllung.....

Gasolausbeute.

000348

|                                       | Gasol | Kontr. | Gasol | Kontr. | Gasol | Kontr. | Gasol | Kontr. |
|---------------------------------------|-------|--------|-------|--------|-------|--------|-------|--------|
| A.K.-Turm                             | 6.6   |        | 6.6   |        | 6.6   |        | 6.6   |        |
| Datum                                 | 4/30  | 4/4    | 5/6   | 1.4.41 | 6/8   | 1.10   | 7/8.1 | 4.1    |
| Zeit                                  | 20-8  | 1-9    | 20-8  | 9-8    | 20-8  | 2-8    | 20-8  | 8-8    |
| Nm <sup>3</sup> /Sygas                |       |        | 3.24  | 1.00   | 1.32  | 2.57   | 3.04  | 2.70   |
| l Restgas                             |       |        |       | 14.24  | 12.23 |        | 15.2  | 17.64  |
| % Kontr.                              |       |        |       | 30.4   |       |        |       | 39.2   |
| l Gasolgem.                           |       |        | 12.27 | 5.1    | 12.32 |        | 14.4  | 17.53  |
| Analyse: CO <sub>2</sub>              |       |        | 5.2   | 5.0    | 5.0   | 5.0    | 5.54  | 6.5    |
| C <sub>3</sub> H <sub>6</sub>         |       |        | 2.0   | 1.0    | 2.0   | 5.0    | 2.46  | 5.6    |
| O <sub>2</sub> H <sub>4</sub>         |       |        | 1.7   | 5.1    | 2.0   |        | 1.6   | 1.7    |
| O <sub>2</sub>                        |       |        | 0.2   | 0.2    | 0.2   | 0.2    | 0.0   | 0.0    |
| CO                                    |       |        | 1.0   | 0.2    | 0.2   | 1.0    | 1.9   | 9.6    |
| H <sub>2</sub>                        |       |        | 1.0   | 2.0    | 1.0   | 1.0    | 16.7  | 3.7    |
| CH <sub>4</sub> +                     |       |        | 1.0   | 1.0    | 1.0   | 1.0    | 15.3  | 11.4   |
| N <sub>2</sub>                        |       |        | 2.4   | 5.0    | 2.4   | 2.4    | 4.7   | 2.8    |
| C-Zahl                                |       |        | 3.0   | 5.0    | 3.0   | 3.0    | 2.93  | 2.06   |
| Litergew. entspr. d.C-Z. (Kurvenwert) |       |        | 1.26  | 1.1    | 1.26  | 1.26   | 1.82  | 0.32   |
| g Gasol/l Gasolgem                    |       |        | 1.16  | 1.1    | 1.16  | 1.16   | 0.74  | 0.14   |
| g Gasol                               |       |        | 1.16  | 1.1    | 1.16  | 1.16   | 0.92  | 7.4    |
| g Gasol/Nm <sup>3</sup> Sygas         |       |        | 0.36  | 0.5    | 0.36  | 0.36   | 0.33  | 2.74   |

Bemerkungen:

1.16 1.1 1.16 1.16 0.92 7.4  
 0.36 0.5 0.36 0.36 0.33 2.74  
 60 50 60 57

Druckversuchsanlage

Ofen M.....

Füllung N<sub>2</sub>...

Gasol ausbeute.

000349

|   | gasol                     | Restgas                   | Gasolgem.                 | Carb. f. gasol            | Carb. f. Restg.         | Carb. f. Gasolgem.        | Carb. f. Gesamt       |
|---|---------------------------|---------------------------|---------------------------|---------------------------|-------------------------|---------------------------|-----------------------|
| A.K.-Turm   | 6.0                       |                           | 6.0                       |                           | 6.6                     | 6.0                       |                       |
| Datum   | 26/27 XI. 28              | 27/28                     | 27/28                     | 11.43                     | 14.24                   | 14.0                      | 12.43                 |
| Zeit  | 20-8                      | 8-8                       | 10-8                      | 8-8                       | 10-8                    | 20-8                      | 8-8                   |
| Nm <sup>3</sup> /Sygas                            | <del>312</del><br>156     | 2.77                      | <del>262</del><br>131     | 2.39                      | <del>228</del><br>114   | <del>208</del><br>104     | 2.07                  |
| l Restgas   |                           | <del>154.2</del><br>149.0 |                           | <del>120.8</del><br>117.6 |                         | <del>150.2</del><br>140.0 |                       |
| % Kontr.  |                           | 44.6                      |                           | 38.7                      |                         | 35.5                      |                       |
| l Gasolgem.                                       | <del>11.88</del><br>15.75 | 45.42                     | <del>18.99</del><br>16.86 | <del>5.2</del><br>4.84    | <del>5.98</del><br>5.06 | <del>1.74</del><br>1.62   | <del>4.8</del><br>4.5 |
| Analyse: CO <sub>2</sub>                          | 23.3                      | 59.2                      | 36.4                      | 57.5                      | 27.6                    | 21.1                      | 55.0                  |
| C <sub>3</sub> H <sub>6</sub>                     | 29.4                      | 5.8                       | 29.9                      | 5.3                       | 21.3                    | 42.5                      | 1.5                   |
| C <sub>2</sub> H <sub>4</sub>                     | 1.9                       | 2.4                       | 0.7                       | 1.2                       | 1.7                     | 2.0                       | 2.2                   |
| O <sub>2</sub>                                    | 0.1                       | 0.1                       | 0.1                       | 0.2                       | 0.0                     | 0.1                       | 0.0                   |
| CO  | 7.3                       | 7.5                       | 2.9                       | 7.9                       | 16.4                    | 7.0                       | 11.4                  |
| H <sub>2</sub>                                    | 10.5                      | 3.8                       | 3.7                       | 3.4                       | 12.3                    | 3.0                       | 3.9                   |
| CH <sub>4</sub> +                                 | 24.0                      | 17.5                      | 22.9                      | 19.5                      | 15.3                    | 22.2                      | 15.7                  |
| N <sub>2</sub>                                    | 3.5                       | 3.7                       | 3.4                       | 5.0                       | 9.4                     | 3.0                       | 3.3                   |
| C-Zahl  | 3.02                      | 2.14                      | 3.02                      | 2.10                      | 2.39                    | 2.13                      | 2.22                  |
| Litergew. entspr. d.O-Z. (Kurvenwert)             | 1.96                      | 0.40                      | 1.94                      | 0.38                      | 0.59                    | 2.08                      | 0.44                  |
| g Gasol/l Gasolgem                                | 0.99                      | 0.18                      | 1.03                      | 0.17                      | 0.54                    | 1.37                      | 0.34                  |
| g Gasol   | 1560                      | 7.6                       | 1725                      | 8.40                      | 270                     | 591                       | 10.8                  |
| g Gasol/Nm <sup>3</sup> Sygas                     | 10.00                     | 2.74                      | 13.00                     | 3.52                      | 2.46                    | 5.68                      | 5.22                  |
| Bemerkungen:                                      |                           |                           |                           |                           |                         |                           |                       |
| g/Km <sup>3</sup> Hydrog.                         | 12.74                     |                           | 16.52                     |                           |                         | 10.90                     |                       |
| g/Km <sup>3</sup> H <sub>2</sub> + H <sub>2</sub> | 14.50                     |                           | 18.90                     |                           |                         | 12.57                     |                       |
| % Pn H <sub>2</sub>                               | 52                        |                           | 53                        |                           |                         | 58                        |                       |

Gasol ausbeute.

000350

|                                       | hant         | Barbr        | hant         | Barbr        | gasol        | barbr        | gasol      | barbr        |
|---------------------------------------|--------------|--------------|--------------|--------------|--------------|--------------|------------|--------------|
| A.K.-Turm                             | 6a           |              | 6a           |              | 6a           |              | 6a         |              |
| Datum                                 | 16/17.       | 11.43        | 18/19.       | 11.43        | 22/25.       | 11.43        | 14/15.     | 11.43        |
| Zeit                                  | 20-8         | 8-8          | 20-8         | 8-8          | 20-8         | 8-8          | 20-8       | 8-8          |
| Nm <sup>3</sup> /Sygas                | 317<br>256   | 2.44         | 310<br>255   | 2.47         | 366<br>262   | 2.30         | 294<br>147 | 2.44         |
| l Restgas                             |              | 1478<br>1376 |              | 1474<br>1378 |              | 1330<br>1245 |            | 1444<br>1350 |
| % Kontr.                              |              | 43.5         |              | 42.0         |              | 41.6         |            | 42.3         |
| l Gasolgem.                           | 1657<br>1524 | 56<br>52     | 1570<br>1405 | 58<br>54     | 1614<br>1510 | 52<br>48.5   | 11<br>10.8 | 55<br>51.5   |
| Analyse: CO <sub>2</sub>              | 26.1         | 58.4         | 30.1         | 59.6         | 24.3         | 58.3         | 24.3       | 59.0         |
| C <sub>3</sub> H <sub>6</sub>         | 26.1         | 6.0          | 24.7         | 6.5          | 30.0         | 3.7          | 30.5       | 4.7          |
| C <sub>2</sub> H <sub>4</sub>         | 2.0          | 0.7          | 0.5          | 7.7          | 1.2          | 1.2          | 0.9        | 2.2          |
| O <sub>2</sub>                        | 0.0          | 0.0          | 0.0          | 0.0          | 0.1          | 0.0          | 0.1        | 0.1          |
| CO                                    | 6.3          | 6.6          | 7.2          | 6.0          | 7.0          | 8.4          | 6.2        | 6.6          |
| H <sub>2</sub>                        | 9.4          | 2.9          | 10.7         | 2.8          | 8.7          | 1.8          | 7.8        | 2.9          |
| CH <sub>4</sub> +                     | 26.3         | 22.6         | 24.0         | 21.8         | 24.5         | 23.9         | 27.0       | 22.2         |
| N <sub>2</sub>                        | 3.8          | 2.8          | 2.8          | 2.2          | 4.2          | 2.7          | 3.2        | 2.3          |
| C-Zahl                                | 2.95         | 2.04         | 2.97         | 2.08         | 3.04         | 2.14         | 3.24       | 2.38         |
| Litergew. entspr. d.C-Z. (Kurvenwert) | 1.87         | 0.28         | 1.90         | 0.34         | 1.96         | 0.40         | 2.10       | 0.88         |
| g Gasol/l Gasolgem                    | 0.98         | 0.98         | 0.92         | 0.80         | 1.07         | 0.17         | 1.22       | 0.28         |
| g Gasol                               | 1517         | 9.36         | 1294         | 108          | 1620         | 8.25         | 2040       | 14.5         |
| g Gasol/Nm <sup>3</sup> Sygas         | 9.68         | 3.84         | 8.35         | 4.37         | 10.10        | 3.60         | 13.90      | 5.95         |
| Bemerkungen:                          |              |              |              |              |              |              |            |              |
| g/Nm <sup>3</sup> Sygas               | 13.52        |              | 12.72        |              | 13.70        |              | 19.85      |              |
| g/Nm <sup>3</sup> CO+H <sub>2</sub>   | 15.57        |              | 14.60        |              | 15.20        |              | 22.80      |              |
| % C <sub>2</sub> H <sub>4</sub>       | 6.5          |              | 4.6          |              | 4.8          |              | 4.7        |              |

Druckversuchsanlage

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Füllung..... 13

Gasol ausbeute.

000351

|                                       | Gasol                   | Carbot.                 | Gasol                   | Carbot.                 | Gasol                   | Carbot.                 | Gasol                   | Carbot.                 |
|---------------------------------------|-------------------------|-------------------------|-------------------------|-------------------------|-------------------------|-------------------------|-------------------------|-------------------------|
| A.K.-Turm                             | 6a                      |                         | 6a                      |                         | 6a                      |                         | 6a                      |                         |
| Datum                                 | 7/8. 11.42              |                         | 7/10. 11.43             |                         | 11/12. 11.43            |                         | 14/15. 11.43            |                         |
| Zeit                                  | 20-8                    | 8-8                     | 20-8                    | 8-8                     | 20-8                    | 8-8                     | 20-8                    | 8-8                     |
| Nm <sup>3</sup> /Sygas                | <del>259</del><br>145   | 2.52                    | <del>343</del><br>162   | 1.87                    | <del>289</del><br>145   | 2.26                    | <del>307</del><br>154   | 2.32                    |
| l Restgas                             |                         | <del>1522</del><br>1610 |                         | <del>1275</del><br>1150 |                         | <del>1327</del><br>1232 |                         | <del>1480</del><br>1378 |
| % Kontr.                              |                         | 41.4                    |                         | 35.8                    |                         | 43.7                    |                         | 40.6                    |
| l Gasolgem.                           | <del>1688</del><br>1562 | 75.78                   | <del>1537</del><br>1426 | 52.48                   | <del>1749</del><br>1620 | 55.57                   | <del>1426</del><br>1327 | 45.42                   |
| Analyse: CO <sub>2</sub>              | 24.7                    | 65.4                    | 23.6                    | 55.7                    | 24.8                    | 60.0                    | 21.3                    | 49.8                    |
| C <sub>3</sub> H <sub>6</sub>         | 30.6                    | 3.8                     | 28.2                    | 5.6                     | 27.0                    | 5.0                     | 29.7                    | 7.4                     |
| O <sub>2</sub> H <sub>4</sub>         | 0.2                     | 0.8                     | 1.2                     | 0.7                     | 0.6                     | 0.9                     | 1.0                     | 1.1                     |
| O <sub>2</sub>                        | 0.2                     | 0.2                     | 0.2                     | 0.0                     | 0.7                     | 0.7                     | 0.0                     | 0.0                     |
| CO                                    | 6.7                     | 5.3                     | 7.7                     | 6.8                     | 6.4                     | 6.5                     | 10.1                    | 10.2                    |
| H <sub>2</sub>                        | 7.7                     | 2.3                     | 9.6                     | 3.4                     | 12.8                    | 3.4                     | 9.3                     | 4.6                     |
| CH <sub>4</sub> <sup>+</sup>          | 27.0                    | 19.2                    | 24.0                    | 27.8                    | 24.7                    | 22.7                    | 25.5                    | 24.0                    |
| N <sub>2</sub>                        | 3.5                     | 3.0                     | 4.7                     | 1.3                     | 5.2                     | 4.0                     | 3.1                     | 2.4                     |
| C-Zahl                                | 3.08                    | 2.18                    | 3.22                    | 2.30                    | 3.77                    | 2.24                    | 3.09                    | 2.27                    |
| Litergew. entspr. d.C-Z. (Kurvenwert) | 1.99                    | 0.52                    | 1.52                    | 0.54                    | 2.07                    | 0.63                    | 1.99                    | 0.57                    |
| g Gasol/l Gasolgem                    | 1.75                    | 0.77                    | 1.77                    | 0.26                    | 1.05                    | 0.22                    | 1.70                    | 0.28                    |
| g Gasol                               | 1800                    | 12.00                   | 1580                    | 12.60                   | 1670                    | 17.30                   | 1460                    | 11.8                    |
| g Gasol/Nm <sup>3</sup> Sygas         | 12.40                   | 4.77                    | 9.75                    | 6.75                    | 11.50                   | 5.00                    | 9.47                    | 5.08                    |
| Bemerkungen:                          |                         |                         |                         |                         |                         |                         |                         |                         |
| g/Nm <sup>3</sup> Sygas               |                         | 17.17                   |                         | 16.50                   |                         | 16.50                   |                         | 14.55                   |
| g/Nm <sup>3</sup> Co + H <sub>2</sub> |                         | 19.65                   |                         | 19.00                   |                         | 19.00                   |                         | 16.62                   |
| % bei H <sub>2</sub> , n              |                         | 48                      |                         | 45                      |                         | 47                      |                         | 47                      |

Gasol ausbeute.

000352

|                                       | Gen       | Kontr. | Gen       | Kontr. | Gen       | Kontr. | Gen       | Kontr. |
|---------------------------------------|-----------|--------|-----------|--------|-----------|--------|-----------|--------|
| A.K.-Turm                             | Gen       |        | Gen       |        | Gen       |        | Gen       |        |
| Datum                                 | 3/4/29    | 10.43  | 3/6/27    | 10.43  | 3/8/29    | 10.43  | 1/6.11    | 43     |
| Zeit                                  | 8-8       | 8-8    | 30-8      | 1-8    | 20-8      | 10-8   | 20-8      | 8-8    |
| Nm <sup>3</sup> /Sygas                | 333/166   | 247    | 307/159   | 234    | 290/147   | 236    | 377/159   | 212    |
| l Restgas                             |           | 1503   |           | 1574   |           | 1503   | 1503      | 1298   |
| % Kontr.                              |           | 37.5   |           | 41.7   |           | 40.8   |           | 39.4   |
| l Gasolgem.                           | 1336/1261 | 75.76  | 1177/1091 | 78.5   | 1050/1011 | 57.47  | 1822/1710 | 70.66  |
| Analysen:                             |           |        |           |        |           |        |           |        |
| CO <sub>2</sub>                       | 16.3      | 17.0   | 25.4      | 63.0   | 20.3      | 58.2   | 23.8      | 62.5   |
| C <sub>3</sub> H <sub>6</sub>         | 22.7      | 6.9    | 25.4      | 4.0    | 29.6      | 5.71   | 30.3      | 3.5    |
| C <sub>2</sub> H <sub>4</sub>         | 3.1       | 0.2    | 7.1       | 1.0    | 7.1       | 1.0    | 2.6       | 0.3    |
| O <sub>2</sub>                        | 0.2       | 0.1    | 0.1       | 0.0    | 0.0       | 0.0    | 0.1       | 0.1    |
| CO                                    | 0.1       | 0.1    | 0.1       | 0.1    | 0.1       | 0.1    | 0.1       | 0.1    |
| H <sub>2</sub>                        | 0.1       | 0.1    | 6.0       | 5.0    | 3.8       | 9.7    | 5.5       | 7.1    |
| CH <sub>4</sub>                       | 0.1       | 0.1    | 12.4      | 0.2    | 14.2      | 3.9    | 8.8       | 2.0    |
| N <sub>2</sub>                        | 4.2       | 0.2    | 11.7      | 0.2    | 21.2      | 29.6   | 23.2      | 16.0   |
| C-Zahl                                | 365       | 17.1   | 176       | 2.71   | 3.34      | 2.11   | 3.25      | 2.35   |
| Litergew. entspr. d.C-Z. (Kurvenwert) | 1.97      | 6.17   | 1.71      | 0.22   | 2.15      | 0.34   | 2.14      | 0.80   |
| g Gasol/l Gasolgem                    | 122       | 0.71   | 142       | 0.22   | 118       | 0.42   | 1.15      | 0.19   |
| g Gasol                               | 1153      | 11.2   | 1103      | 16.0   | 1553      | 8.46   | 1985      | 12.65  |
| g Gasol/Nm <sup>3</sup> Sygas         | 9.86      | 1.01   | 7.27      | 5.85   | 10.52     | 3.99   | 12.45     | 5.96   |

Bemerkungen:

g Nm<sup>3</sup> Sygas 16.66 15.52 14.46 18.41  
 g Gasol 18.93 13.25 16.22 21.00  
 % C<sub>2</sub>H<sub>4</sub> 46 43 53 51



Gasol ausbeute

000353

|  | Gasol       | karbol    | Gasol       | karbol    | Gasol       | karbol    | Gasol       | karbol |
|--|-------------|-----------|-------------|-----------|-------------|-----------|-------------|--------|
| A.K.-Turm  | 6a          |           | 6a          |           | 6a          |           | 6a          |        |
| Datum  | 16/17.10.43 |           | 18/19.10.43 |           | 20/21.10.43 |           | 22/23.10.43 |        |
| Zeit   | 20-8        | 8-8       | 20-8        | 8-8       | 20-8        | 8-8       | 20-8        | 8-8    |
| Nm <sup>3</sup> /Sygas                           | 305/152     | 2.67      | 306/154     | 2.38      | 302/150.5   | 2.148     | 240         |        |
| l Restgas  |             | 1543/1438 |             | 1342/1250 |             | 1543/1435 |             | 1242   |
| % Kontr.   |             | 43.2      |             | 44.8      |             | 39.5      |             |        |
| l Gasolgem.                                      | 1786/1660   | 25.79     | 1733/1610   | 70.65     | 1701/1580   | 73.47     | 1402        | 62     |
| Analyse: CO <sub>2</sub>                         | 25.2        | 6.06      | 20.5        | 5.83      | 23.3        | 62.7      | 22.9        | 60.3   |
| C <sub>3</sub> H <sub>6</sub>                    | 26.0        | 4.9       | 26.5        | 3.1       | 25.6        | 4.7       | 27.0        | 4.8    |
| C <sub>2</sub> H <sub>4</sub>                    | 2.5         | 1.2       | 2.0         | 2.1       | 3.9         | 1.7       | 1.3         | 1.3    |
| O <sub>2</sub>                                   | 0.2         | 0.7       | 0.3         | 0.7       | 0.2         | 0.7       | 0.7         | 0.7    |
| CO   | 4.3         | 4.7       | 5.0         | 2.6       | 6.9         | 5.2       | 12.2        | 10.7   |
| H <sub>2</sub>                                   | 7.9         | 11.8      | 10.6        | 2.5       | 2.6         | 2.2       | 17.0        | 7.2    |
| CH <sub>4</sub>                                  | 28.3        | 23.7      | 29.7        | 23.0      | 23.2        | 20.5      | 17.0        | 15.5   |
| N <sub>2</sub>                                   | 4.6         | 3.0       | 3.0         | 4.9       | 4.2         | 3.5       | 6.5         | 4.8    |
| C-Zahl   | 3.10        | 2.20      | 2.76        | 2.34      | 2.22        | 2.33      | 3.08        | 2.30   |
| Litergew. entspr. d.C-Z. (Kurvelement)           | 2.100       | 0.56      | 2.153       | 0.52      | 2.111       | 0.78      | 1.99        | 0.74   |
| g Gasol/l Gasolgem                               | 1.09        | 0.23      | 1.14        | 0.23      | 1.11        | 0.25      |             |        |
| g Gasol  | 1800        | 17.80     | 133.8       | 14.8      | 1760        | 17.4      |             |        |
| g Gasol/Nm <sup>3</sup> Sygas                    | 17.80       | 6.66      | 11.90       | 6.20      | 11.70       | 7.10      |             |        |
| Bemerkungen:                                     |             |           |             |           |             |           |             |        |
| g/Nm <sup>3</sup> U.g.H.                         | 18.46       |           | 18.10       |           | 18.70       |           |             |        |
| g/Nm <sup>3</sup> C <sub>2</sub> -H <sub>2</sub> | 20.80       |           | 20.40       |           | 21.75       |           |             |        |
| % C <sub>2</sub> H <sub>2</sub> H <sub>2</sub>   | 4.1         |           | 4.1         |           | 4.2         |           |             |        |

Druckversuchsanlage

Ofen . . . . .

Füllung . . . . . 13

Gasolausbeute

000354

|  | 1. Versuch | 2. Versuch | 3. Versuch | 4. Versuch | 5. Versuch | 6. Versuch | 7. Versuch | 8. Versuch | 9. Versuch |
|--|------------|------------|------------|------------|------------|------------|------------|------------|------------|
| A.K.-Turm                              | 67         | 60         |            | 60         |            | 69         |            | 66         |            |
| Datum                                  | 7/2        | 10         | 6/2        | 10/11      | 8-8        |            |            | 14/18      | 20         |
| Zeit                                   | 2-20       | 20-1       | 11-1       | 20-8       | 8-8        |            |            | 20-1       | 8          |
| Nm <sup>3</sup> /Sygas                 | 160        | 160        | 2.74       | 32.160     | 1.74       |            |            | 1.55       | 3.02       |
| l Restgas                              |            |            |            |            | 1585       |            |            |            | 4.20       |
| l Kontr.                               |            |            |            |            | 1450       |            |            |            | 4.19       |
| l Gasolgem.                            |            |            |            | 178        | 16.5       | 56         |            |            | 10.20      |
| Analyse: CO <sub>2</sub>               |            |            | 6.3        | 22.5       | 56.5       |            |            | 24.0       | 62.5       |
| C <sub>3</sub> H <sub>6</sub>          |            |            |            | 27.3       | 6.7        |            |            | 1.2        | 12.0       |
| C <sub>2</sub> H <sub>4</sub>          |            |            |            | 3.0        | 3.4        |            |            |            | 0.7        |
| O <sub>2</sub>                         |            |            |            | 0.0        | 0.0        |            |            | 0.0        | 0.1        |
| CO                                     |            |            |            | 4.1        | 4.6        |            |            | 7.2        | 7.8        |
| H <sub>2</sub>                         |            |            |            | 6.1        | 3.1        |            |            |            | 2.8        |
| CH <sub>4</sub> +                      |            |            |            | 30.6       | 20.5       |            |            |            | 1.4        |
| N <sub>2</sub>                         |            |            |            | 6.4        | 6.7        |            |            |            | 1.4        |
| C-Zahl                                 |            |            |            | 2.82       | 2.25       |            |            | 2.24       | 2.34       |
| Litergew. entspr. d. C-Z. (Kurvenwert) |            |            |            | 1.64       | 0.60       |            |            | 1.50       | 0.78       |
| g Gasol/l Gasolgem                     |            |            |            | 1.02       | 0.24       |            |            | 1.20       | 0.11       |
| g Gasol                                |            |            |            | 17.00      | 13.5       | 1530       |            | 13.40      | 12.7       |
| g Gasol/Nm <sup>3</sup> Sygas          |            |            |            | 10.5       | 4.94       |            |            | 7.5        | 4.6        |
| Bemerkungen:                           |            |            |            |            |            |            |            |            |            |
| g/Nm <sup>3</sup> Syg                  |            |            |            | 15.44      |            |            |            | 4.1        |            |
| g/Nm <sup>3</sup> (C-Zahl)             |            |            |            | 17.52      |            |            |            | 13.4       |            |
| g/l Gasol                              |            |            |            | 43         |            |            |            | 48         |            |

Druckversuchsanlage

Ofen ... 119 ...

Füllung... 1.3 ...

Gasol ausbeute.

000355

|                                       | Gasol       | Gasol       | Gasol        | Gasol        | Gasol        | Gasol        |      |       |      |
|---------------------------------------|-------------|-------------|--------------|--------------|--------------|--------------|------|-------|------|
| A.K.-Turn                             | 6.6         | 6.9         |              | 6.6          | 6.9          |              |      |       |      |
| Datum                                 | 17/11.9.    | 18.9.       | 13           | 29/10.9.     | 13           |              |      |       |      |
| Zeit                                  | 8-20        | 20-8        | 8-8          | 8-20         | 20-8         | 9-8          |      |       |      |
| Nm <sup>3</sup> /Sygas                | 373<br>157  | 373<br>157  | 2.58<br>1360 | 269<br>100   | 269<br>100   | 2.53         |      |       | 2.34 |
| l Restgas                             |             |             | 1350<br>1360 |              |              | 1400<br>1370 |      |       | 1170 |
| % Kontr.                              |             |             | 47.2         |              |              | 46.2         |      |       | 11.3 |
| l Gasolgem.                           | 144<br>1780 | 177<br>1470 | 62<br>516    | 2208<br>2920 | 2017<br>2920 | 66<br>673    | 1100 | 1330  | 2260 |
| Analyse: CO <sub>2</sub>              | 22.0        | 22.0        | 54.9         | 25.7         | 34.4         | 55.6         | 2.8  | 2.5   | 6.2  |
| C <sub>3</sub> H <sub>6</sub>         | 23.9        | 27.5        | 6.7          | 14.3         | 12.7         | 5.7          |      | 2.6   | 5.1  |
| O <sub>2</sub> H <sub>4</sub>         | 1.6         | 1.2         | 0.8          | 1.0          | 0.6          | 1.1          |      | 1.0   | 0.8  |
| O <sub>2</sub>                        | 0.2         | 0.1         | 0.1          | 0.1          | 0.1          | 0.1          |      | 0.2   | 0.1  |
| CO                                    | 5.4         | 6.2         | 0.5          | 6.7          | 7.9          | 5.3          |      |       | 1.2  |
| H <sub>2</sub>                        | 11.3        | 10.5        | 2.6          | 7.0          | 13.8         | 2.7          |      |       | 2.0  |
| CH <sub>4</sub> +                     | 24.4        | 27.9        | 25.0         | 28.8         | 23.2         | 26.5         |      |       | 1.8  |
| N <sub>2</sub>                        | 0.5         | 5.6         | 4.0          | 5.0          | 7.0          | 3.0          |      |       | 1.0  |
| C-Zahl                                | 3.26        | 3.15        | 2.38         | 3.02         | 3.00         | 2.28         |      |       | 2.76 |
| Litergew. entspr. d.C-Z. (Kurvenwert) | 2.09        | 2.12        | 0.88         | 1.95         | 1.94         | 0.70         | 2.00 | 2.00  | 1.8  |
| g Gasol/l. Gasolgem.                  | 1.12        | 1.12        | 0.36         | 1.05         | 0.70         | 0.29         | 1.10 | 1.10  | 0.19 |
| g Gasol                               | 1990        | 1850        | 19.3         | 220          | 1360         | 18.0         | 220  | 1600  | 9.2  |
| g Gasol/Nm <sup>3</sup> Sygas         | 12.7        | 17.8        | 7.73         | 14.4         | 9.00         | 7.10         |      |       | 4.1  |
| Bemerkungen:                          |             |             |              |              |              |              |      |       |      |
| g/Nm <sup>3</sup> H <sub>2</sub> O    |             | 20.00       |              |              | 18.10        |              |      |       |      |
| g/Nm <sup>3</sup> h <sub>2</sub> O    |             | 23.00       |              |              | 22.00        |              |      | 22.10 |      |
| % h <sub>2</sub> O                    |             | 40          |              |              | 35           |              |      |       |      |

Druckversuchsanlage

Ofen... 11...

Füllung... 13...

Gasol ausbeute.

000356

|   | hant         | hant         | Castrol      | hant         | Castrol      | hant         | hant         | Castrol      |
|---|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| A.K.-Turm                                 | 64           | 6a           |              | 6a           |              | 64           | 6a           |              |
| Datum                                     | 16           | 17.9.        | 43           | 3/4.         | 16.10.       | 5/6.         | 10.          | 43           |
| Zeit                                      | 8-20         | 20-8         | 8-8          | 8-8          | 8-8          | 8-20         | 20-8         | 8-8          |
| Nm <sup>3</sup> /Sygas                    | 378<br>459   | 378<br>459   | 2,69         | 321<br>160   | 2,57         | 372<br>457   | 373<br>452   | 2,57         |
| l Restgas                                 |              |              | 1503<br>1402 |              | 1618<br>1500 |              |              | 1510<br>1419 |
| % Kontr.                                  |              |              | 47,8         |              | 47,5         |              |              | 43,7         |
| l Gasolgem.                               | 1906<br>1772 | 1876<br>1688 | 59<br>55     | 1622<br>1531 | 59           | 2153<br>2020 | 1872<br>1741 | 62<br>58     |
| Analys: CO <sub>2</sub>                   | 22.9         | 25.3         | 58.0         | 22.1         | 37.1         | 24.0         | 18.4         | 60.7         |
| C <sub>3</sub> H <sub>6</sub>             | 25.2         | 27.4         | 6.3          | 31.6         | 14.2         | 31.5         | 34.6         | 6.6          |
| C <sub>2</sub> H <sub>4</sub>             | 0.7          | 0.8          | 0.8          | 0.7          | 1.2          | 1.5          | 0.9          | 1.1          |
| O <sub>2</sub>                            | 0.0          | 0.0          | 0.0          | 0.0          | 0.0          | 0.0          | 0.0          | 0.0          |
| CO  | 0.3          | 0.4          | 6.5          | 0.0          | 0.0          | 0.0          | 0.0          | 0.0          |
| H <sub>2</sub>                            | 11.7         | 8.4          | 2.7          | 7.5          | 8.1          | 6.6          | 4.4          | 5.7          |
| CH <sub>4</sub> <sup>+</sup>              | 24.6         | 27.0         | 23.0         | 20.0         | 20.5         | 26.6         | 31.5         | 21.4         |
| N <sub>2</sub>                            | 2.2          | 4.7          | 2.7          | 5.1          | 2.1          | 2.5          | 3.7          | 2.1          |
| C-Zahl                                    | 3.77         | 3.05         | 2.32         | 3.01         | 2.7          | 3.06         | 2.99         | 2.31         |
| Litergew. entspr.<br>d. C-Z. (Kurvenwert) | 2.01         | 1.97         | 0.76         | 1.99         | 1.56         | 1.97         | 1.93         | 0.75         |
| g Gasol/l Gasolgem                        | 1.10         | 1.08         | 0.29         | 1.20         | 0.42         | 1.14         | 1.06         | 0.29         |
| g Gasol                                   | 1948         | 1822         | 16.0         | 1826         | 20.8         | 2220         | 2100         | 11.8         |
| g Gasol/Nm <sup>3</sup> Sygas             | 11.3         | 11.5         | 5.40         | 11.6         | 8.48         | 11.5         | 11.0         | 6.70         |
| Bemerkungen:                              |              |              |              |              |              |              |              |              |
| g/Nm <sup>3</sup> Sygas                   |              | 17.86        |              | 19.88        |              |              | 10.40        |              |
| g/Nm <sup>3</sup> Castrol                 |              | 20.5         |              | 22.6         |              |              | 23.80        |              |
| g/l Gasol                                 |              | 46           |              | 50           |              |              | 48           |              |

Druckversuchsanlage

Ofen ... 11.

Füllung ... 13.

Gasol ausbeute.

000357

|  | Gasol      | Carbol | Gasol  | Gasol | Carbol | Gasol        | Gasol | Carbol |
|--|------------|--------|--------|-------|--------|--------------|-------|--------|
| A.K.-Turm                              | 6a         |        | 6b     | 6a    |        | 6c           | 6a    |        |
| Datum                                  | 10/2. 2.63 |        | 12/23. | 9. 43 |        | 14/15. 9. 43 |       |        |
| Zeit                                   | 8-8        | 8-8    | 8-8    | 8-8   | 8-8    | 8-8          | 8-8   | 8-8    |
| Nm <sup>3</sup> /Sygas                 | 302        | 274    | 280    | 255   | 312    | 376          | 316   | 263    |
| 1 Restgas                              |            | 149    |        |       | 194    |              |       | 153    |
| % Kontr.                               |            | 43.5   |        |       | 41.3   |              |       | 45.5   |
| 1 Gasolgem.                            | 1797       | 58     | 2285   | 2657  | 66     | 2265         | 1908  | 60     |
| Analysé:                               |            |        |        |       |        |              |       |        |
| CO <sub>2</sub>                        | 24.5       | 21.5   | 22.0   | 25.0  | 32.2   | 16.7         | 21.6  | 57.3   |
| C <sub>3</sub> H <sub>6</sub>          | 24.4       | 3.3    | 26.7   | 21.9  | 7.3    | 35.4         | 27.0  | 7.1    |
| O <sub>2</sub> H <sub>4</sub>          | 0.7        | 0.7    | 1.0    | 0.7   | 0.2    | 1.3          | 0.9   | 0.9    |
| O <sub>2</sub>                         | 0.7        | 0.7    | 0.0    | 0.0   | 0.0    | 0.0          | 0.0   | 0.0    |
| CO                                     | 16.2       | 4.9    | 4.2    | 5.7   | 3.9    | 4.7          | 5.9   | 5.3    |
| H <sub>2</sub>                         | 12.0       | 2.4    | 4.8    | 9.2   | 7.3    | 4.5          | 7.5   | 7.9    |
| CH <sub>4</sub> <sup>+</sup>           | 25.2       | 12.0   | 37.8   | 33.8  | 24.6   | 24.7         | 33.3  | 24.5   |
| N <sub>2</sub>                         | 5.5        | 3.2    | 3.5    | 4.3   | 2.4    | 3.3          | 4.6   | 3.0    |
| C-Zahl                                 | 2.09       | 2.22   | 2.84   | 3.02  | 2.39   | 3.20         | 2.85  | 2.40   |
| Litergew. entspr. d. C-Z. (Kurvenwert) | 1.72       | 2.09   | 1.62   | 1.95  | 1.89   | 2.06         | 1.69  | 0.90   |
| g Gasol/l Gasolgem                     | 0.98       | 0.94   | 1.14   | 1.09  | 0.40   | 1.14         | 1.07  | 0.36   |
| g Gasol                                | 1648       | 7.4    | 2302   | 2559  | 24.4   | 3025         | 1920  | 20.2   |
| g Gasol/Nm <sup>3</sup> Sygas          | 10.9       | 3.05   | 16.1   | 17.9  | 7.5    | 10.5         | 12.0  | 7.62   |
| Bemerkungen:                           |            |        |        |       |        |              |       |        |
| g/l                                    | 13.62      |        | 21.1   |       |        |              | 23.27 |        |
| g/l                                    | 16.10      |        | 22.3   |       |        |              | 27.1  |        |
| g/l                                    | 25         |        | 36     |       |        |              | 43    |        |

Gaslausbeute

000358

|  | Gasol        | Gasol        | Carbot.      | Gasol        | Gasol        | Carbot.      | Gasol        | Gasol        | Carbot.      |
|--|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| A.K.-Turn                              | 66           | 6a           |              | 6b           | 6a           |              | 66           | 6a           |              |
| Datum                                  | 4/5. 9. 43   |              |              | 5/8. 9. 43   |              |              | 8/9. 9. 43   |              |              |
| Zeit                                   | 8-20         | 20-8         | 8-8          | 8-20         | 20-8         | 8-8          | 8-20         | 20-8         | 8-8          |
| Nm <sup>3</sup> /Sygas                 | 307<br>153   | 307<br>153   | 2.54         | 310<br>155   | 310<br>155   | 2.63         | 303<br>150   | 303<br>150   | 2.20         |
| l Restgas                              |              |              | 1485<br>1380 |              |              | 1573<br>1465 |              |              | 1305<br>1210 |
| % Kontr.                               |              |              | 43.8         |              |              | 42.4         |              |              | 42.4         |
| l Gasolgem.                            | 1932<br>1790 | 1772<br>1652 | 53<br>49.4   | 2128<br>1980 | 1778<br>1600 | 54<br>50     | 1863<br>2020 | 1827<br>1722 | 57<br>53     |
| Analyse: CO <sub>2</sub>               | 21.2         | 24.2         | 59.9         | 28.0         | 23.0         | 20.0         | 27.9         | 24.0         | 61.0         |
| C <sub>3</sub> H <sub>6</sub>          | 37.6         | 37.7         | 7.2          | 23.3         | 20.5         | 21.0         | 33.7         | 27.0         | 5.0          |
| O <sub>2</sub> H <sub>4</sub>          | 1.4          | 0.9          | 0.9          | 1.0          | 1.0          | 0.9          | 1.2          | 0.7          | 0.9          |
| O <sub>2</sub>                         | 0.2          | 0.7          | 0.2          | 0.2          | 0.7          | 0.2          | 0.7          | 0.7          | 0.7          |
| CO                                     | 6.8          | 6.5          | 5.7          | 2.9          | 2.0          | 6.9          | 5.7          | 6.8          | 6.7          |
| H <sub>2</sub>                         | 10.2         | 8.2          | 3.7          | 12.0         | 6.0          | 3.2          | 6.7          | 10.7         | 2.9          |
| CH <sub>4</sub> +                      | 24.6         | 23.7         | 18.2         | 27.0         | 22.4         | 19.0         | 27.6         | 21.7         | 20.5         |
| N <sub>2</sub>                         | 5.0          | 5.3          | 4.4          | 5.7          | 7.0          | 4.4          | 5.0          | 5.0          | 3.5          |
| C-Zahl                                 | 3.25         | 3.44         | 2.33         | 2.94         | 3.22         | 2.30         | 3.24         | 3.17         | 2.26         |
| Litergew. entspr. d. C-Z. (Kurvenwert) | 2.08         | 2.20         | 0.60         | 1.86         | 2.19         | 0.74         | 2.02         | 2.14         | 0.57         |
| g Gasol/l Gasolgem                     | 1.17         | 1.27         | 0.24         | 0.25         | 1.96         | 0.25         | 1.27         | 1.12         | 0.23         |
| g Gasol                                | 2095         | 1990         | 12.0         | 1676         | 1850         | 12.7         | 2556         | 1930         | 12.3         |
| g Gasol/Nm <sup>3</sup> Sygas          | 13.7         | 13.0         | 4.73         | 10.8         | 11.9         | 4.83         | 12.0         | 12.7         | 5.60         |
| Bemerkungen:                           |              |              |              |              |              |              |              |              |              |
| g/Nm <sup>3</sup> Ugas                 |              | 18.20        |              |              | 16.13        |              |              |              |              |
| g/Nm <sup>3</sup> G + H <sub>2</sub>   |              | 20.50        |              |              | 19.00        |              |              |              |              |
| % l <sub>1</sub> H <sub>2</sub> in     |              | 53           |              |              | 50           |              |              | 49           |              |

Druckversuchsanlage

Ofen ..... 1.1

Füllung..... 13

Gaslausbeute.

000359

|  | 1. Versuch         | 2. Versuch          | 3. Versuch          |
|--|--------------------|---------------------|---------------------|
| A.K.-Turm                              | 6.8                | 6.02                |                     |
| Datum                                  | 9/10 VIII          |                     | 4.3                 |
| Zeit                                   | 2-20               | 20-5                | 17-8                |
| Nm <sup>3</sup> /Sygas                 | $\frac{322}{261}$  | $\frac{322}{261}$   | 2,27                |
| 1 Restgas                              |                    |                     | $\frac{1525}{1420}$ |
| % Kontr.                               |                    |                     | 35,2                |
| 1 Gasolgem.                            | $\frac{164}{1525}$ | $\frac{1562}{1450}$ | $\frac{50}{44}$     |
| Analyse: CO <sub>2</sub>               | 26,6               | 25,0                | 62,5                |
| CO <sub>2</sub> H <sub>6</sub>         | 25,4               | 28,5                | 5,1                 |
| CO <sub>2</sub> H <sub>4</sub>         | 0,7                | 0,9                 | 0,9                 |
| O <sub>2</sub>                         | 0,0                | 0,0                 | 0,0                 |
| CO                                     | 8,9                | 7,1                 | 1,8                 |
| H <sub>2</sub>                         | 14,4               | 12,8                | 4,1                 |
| CH <sub>4</sub> +                      | 19,0               | 21,0                | 16,1                |
| N <sub>2</sub>                         | 4,4                | 4,7                 | 3,5                 |
| C-Zahl                                 | 3,26               | 3,24                | 2,63                |
| Litergew. entspr. d. C-Z. (Kurvenwert) | 2,16               | 2,07                | 1,30                |
| g Gasol/l Gasolgem                     | 0,96               | 1,02                | 0,30                |
| g Gasol                                | 1460               | 1480                | 141                 |
| g Gasol/Nm <sup>3</sup> Sygas          | 9,10               | 1,20                | 6,5                 |

Bemerkungen:

$\frac{1}{1} \text{ Nm}^3 \text{ Wagn. S.}$  15,65  
 $\frac{1}{1} \text{ Nm}^3 \text{ Bo + Bo.}$  18,30  
 $\frac{1}{1} \text{ Nm}^3 \text{ Bo. h.}$  49

Druckversuchsanlage

Ofen ... 11 ...

Füllung ... 13 ...

Gasolanalyse

000360

|                                       | Resul     | Korrek.   | Werte  | Werte  | Werte     | Werte  | Werte     | Werte     |
|---------------------------------------|-----------|-----------|--------|--------|-----------|--------|-----------|-----------|
| A.K.-Turm                             | 6a        |           | 6b     | 6b     |           | 6b     | 6b        |           |
| Datum                                 | 6/7       | 4.43      | 7/1    | 7/1    | 43        | 8/9    |           |           |
| Zeit                                  | 20-8      | 20-8      | 20-8   | 20-8   | 20-8      | 20-8   | 20-8      | 20-8      |
| Nm <sup>3</sup> /Sygas                | 305/50    | 2,82      | 289/44 | 289/44 | 2,36      | 298/49 | 298/49    | 2,34      |
| 1 Restgas                             |           | 1458/2359 |        |        | 2542/1435 |        |           | 1527/1435 |
| % Kontr.                              |           | 37,3      |        |        | 37,0      |        |           | 37,4      |
| 1 Gasolgem.                           | 1472/1370 | 458/42    | 1690   | 1550   | 50        | 1620   | 1222/1180 | 458/42    |
| Analyse: CO <sub>2</sub>              | 23,2      | 55,3      | 25,0   | 25,2   | 57,0      | 25,2   | 25,2      | 62,0      |
| C <sub>3</sub> H <sub>6</sub>         | 29,0      | 6,0       | 27,3   | 23,8   | 6,2       | 30,7   | 26,0      | 6,0       |
| C <sub>2</sub> H <sub>4</sub>         | 0,8       | 2,4       | 0,6    | 1,2    | 0,7       | 1,2    | 1,3       | 1,1       |
| O <sub>2</sub>                        | 0,2       | 0,7       | 0,1    | 0,3    | 0,1       | 0,1    | 0,1       | 0,1       |
| CO                                    | 7,6       | 8,4       | 8,1    | 6,7    | 7,5       | 7,9    | 8,3       | 7,2       |
| H <sub>2</sub>                        | 9,8       | 3,7       | 10,1   | 15,6   | 3,0       | 9,1    | 10,5      | 3,6       |
| CH <sub>4</sub> +                     | 23,4      | 19,9      | 22,7   | 21,4   | 20,2      | 21,2   | 20,7      | 19,9      |
| N <sub>2</sub>                        | 6,0       | 4,2       | 6,2    | 3,0    | 4,5       | 6,8    | 5,3       | 6,0       |
| C-Zahl                                | 3,78      | 2,33      | 3,2    | 3,17   | 2,45      | 3,44   | 2,55      | 3,2       |
| Litergew. entspr. d.C-Z. (Kurvenwert) | 2,04      | 0,73      | 2,16   | 2,04   | 0,98      | 2,20   | 2,44      | 0,56      |
| g Gasol/l Gasolgem                    | 1,07      | 0,26      | 0,93   | 0,93   | 0,32      | 1,14   | 1,14      | 0,26      |
| g Gasol                               | 1463      | 10,82     | 1570   | 1350   | 1600      | 1850   | 1350      | 1455      |
| g Gasol/Nm <sup>3</sup> Sygas         | 4,65      | 4,90      | 10,90  | 9,88   | 6,8       | 12,40  | 9,05      | 4,10      |
| Bemerkungen:                          |           |           |        |        |           |        |           |           |
| g/Nm <sup>3</sup> Sygas               | 14,55     |           | 16,94  |        |           | 15,02  |           |           |
| g/liter Gasol                         | 17,00     |           | 19,95  |        |           | 17,65  |           |           |
| # l/n                                 | 49        |           | 5      |        |           | 52,5   |           |           |



Druckversuchsanlage

Ofen ... *1.1.*

Füllung ... *1.3*

Gasolausbeute.

000361

|  | Gasol        | Gasol        | Carbol.      | Gasol        | Gasol        | Carbol.    | Gasol        | Gasol        | Carbol.      |
|--|--------------|--------------|--------------|--------------|--------------|------------|--------------|--------------|--------------|
| A.K.-Turm                              | 6b           | 6a           |              | 6b           | 6a           |            | 6b           | 6a           |              |
| Datum                                  | 2/3. 8.      | 1/3. 8.      | 43           | 2/4. 8.      | 2/4. 8.      | 43         | 5/6. 8.      | 5/6. 8.      | 43           |
| Zeit                                   | 8-20         | 8-20         | 20-8         | 8-20         | 20-8         | 8-8        | 8-20         | 20-8         | 20-8         |
| Nm <sup>3</sup> /Sygas                 | 379<br>159   | 390<br>155   | 333          | 305<br>153   | 305<br>153   |            | 240<br>302   | 302<br>157   | 2.20         |
| l Restgas                              |              |              | 1547<br>1440 |              |              |            | 1562<br>1453 |              | 1508<br>1399 |
| % Kontr.                               |              |              | 34.5         |              |              |            | 37.9         |              | 34.9         |
| l Gasolgem.                            | 1678<br>1560 | 1479<br>1325 | 23<br>47     | 1540<br>1420 | 1293<br>1262 | 47<br>23.5 | 1512<br>1410 | 1391<br>1300 | 40<br>37     |
| Analyse: CO <sub>2</sub>               | 20.8         | 37.2         | 32.5         | 25.7         | 25.5         | 07.9       | 24.7         | 23.5         | 57.0         |
| C <sub>3</sub> H <sub>6</sub>          | 26.8         | 32.4         | 7.9          | 27.6         | 25.9         | 5.0        | 26.4         | 25.0         | 1.8          |
| C <sub>2</sub> H <sub>4</sub>          | 0.5          | 0.2          | 1.2          | 2.8          | 0.8          | 1.3        | 0.9          | 0.7          | 1.0          |
| O <sub>2</sub>                         | 0.0          | 0.9          | 0.2          | 0.0          | 0.1          | 0.7        | 0.0          | 0.7          | 0.7          |
| CO                                     | 7.7          | 2.7          | 2.4          | 5.6          | 7.2          | 7.2        | 8.2          | 8.2          | 6.4          |
| H <sub>2</sub>                         | 14.0         | 10.6         | 4.9          | 15.5         | 14.9         | 4.2        | 17.8         | 14.7         | 1.7          |
| CH <sub>4</sub> +                      | 23.4         | 22.0         | 14.1         | 27.2         | 22.5         | 25.2       | 23.2         | 27.5         | 27.5         |
| N <sub>2</sub>                         | 2.3          | 4.3          | 2.2          | 7.0          | 7.0          | 4.5        | 5.9          | 6.5          | 3.5          |
| C-Zahl                                 | 3.38         | 3.28         | 2.52         | 2.13         | 2.22         | 2.62       | 3.44         | 3.43         | 2.56         |
| Litergew. entspr. d. C-Z. (Kurvenwert) | 2.16         | 2.35         | 1.72         | 2.34         | 2.76         | 1.30       | 2.20         | 2.19         | 1.20         |
| g Gasol/l Gasolgem                     | 1.10         | 1.25         | 0.36         | 0.27         | 1.02         | 0.32       | 1.09         | 1.02         | 0.92         |
| g Gasol                                | 1790         | 1720         | 14.4         | 1243         | 1243         | 13.9       | 1535         | 1330         | 15.7         |
| g Gasol/Nm <sup>3</sup> Sygas          | 4.45         | 4.44         | 2.20         | 2.9          | 2.9          | 5.8        | 10.2         | 8.87         | 7.1          |
| Bemerkungen:                           |              |              |              |              |              |            |              |              |              |
| <i>8.11.11</i>                         |              | 17.34        |              |              | 13.9         |            | 16.63        |              |              |
| <i>9.11.11</i>                         |              | 20.20        |              |              | 16.4         |            | 19.50        |              |              |
| <i>9.11.11</i>                         |              | 50           |              |              | 45           |            | 45           |              |              |

Druckversuchsanlage

Ofen ..1.1...

Füllung...1.3...

Gaslaubeute.

000362

|                                       | 1. Lauf              | 2. Lauf              | 3. Lauf             | 4. Lauf              | 5. Lauf              | 6. Lauf             | 7. Lauf              | 8. Lauf              | 9. Lauf             |
|---------------------------------------|----------------------|----------------------|---------------------|----------------------|----------------------|---------------------|----------------------|----------------------|---------------------|
| A.K.-Turm                             | 6a                   | 6a                   |                     | 6a                   | 6a                   |                     | 6a                   | 6a                   |                     |
| Datum                                 | 26/27.7.             | 27.7.                | 28.7.               | 29/30.7.             | 30.7.                | 31.7.               | 31.7.                | 31.7.                | 31.7.               |
| Zeit                                  | 8-20                 | 8-8                  | 14-8                | 13-20                | 20-8                 | 20-8                | 8-20                 |                      |                     |
| Nm <sup>3</sup> /Sygas                | <del>303/150</del>   | <del>307/150</del>   | 2.47                | <del>245/77</del>    | <del>245/155</del>   | 2.77                | <del>249/115</del>   | <del>249/115</del>   |                     |
| 1 Restgas                             |                      |                      | <del>1698/488</del> |                      |                      | <del>1647/529</del> |                      |                      | <del>1535/418</del> |
| % Kontr.                              |                      |                      | 38.3                |                      |                      | 43.4                |                      |                      |                     |
| 1 Gasolgem.                           | <del>1635/1622</del> | <del>1894/1688</del> | <del>48/45</del>    | <del>1715/1595</del> | <del>1379/1182</del> | <del>117/84</del>   | <del>1711/1602</del> | <del>1540/1632</del> | <del>46/43</del>    |
| Analysc:                              |                      |                      |                     |                      |                      |                     |                      |                      |                     |
| CO <sub>2</sub>                       | 25.6                 | 23.6                 | 58.5                | 27.3                 | 28.6                 | 56.8                | 24.7                 | 29.1                 | 62.1                |
| C <sub>3</sub> H <sub>6</sub>         | 24.6                 | 25.2                 | 7.2                 | 28.6                 | 22.3                 | 8.1                 | 30.1                 | 22.9                 | 7.0                 |
| O <sub>2</sub> H <sub>4</sub>         | 0.6                  | 0.5                  | 0.6                 | 0.5                  | 0.6                  | 0.8                 | 0.6                  | 0.6                  | 0.4                 |
| O <sub>2</sub>                        | 0.0                  | 0.0                  | 0.0                 | 0.0                  | 0.0                  | 0.0                 | 0.0                  | 0.0                  | 0.0                 |
| CO                                    | 6.3                  | 6.9                  | 6.7                 | 6.7                  | 8.5                  | 7.0                 | 6.5                  | 9.6                  | 7.3                 |
| H <sub>2</sub>                        | 14.0                 | 13.6                 | 2.9                 | 9.3                  | 12.5                 | 3.1                 | 9.7                  | 12.3                 | 3.8                 |
| CH <sub>4</sub> +                     | 23.6                 | 25.3                 | 22.6                | 22.5                 | 21.5                 | 20.6                | 24.0                 | 19.8                 | 15.2                |
| N <sub>2</sub>                        | 5.3                  | 5.7                  | 4.0                 | 5.7                  | 6.0                  | 3.7                 | 4.4                  | 5.7                  | 4.2                 |
| C-Zahl                                | 3.44                 | 3.42                 | 2.53                | 3.08                 | 3.06                 | 2.31                | 3.23                 | 3.05                 | 2.53                |
| Litergew. entspr. d.C-Z. (Kurvenwert) | 2.20                 | 2.19                 | 1.13                | 1.99                 | 1.97                 | 0.75                | 2.07                 | 1.97                 | 1.23                |
| g Gasol/l Gasolgem                    | 1.06                 | 1.17                 | 0.57                | 1.02                 | 0.86                 | 0.37                | 1.12                 | 0.84                 | 0.32                |
| g Gasol                               | 1673                 | 1872                 | 167                 | 1628                 | 1113                 | 13.6                | 1793                 | 1704                 | 13.8                |
| g Gasol/Nm <sup>3</sup> Sygas         | 10.8                 | 12.5                 | 6.93                | 21.1                 | 7.98                 | 5.0                 |                      |                      |                     |
| Bemerkungen:                          |                      |                      |                     |                      |                      |                     |                      |                      |                     |

g/Nm<sup>3</sup> Sygas 18.58 19.14  
 g/Nm<sup>3</sup> C<sub>3</sub>H<sub>6</sub> 21.67 22.50  
 % C<sub>3</sub>H<sub>6</sub> 46 49

Druckversuchsanlage

Ofen ...11...

Füllung...13..

Gasol ausbeute.

000363

|  | 1. Versuch   | 2. Versuch   | 3. Versuch   | 4. Versuch | 5. Versuch | 6. Versuch | 7. Versuch   | 8. Versuch   | 9. Versuch   |
|--|--------------|--------------|--------------|------------|------------|------------|--------------|--------------|--------------|
| A.K.-Turm                              | 600          | 62           |              |            |            |            |              |              |              |
| Datum                                  | 18/10        | VII          | 43           |            |            |            |              |              |              |
| Zeit                                   | 8-20         | 20-8         | 8-8          |            |            |            |              |              |              |
| Nm <sup>3</sup> /Sygas                 | 320<br>160   | 320<br>160   | 2,98         | 302<br>151 | 302<br>151 | 2,24       | 295<br>148   | 295<br>148   | 2,43         |
| 1 Restgas                              |              |              | 1568<br>1470 |            |            | 1420       |              |              | 1557<br>1450 |
| % Kontr.                               |              |              | 33,8         |            |            | 34,7       |              |              | 38,1         |
| 1 Gasolgem.                            | 1161<br>1085 | 1121<br>1520 | 49<br>37,4   | 1258       | 1510       | 42         | 1127<br>1540 | 1177<br>1385 | 54<br>50,5   |
| Analys: CO <sub>2</sub>                | 20,6         | 24,0         | 59,0         |            |            |            | 27,5         | 26,2         | 57,5         |
| C <sub>3</sub> H <sub>6</sub>          | 30,9         | 25,0         | 5,2          |            |            | 6,7        | 21,2         | 25,3         | 5,5          |
| C <sub>2</sub> H <sub>4</sub>          | 1,1          | 1,1          | 0,8          |            |            |            | 0,8          | 0,8          | 0,9          |
| O <sub>2</sub>                         | 0,1          | 0,1          | 0,1          |            |            |            | 0,1          | 0,0          | 0,1          |
| CO                                     | 7,9          | 9,1          | 10,9         | 8,5        |            | 8,6        | 7,2          | 8,7          | 8,5          |
| H <sub>2</sub>                         | 11,9         | 12,3         | 2,4          | 11,5       |            |            | 16,2         | 12,9         | 5,2          |
| CH <sub>4</sub> <sup>+</sup>           | 18,5         | 18,1         | 16,3         | 19,8       |            |            | 21,0         | 21,0         | 16,8         |
| N <sub>2</sub>                         | 9,0          | 10,3         | 5,3          | 5,7        |            |            | 6,0          | 5,1          | 5,5          |
| C-Zahl                                 | 3,36         | 3,14         | 2,34         | 2,27       |            |            | 3,62         | 3,68         | 2,55         |
| Litergew. entspr. d. C-Z. (Kurvenwert) | 2,15         | 2,02         | 0,85         | 2,10       | 2,46       | 1,38       | 2,32         | 2,34         | 1,10         |
| g Gasol/l Gasolgem                     | 1,176        | 0,87         | 0,23         | 0,96       | 1,00       | 0,30       | 0,75         | 1,08         | 0,29         |
| g Gasol                                | 1115         | 1320         | 8,6          | 1210       | 1510       | 12,6       | 1510         | 1490         | 147          |
| g Gasol/Nm <sup>3</sup> Sygas          | 7,2          | 8,2          | 3,8          | 8,0        | 10,0       | 5,6        | 10,2         | 10,1         | 6,1          |
| Bemerkungen:                           |              |              |              |            |            |            |              |              |              |
| g/Nm <sup>3</sup> Sygas                |              | 11,5         |              |            | 14,6       |            |              | 16,3         |              |
| g/Nm <sup>3</sup> - 80 + 36            |              | 13,3         |              |            | 16,9       |            |              | 18,9         |              |
| g/o Bu 36                              |              | 53,5         |              |            | 58,1       |            |              | 47,0         |              |



Druckversuchsanlage

Ofen ... 11.

Füllung... 13...

Gasol ausbeute

000365

|   | Gasol        | Gasol        | Gasol      | Carbot.    | Gasol        | Gasol        | Gasol      | Carbot.     |
|---|--------------|--------------|------------|------------|--------------|--------------|------------|-------------|
| A.K.-Turm   | 6a           | 6a           | 5b         |            | 6a           | 6b           |            |             |
| Datum   |              | 18/19.6.     | 43         |            | 20/21.6.     | 43           |            |             |
| Zeit  | 8-16         | 0-8          | 8-8        | 8-8        | 8-20         | 20-8         | 8-8        | 8-8         |
| Nm <sup>3</sup> /Sygas                            | 309<br>102   | 309<br>103   | 309        | 2,14       | 380<br>43    | 380<br>63    | 280        | 2,48        |
| l Restgas   |              |              |            | 144<br>315 |              |              |            | 154<br>1480 |
| % Kontr.  |              |              |            | 36,5       |              |              |            | 38,7        |
| l Gasolgem.                                       | 1512<br>1410 | 1503<br>1407 | 508<br>522 | 45<br>22   | 1565<br>1455 | 1762<br>1640 | 312<br>729 | 47<br>33,7  |
| Analyse: CO <sub>2</sub>                          | 29,4         | 33,5         | 26,7       | 69,7       | 22,7         | 23,2         | 22,7       | 63,5        |
| C <sub>3</sub> H <sub>6</sub>                     | 26,8         | 10,3         | 8,4        | 2,3        | 24,2         | 27,9         | 11,6       | 5,2         |
| C <sub>2</sub> H <sub>4</sub>                     | 0,9          | 0,7          | 0,4        | 0,6        | 0,7          | 0,7          | 0,6        | 0,6         |
| O <sub>2</sub>                                    | 0,1          | 0,1          | 0,1        | 0,0        | 0,1          | 0,1          | 0,1        | 0,0         |
| CO  | 9,2          | 12,3         | 12,5       | 2,0        | 7,2          | 7,7          | 12,2       | 8,2         |
| H <sub>2</sub>                                    | 14,7         | 22,7         | 33,6       | 3,4        | 17,3         | 17,4         | 22,5       | 3,2         |
| CH <sub>4</sub> +                                 | 15,9         | 17,5         | 7,8        | 17,9       | 27,8         | 22,9         | 14,9       | 15,9        |
| N <sub>2</sub>                                    | 7,0          | 9,5          | 12,5       | 4,2        | 6,0          | 5,5          | 11,0       | 3,4         |
| C-Zahl  | 2,90         | 2,72         | 2,70       | 2,107      | 2,98         | 3,24         | 2,68       | 2,02        |
| Litergew. entspr.<br>d.C-Z. (Kurvenwert)          | 1,78         | 1,48         | 3,07       | 0,20       | 1,93         | 2,08         | 1,40       | 0,33        |
| g Gasol/l Gasolgem                                | 0,68         | 0,36         | 0,23       | 0,07       | 0,87         | 0,51         | 0,43       | 0,15        |
| g Gasol   | 960          | 510          | 150        | 2,89       | 1238         | 834          | 312        | 6,55        |
| g Gasol/Nm <sup>3</sup> Sygas                     | 9,3          | 4,95         | 0,48       | 1,31       | 13,7         | 8,99         | 1,17       | 2,54        |
| Bemerkungen:                                      |              |              |            |            |              |              |            |             |
| g / Nm <sup>3</sup> H <sub>2</sub> gas            |              |              | 8,91       |            |              | 15,00        |            |             |
| g / Nm <sup>3</sup> C <sub>2</sub> H <sub>4</sub> |              |              | 10,02      |            |              | 17,20        |            |             |
| % in H <sub>2</sub> gas                           |              |              | 50         |            |              | 49           |            |             |

Druckversuchsanlage

Ofen ... 11.

Füllung... 1.3...

Gasolausbeute.

000366

|  | Gasol | Gasol | Gasol | Carbol | Gasol  | Gasol | Gasol  | Carbol |
|--|-------|-------|-------|--------|--------|-------|--------|--------|
| A.K.-Turm                              | 6a    | 6a    | 5a    |        | 6a     | 6a    | 5a     |        |
| Datum                                  |       | 12/11 | 12/11 |        |        | 16/12 | 6. 4 3 |        |
| Zeit                                   | 8-8   | 0-8   | 8-8   | 8-8    | 8-16   | 0-8   | 8-8    | 8-8    |
| Nm <sup>3</sup> /Sygas                 | 297   | 297   | 307   | 296    | 297    | 297   | 297    | 1189   |
| l Restgas                              |       |       |       | 1068   |        |       |        | 990    |
| % Kontr.                               |       |       |       | 35.2   |        |       |        | 36.3   |
| l Gasolgem.                            | 1795  | 1202  | 1437  | 48     | 1567   | 1178  | 689    | 4238   |
| Analyse: CO <sub>2</sub>               | 35.2  | 20.2  | 37.6  | 20.2   | 31.2   | 30.9  | 36.3   | 66.4   |
| C <sub>3</sub> H <sub>6</sub>          | 18.9  | 10.4  | 10.2  | 1.5    | 27.1   | 16.7  | 17.3   | 4.1    |
| C <sub>2</sub> H <sub>4</sub>          | 0.4   | 3.2   | 2.6   | 0.7    | 1.7    | 0.8   | 0.8    | 0.7    |
| O <sub>2</sub>                         | 0.1   | 0.1   | 0.1   | 0.1    | 0.1    | 0.1   | 0.1    | 0.0    |
| CO                                     | 0.1   | 0.1   | 0.1   | 0.1    | 0.1    | 0.1   | 0.1    | 0.0    |
| H <sub>2</sub>                         | 16.6  | 15.1  | 15.2  | 7.7    | 9.3    | 11.3  | 12.5   | 8.0    |
| CH <sub>4</sub> <sup>+</sup>           | 49.1  | 18.1  | 18.2  | 2.1    | 14.7   | 20.3  | 27.5   | 5.3    |
| N <sub>2</sub>                         | 6.7   | 3.7   | 7.1   | 1.5    | 16.5   | 12.5  | 10.0   | 17.9   |
| C-Zahl                                 | 8.5   | 3.7   | 3.7   | 0.19   | 6.0    | 8.0   | 7.5    | 3.6    |
| Litergew. entspr. d. C-Z. (Kurvenwert) | 127   | 1.07  | 1.11  | 0.5    | 2.03   | 1.97  | 1.70   | 0.94   |
| g Gasol/l Gasolgem                     | 0.66  | 0.86  | 0.77  | 0.00   | 0.76   | 0.56  | 0.75   | 0.29   |
| g Gasol                                | 1194  | 966   | 205   | 6.7    | 1110.0 | 773   | 2110   | 111.1  |
| g Gasol/Nm <sup>3</sup> Sygas          | 1088  | 5.57  | 1.13  | 2.00   | 11.2   | 7.80  | 0.82   | 6.80   |
| Bemerkungen:                           |       |       |       |        |        |       |        |        |

g/l Nm<sup>3</sup> Sygas

13.56

17.12

g/l Nm<sup>3</sup> Carbol

16.10

19.50

g/l Nm<sup>3</sup> Gasol

14.18

4.8

Druckversuchsanlage

Ofen .../1/1...

Füllung...13...

Gaslausbeute.

000367

|   | 1. Lauf      | 2. Lauf      | 3. Lauf    | 4. Lauf    | 5. Lauf    | 6. Lauf      | 7. Lauf     | 8. Lauf      |
|---|--------------|--------------|------------|------------|------------|--------------|-------------|--------------|
| A.K.-Turm                                 | 6a           | 6a           | 5a         |            | 6a         | 6a           | 5a          |              |
| Datum                                     |              | 9/10.        | 6. 43      |            |            | 10/11.       | 6.          | 43           |
| Zeit                                      | 8-76         | 0-8          | 8-8        | 8-8        | 8-16       | 0-8          | 8-8         | 8-8          |
| Nm <sup>3</sup> /Sygas                    | 298<br>99    | 258<br>99    | 298        | 277        | 286<br>85  | 286<br>85    | 286         | 237          |
| l Restgas                                 |              |              |            | 155<br>411 |            |              |             | 154<br>413.5 |
| % Kontr.                                  |              |              |            | 33,3       |            |              |             | 39,6         |
| l Gasolgem.                               | 1828<br>2682 | 1408<br>1370 | 856<br>889 | 69<br>26   | 852<br>253 | 2439<br>2338 | 1084<br>958 | 24<br>106    |
| Analyse: CO <sub>2</sub>                  | 31.9         | 30.8         | 44.0       | 70.6       | 36.8       | 32.3         | 39.0        | 70.0         |
| C <sub>3</sub> H <sub>6</sub>             | 17.9         | 22.2         | 4.0        | 1.8        | 16.2       | 16.2         | 6.0         | 1.7          |
| C <sub>2</sub> H <sub>4</sub>             | 0.5          | 1.5          | 2.4        | 0.3        | 0.6        | 1.2          | 1.9         | 0.4          |
| O <sub>2</sub>                            | 0.7          | 0.7          | 0.7        | 0.7        | 0.7        | 0.7          | 0.7         | 0.7          |
| CO  | 8.2          | 6.6          | 10.8       | 6.7        | 6.3        | 9.2          | 11.2        | 6.8          |
| H <sub>2</sub>                            | 14.6         | 11.8         | 19.2       | 3.2        | 15.0       | 21.4         | 24.8        | 3.9          |
| CH <sub>4</sub> <sup>+</sup>              | 19.7         | 19.2         | 10.5       | 13.3       | 18.7       | 14.0         | 12.0        | 13.6         |
| N <sub>2</sub>                            | 6.1          | 7.8          | 0.0        | 4.0        | 6.5        | 2.0          | 8.0         | 3.5          |
| -C-Zahl                                   | 2.43         | 2.84         | 2.52       | 2.17       | 2.94       | 2.52         | 2.80        | 2.16         |
| Litergew.entspr.<br>d.C-Z. (Kurvegewicht) | 1.87         | 1.79         | 1.72       | 0.33       | 1.84       | 1.72         | 1.60        | 0.32         |
| g Gasol/l Gasolgem                        | 0.69         | 0.76         | 0.14       | 0.02       | 0.63       | 0.48         | 0.31        | 0.08         |
| g Gasol                                   | 1168         | 996          | 169        | 3.68       | 970        | 642          | 297         | 3.68         |
| g Gasol/Nm <sup>3</sup> Sygas             | 11.8         | 9.7          | 0.57       | 1.70       | 10.2       | 6.95         | 1.04        | 1.55         |
| Bemerkungen:                              |              |              |            |            |            |              |             |              |

g / Nm<sup>3</sup> Sygas 13.02 11.06  
 g / Nm<sup>3</sup> C<sub>2</sub>H<sub>4</sub> 15.47 12.73  
 % C<sub>2</sub>H<sub>4</sub> 47 47

Gasol ausbeute.

000368

|  | Gasol                   | Gasol                   | Gasol                  | Carbol                 | Gasol                   | Gasol                   | Gasol                  | Carbol                 |
|--|-------------------------|-------------------------|------------------------|------------------------|-------------------------|-------------------------|------------------------|------------------------|
| A.K.-Turm  | 6.6                     | 6.6                     |                        |                        | 6.0                     | 6.0                     | 5.6                    |                        |
| Datum  |                         | 7/8.                    | 6.4.3                  |                        | 8/9.                    | 6.                      | 4.3                    |                        |
| Zeit   | 8-76                    | 0-8                     | 8-8                    | 8-8                    | 8-16                    | 0-8                     | 8-8                    | 8-8                    |
| Nm <sup>3</sup> /Sygas                             | <del>310</del><br>103   | <del>310</del><br>103   | 310                    | 2140                   | <del>245</del><br>48    | <del>245</del><br>48    | 245                    | 2,39                   |
| l Restgas  |                         |                         |                        | <del>159</del><br>1478 |                         |                         |                        | <del>169</del><br>1575 |
| % Kontr.   |                         |                         |                        | 38,5                   |                         |                         |                        | 34,0                   |
| l Gasolgem.  | <del>1708</del><br>1840 | <del>1407</del><br>1303 | <del>1033</del><br>462 | <del>49</del><br>46    | <del>1436</del><br>2338 | <del>1577</del><br>2668 | <del>1076</del><br>446 | <del>51</del><br>47    |
| Analys: CO <sub>2</sub>                            | 30,5                    | 30,3                    | 41,8                   | 79,3                   | 30,1                    | 37,0                    | 46,0                   | 70,7                   |
| C <sub>3</sub> H <sub>6</sub>                      | 25,0                    | 19,6                    | 6,2                    | 1,0                    | 23,4                    | 17,0                    | 6,0                    | 1,4                    |
| C <sub>2</sub> H <sub>4</sub>                      | 0,5                     | 1,1                     | 1,2                    | 0,4                    | 1,5                     | 0,4                     | 1,4                    | 0,5                    |
| O <sub>2</sub>                                     | 0,1                     | 0,1                     | 0,1                    | 0,0                    | 0,4                     | 0,1                     | 0,1                    | 0,1                    |
| CO   | 8,6                     | 8,4                     | 10,5                   | 8,0                    | 8,4                     | 5,8                     | 10,2                   | 5,8                    |
| H <sub>2</sub>                                     | 11,2                    | 14,8                    | 20,0                   | 3,8                    | 9,1                     | 13,7                    | 15,7                   | 13,3                   |
| CH <sub>4</sub> <sup>+</sup>                       | 19,5                    | 20,2                    | 12,2                   | 13,2                   | 23,2                    | 20,5                    | 19,8                   | 16,5                   |
| N <sub>2</sub>                                     | 4,6                     | 5,5                     | 8,0                    | 2,3                    | 3,8                     | 5,0                     | 7,5                    | 3,3                    |
| C-Zahl   | 3,13                    | 3,24                    | 2,64                   | 1,84                   | 3,09                    | 2,46                    | 2,44                   | 2,70                   |
| Litergew. entspr. d. C-Z. (Korrekturentwert)       | 2,47                    | 2,68                    | 1,92                   | 0,77                   | 1,44                    | 1,88                    | 1,82                   | 0,38                   |
| g Gasol/l Gasolgem                                 | 0,40                    | 0,83                    | 0,28                   | 0,00                   | 0,43                    | 0,70                    | 0,35                   | 0,08                   |
| g Gasol  | 1432                    | 1082                    | 270                    | 1,84                   | 1245                    | 1027                    | 331                    | 3,76                   |
| g Gasol/Nm <sup>3</sup> Sygas                      | 10,9                    | 10,5                    | 0,87                   | 0,77                   | 12,7                    | 10,5                    | 11,2                   | 1,58                   |
| Bemerkungen:                                       |                         |                         |                        |                        |                         |                         |                        |                        |
| g / Nm <sup>3</sup> Sygas                          |                         | 13,84                   |                        |                        |                         | 14,30                   |                        |                        |
| g / Nm <sup>3</sup> C <sub>0</sub> +C <sub>1</sub> |                         | 15,8                    |                        |                        |                         | 16,54                   |                        |                        |
| % C <sub>2</sub> H <sub>4</sub> in                 |                         | 57                      |                        |                        |                         | 47                      |                        |                        |



Gasol ausbeute.

000369

|  | hawl                    | hawl                    | hawl                  | Controll               | hawl                    | hawl                    | hawl                   | Controll               |
|--|-------------------------|-------------------------|-----------------------|------------------------|-------------------------|-------------------------|------------------------|------------------------|
| A.K.-Turm                              |                         | 6a                      | 5b                    |                        | 6a                      | 6a                      |                        |                        |
| Datum                                  |                         | 5/6. 6.                 | 4.3.                  |                        |                         | 6/7. 6.                 | 4.3.                   |                        |
| Zeit                                   | 8-76                    | 0-8                     |                       | 8-8                    | 8-76                    | 0-8                     | 8-8                    | 8-8                    |
| Nm <sup>3</sup> /Sygas                 | <del>323</del><br>108   | <del>323</del><br>108   | 323                   | 2,74                   | <del>309</del><br>103   | <del>309</del><br>103   | 323                    | <del>285</del><br>103  |
| l Restgas                              |                         |                         |                       | <del>1480</del><br>177 |                         |                         |                        | <del>1528</del><br>176 |
| % Kontr.                               |                         |                         |                       | 37,7                   |                         |                         |                        | 37,0                   |
| l Gasolgem.                            | <del>1605</del><br>1492 | <del>1399</del><br>1300 | <del>938</del><br>873 | <del>42</del><br>39    | <del>1107</del><br>1060 | <del>1293</del><br>1340 | <del>1071</del><br>998 | <del>52</del><br>48    |
| Analysse: CO <sub>2</sub>              | 30,2                    | 27,1                    | 36,2                  | 67,5                   | 27,3                    | 28,6                    | 34,5                   | 64,3                   |
| C <sub>3</sub> H <sub>6</sub>          | 29,0                    | 23,9                    | 7,3                   | 1,2                    | 15,2                    | 24,2                    | 7,7                    | 0,3                    |
| C <sub>2</sub> H <sub>4</sub>          | 1,3                     | 0,9                     | 0,5                   | 1,1                    | 1,2                     | 0,9                     | 1,4                    | 0,6                    |
| O <sub>2</sub>                         | 0,1                     | 0,1                     | 0,1                   | 0,1                    | 0,1                     | 0,1                     | 0,1                    | 0,1                    |
| CO                                     | 8,9                     | 11,0                    | 13,9                  | 11,1                   | 16,0                    | 8,2                     | 12,3                   | 7,9                    |
| H <sub>2</sub>                         | 15,3                    | 15,6                    | 23,8                  | 4,2                    | 22,5                    | 12,5                    | 20,5                   | 4,3                    |
| CH <sub>4</sub> +                      | 16,2                    | 14,1                    | 10,0                  | 10,8                   | 10,7                    | 21,7                    | 10,7                   | 14,0                   |
| N <sub>2</sub>                         | 8,0                     | 7,3                     | 9,4                   | 4,0                    | 7,0                     | 4,4                     | 7,8                    | 3,5                    |
| C-Zahl                                 | 3,74                    | 3,21                    | 3,05                  | 2,17                   | 3,74                    | 2,93                    | 2,69                   | 2,52                   |
| Litergew. entspr. d. C-Z. (KURZWEICHT) | 2,02                    | 2,07                    | 1,92                  | 0,39                   | 2,02                    | 1,87                    | 1,47                   | 0,30                   |
| g Gasol/l Gasolgem                     | 0,73                    | 0,79                    | 0,33                  | 0,07                   | 0,52                    | 0,84                    | 0,30                   | 0,03                   |
| g Gasol                                | 1090                    | 1030                    | 288                   | 273                    | 550                     | 1168                    | 310                    | 144                    |
| g Gasol/Nm <sup>3</sup> Sygas          | 10,1                    | 9,6                     | 0,89                  | 1,25                   | 5,36                    | 11,3                    | 0,93                   | 0,66                   |
| Bemerkungen:                           |                         |                         |                       |                        |                         |                         |                        |                        |
| g/Nm <sup>3</sup> Sygas                |                         |                         | 12,04                 |                        |                         | 9,89                    |                        |                        |
| g/Nm <sup>3</sup> CO <sub>2</sub>      |                         |                         | 13,70                 |                        |                         | 11,24                   |                        |                        |
| % C <sub>3</sub> H <sub>6</sub>        |                         |                         | 5,8                   |                        |                         | 5,4                     |                        |                        |

Füllung -13.

Stillstände!

|           |                                     |                               |
|-----------|-------------------------------------|-------------------------------|
| 5.11.43   | 13 <sup>00</sup> - 16 <sup>00</sup> | Gasausfall KW.Betriebe.       |
| 7.11.43   | 11 <sup>30</sup> - 13 <sup>15</sup> | wegen erhöhter Einfluggefahr. |
| 11.11.43  | 14 <sup>20</sup> - 15 <sup>20</sup> | " " Feindeinflüge.            |
| 15.11.43  | 22 <sup>10</sup> - 22 <sup>15</sup> | Strom u. Gasausfall.          |
| 19.11.43  | 12 <sup>15</sup> - 14 <sup>15</sup> | Strom u. Gasausfall.          |
| 19.11.43  | 19 <sup>30</sup> - 23 <sup>20</sup> | Strom u. Gasausfall.          |
| 27.11.43  | 5 <sup>30</sup> - 9 <sup>30</sup>   | Stromausfall.                 |
| 5/6.12.43 | 23 <sup>00</sup> - 12 <sup>00</sup> | Gasleitung eingefroren.       |
| 7.12.43   | 20 <sup>30</sup> - 22 <sup>30</sup> | Stromausfall.                 |
| 21.12.43  | 13 <sup>15</sup> - 16 <sup>40</sup> | Gasausfall.                   |
| 27.12.43  | 18 <sup>20</sup> - 22 <sup>20</sup> | Strom u. Gasausfall.          |
| 28.12.43  |                                     | } Komprs. in Repar.           |
| 29.12.43  |                                     |                               |
| 3.1.44    | 8 <sup>00</sup> - 11 <sup>00</sup>  | A.K. Turm in repar.           |
| 2.1.44    | 11 <sup>10</sup> - 11 <sup>50</sup> | Riemenbruch am Komprs.        |

O f e n 11 Fe-Kontakt.

000371

Füllung 13.

O-haltige Produkte.

3./4. 1.44 Reaktionswasser,  
=0,71 gr.Nm<sup>3</sup> W-Gas 0,8 gr.Nm<sup>3</sup> Nutzgas D<sup>20</sup> 0,855

11./12. 1.44 Reaktionswasser,  
=0,82 gr.Nm<sup>3</sup> W-Gas 0,93 gr.Nm<sup>3</sup> Nutzgas D<sup>20</sup> 0,857

22./23. 1.44 AK.Abtrieb ~~ben~~gewandt wurden die ersten 5 Ltr.Wasser  
0,088 gr.Nm<sup>3</sup> W-Gas 0,11 gr.Nm<sup>3</sup> Nutzgas D<sup>20</sup> 0,143

000372

Ofen M. P. Nordhoff 13 Pflanz

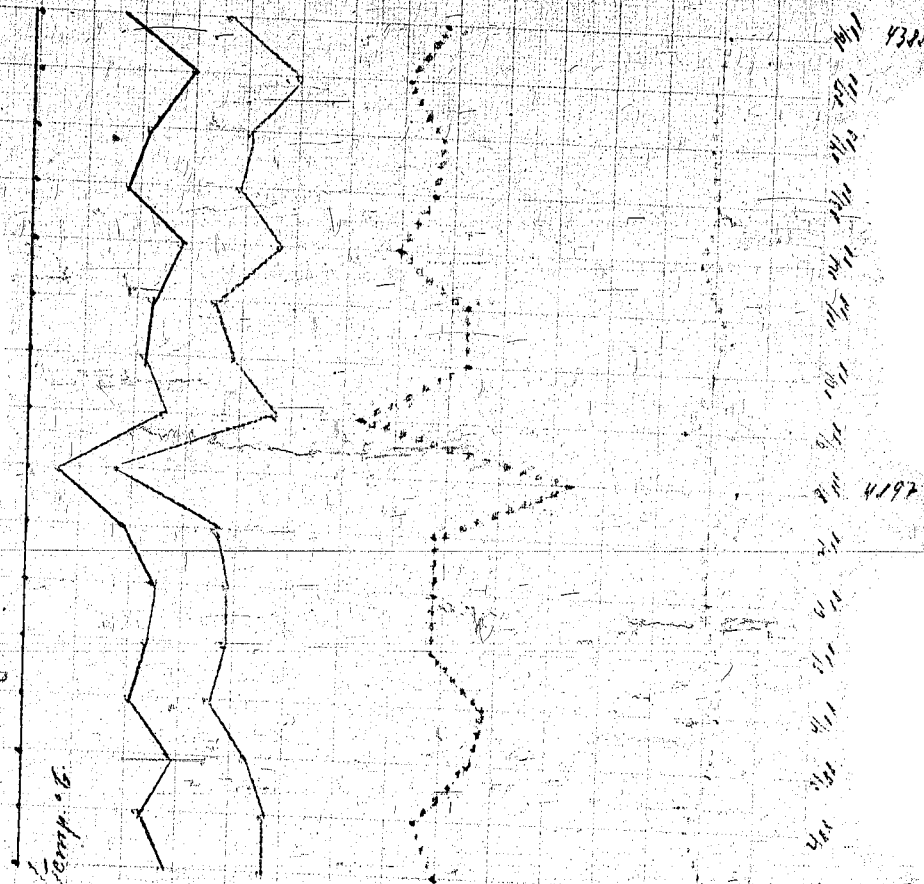
Camp 06

————— 1/200 220000000  
 ————— 1/200 180000000  
 - - - - - 1/200 140000000  
 ······ 1/200 100000000  
 ······ 1/200 60000000  
 ······ 1/200 20000000

20  
 10 230  
 0

70 220  
 60 210  
 50 200  
 40 190  
 30 180  
 20 170  
 10 160  
 0 150

↑ Dist  
 ↑ Health



10/1 400  
 10/2 400  
 10/3 400  
 10/4 400  
 10/5 400  
 10/6 400  
 10/7 400  
 10/8 400  
 10/9 400  
 10/10 400  
 10/11 400  
 10/12 400  
 10/13 400  
 10/14 400  
 10/15 400  
 10/16 400  
 10/17 400

4321

4197

4037

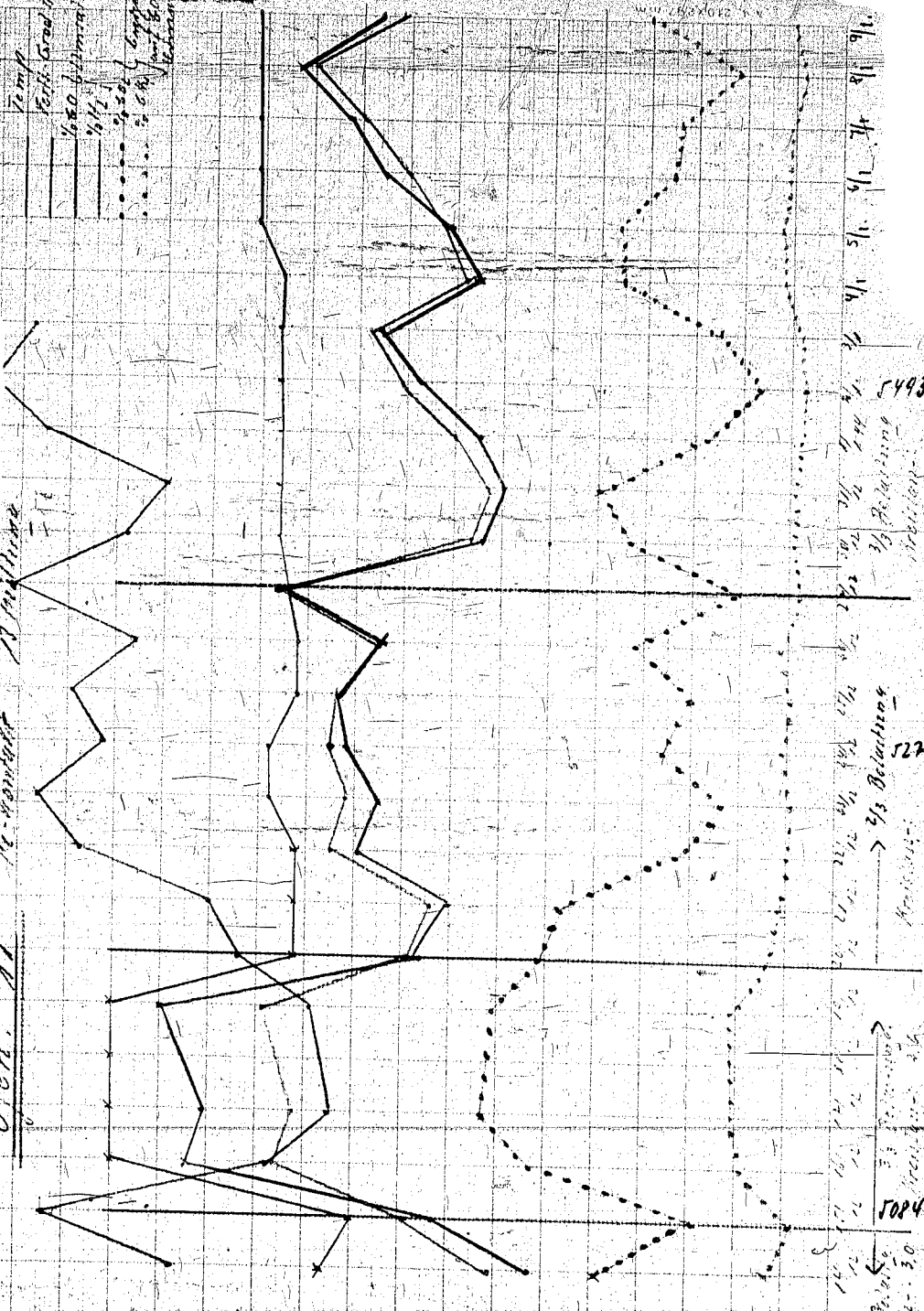


000374

Temp  
 Felt Grad  
 16.50 (normal)  
 1/12  
 1/20  
 1/30  
 1/40  
 1/50  
 1/60  
 1/70  
 1/80  
 1/90  
 1/100

Open: 11  
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90 240  
 80 230  
 70 220  
 60 210  
 50 200  
 40 190  
 30 180  
 20 170  
 10 160  
 150  
 140  
 130  
 120  
 110  
 100  
 90  
 80  
 70  
 60  
 50  
 40  
 30  
 20  
 10  
 0



5493  
 1/12  
 1/20  
 1/30  
 1/40  
 1/50  
 1/60  
 1/70  
 1/80  
 1/90  
 1/100

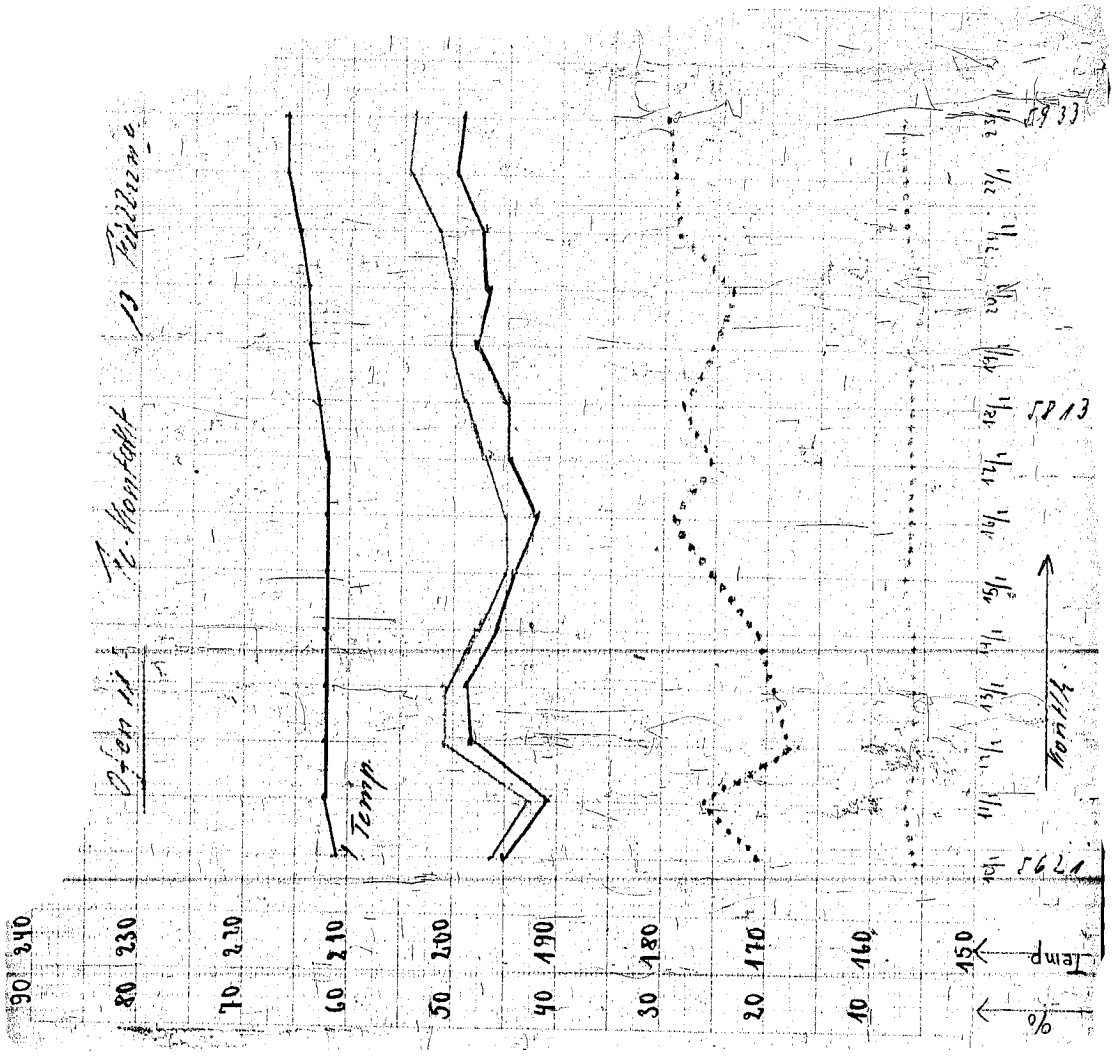
5270  
 1/12  
 1/20  
 1/30  
 1/40  
 1/50  
 1/60  
 1/70  
 1/80  
 1/90  
 1/100

5024  
 1/12  
 1/20  
 1/30  
 1/40  
 1/50  
 1/60  
 1/70  
 1/80  
 1/90  
 1/100

000375

— 1/2 50% 21mm 100%  
 — 1/2 42%  
 — 1/2 50% 21mm 100%  
 — 1/2 50% 21mm 100%

Ofen 113  
 E. Non-falt  
 13



583

571

562

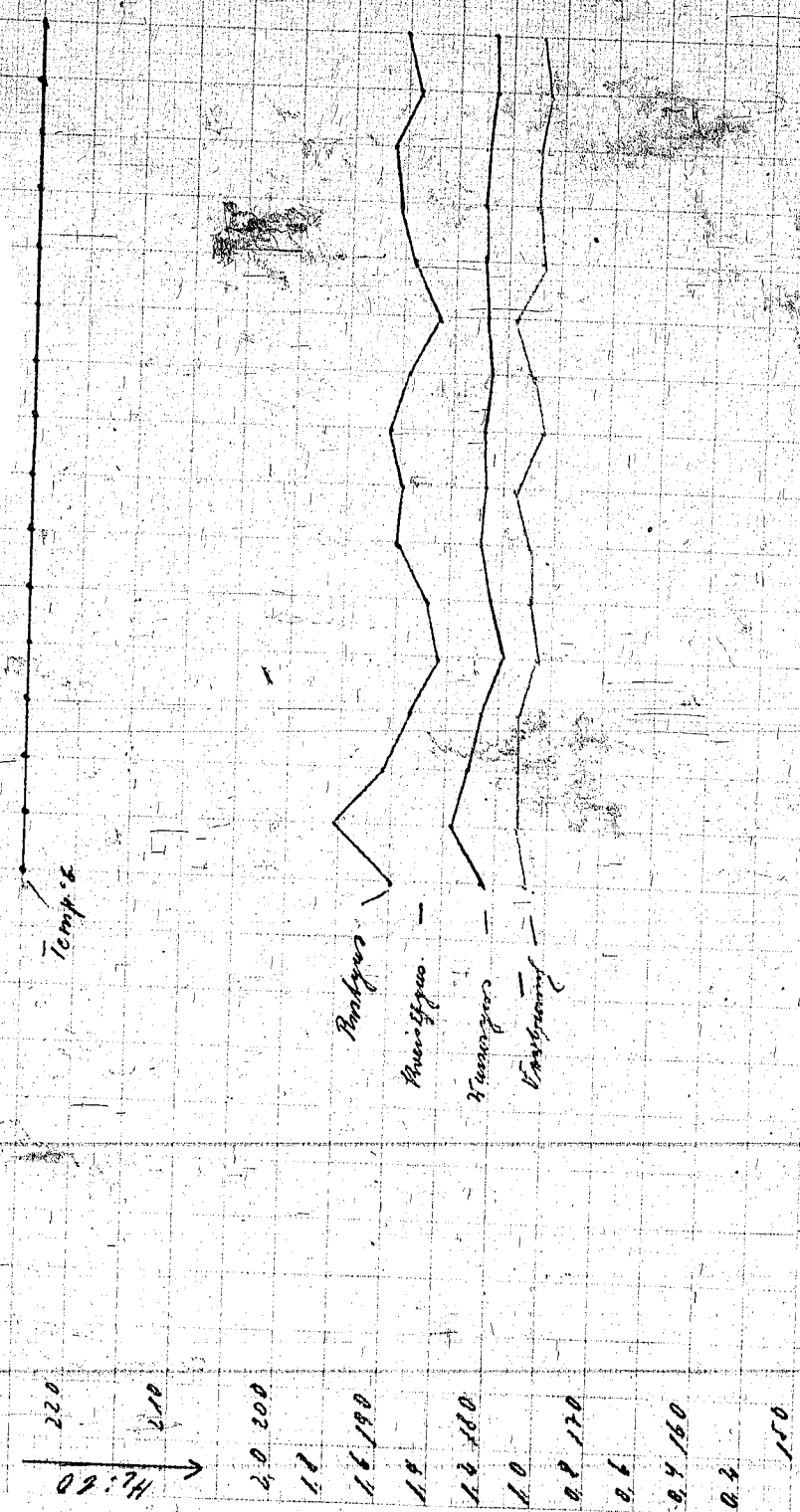
Temp

%

000376

Observations  
No. 400376

Temp. 280  
HL: 60



4035  
 4197  
 4385  
 111 214 211 410 510 610 710 810 910 1010 1110 1210 1310 1410 1510  
 Dist. →  
 Cont'd. →





000378

Heuer  
Heißgas  
Reißgas  
Verbrauch

Ofen: 11 Kontakt 1500/1500

Temp. 6.  
230  
220  
210

As: 20  
→

Temp

5.0 200

1.2

1.6 190

1.4

1.000

1.4 190

1.0

0.8 130

0.6

0.4 160

0.3

150

Verbrauch



140  
130  
120  
110  
100  
90  
80  
70  
60  
50  
40  
30  
20  
10  
0

400

140  
130  
120  
110  
100  
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70  
60  
50  
40  
30  
20  
10  
0

1270

1493

140  
130  
120  
110  
100  
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80  
70  
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50  
40  
30  
20  
10  
0

140  
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120  
110  
100  
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70  
60  
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40  
30  
20  
10  
0

140  
130  
120  
110  
100  
90  
80  
70  
60  
50  
40  
30  
20  
10  
0

000379

Handwritten notes on a piece of paper, possibly a ledger or account book. The text is very faint and difficult to read, but appears to include:

40 - 10 1/2

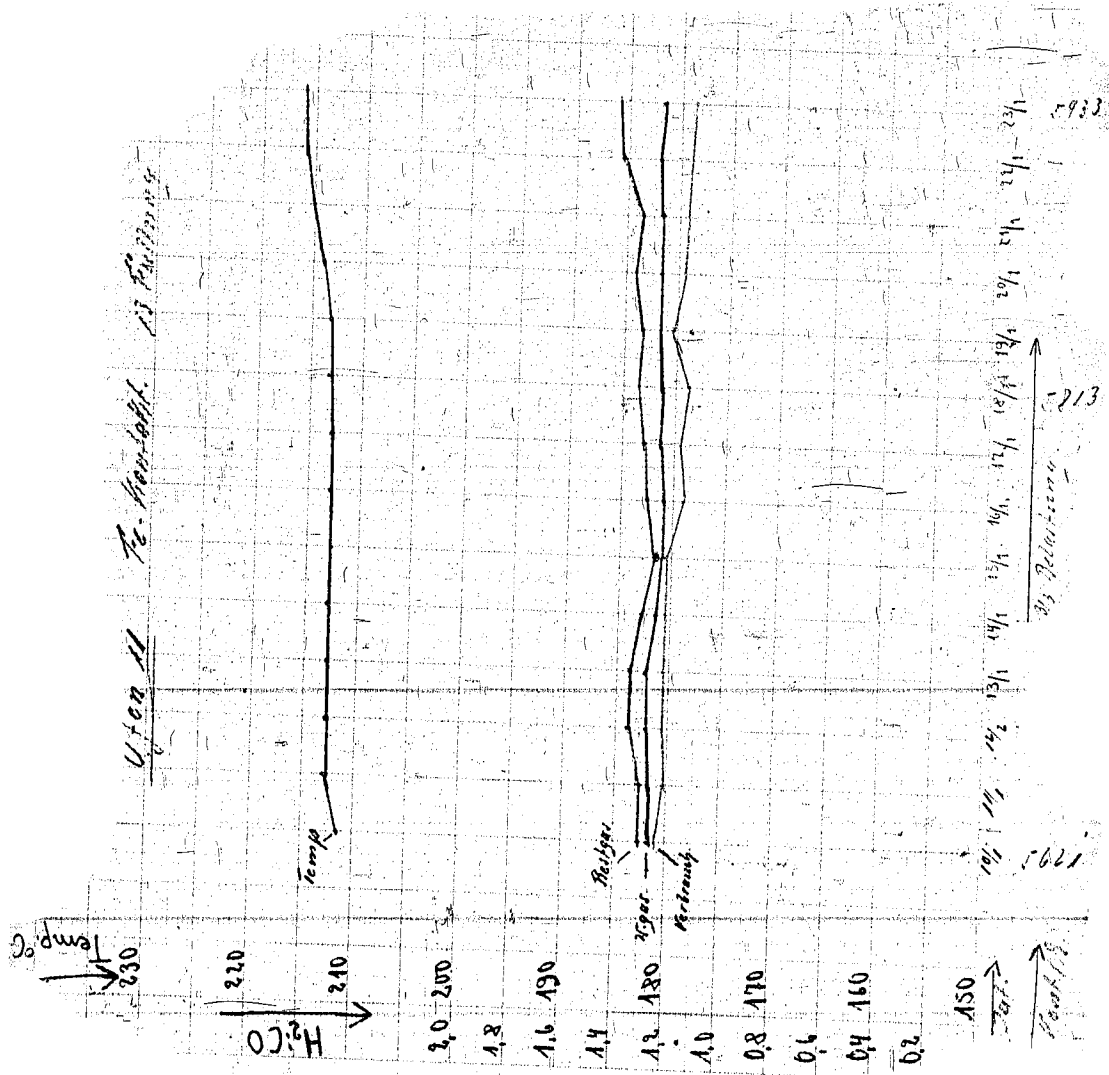
Kreis...

9 - 15

000380

Kugel  
Kochgas  
Beleggas  
Verdrängung

U von H<sub>2</sub> Fe. Hartstoff. in Fe. Bismut



100  
110  
120  
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170  
180  
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200  
210  
220  
230

100  
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200  
210  
220  
230

000381

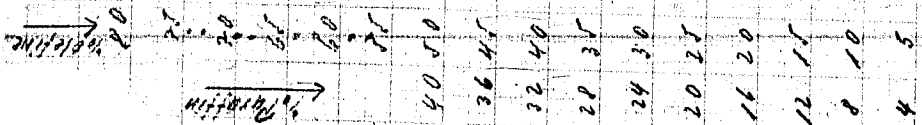
Ofers MA.

19 Feb 1946

Mc Kean Is.

Paraffin

100-200°C  
200-300°C  
300-400°C  
400-500°C  
500-600°C  
600-700°C  
700-800°C  
800-900°C  
900-1000°C  
1000-1100°C  
1100-1200°C  
1200-1300°C  
1300-1400°C  
1400-1500°C  
1500-1600°C  
1600-1700°C  
1700-1800°C  
1800-1900°C  
1900-2000°C  
2000-2100°C  
2100-2200°C  
2200-2300°C  
2300-2400°C  
2400-2500°C  
2500-2600°C  
2600-2700°C  
2700-2800°C  
2800-2900°C  
2900-3000°C  
3000-3100°C  
3100-3200°C  
3200-3300°C  
3300-3400°C  
3400-3500°C  
3500-3600°C  
3600-3700°C  
3700-3800°C  
3800-3900°C  
3900-4000°C  
4000-4100°C  
4100-4200°C  
4200-4300°C  
4300-4400°C  
4400-4500°C  
4500-4600°C  
4600-4700°C  
4700-4800°C  
4800-4900°C  
4900-5000°C



241. →  
2400. →

4035  
4197  
4328

000382

200 g Paraffin  
200 g Paraffin  
1/2 Paraffin

Te. Kontakt  
12 Füllhöhe

Te. Kontakt

Ofen 11

→ % Paraffin

→ % Paraffin

14, 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29 30 1 2 3 4 5 6 7 8 9 10 11 12, 13

4892

4237

4571

→ Kontakt

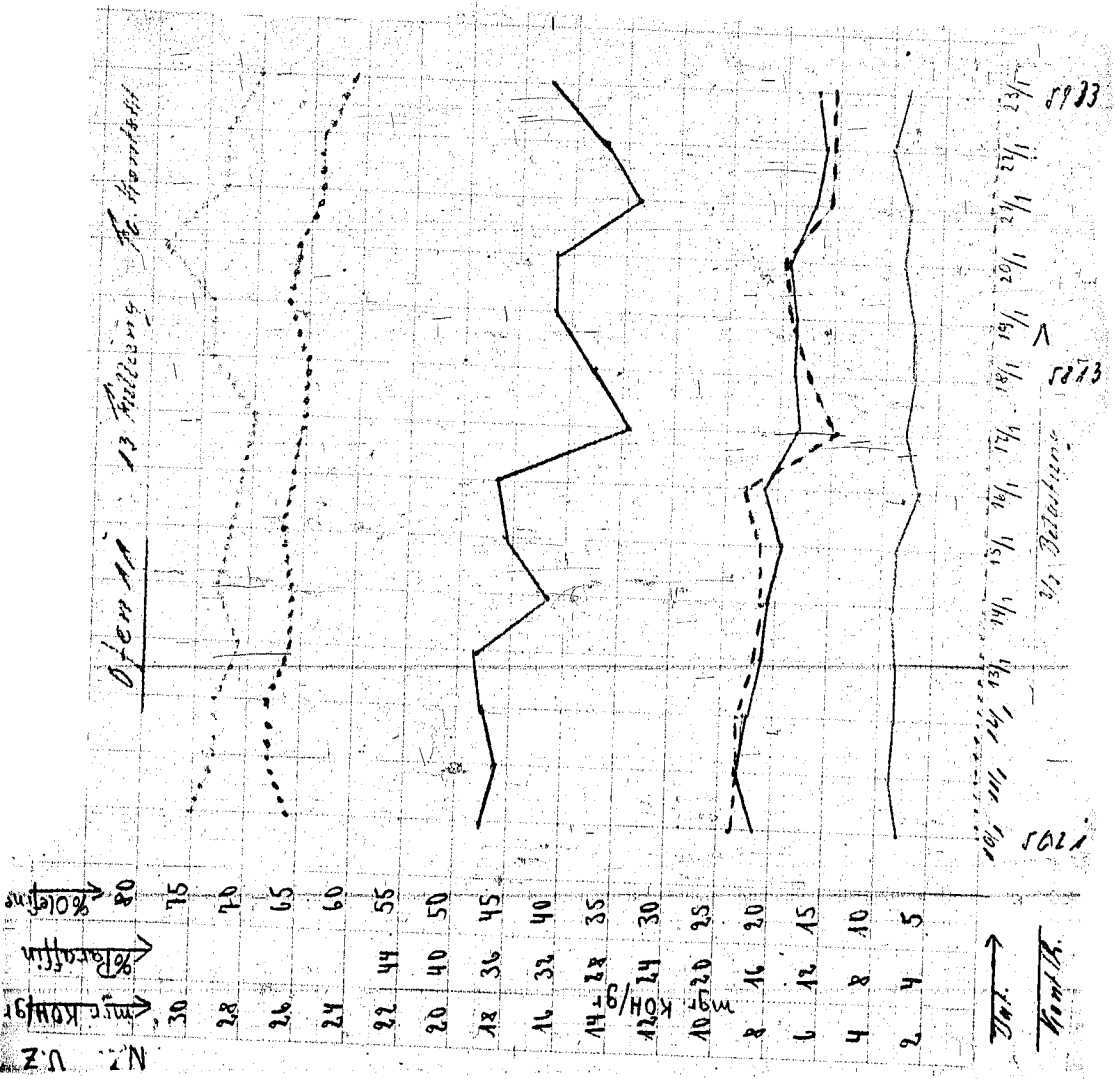
80  
75  
70  
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60  
55  
40 50  
36 45  
33 40  
28 35  
24 30  
20 25  
16 20  
14 15  
8 10  
4 5

V. 210 212 214



000384

200-320-200  
-200-  
% Paraffin  
#2 } Oct. number.  
#2 }  
#2 } Prod. - Tower  
#2 }  
#2 } A. H. Dennis



8923

5873



# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 8.9.144 Zeit          Betr. Tage         

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,40      | 38,8       | 40,4                   | 32,8                                | 32,3                  |
| Kondens.-Öl    | 5,40      | 45,7       | 57,7                   | 44,9                                | 35,5                  |
| Paraffingatsch | 3,00      | 25,5       | 38,9                   | 22,4                                | 19,2                  |
| Ges.-Prod.     | 11,80     | 100,0      | 139,0                  | 100,0                               | 24,5                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,610       | 0,794   | 0,89           |                | 0,883           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            | 152,84      | 283,133 |                |                | 1958            |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 41     |        |
| 60 "          |        |        |        |        | 80     |        |
| 80 "          |        |        |        |        | 100    |        |
| 100 "         |        |        |        |        | 35,0   |        |
| 120 "         |        |        |        |        | 31,0   |        |
| 140 "         |        |        |        |        | 27,0   | 55,2   |
| 160 "         |        |        |        |        | 15,0   |        |
| 180 "         |        |        |        |        | 7,0    |        |
| 200 "         |        |        |        |        | 5,0    |        |
| 220 "         |        |        |        |        | 4,0    |        |
| 240 "         |        |        |        |        | 3,5    |        |
| 260 "         |        |        |        |        | 2,5    |        |
| 280 "         |        |        |        |        | 2,5    | 30,3   |
| 300 "         |        |        |        |        | 2,0    |        |
| 320 "         |        |        |        |        | 1,0    |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 33,3   |
| Verlust       |        |        |        |        |        | 1,3    |

| Stockpunkt °C     | Destill.-Prod. |     |     | Olefin |  |
|-------------------|----------------|-----|-----|--------|--|
|                   | SPL            | N Z | V Z |        |  |
| Benzin (bis 200°) |                |     |     | 176    |  |
| Öl (200-320°)     |                |     |     | 66     |  |

Bemerkungen: *Wasser Paraffin*

000385

*[Signature]*

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 1.2.1.44 Zeit        Betr. Tage       

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,40      | 35,6       | 37,5                   | 39,1                                | 19,9                  |
| Kondens.-Öl    | 6,60      | 49,6       | 62,6                   | 48,7                                | 38,6                  |
| Paraffingatsch | 3,30      | 34,8       | 28,5                   | 23,2                                | 19,3                  |
| Ges.-Prod.     | 13,30     | 100,0      | 128,6                  | 100,0                               | 77,8                  |

| Kondens.-Prod.       | A K - Benzin | Ölkond.    | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|--------------|------------|-----------------|----------------|------------------|
| Dichte bei 20 °C     | 0,683        | 0,794      | 0,87            |                | 0,493            |
| Olefine „SPL“ Vol. % |              |            |                 |                |                  |
| Jodzahl (Wijss)      |              |            |                 |                |                  |
| N Z / V Z            | 0,7 / 3,3    | 8,8 / 18,0 |                 |                |                  |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 4,5    |        |
| 60 "          |        |        |        |        | 6,0    |        |
| 80 "          |        |        |        |        | 11,0   |        |
| 100 "         |        |        |        |        | 32,0   |        |
| 120 "         |        |        |        | 1      | 30,0   |        |
| 140 "         |        |        |        |        | 37,0   | 54,0   |
| 160 "         |        |        |        |        | 44,0   |        |
| 180 "         |        |        |        |        | 53,0   |        |
| 200 "         |        |        |        |        | 57,0   |        |
| 220 "         |        |        |        |        | 62,0   |        |
| 240 "         |        |        |        |        | 77,0   |        |
| 260 "         |        |        |        |        | 81,0   |        |
| 280 "         |        |        |        |        | 83,0   | 33,0   |
| 300 "         |        |        |        |        | 76,0   |        |
| 320 "         |        |        |        |        | 79,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 33,0   |
| Verlust       |        |        |        |        |        | 0,0    |

| Stockpunkt °C | Destill.-Prod.    | SPL | N Z | V Z    |
|---------------|-------------------|-----|-----|--------|
|               | Benzin (bis 200°) |     |     | Olefin |
|               | Öl (200-320°)     |     |     | 73     |
|               |                   |     |     | 85     |

Bemerkungen: *tr. Rückst. Paraffin*

000386

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 6.7.1.44 Zeit            Betr. Tage           

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 2,40      | 26,3       | 38,7                   | 39,7                                 | 30,2                  |
| Kondens.-Öl    | 6,20      | 48,1       | 64,7                   | 49,0                                 | 36,9                  |
| Paraffingatsch | 2,30      | 35,6       | 39,4                   | 26,3                                 | 19,6                  |
| Ges.-Prod.     | 10,90     | 100,0      | 13,05                  | 100,0                                | 20,7                  |

| Kondens.-Prod.       | A.K. Benzin  | Ölkond.     | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|--------------|-------------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0,680        | 0,769       | 0,81            |                | 0,928            |
| Olefine „SPL“ Vol. % |              |             |                 |                |                  |
| Jodzahl (Wijss)      |              |             |                 |                |                  |
| N Z / V Z            | 0,107 / 3,37 | 4,08 / 1,08 |                 |                | 8,36             |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| — 40 °C       |        |        |        |        | 41     |        |
| 60 "          |        |        |        |        | 00     |        |
| 80 "          |        |        |        |        | 140    |        |
| 100 "         |        |        |        |        | 360    |        |
| 120 "         |        |        |        |        | 330    |        |
| 140 "         |        |        |        |        | 400    | 13,3   |
| 160 "         |        |        |        |        | 450    |        |
| 180 "         |        |        |        |        | 520    |        |
| 200 "         |        |        |        |        | 520    |        |
| 220 "         |        |        |        |        | 610    |        |
| 240 "         |        |        |        |        | 650    |        |
| 260 "         |        |        |        |        | 680    |        |
| 280 "         |        |        |        |        | 715    |        |
| 300 "         |        |        |        |        | 745    |        |
| 320 "         |        |        |        |        | 760    |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 2,45   |
| Verlust       |        |        |        |        |        | 2,4    |

|                   |     |     |     |  |        |  |
|-------------------|-----|-----|-----|--|--------|--|
| Stockpunkt °C     |     |     |     |  |        |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |        |  |
| Benzin (bis 200°) |     |     |     |  | Olefin |  |
| Öl (200—320°)     |     |     |     |  | 71     |  |
|                   |     |     |     |  | 69     |  |

Bemerkungen: *Produkt Haraffin*

000387

Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 5.6.144 Zeit            Betr. Tage           

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,85      | 28,5       | 48,1                   | 33,9                                | 23,2                  |
| Kondens.-Öl    | 5,95      | 44,1       | 55,5                   | 43,3                                | 34,5                  |
| Paraffingatsch | 3,70      | 27,4       | 20,5                   | 23,8                                | 31,4                  |
| Ges.-Prod.     | 13,50     | 100,0      | 138,1                  | 100,0                               | 79,1                  |

| Kondens.-Prod.       | A K-Benzin | Ölkond.    | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|------------|------------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0,672      | 0,798      | 0,90            |                | 0,986            |
| Olefine „SPL“ Vol. % |            |            |                 |                |                  |
| Jodzahl (Wijss)      |            |            |                 |                |                  |
| N Z / V Z            | 1056 / 199 | 958 / 1534 |                 |                | 1054             |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        | 43     |        |
|               | 60 "        |        |        |        |        | 80     |        |
|               | 80 "        |        |        |        |        | 190    |        |
|               | 100 "       |        |        |        |        | 340    |        |
|               | 120 "       |        |        |        |        | 300    |        |
|               | 140 "       |        |        |        |        | 320    | 50,7   |
|               | 160 "       |        |        |        |        | 20     |        |
|               | 180 "       |        |        |        |        | 10     |        |
|               | 200 "       |        |        |        |        | 10     |        |
|               | 220 "       |        |        |        |        | 610    |        |
|               | 240 "       |        |        |        |        | 650    |        |
|               | 260 "       |        |        |        |        | 60     |        |
|               | 280 "       |        |        |        |        | 720    | 20,9   |
|               | 300 "       |        |        |        |        | 250    |        |
|               | 320 "       |        |        |        |        | 275    |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 25,2   |
| Verlust       |             |        |        |        |        |        | 1,2    |

|                   |     |     |     |  |     |  |  |
|-------------------|-----|-----|-----|--|-----|--|--|
| Stockpunkt °C     |     |     |     |  |     |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |     |  |  |
| Benzin (bis 200°) |     |     |     |  | 0,6 |  |  |
| Öl (200-320°)     |     |     |     |  | 69  |  |  |
|                   |     |     |     |  | 70  |  |  |

Bemerkungen: Arbeitsparaffin

000388

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 12 Dat. 4.5.1.44 Zeit 6 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 3,50         | 27,5           | 40,9                   | 31,9                                 | 21,4                  |
| Kondens.-Öl    | 5,85         | 45,8           | 57,5                   | 44,9                                 | 35,8                  |
| Paraffingatsch | 3,40         | 26,7           | 39,7                   | 32,0                                 | 20,9                  |
| Ges.-Prod.     | 12,75        | 100,0          | 122,4                  | 100,0                                | 78,1                  |

| Kondens.-Prod.       | A.K.-Benzin   | Ölkond.      | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|---------------|--------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,623         | 0,797        | 0,90                |                | 0,984                |
| Olefine „SPL“ Vol. % |               |              |                     |                |                      |
| Jodzahl (Wjss)       |               |              |                     |                |                      |
| N Z / V Z            | 0,653 / 0,868 | 1,14 / 1,205 |                     |                | 10,42                |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 3,8    |        |
| 60 "          |        |        |        |        | 7,0    |        |
| 80 "          |        |        |        |        | 18,0   |        |
| 100 "         |        |        |        |        | 33,0   |        |
| 120 "         |        |        |        |        | 38,0   |        |
| 140 "         |        |        |        |        | 35,0   | 29,4   |
| 160 "         |        |        |        |        | 43,0   |        |
| 180 "         |        |        |        |        | 48,0   |        |
| 200 "         |        |        |        |        | 53,0   |        |
| 220 "         |        |        |        |        | 59,0   |        |
| 240 "         |        |        |        |        | 64,0   |        |
| 260 "         |        |        |        |        | 68,0   |        |
| 280 "         |        |        |        |        | 71,0   | 33,5   |
| 300 "         |        |        |        |        | 73,5   |        |
| 320 "         |        |        |        |        | 76,5   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 2,5, 0 |

| Stockpunkt °C     | SPL | N Z | V Z |           |
|-------------------|-----|-----|-----|-----------|
| Destill.-Prod.    |     |     |     | Öl-Benzin |
| Benzin (bis 200°) |     |     |     | 74        |
| Öl (200-320°)     |     |     |     | 73        |

Remerkungen: *benzin & karolin*

000389

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 3.4.1.44 Zeit      Betr. Tage     

| Produkt        | Anfall, kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|------------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 7,40       | 29,0       | 57,7                   | 45,3                                 | 30,6                  |
| Kondens.-Ol    | 0,85       | 12,8       | 17,3                   | 13,6                                 | 10,9                  |
| Paraffingatsch | 2,90       | 47,2       | 52,5                   | 41,1                                 | 27,0                  |
| Ges.-Prod.     | 11,15      | 100,0      | 127,5                  | 100,0                                | 78,5                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|---------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0,676       | 0,299   | 0,90            |                | 0,024            |
| Olefine „SPL“ Vol. % |             |         |                 |                |                  |
| Jodzahl (Wijs)       |             |         |                 |                |                  |
| N Z V Z              | 10 107 982  | 109 154 |                 |                | 11,52            |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 5,0    |        |
| 60 "          |        |        |        |        | 18,0   |        |
| 80 "          |        |        |        |        | 36,0   |        |
| 100 "         |        |        |        |        | 33,0   |        |
| 120 "         |        |        |        |        | 37,0   | 46,0   |
| 140 "         |        |        |        |        | 42,0   |        |
| 160 "         |        |        |        |        | 46,0   |        |
| 180 "         |        |        |        |        | 49,0   |        |
| 200 "         |        |        |        |        | 51,0   |        |
| 220 "         |        |        |        |        | 53,0   |        |
| 240 "         |        |        |        |        | 55,0   |        |
| 260 "         |        |        |        |        | 57,5   | 10,9   |
| 280 "         |        |        |        |        | 59,0   |        |
| 300 "         |        |        |        |        | 60,5   |        |
| 320 "         |        |        |        |        | 62,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 40,7   |
| Verlust       |        |        |        |        |        | 3,4    |

|                   |     |     |     |       |  |
|-------------------|-----|-----|-----|-------|--|
| Stockpunkt °C     |     |     |     |       |  |
| Destill.-Prod.    | SPL | N Z | V Z | Ölfen |  |
| Benzin (bis 200°) |     |     |     | 69    |  |
| Öl (200-320°)     |     |     |     | 72    |  |

Bemerkungen: *Arvinnol Paraffin*

000390

## Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 3.3.1.44 Zeit          Betr. Tage         

| Produkt         | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|-----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin     | 3,40         | 39,8           | 43,2                   | 33,1                                 | 33,8                  |
| Kondens.-Öl     | 3,50         | 42,7           | 53,7                   | 41,8                                 | 33,2                  |
| Paraffingatsch. | 3,30         | 38,1           | 34,2                   | 24,4                                 | 31,9                  |
| Ges.-Prod.      | 10,20        | 100,0          | 131,1                  | 100,0                                | 97,9                  |

| Kondens.-Prod.       | A K-Benzin | Ölkond.   | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|------------|-----------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,676      | 0,798     | 0,90                |                | 0,906                |
| Olefine „SPL“ Vol. % |            |           |                     |                |                      |
| Jodzahl (Wijss)      |            |           |                     |                |                      |
| N Z / V Z            | 105 / 387  | 119 / 231 |                     |                | 1104                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | — 40 °C     |        |        |        |        | 40     |        |
| 60 „          |             |        |        |        | 100    |        |        |
| 80 „          |             |        |        |        | 190    |        |        |
| 100 „         |             |        |        |        | 300    |        |        |
| 120 „         |             |        |        |        | 330    |        |        |
| 140 „         |             |        |        |        | 380    | 59,4   |        |
| 160 „         |             |        |        |        | 440    |        |        |
| 180 „         |             |        |        |        | 500    |        |        |
| 200 „         |             |        |        |        | 530    |        |        |
| 220 „         |             |        |        |        | 600    |        |        |
| 240 „         |             |        |        |        | 640    |        |        |
| 260 „         |             |        |        |        | 675    |        |        |
| 280 „         |             |        |        |        | 710    | 90,2   |        |
| 300 „         |             |        |        |        | 730    |        |        |
| 320 „         |             |        |        |        | 760    |        |        |
| 340 „         |             |        |        |        |        |        |        |
| 360 „         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 35,4   |
| Verlust       |             |        |        |        |        |        | 2,0    |

|                   |     |     |     |        |  |
|-------------------|-----|-----|-----|--------|--|
| Stockpunkt °C     |     |     |     |        |  |
| Destill.-Prod.    | SPL | N Z | V Z | Olefin |  |
| Benzin (bis 200°) |     |     |     | 45     |  |
| Öl (200–320°)     |     |     |     | 70     |  |

Bemerkungen: *benzines karott...*

000391

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 13.1.44 Zeit            Betr. Tage           

| Produkt       | Anfall<br>kg | Gewichts-<br>% / | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|---------------|--------------|------------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin   | 3,50         | 3,18             | 28,8                   | 32,9                                | 17,3                  |
| Kondens.-Öl   | 5,80         | 50,4             | 36,5                   | 52,2                                | 39,9                  |
| Paraffingtsch | 3,20         | 27,9             | 30,8                   | 24,4                                | 22,0                  |
| Ges.-Prod.    | 12,50        | 100,0            | 138,1                  | 100,0                               | 79,2                  |

| Kondens.-Prod.       | A K Benzin | Ölkond. | Paraffin-<br>gtsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|------------|---------|--------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,757      |         | 0,80               |                | 0,982                |
| Olefine „SPL“ Vol. % |            |         |                    |                |                      |
| Jodzahl (Wijss)      |            |         |                    |                |                      |
| N.Z. / V.Z.          | 8,1        | 13,21   |                    |                | 16,69                |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 4,3    |        |
| 60 "          |        |        |        |        | 0,0    |        |
| 80 "          |        |        |        |        | 7,0    |        |
| 100 "         |        |        |        |        | 31,0   |        |
| 120 "         |        |        |        |        | 36,0   |        |
| 140 "         |        |        |        |        | 32,0   | 50,3   |
| 160 "         |        |        |        |        | 41,0   |        |
| 180 "         |        |        |        |        | 42,0   |        |
| 200 "         |        |        |        |        | 44,0   |        |
| 220 "         |        |        |        |        | 47,5   |        |
| 240 "         |        |        |        |        | 22,0   |        |
| 260 "         |        |        |        |        | 52,0   | 13,0   |
| 280 "         |        |        |        |        | 50,0   |        |
| 300 "         |        |        |        |        | 52,0   |        |
| 320 "         |        |        |        |        | 53,5   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 26,2   |
| Verlust       |        |        |        |        |        | 0,9    |

|                   |     |      |      |  |       |  |
|-------------------|-----|------|------|--|-------|--|
| Stockpunkt °C     |     |      |      |  |       |  |
| Destill.-Prod.    | SPL | NZ   | VZ   |  |       |  |
| Benzin (bis 200°) |     | 9,39 | 18,6 |  | 26,99 |  |
| Öl (200-320°)     |     | 2,1  | 16,4 |  | 21    |  |

Bemerkungen: *holiness. per. in.*

000392

✓



DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 3.10.49 Zeit 11.14 Betr. Tage 1

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 2,80         | 24,1           | 35,1                   | 37,6                                | 19,0                  |
| Kondens.-Öl    | 5,70         | 49,2           | 61,2                   | 48,6                                | 38,8                  |
| Paraffingatsch | 2,10         | 18,2           | 30,3                   | 22,8                                | 30,9                  |
| Ges.-Prod.     | 10,60        | 100,0          | 127,7                  | 109,0                               | 88,7                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,688       | 0,798   | 0,88                |                | 0,994                |
| Olefine „SPL“/Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            | 284/298     | 119/242 |                     |                | 11,15                |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 4,3    |        |
| 60 "          |        |        |        |        | 7,0    |        |
| 80 "          |        |        |        |        | 16,0   |        |
| 100 "         |        |        |        |        | 31,0   |        |
| 120 "         |        |        |        |        | 36,0   | 51,6   |
| 140 "         |        |        |        |        | 33,0   |        |
| 160 "         |        |        |        |        | 43,0   |        |
| 180 "         |        |        |        |        | 50,0   |        |
| 200 "         |        |        |        |        | 55,0   |        |
| 220 "         |        |        |        |        | 60,0   |        |
| 240 "         |        |        |        |        | 65,0   |        |
| 260 "         |        |        |        |        | 69,5   | 33,5   |
| 280 "         |        |        |        |        | 72,5   |        |
| 300 "         |        |        |        |        | 76,5   |        |
| 320 "         |        |        |        |        | 78,5   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 24,3   |
| Verlust       |        |        |        |        |        | 0,6    |

|                   |     |     |     |  |    |      |
|-------------------|-----|-----|-----|--|----|------|
| Stockpunkt °C     |     |     |     |  |    | 24,3 |
| Destill.-Prod.    | SPL | N Z | V Z |  |    |      |
| Benzin (bis 200°) |     |     |     |  | 77 |      |
| Öl (200-320°)     |     |     |     |  | 72 |      |

Bemerkungen: *Residuum vers. zu* **000393**

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 30.11.1943 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 1,50         | 22,4           | 30,4                   | 35,8                                | 17,8                  |
| Kondens.-Öl    | 2,80         | 41,8           | 53,4                   | 41,7                                | 33,3                  |
| Paraffingatsch | 2,40         | 35,8           | 40,7                   | 30,5                                | 28,6                  |
| Ges.-Prod.     | 6,70         | 100,0          | 125,5                  | 100,0                               | 79,7                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.    | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,690       | 0,700      | 0,88                |                | 0,812                |
| Ölefine „SPL“ Vol. % |             |            |                     |                |                      |
| Jodzahl (Wijss)      |             |            |                     |                |                      |
| N Z / V Z            | 2154 / 2134 | 141 / 2348 |                     |                | 145                  |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. $\frac{v}{v}$ % | Vol. $\frac{v}{v}$ % | Vol. % | Vol. % | Gew. % |
|---------------|--------|----------------------|----------------------|--------|--------|--------|
| - 40 °C       |        |                      |                      |        | 4,8    |        |
| 60 "          |        |                      |                      |        | 5,0    |        |
| 80 "          |        |                      |                      |        | 13,0   |        |
| 100 "         |        |                      |                      |        | 12,0   |        |
| 120 "         |        |                      |                      |        | 20,0   |        |
| 140 "         |        |                      |                      |        | 31,0   | 2,5    |
| 160 "         |        |                      |                      |        | 37,0   |        |
| 180 "         |        |                      |                      |        | 43,0   |        |
| 200 "         |        |                      |                      |        | 48,0   |        |
| 220 "         |        |                      |                      |        | 54,0   |        |
| 240 "         |        |                      |                      |        | 59,0   |        |
| 260 "         |        |                      |                      |        | 65,0   | 2,4,0  |
| 280 "         |        |                      |                      |        | 68,0   |        |
| 300 "         |        |                      |                      |        | 70,5   |        |
| 320 "         |        |                      |                      |        |        |        |
| 340 "         |        |                      |                      |        |        |        |
| 360 "         |        |                      |                      |        |        |        |
| Siede-Ende °C |        |                      |                      |        |        |        |
| Rückstand     |        |                      |                      |        |        |        |
| Verlust       |        |                      |                      |        |        | 32,4   |

|                              |     |     |     |    |  |  |
|------------------------------|-----|-----|-----|----|--|--|
| Stockpunkt °C                |     |     |     |    |  |  |
| Destill.-Prod. $\frac{v}{v}$ | SPL | N Z | V Z |    |  |  |
| Benzin (bis 200°)            |     |     |     | Öl |  |  |
| Öl (200-320°)                |     |     |     |    |  |  |

Bemerkungen:

000394

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 27.11.42 Zeit 12.42 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 1.10         | 22.0           | 22.2                   | 85.1                                | 17.2                  |
| Kondens.-Öl    | 3.00         | 60.1           | 58                     | 9.2                                 | 26.9                  |
| Paraffingatsch | 0.90         | 19             | 20.1                   | 7.7                                 | 4.0                   |
| Ges.-Prod.     | 5.00         | 100.0          | 29.1                   | 100.0                               | 48.1                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.   | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|-----------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0.684       | 0.794     | 0.89                |                | 0.884                |
| Olefine „SPL“ Vol. % |             |           |                     |                |                      |
| Jodzahl (Wijss)      |             |           |                     |                |                      |
| N Z V Z              | 0.02 3.92   | 9.42 2.04 |                     |                | 9.84                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |  |
|---------------|-------------|--------|--------|--------|--------|--------|--------|--|
|               | 40 °C       |        |        |        |        |        |        |  |
|               | 60 "        |        |        |        |        |        |        |  |
|               | 80 "        |        |        |        |        |        |        |  |
|               | 100 "       |        |        |        |        |        |        |  |
|               | 120 "       |        |        |        |        |        |        |  |
|               | 140 "       |        |        |        |        |        |        |  |
|               | 160 "       |        |        |        |        |        |        |  |
|               | 180 "       |        |        |        |        |        |        |  |
|               | 200 "       |        |        |        |        |        |        |  |
|               | 220 "       |        |        |        |        |        |        |  |
|               | 240 "       |        |        |        |        |        |        |  |
|               | 260 "       |        |        |        |        |        |        |  |
|               | 280 "       |        |        |        |        |        |        |  |
|               | 300 "       |        |        |        |        |        |        |  |
|               | 320 "       |        |        |        |        |        |        |  |
| 340 "         |             |        |        |        |        |        |        |  |
| 360 "         |             |        |        |        |        |        |        |  |
| Siede-Ende °C |             |        |        |        |        |        |        |  |
| Rückstand     |             |        |        |        |        |        |        |  |
| Verlust       |             |        |        |        |        |        |        |  |

|                   |     |     |     |  |  |  |
|-------------------|-----|-----|-----|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |
| Öl (200-320°)     |     |     |     |  |  |  |

Bemerkungen: *Handwritten notes and signature*

**000395**

DVA

# Untersuchung der flüssigen Produkte

 Ofen Nr. 11 Füllung 13 Dat. 26.37.13.43 Zeit        Betr. Tage       

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 3,30         | 35,8           | 37,4                   | 39,6                                 | 39,4                  |
| Kondens.-Öl    | 4,10         | 46,1           | 57,6                   | 45,6                                 | 36,6                  |
| Paraffingatsch | 3,50         | 38,1           | 31,3                   | 34,8                                 | 35,3                  |
| Ges.-Prod.     | 10,90        | 100,0          | 36,3                   | 100,0                                | 29,3                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.   | Paraffin-<br>gatsch | Gesamt-Produkt |   | Reaktions-<br>wasser |
|----------------------|-------------|-----------|---------------------|----------------|---|----------------------|
| Dichte bei 20 °C     | 0,690       | 0,703     | 0,90                | =              | = | 0,779                |
| Olefine „SPL“ Vol. % |             |           |                     |                |   |                      |
| Jodzahl (Wijss)      |             |           |                     |                |   |                      |
| NZ / VZ              | 0,192/3,53  | 1,92/23,4 |                     |                |   | 10,6                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 „          |        |        |        |        | 4,1    |        |
| 80 „          |        |        |        |        | 6,0    |        |
| 100 „         |        |        |        |        | 16,0   |        |
| 120 „         |        |        |        |        | 30,0   |        |
| 140 „         |        |        |        |        | 50,0   |        |
| 160 „         |        |        |        |        | 52,0   | 50,1   |
| 180 „         |        |        |        |        | 49,0   |        |
| 200 „         |        |        |        |        | 47,0   |        |
| 220 „         |        |        |        |        | 53,0   |        |
| 240 „         |        |        |        |        | 59,0   |        |
| 260 „         |        |        |        |        | 62,0   |        |
| 280 „         |        |        |        |        | 55,0   | 33,2   |
| 300 „         |        |        |        |        | 60,0   |        |
| 320 „         |        |        |        |        | 62,0   |        |
| 340 „         |        |        |        |        | 2,5    |        |
| 360 „         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 26,3   |
| Verlust       |        |        |        |        |        | 0,8    |
| Stockpunkt °C |        |        |        |        |        |        |

| Destill.-Prod.    | SPL | NZ | VZ |        |
|-------------------|-----|----|----|--------|
| Benzin (bis 200°) |     |    |    | Ölbenz |
| Öl (200-320°)     |     |    |    | 2,5    |

 Bemerkungen: *Produkt paraffin*

000396

Untersuchung der flüssigen Produkte

Ofen-Nr. *11* Füllung *13* Dat. *14.11.1949* Zeit *10.49* Betr. Tage

| Produkt        | Anfall kg   | Gewichts-%   | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-------------|--------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | <i>2,40</i> | <i>36,1</i>  | <i>37,5</i>            | <i>29,5</i>                         | <i>2,03</i>           |
| Kondens.-Öl    | <i>4,30</i> | <i>45,2</i>  | <i>58,6</i>            | <i>4,27</i>                         | <i>3,57</i>           |
| Paraffingatsch | <i>2,60</i> | <i>28,3</i>  | <i>31,7</i>            | <i>3,29</i>                         | <i>2,21</i>           |
| Ges.-Prod.     | <i>9,30</i> | <i>100,0</i> | <i>128,0</i>           | <i>100,0</i>                        | <i>2,21</i>           |

| Kondens.-Prod.       | A.K. Benzin          | Ölkond.            | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|----------------------|--------------------|----------------|----------------|-----------------|
| Dichte bei 20° C     | <i>0,691</i>         | <i>0,780</i>       | <i>0,83</i>    |                | <i>0,26</i>     |
| Olefine „SPL“ Vol. % |                      |                    |                |                |                 |
| Jodzahl (Wijss)      |                      |                    |                |                |                 |
| N Z / V Z            | <i>0,054 / 2,899</i> | <i>12,5 / 22,6</i> |                |                | <i>12,5</i>     |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. %        | Gew. %      |
|---------------|--------|--------|--------|--------|---------------|-------------|
| 40 °C         |        |        |        |        | <i>44</i>     |             |
| 60 "          |        |        |        |        | <i>50</i>     |             |
| 80 "          |        |        |        |        | <i>50</i>     |             |
| 100 "         |        |        |        |        | <i>50,0</i>   |             |
| 120 "         |        |        |        |        | <i>55,0</i>   |             |
| 140 "         |        |        |        |        | <i>32,0,0</i> | <i>4,7</i>  |
| 160 "         |        |        |        |        | <i>41,0</i>   |             |
| 180 "         |        |        |        |        | <i>45,0</i>   |             |
| 200 "         |        |        |        |        | <i>52,0</i>   |             |
| 220 "         |        |        |        |        | <i>56,0</i>   |             |
| 240 "         |        |        |        |        | <i>61,0</i>   |             |
| 260 "         |        |        |        |        | <i>65,0</i>   | <i>3,3</i>  |
| 280 "         |        |        |        |        | <i>69,0</i>   |             |
| 300 "         |        |        |        |        | <i>74,0</i>   |             |
| 320 "         |        |        |        |        | <i>75,0</i>   |             |
| 340 "         |        |        |        |        |               |             |
| 360 "         |        |        |        |        |               |             |
| Siede-Ende °C |        |        |        |        |               |             |
| Rückstand     |        |        |        |        |               | <i>26,3</i> |
| Verlust       |        |        |        |        |               | <i>2,8</i>  |

| Stockpunkt °C | Destill.-Prod.    | SPL | N Z | V Z         |
|---------------|-------------------|-----|-----|-------------|
|               | Benzin (bis 200°) |     |     | <i>26,3</i> |
|               | Öl (200-320°)     |     |     | <i>2,8</i>  |

Bemerkungen: *...*

000397

DVA

# Untersuchung der flüssigen Produkte

 Ofen Nr. 11 Füllung 13 Dat. 22.24.24 Zeit 12.4 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,00         | 33,3           | 243                    | 272                                 | 18,5                  |
| Kondens.-Öl    | 3,00         | 44,3           | 150                    | 43,2                                | 35,0                  |
| Paraffingatsch | 2,00         | 22,5           | 100                    | 28,9                                | 25,7                  |
| Ges.-Prod.     | 8,00         | 100,0          | 180,3                  | 100,0                               | 29,3                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,680       | 0,732   | 0,719               |                |                      |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wjss)       |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

| Siedeanalyse      | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|-------------|--------|--------|--------|--------|--------|--------|
|                   | - 40 °C     |        |        |        |        | 2,0    |        |
|                   | 60 „        |        |        |        |        | 3,0    |        |
|                   | 80 „        |        |        |        |        | 4,0    |        |
|                   | 100 „       |        |        |        |        | 5,0    |        |
|                   | 120 „       |        |        |        |        | 6,0    |        |
|                   | 140 „       |        |        |        |        | 7,0    | 49,7   |
|                   | 160 „       |        |        |        |        | 8,0    |        |
|                   | 180 „       |        |        |        |        | 9,0    |        |
|                   | 200 „       |        |        |        |        | 10,0   |        |
|                   | 220 „       |        |        |        |        | 11,0   |        |
|                   | 240 „       |        |        |        |        | 12,0   |        |
|                   | 260 „       |        |        |        |        | 13,0   |        |
|                   | 280 „       |        |        |        |        | 14,0   |        |
|                   | 300 „       |        |        |        |        | 15,0   | 31,9   |
|                   | 320 „       |        |        |        |        | 16,0   |        |
| 340 „             |             |        |        |        | 17,0   |        |        |
| 360 „             |             |        |        |        | 18,0   |        |        |
| Siede-Ende °C     |             |        |        |        |        |        |        |
| Rückstand         |             |        |        |        |        |        | 3,9    |
| Verlust           |             |        |        |        |        |        | 1,4    |
| Stockpunkt °C     |             |        |        |        |        |        |        |
| Destill.-Prod.    | SPL         | N Z    | V Z    |        |        |        |        |
| Benzin (bis 200°) |             |        |        |        | 11,5   |        |        |
| Öl (200-320°)     |             |        |        |        | 7,5    |        |        |
|                   |             |        |        |        | 6,8    |        |        |

 Bemerkungen: *zusätzlich Paraffin*

000398

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 23.3.1945 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 2,10         | 24,0           | 249                    | 274                                 | 188                   |
| Kondens.-Öl    | 2,25         | 49,6           | 223                    | 488                                 | 29,3                  |
| Paraffingatsch | 2,40         | 37,4           | 224                    | 232                                 | 214                   |
| Ges.-Prod.     | 6,75         | 100,0          | 224                    | 100,0                               | 29,4                  |

| Kondens.-Prod.         | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|------------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C       | 0,684       | 0,781   | 0,90                |                |                      |
| Olefine „SPL“ Vol. %/n |             |         |                     |                | 0,986                |
| Jodzahl (Wijs)         |             |         |                     |                |                      |
| N Z / V Z              |             |         |                     |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |        |
| 80 "          |        |        |        |        |        |        |
| 100 "         |        |        |        |        |        |        |
| 120 "         |        |        |        |        |        |        |
| 140 "         |        |        |        |        |        |        |
| 160 "         |        |        |        |        |        |        |
| 180 "         |        |        |        |        |        |        |
| 200 "         |        |        |        |        |        |        |
| 220 "         |        |        |        |        |        |        |
| 240 "         |        |        |        |        |        |        |
| 260 "         |        |        |        |        |        |        |
| 280 "         |        |        |        |        |        |        |
| 300 "         |        |        |        |        |        |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 33,5   |

| Stöckpunkt °C | Destill.-Prod.    | SPL | N Z | V Z |
|---------------|-------------------|-----|-----|-----|
|               | Benzin (bis 200°) |     |     |     |
|               | Öl (200-320°)     |     |     |     |

Bemerkungen:

000399

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 31.12.1952 Zeit 10.00 Betr. Tage 1

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 1,10      | 39,0       | 40,7                   | 31,9                                | 33,0                  |
| Kondens.-Öl    | 1,50      | 46,7       | 158,6                  | 45,9                                | 36,8                  |
| Paraffingatsch | 1,50      | 35,3       | 51,1                   | 30,8                                | 19,9                  |
| Ges.-Prod.     | 2,50      | 100,0      | 134,4                  | 100,0                               | 29,7                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.     | Paraffin-gatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|-------------|-----------------|----------------|-----------------|
| Dichte bei 20 ° C    | 0,689       | 0,799       | 0,40            |                | 0,776           |
| Olefine „SPL“ Vol. % |             |             |                 |                |                 |
| Jodzahl (Wijss)      |             |             |                 |                |                 |
| N Z / V Z            | 0,32 / 3,66 | 1,49 / 2,06 |                 |                | 10,29           |

Siedeanalyse

| Siedebeginn        | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|--------------------|--------|--------|--------|--------|--------|--------|
| - 40 ° C           |        |        |        |        | 4,5    |        |
| 60 "               |        |        |        |        | 4,0    |        |
| 80 "               |        |        |        |        | 10,0   |        |
| 100 "              |        |        |        |        | 53,0   |        |
| 120 "              |        |        |        |        | 33,0   | 7,1    |
| 140 "              |        |        |        |        | 2,0    |        |
| 160 "              |        |        |        |        | 1,0    |        |
| 180 "              |        |        |        |        | 1,0    |        |
| 200 "              |        |        |        |        | 1,0    |        |
| 220 "              |        |        |        |        | 1,0    |        |
| 240 "              |        |        |        |        | 1,0    |        |
| 260 "              |        |        |        |        | 1,0    |        |
| 280 "              |        |        |        |        | 1,0    | 1,6    |
| 300 "              |        |        |        |        | 1,0    |        |
| 320 "              |        |        |        |        | 1,0    |        |
| 340 "              |        |        |        |        | 1,0    |        |
| 360 "              |        |        |        |        | 1,0    |        |
| Siede-Ende ° C     |        |        |        |        |        |        |
| Rückstand          |        |        |        |        |        |        |
| Verlust            |        |        |        |        |        | 0,4    |
| Stockpunkt ° C     |        |        |        |        |        |        |
| Destill.-Prod.     | SPL    | N Z    | V Z    |        |        |        |
| Benzin (bis 200 °) |        |        |        |        | 0,1    |        |
| Öl (200—320 °)     |        |        |        |        | 0,8    |        |

Bemerkungen: *Keine Analyse*

000400





DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 19.3.0.13.43 Zeit      Betr. Tage     

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 7,00      | 45,8       | 18,3                   | 110                                 | 34,2                  |
| Kondens.-Öl    | 5,30      | 34,6       | 43,8                   | 32,7                                | 25,8                  |
| Paraffingatsch | 3,00      | 19,6       | 21,8                   | 16,3                                | 14,6                  |
| Ges.-Prod.     | 15,30     | 100,0      | 133,9                  | 120,0                               | 74,6                  |

| Kondens.-Prod.       | A K-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,671      | 0,790   | 0,90           |                | 0,478           |
| Olefine „SPL“ Vol. % |            |         |                |                |                 |
| Jodzahl (Wijs)       |            |         |                |                |                 |
| N Z / V Z            | 1034/500   | 136/144 |                |                | 115/115         |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| 40 °C         |        |        |        |        | 22,0   |        |
| 60 "          |        |        |        |        | 30,0   |        |
| 80 "          |        |        |        |        | 31,0   |        |
| 100 "         |        |        |        |        | 30,0   |        |
| 120 "         |        |        |        |        | 46,0   | 13,8   |
| 140 "         |        |        |        |        | 52,0   |        |
| 160 "         |        |        |        |        | 57,0   |        |
| 180 "         |        |        |        |        | 64,0   |        |
| 200 "         |        |        |        |        | 68,0   |        |
| 220 "         |        |        |        |        | 71,0   |        |
| 240 "         |        |        |        |        | 74,0   |        |
| 260 "         |        |        |        |        | 76,0   |        |
| 280 "         |        |        |        |        | 78,0   |        |
| 300 "         |        |        |        |        | 78,0   |        |
| 320 "         |        |        |        |        | 80,5   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 18,8   |
| Verlust       |        |        |        |        |        | 3,7    |

|                   |     |     |     |     |  |  |
|-------------------|-----|-----|-----|-----|--|--|
| Stockpunkt °C     |     |     |     |     |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |     |  |  |
| Benzin (bis 200°) |     |     |     | 0,1 |  |  |
| Öl (200-320°)     |     |     |     | 68  |  |  |
|                   |     |     |     | 61  |  |  |

Bemerkungen: *gelbes Kristallin*

000402

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 18.19.13.43 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 3,10         | 36,9           | 54,0                   | 41,2                                 | 38,1                  |
| Kondens.-Öl    | 4,20         | 46,6           | 58,9                   | 44,7                                 | 37,4                  |
| Paraffingatsch | 1,70         | 16,5           | 18,5                   | 14,1                                 | 12,5                  |
| Ges.-Prod.     | 9,00         | 100,0          | 131,6                  | 100,0                                | 76,0                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.   | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|-----------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,682       | 0,791     | 0,89                |                | 0,782                |
| Oletine „SPL“ Vol. % |             |           |                     |                |                      |
| Jodzahl (Wijs)       |             |           |                     |                |                      |
| N Z / V Z            | 104 / 354   | 758 / 123 |                     |                | 813 / 813            |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        |        | 2,0    |
| 60 "          |             |        |        |        |        | 10,0   |        |
| 80 "          |             |        |        |        |        | 23,0   |        |
| 100 "         |             |        |        |        |        | 20,0   |        |
| 120 "         |             |        |        |        |        | 22,0   |        |
| 140 "         |             |        |        |        |        | 43,0   | 62,7   |
| 160 "         |             |        |        |        |        | 5,0    |        |
| 180 "         |             |        |        |        |        | 61,0   |        |
| 200 "         |             |        |        |        |        | 67,0   |        |
| 220 "         |             |        |        |        |        | 71,0   |        |
| 240 "         |             |        |        |        |        | 75,0   |        |
| 260 "         |             |        |        |        |        | 78,0   | 18,6   |
| 280 "         |             |        |        |        |        | 81,0   |        |
| 300 "         |             |        |        |        |        | 83,0   |        |
| 320 "         |             |        |        |        |        | 85,0   |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 16,3   |
| Verlust       |             |        |        |        |        |        | 1,4    |

| Stöckpunkt °C | Destill.-Prod.    | SPL | N Z | V Z |             |
|---------------|-------------------|-----|-----|-----|-------------|
|               | Benzin (bis 200°) |     |     |     | 0,1 bis 7,1 |
|               | Öl (200-320°)     |     |     |     | 6,2         |

Bemerkungen: *Yellow's paraffin* 000403

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 17.10.18 Zeit 43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 5,50      | 33,4       | 49,5                   | 33,5                                 | 25,4                  |
| Kondens.-Öl    | 8,00      | 49,4       | 61,8                   | 46,8                                 | 36,6                  |
| Paraffingatsch | 3,00      | 18,2       | 30,7                   | 15,7                                 | 13,8                  |
| Ges.-Prod.     | 16,50     | 100,0      | 132,0                  | 100,0                                | 75,8                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.     | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|-------------|----------------|----------------|-----------------|
| Dichte bei 20 °C     | 0,67        | 0,783       | 0,88           |                | 0,924           |
| Olefine „SPL“ Vol. % |             |             |                |                |                 |
| Jodzahl (Wijs)       |             |             |                |                |                 |
| N Z / V Z            | 0,12 / 2,71 | 9,00 / 8,16 |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        |        |        |
| 60 "          |        |        |        |        | 3,7    |        |
| 80 "          |        |        |        |        | 11,0   |        |
| 100 "         |        |        |        |        | 33,0   |        |
| 120 "         |        |        |        |        | 31,0   |        |
| 140 "         |        |        |        |        | 30,0   |        |
| 160 "         |        |        |        |        | 26,0   | 61,6   |
| 180 "         |        |        |        |        | 2,0    |        |
| 200 "         |        |        |        |        | 2,0    |        |
| 220 "         |        |        |        |        | 65,0   |        |
| 240 "         |        |        |        |        | 20,0   |        |
| 260 "         |        |        |        |        | 24,0   |        |
| 280 "         |        |        |        |        | 22,0   | 18,5   |
| 300 "         |        |        |        |        | 2,0    |        |
| 320 "         |        |        |        |        | 1,0    |        |
| 340 "         |        |        |        |        | 1,0    |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        |        |
| Verlust       |        |        |        |        |        | 19,3   |

| Stockpunkt °C     |     |     |      |
|-------------------|-----|-----|------|
| Destill.-Prod.    | SPL | N Z | V Z  |
| Benzin (bis 200°) |     |     | 0,12 |
| Öl (200-320°)     |     |     | 6,8  |

Bemerkungen: *Opfer Paraffin* 000404

# Untersuchung der flüssigen Produkte

Ofen-Nr. 11 Füllung 13 Dat. 16. 17. 19. 43 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 5,80         | 33,6           | 49,3                   | 37,9                                 | 35,8                  |
| Kondens.-Öl    | 7,30         | 41,4           | 54,6                   | 40,5                                 | 31,9                  |
| Paraffingatsch | 4,35         | 23,0           | 38,1                   | 24,6                                 | 10,2                  |
| Ges.-Prod.     | 17,40        | 100,0          | 120,0                  | 100,0                                | 76,9                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,681       | 0,788   | 0,80                |                | 0,786                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            | 55          | 59      | 99                  |                | 87 / 96              |

| Siedeanalyse  | Siedebeginn |        | Vol. % |        |        |        | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | Vol. %      | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % |        |
|               |             |        |        |        |        | 34,0   |        |
| 40 °C         |             |        |        |        |        | 1,0    |        |
| 60 "          |             |        |        |        |        | 10,0   |        |
| 80 "          |             |        |        |        |        | 23,0   |        |
| 100 "         |             |        |        |        |        | 38,0   |        |
| 120 "         |             |        |        |        |        | 34,0   | 54,7   |
| 140 "         |             |        |        |        |        | 40,0   | 4,7    |
| 160 "         |             |        |        |        |        | 40,0   |        |
| 180 "         |             |        |        |        |        | 40,0   |        |
| 200 "         |             |        |        |        |        | 43,0   |        |
| 220 "         |             |        |        |        |        | 58,0   |        |
| 240 "         |             |        |        |        |        | 63,0   |        |
| 260 "         |             |        |        |        |        | 67,0   |        |
| 280 "         |             |        |        |        |        | 71,0   |        |
| 300 "         |             |        |        |        |        | 75,0   | 21,3   |
| 320 "         |             |        |        |        |        | 77,0   |        |
| 340 "         |             |        |        |        |        | 79,0   |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 23,4   |
| Verlust       |             |        |        |        |        |        | 1,6    |

| Stockpunkt °C     | SPL | N Z | V Z | Öl |
|-------------------|-----|-----|-----|----|
| Destill.-Prod.    |     |     |     | Öl |
| Benzin (bis 200°) |     |     |     | 70 |
| Öl (200-320°)     |     |     |     | 60 |

Bemerkungen: *Paraffin* 000405

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 15.16.18.42 Zeit 2 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 8,90      | 38,9       | 55,7                   | 43,6                                 | 30,5                  |
| Kondens.-Öl    | 1,95      | 8,2        | 32,3                   | 8,3                                  | 20,5                  |
| Paraffingatsch | 3,60      | 34,9       | 39,7                   | 31,1                                 | 37,4                  |
| Ges.-Prod.     | 2,45      | 100,0      | 19,2                   | 100,0                                | 27,4                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.      | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|--------------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,700       | 0,810        | 0,88           |                | 0,987           |
| Olefine „SPL“ Vol. % |             |              |                |                |                 |
| Jodzahl (Wijss)      |             |              |                |                |                 |
| N Z / V Z            | 0,64 / 3,07 | 22,77 / 24,4 |                |                | 16,5 / 16,65    |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 35     |        |
| 60 "          |        |        |        |        | 90     |        |
| 80 "          |        |        |        |        | 16,0   |        |
| 100 "         |        |        |        |        | 63,0   |        |
| 120 "         |        |        |        |        | 37,0   |        |
| 140 "         |        |        |        |        | 23,0   | 46,8   |
| 160 "         |        |        |        |        | 29,0   |        |
| 180 "         |        |        |        |        | 44,0   |        |
| 200 "         |        |        |        |        | 50,0   |        |
| 220 "         |        |        |        |        | 54,0   |        |
| 240 "         |        |        |        |        | 58,0   |        |
| 260 "         |        |        |        |        | 63,0   | 30,2   |
| 280 "         |        |        |        |        | 66,0   |        |
| 300 "         |        |        |        |        | 82,5   |        |
| 320 "         |        |        |        |        |        |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 31,3   |
| Verlust       |        |        |        |        |        | 0,7    |

| Stockpunkt °C     | SPL | N Z | V Z    |
|-------------------|-----|-----|--------|
| Destill.-Prod.    |     |     |        |
| Benzin (bis 200°) |     |     | Diälin |
| Öl (200-320°)     |     |     | 71     |
|                   |     |     | 75     |

Bemerkungen: *kein Paraffin*

000406

DVA

# Untersuchung der flüssigen Produkte

Öfen Nr. 11 Füllung 13 Dat. 14.15.1943 Zeit 12 Betr. Tage

| P r o d u k t  | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 2,60         | 34,6           | 49,6                   | 39,1                                | 33,3                  |
| Kondens.-Öl    | 3,10         | 38,0           | 34,7                   | 37,4                                | 32,1                  |
| Paraffingatsch | 2,80         | 37,4           | 42,5                   | 32,5                                | 32,5                  |
| Ges.-Prod.     | 7,50         | 100,0          | 42,2                   | 100,0                               | 32,9                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.     | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|-------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,699       | 0,800       | 0,89                |                | 0,99                 |
| Olefine „SPL“ Vol. % |             |             |                     |                |                      |
| Jodzahl (Wijss)      |             |             |                     |                |                      |
| N Z / V Z            | 320 / 328   | 1941 / 1994 |                     |                | 184 / 187            |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| — 40 °C       |        |        |        |        | 32     |        |
| 60 „          |        |        |        |        | 30     |        |
| 80 „          |        |        |        |        | 14,0   |        |
| 100 „         |        |        |        |        | 18,0   |        |
| 120 „         |        |        |        |        | 32,0   |        |
| 140 „         |        |        |        |        | 32,0   | 41,4   |
| 160 „         |        |        |        |        | 34,0   |        |
| 180 „         |        |        |        |        | 40,0   |        |
| 200 „         |        |        |        |        | 45,0   |        |
| 220 „         |        |        |        |        | 50,0   |        |
| 240 „         |        |        |        |        | 55,0   |        |
| 260 „         |        |        |        |        | 59,0   |        |
| 280 „         |        |        |        |        | 62,0   | 33,6   |
| 300 „         |        |        |        |        | 65,0   |        |
| 320 „         |        |        |        |        | 70,0   |        |
| 340 „         |        |        |        |        | 70,0   |        |
| 360 „         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 33,1   |
| Verlust       |        |        |        |        |        | 3,9    |

|                   |     |     |     |    |  |
|-------------------|-----|-----|-----|----|--|
| Stockpunkt °C     |     |     |     |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |    |  |
| Benzin (bis 200°) |     |     |     | 23 |  |
| Öl (200–320°)     |     |     |     | 21 |  |

Bemerkungen: *Prozessparaffin*

000407

Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 13.14.1942 Zeit Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 0,90      | 32,1       | 44,2                   | 35,8                                | 26,1                  |
| Kondens.-Öl    | 0,90      | 32,1       | 39,5                   | 32,0                                | 26,0                  |
| Paraffingatsch | 1,00      | 35,8       | 39,8                   | 32,2                                | 23,0                  |
| Ges.-Prod.     | 2,80      | 100,0      | 123,5                  | 100,0                               | 81,1                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
|                      |             |         |                |                |                 |
| Dichte bei 20° C     | 0,729       | 0,813   | 0,90           |                | 0,998           |
| Oleline „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijs)       |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 1,3    |        |
| 60 "          |        |        |        |        | 1,0    |        |
| 80 "          |        |        |        |        | 8,0    |        |
| 100 "         |        |        |        |        | 11,2   |        |
| 120 "         |        |        |        |        | 15,0   |        |
| 140 "         |        |        |        |        | 22,0   | 37,2   |
| 160 "         |        |        |        |        | 30,0   |        |
| 180 "         |        |        |        |        | 27,0   |        |
| 200 "         |        |        |        |        | 43,0   |        |
| 220 "         |        |        |        |        | 45,0   |        |
| 240 "         |        |        |        |        | 52,0   |        |
| 260 "         |        |        |        |        | 50,0   |        |
| 280 "         |        |        |        |        | 64,0   | 30,2   |
| 300 "         |        |        |        |        | 59,0   |        |
| 320 "         |        |        |        |        | 23,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 31,4   |
| Verlust       |        |        |        |        |        | 0,7    |

| Stockpunkt °C | Destill.-Prod.    | SPL | N Z | V Z |      |
|---------------|-------------------|-----|-----|-----|------|
|               |                   |     |     |     |      |
|               | Benzin (bis 200°) |     |     |     | 0,01 |
|               | Öl (200-320°)     |     |     |     | 73   |
|               |                   |     |     |     | 71   |

Bemerkungen: *Spezial Paraffin*

000408



DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 12.12.13 Zeit 42 Betr. Tage

| Produkt        | Anfall-kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 1,35      | 42,9       | 94                     | 43,0                                | 33,9                  |
| Kondens.-Öl    | 0,80      | 25,3       | 31,8                   | 34,2                                | 30,1                  |
| Paraffingatsch | 1,00      | 31,8       | 35,2                   | 39,3                                | 35,3                  |
| Ges.-Prod.     | 3,15      | 100,0      | 36,3                   | 40,0                                | 44,2                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,722       | 0,818   | 0,89           |                | 1,000           |
| Oleline „SPL“-Vol.-% |             |         |                |                |                 |
| Jodzahl (Wijss)      |             |         |                |                |                 |
| N Z / V Z            |             |         |                |                |                 |

| Siedeanalyse        | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |      |
|---------------------|-------------|--------|--------|--------|--------|--------|--------|------|
|                     | — 40 °C     |        |        |        |        |        | 2,8    |      |
|                     | 60 "        |        |        |        |        |        | 3,0    |      |
|                     | 80 "        |        |        |        |        |        | 3,1    |      |
|                     | 100 "       |        |        |        |        |        | 3,2    |      |
|                     | 120 "       |        |        |        |        |        | 3,3    |      |
|                     | 140 "       |        |        |        |        |        | 3,4    | 45,2 |
|                     | 160 "       |        |        |        |        |        | 3,5    |      |
|                     | 180 "       |        |        |        |        |        | 3,6    |      |
|                     | 200 "       |        |        |        |        |        | 3,7    |      |
|                     | 220 "       |        |        |        |        |        | 3,8    |      |
|                     | 240 "       |        |        |        |        |        | 3,9    |      |
|                     | 260 "       |        |        |        |        |        | 4,0    |      |
|                     | 280 "       |        |        |        |        |        | 4,1    | 31,9 |
|                     | 300 "       |        |        |        |        |        | 4,2    |      |
| 320 "               |             |        |        |        |        | 4,3    |        |      |
| 340 "               |             |        |        |        |        | 4,4    |        |      |
| 360 "               |             |        |        |        |        | 4,5    |        |      |
| Siede-Ende °C       |             |        |        |        |        |        |        |      |
| Rückstand           |             |        |        |        |        |        | 30,5   |      |
| Verlust             |             |        |        |        |        |        | 0,0    |      |
| Stockpunkt °C       |             |        |        |        |        |        |        |      |
| Destill.-Prod.      | SPL         | N Z    | V Z    |        |        |        |        |      |
| % Benzin (bis 200°) |             |        |        |        |        | 40     |        |      |
| Öl (200—320°)       |             |        |        |        |        | 22     |        |      |

Bemerkungen: 000409

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 · Füllung 13      Dat. 11.13.13 Zeit 43      Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100cm <sup>3</sup> |
|----------------|--------------|----------------|-----------------------|-------------------------------------|----------------------|
| A.K.-Benzin    | 3,80         | 42,7           | 61,7                  | 47,6                                | 39,0                 |
| Kondens.-Öl    | 3,30         | 35,9           | 31,1                  | 34,8                                | 30,0                 |
| Paraffingatsch | 1,20         | 13,4           | 35,7                  | 37,6                                | 34,3                 |
| Ges.-Prod.     | 8,40         | 100,0          | 139,5                 | 100,0                               | 74,3                 |

| Kondens.-Prod.       | A.K. Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,694       | 0,806   | 0,80                |                | 0,996                |
| Öleffne „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z V Z              |             |         |                     |                |                      |

| Siedeanalyse      | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|-------------|--------|--------|--------|--------|--------|--------|
|                   | 40 °C       |        |        |        |        | 3,0    |        |
|                   | 60 "        |        |        |        |        | 13,0   |        |
|                   | 80 "        |        |        |        |        | 18,0   |        |
|                   | 100 "       |        |        |        |        | 34,0   |        |
|                   | 120 "       |        |        |        |        | 30,0   | 50,0   |
|                   | 140 "       |        |        |        |        | 30,0   |        |
|                   | 160 "       |        |        |        |        | 43,0   |        |
|                   | 180 "       |        |        |        |        | 40,0   |        |
|                   | 200 "       |        |        |        |        | 52,0   |        |
|                   | 220 "       |        |        |        |        | 50,0   |        |
|                   | 240 "       |        |        |        |        | 52,0   |        |
|                   | 260 "       |        |        |        |        | 66,0   | 19,6   |
|                   | 280 "       |        |        |        |        | 70,0   |        |
|                   | 300 "       |        |        |        |        | 78,0   |        |
| 320 "             |             |        |        |        | 40     |        |        |
| 340 "             |             |        |        |        |        |        |        |
| 360 "             |             |        |        |        |        |        |        |
| Siede-Ende °C     |             |        |        |        |        |        |        |
| Rückstand         |             |        |        |        |        |        | 38,0   |
| Verlust           |             |        |        |        |        |        | 3,4    |
| Stockpunkt °C     |             |        |        |        |        |        |        |
| Destill.-Prod.    | SPL         | N Z    | V Z    |        |        |        |        |
| Benzin (bis 200°) |             |        |        |        |        |        |        |
| Öl (200–320°)     |             |        |        |        |        |        |        |

Bemerkungen: Leeres Karabin      000410

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 10.11.13 Zeit 43 Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,70      | 43,5       | 60,8                   | 46,9                                | 33,8                  |
| Kondens.-Öl    | 1,65      | 36,0       | 31,9                   | 24,7                                | 20,1                  |
| Paraffingatsch | 3,00      | 37,5       | 36,7                   | 38,4                                | 24,4                  |
| Ges.-Prod.     | 8,35      | 100,0      | 133,4                  | 100,0                               | 48,3                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|---------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,700       | 0,914   | 0,86           |                | 0,998           |
| Olefine „SPL“ Vol. % |             |         |                |                |                 |
| Jodzahl (Wijs)       |             |         |                |                |                 |
| N.Z. / V.Z.          |             |         |                |                |                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        | 26,0   |        |
|               | 60 „        |        |        |        |        | 12,0   |        |
|               | 80 „        |        |        |        |        | 12,0   |        |
|               | 100 „       |        |        |        |        | 31,0   |        |
|               | 120 „       |        |        |        |        | 32,0   |        |
|               | 140 „       |        |        |        |        | 34,0   | 40,3   |
|               | 160 „       |        |        |        |        | 41,0   |        |
|               | 180 „       |        |        |        |        | 42,0   |        |
|               | 200 „       |        |        |        |        | 52,0   |        |
|               | 220 „       |        |        |        |        | 57,0   |        |
|               | 240 „       |        |        |        |        | 61,0   |        |
|               | 260 „       |        |        |        |        | 65,0   |        |
|               | 280 „       |        |        |        |        | 68,0   | 21,1   |
|               | 300 „       |        |        |        |        | 71,0   |        |
| 320 „         |             |        |        |        | 76,0   |        |        |
| 340 „         |             |        |        |        |        |        |        |
| 360 „         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 37,5   |
| Verlust       |             |        |        |        |        |        | 1,7    |

|                   |     |     |     |  |  |  |  |
|-------------------|-----|-----|-----|--|--|--|--|
| Stockpunkt °C     |     |     |     |  |  |  |  |
| Desfill.-Prod.    | SPL | N Z | V Z |  |  |  |  |
| Benzin (bis 200°) |     |     |     |  |  |  |  |
| Öl (200-320°)     |     |     |     |  |  |  |  |

Bemerkungen: hoheres Paraffin 000411

DVA

# Untersuchung der flüssigen-Produkte

Ofen Nr. M Füllung 13 Dat. 9.10.13. Zeit 43 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 3,30         | 36,7           | 53,2                   | 41,0                                 | 38,4                  |
| Kondens.-Öl    | 3,10         | 34,5           | 49,8                   | 33,3                                 | 36,8                  |
| Paraffingutsch | 2,60         | 28,8           | 33,1                   | 25,8                                 | 33,5                  |
| Ges.-Prod.     | 9,00         | 100,0          | 38,2                   | 100,0                                | 34,7                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gutsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20°C      | 0,68        | 0,706   | 0,72                |                | 0,71                 |
| Oleline „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            |             |         |                     |                |                      |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |  |
|---------------|-------------|--------|--------|--------|--------|--------|--------|--|
|               | — 40 °C     |        |        |        |        | 31     |        |  |
|               | 60 "        |        |        |        |        | 18,0   |        |  |
|               | 80 "        |        |        |        |        | 18,0   |        |  |
|               | 100 "       |        |        |        |        | 33,0   |        |  |
|               | 120 "       |        |        |        |        | 25,0   |        |  |
|               | 140 "       |        |        |        |        | 24,0   | 4,2    |  |
|               | 160 "       |        |        |        |        | 33,0   |        |  |
|               | 180 "       |        |        |        |        | 45,0   |        |  |
|               | 200 "       |        |        |        |        | 50,0   |        |  |
|               | 220 "       |        |        |        |        | 50,0   |        |  |
|               | 240 "       |        |        |        |        | 50,0   |        |  |
|               | 260 "       |        |        |        |        | 17,0   | 38,1   |  |
|               | 280 "       |        |        |        |        | 23,0   |        |  |
|               | 300 "       |        |        |        |        | 20,0   |        |  |
| 320 "         |             |        |        |        | 20,0   |        |        |  |
| 340 "         |             |        |        |        |        |        |        |  |
| 360 "         |             |        |        |        |        |        |        |  |
| Siede-Ende °C |             |        |        |        |        |        |        |  |
| Rückstand     |             |        |        |        |        |        | 34,3   |  |
| Verlust       |             |        |        |        |        |        | 3,4    |  |

|                   |     |     |     |  |    |  |
|-------------------|-----|-----|-----|--|----|--|
| Stockpunkt °C     |     |     |     |  |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |    |  |
| Benzin (bis 200°) |     |     |     |  | 73 |  |
| Öl (200—320°)     |     |     |     |  | 70 |  |

**Bemerkungen:** 000412

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 14 Dat. 29. 30. 1. 44 Zeit      Betr. Tage     

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    |              |                |                        |                                      |                       |
| Kondens.-Öl    |              |                |                        |                                      |                       |
| Paraffingatsch |              |                |                        |                                      |                       |
| Ges.-Prod.     |              |                |                        |                                      |                       |

| Kondens.-Prod.          | A.K.-Benzin | Ölkond.           | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|-------------------------|-------------|-------------------|---------------------|----------------|----------------------|
| Dichte bei 20° C        |             |                   |                     |                |                      |
| Olefine „SPL“ Vol. %/10 |             |                   |                     |                |                      |
| Jodzahl (Wijss)         |             |                   |                     |                |                      |
| N Z / V Z               |             | <u>368 / 1168</u> |                     |                | <u>0,969</u>         |

**Siedeanalyse**

| Siedebeginn       | Vol. % | Vol. %       | Vol. % | Vol. % | Vol. %      | Gew. %       |
|-------------------|--------|--------------|--------|--------|-------------|--------------|
| - 40 °C           |        | <u>0,293</u> |        |        |             | <u>0,991</u> |
| 60 "              |        |              |        |        |             |              |
| 80 "              |        |              |        |        |             |              |
| 100 "             |        |              |        |        |             |              |
| 120 "             |        |              |        |        | <u>3,0</u>  |              |
| 140 "             |        |              |        |        | <u>5,0</u>  |              |
| 160 "             |        |              |        |        | <u>6,0</u>  |              |
| 180 "             |        |              |        |        | <u>8,0</u>  |              |
| 200 "             |        |              |        |        | <u>12,0</u> |              |
| 220 "             |        |              |        |        | <u>31,0</u> | <u>81,0</u>  |
| 240 "             |        |              |        |        | <u>46,0</u> |              |
| 260 "             |        |              |        |        | <u>5,0</u>  |              |
| 280 "             |        |              |        |        | <u>66,0</u> |              |
| 300 "             |        |              |        |        | <u>74,0</u> |              |
| 320 "             |        |              |        |        | <u>81,0</u> |              |
| 340 "             |        |              |        |        |             |              |
| 360 "             |        |              |        |        |             |              |
| Siede-Ende °C     |        |              |        |        |             |              |
| Rückstand         |        |              |        |        |             | <u>18,9</u>  |
| Verlust           |        |              |        |        |             | <u>0,1</u>   |
| Stockpunkt °C     |        |              |        |        |             |              |
| Destill.-Prod.    | SPL    | N Z          | V Z    |        |             |              |
| Benzin (bis 200°) |        |              |        |        | <u>0,11</u> |              |
| Öl (200-320°)     |        |              |        |        | <u>6,8</u>  |              |

Bemerkungen:

000413

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 23.24.1944 Zeit            Betr. Tage 1

| Produkt        | Anfall<br>kg | Gewichts-<br>% <sub>o</sub> | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|-----------------------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 5,05         | 34,4                        | 51,0                   | 38,7                                | 80,1                  |
| Kondens.-Öl    | 6,65         | 45,2                        | 57,2                   | 43,4                                | 34,4                  |
| Paraffingatsch | 3,00         | 20,4                        | 23,5                   | 12,9                                | 15,6                  |
| Ges.-Prod.     | 14,70        | 100,0                       | 131,7                  | 100,0                               | 110,1                 |

| Kondens.-Prod.                    | A.K.-Benzin | Ölkond.    | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|-----------------------------------|-------------|------------|---------------------|----------------|----------------------|
| Dichte bei 20° C                  | 0,625       | 0,792      | 0,82                |                | 0,995                |
| Olefine „SPL“ Vol. % <sub>o</sub> |             |            |                     |                |                      |
| Jodzahl (Wijss)                   |             |            |                     |                |                      |
| N Z / V Z                         | 215 / 352   | 625 / 1195 |                     |                | 1625                 |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 0,0    |        |
| 60 "          |        |        |        |        | 13,0   |        |
| 80 "          |        |        |        |        | 5,0    |        |
| 100 "         |        |        |        |        | 20,0   |        |
| 120 "         |        |        |        |        | 37,0   |        |
| 140 "         |        |        |        |        | 42,0   | 59,3   |
| 160 "         |        |        |        |        | 37,0   |        |
| 180 "         |        |        |        |        | 37,0   |        |
| 200 "         |        |        |        |        | 60,0   |        |
| 220 "         |        |        |        |        | 40     |        |
| 240 "         |        |        |        |        | 80,0   |        |
| 260 "         |        |        |        |        | 20,0   |        |
| 280 "         |        |        |        |        | 25,0   | 19,6   |
| 300 "         |        |        |        |        | 27,5   |        |
| 320 "         |        |        |        |        | 20,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 18,7   |
| Verlust       |        |        |        |        |        | 13,3   |

| Stockpunkt °C     | SPL | N Z | V Z | Ölwert |
|-------------------|-----|-----|-----|--------|
| Destill.-Prod.    |     |     |     |        |
| Benzin (bis 200°) |     |     |     | 71     |
| Öl (200-320°)     |     |     |     | 61     |

Bemerkungen: *hellgelb karaffin*

000414

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 22.23.144 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 5,20         | 33,2           | 50,3                   | 38,2                                 | 25,6                  |
| Kondens.-Öl    | 6,80         | 44,3           | 55,8                   | 42,4                                 | 33,6                  |
| Paraffingatsch | 3,40         | 22,1           | 35,5                   | 16,2                                 | 16,9                  |
| Ges.-Prod.     | 15,40        | 100,0          | 131,6                  | 100,0                                | 76,1                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.      | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|--------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,670       | 0,792        | 0,813               |                | 0,922                |
| Olefine „SPL“ Vol. % |             |              |                     |                |                      |
| Jodzahl (Wijss)      |             |              |                     |                |                      |
| N Z / V Z -          | 0,59 / 3,40 | 6,10 / 21,81 |                     |                | 6,53                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | - 40 °C     |        |        |        |        |        | 2,8    |
| 60 "          |             |        |        |        |        | 10,0   |        |
| 80 "          |             |        |        |        |        | 22,0   |        |
| 100 "         |             |        |        |        |        | 31,0   |        |
| 120 "         |             |        |        |        |        | 40,0   | 56,8   |
| 140 "         |             |        |        |        |        | 47,0   |        |
| 160 "         |             |        |        |        |        | 49,0   |        |
| 180 "         |             |        |        |        |        | 55,0   |        |
| 200 "         |             |        |        |        |        | 61,0   |        |
| 220 "         |             |        |        |        |        | 65,0   |        |
| 240 "         |             |        |        |        |        | 68,0   |        |
| 260 "         |             |        |        |        |        | 70,0   | 32,1   |
| 280 "         |             |        |        |        |        | 74,0   |        |
| 300 "         |             |        |        |        |        | 75,0   |        |
| 320 "         |             |        |        |        |        | 77,5   |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        |        | 20,5   |
| Verlust       |             |        |        |        |        |        | 8,6    |

|                   |     |     |     |  |    |  |
|-------------------|-----|-----|-----|--|----|--|
| Stockpunkt °C     |     |     |     |  |    |  |
| Destill.-Prod.    | SPL | N Z | V Z |  |    |  |
| Benzin (bis 200°) |     |     |     |  | 73 |  |
| Öl (200—320°)     |     |     |     |  | 64 |  |

Bemerkungen: *beim Paraffin* 000415

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 21.2.1.44 Zeit 2 Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 2,80         | 22,5           | 33,5                   | 26,0                                | 17,5                  |
| Kondens.-Öl    | 6,60         | 52,7           | 67,0                   | 51,9                                | 40,8                  |
| Paraffingatsch | 3,10         | 24,8           | 38,5                   | 32,1                                | 19,2                  |
| Ges.-Prod.     | 12,50        | 100,0          | 129,0                  | 100,0                               | 77,5                  |

| Kondens.-Prod.       | A K-Benzin | Ölkond.    | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|------------|------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,674      | 0,788      | 0,82                |                | 0,983                |
| Olefine „SPL“ Vol. % |            |            |                     |                |                      |
| Jodzahl (Wijss)      |            |            |                     |                |                      |
| N Z / V Z            | 0187 / 331 | 631 / 1968 |                     |                | 694                  |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|-------------|--------|--------|--------|--------|--------|--------|
|               | — 40 °C     |        |        |        |        | 36     |        |
|               | 60 "        |        |        |        |        | 40     |        |
|               | 80 "        |        |        |        |        | 18,0   |        |
|               | 100 "       |        |        |        |        | 32,0   |        |
|               | 120 "       |        |        |        |        | 35,0   |        |
|               | 140 "       |        |        |        |        | 53,4   |        |
|               | 160 "       |        |        |        |        | 42,0   |        |
|               | 180 "       |        |        |        |        | 42,0   |        |
|               | 200 "       |        |        |        |        | 54,0   |        |
|               | 220 "       |        |        |        |        | 59,5   |        |
|               | 240 "       |        |        |        |        | 65,0   |        |
|               | 260 "       |        |        |        |        | 68,5   | 35,1   |
|               | 280 "       |        |        |        |        | 72,0   |        |
|               | 300 "       |        |        |        |        | 75,5   |        |
| 320 "         |             |        |        |        | 79,0   |        |        |
| 340 "         |             |        |        |        |        |        |        |
| 360 "         |             |        |        |        |        |        |        |
| Siede-Ende °C |             |        |        |        |        |        |        |
| Rückstand     |             |        |        |        |        | 30,7   |        |
| Verlust       |             |        |        |        |        | 1,8    |        |

|                   |     |     |     |    |  |  |
|-------------------|-----|-----|-----|----|--|--|
| Stockpunkt °C     |     |     |     |    |  |  |
| Destill.-Prod.    | SPL | N Z | V Z |    |  |  |
| Benzin (bis 200°) |     |     |     | Öl |  |  |
| Öl (200—320°)     |     |     |     | 73 |  |  |
|                   |     |     |     | 64 |  |  |

Bemerkungen:

000416



# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 20.21.1.44 Zeit            Betr. Tage           

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,50      | 31,6       | 47,1                   | 36,1                                | 34,2                  |
| Kondens.-Öl    | 6,05      | 43,4       | 53,2                   | 40,8                                | 32,5                  |
| Paraffingatsch | 3,20      | 23,0       | 30,2                   | 23,1                                | 19,9                  |
| Ges.-Prod.     | 14,25     | 100,0      | 130,5                  | 100,0                               | 26,6                  |

| Kondens.-Prod.       | A K Benzin  | Ölkond.     | Paraffin-gatsch | Gesamt-Produkt | Reaktions-wasser |
|----------------------|-------------|-------------|-----------------|----------------|------------------|
| Dichte bei 20° C     | 0,671       | 0,796       | 0,86            |                | 0,993            |
| Olefine „SPL“ Vol. % |             |             |                 |                |                  |
| Jodzahl (Wjss.)      |             |             |                 |                |                  |
| N Z / V Z            | 0,14 / 3,52 | 1,86 / 1,66 |                 |                | 4,28             |

Siedeanalyse

| Siedebeginn       | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|--------|--------|--------|--------|--------|--------|
| - 40 °C           |        |        |        |        | 24     |        |
| 60 "              |        |        |        |        | 11,0   |        |
| 80 "              |        |        |        |        | 33,0   |        |
| 100 "             |        |        |        |        | 38,0   |        |
| 120 "             |        |        |        |        | 34,0   |        |
| 140 "             |        |        |        |        | 41,0   | 53,3   |
| 160 "             |        |        |        |        | 44,0   |        |
| 180 "             |        |        |        |        | 53,0   |        |
| 200 "             |        |        |        |        | 58,0   |        |
| 220 "             |        |        |        |        | 63,0   |        |
| 240 "             |        |        |        |        | 67,0   |        |
| 260 "             |        |        |        |        | 71,0   |        |
| 280 "             |        |        |        |        | 74,0   | 31,8   |
| 300 "             |        |        |        |        | 76,5   |        |
| 320 "             |        |        |        |        | 78,0   |        |
| 340 "             |        |        |        |        |        |        |
| 360 "             |        |        |        |        |        |        |
| Siede-Ende °C     |        |        |        |        |        |        |
| Rückstand         |        |        |        |        |        | 53,9   |
| Verlust           |        |        |        |        |        | 0,0    |
| Stockpunkt °C     |        |        |        |        |        |        |
| Destill.-Prod.    | SPL    | N Z    | V Z    |        |        |        |
| Benzin (bis 200°) |        |        |        |        | Ölbenz |        |
| Öl (200-320°)     | 4      |        |        |        | 79     |        |
|                   |        |        |        |        | 66     |        |

Bemerkungen: *reines Paraffin* 000417

DVA

# Untersuchung der flüssigen Produkte

 Ofen Nr. 11 Füllung 13 Dat. 19.30.1.44 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,30         | 30,6           | 45,3                   | 24,8                                | 23,5                  |
| Kondens.-Öl    | 6,45         | 45,8           | 57,7                   | 44,3                                | 25,3                  |
| Paraffingatsch | 3,30         | 23,6           | 27,1                   | 30,9                                | 18,3                  |
| Ges.-Prod.     | 14,05        | 100,0          | 130,1                  | 100,0                               | 26,9                  |

| Kondens.-Prod.       | A K - Benzin  | Ölkond.     | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|---------------|-------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,675         | 0,75        | 0,72                |                | 0,784                |
| Olefine „SPL“ Vol. % |               |             |                     |                |                      |
| Jodzahl (Wijss)      |               |             |                     |                |                      |
| N Z / V Z            | 0,094 / 3,004 | 0,43 / 1,66 |                     |                | 1,54                 |

Siedeanalyse

| Siedebeginn       | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|--------|--------|--------|--------|--------|--------|
| - 40 °C           |        |        |        |        | 3,2    |        |
| - 60 „            |        |        |        |        | 5,0    |        |
| - 80 „            |        |        |        |        | 1,5    |        |
| - 100 „           |        |        |        |        | 5,0    |        |
| - 120 „           |        |        |        |        | 5,0    |        |
| - 140 „           |        |        |        |        | 38,0   | 24,3   |
| - 160 „           |        |        |        |        | 4,0    |        |
| - 180 „           |        |        |        |        | 53,0   |        |
| - 200 „           |        |        |        |        | 1,0    |        |
| - 220 „           |        |        |        |        | 1,0    |        |
| - 240 „           |        |        |        |        | 6,0    |        |
| - 260 „           |        |        |        |        | 1,0    |        |
| - 280 „           |        |        |        |        | 1,0    | 2,15   |
| - 300 „           |        |        |        |        | 2,0    |        |
| - 320 „           |        |        |        |        | 2,0    |        |
| - 340 „           |        |        |        |        |        |        |
| - 360 „           |        |        |        |        |        |        |
| Siede-Ende °C     |        |        |        |        |        |        |
| Rückstand         |        |        |        |        |        | 2,12   |
| Verlust           |        |        |        |        |        | 3,4    |
| Stockpunkt °C     |        |        |        |        |        |        |
| Destill.-Prod.    | SPL    | N Z    | V Z    |        |        |        |
| Benzin (bis 200°) |        |        |        |        | 26,1   |        |
| Öl (200-320°)     |        |        |        |        | 7,4    |        |
|                   |        |        |        |        | 6,2    |        |

Bemerkungen: *Ergebnis...*

000418

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 18.10.1944 Zeit      Betr. Tage     

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,85         | 27,4           | 43,8                   | 33,6                                | 22,6                  |
| Kondens.-Öl    | 6,85         | 47,7           | 60,3                   | 46,2                                | 36,6                  |
| Paraffingatsch | 2,00         | 22,9           | 36,3                   | 30,3                                | 17,5                  |
| Ges.-Prod.     | 12,70        | 100,0          | 12,04                  | 100,0                               | 76,7                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.      | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|--------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,671       | 0,794        | 0,87                |                | 0,984                |
| Olefine „SPL“ Vol. % |             |              |                     |                |                      |
| Jodzahl (Wijss)      |             |              |                     |                |                      |
| N.Z. / V.Z.          | 0,12 / 2,94 | 0,96 / 18,67 |                     |                | 1,54                 |

**Siedeanalyse**

| Siedebeginn   | Vol. % |        |        |        | Gew. % |
|---------------|--------|--------|--------|--------|--------|
|               | Vol. % | Vol. % | Vol. % | Vol. % |        |
| -40 °C        |        |        |        |        |        |
| 60 "          |        |        |        |        |        |
| 80 "          |        |        |        |        |        |
| 100 "         |        |        |        |        |        |
| 120 "         |        |        |        |        |        |
| 140 "         |        |        |        |        | 56,2   |
| 160 "         |        |        |        |        |        |
| 180 "         |        |        |        |        |        |
| 200 "         |        |        |        |        |        |
| 220 "         |        |        |        |        |        |
| 240 "         |        |        |        |        |        |
| 260 "         |        |        |        |        |        |
| 280 "         |        |        |        |        | 23,3   |
| 300 "         |        |        |        |        |        |
| 320 "         |        |        |        |        |        |
| 340 "         |        |        |        |        |        |
| 360 "         |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |
| Rückstand     |        |        |        |        | 17,3   |
| Verlust       |        |        |        |        | 3,2    |

|                   |     |      |      |          |  |
|-------------------|-----|------|------|----------|--|
| Stockpunkt °C     |     |      |      |          |  |
| Destill.-Prod.    | SPL | N.Z. | V.Z. |          |  |
| Benzin (bis 200°) |     |      |      | Ölfrakt. |  |
| Öl (200-320°)     |     |      |      | 7,4      |  |

Bemerkungen: *Reinigt...* 000419

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 17.10.1944 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewicht<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|--------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,80         | 31,2         | 46,2                   | 34,7                                | 23,4                  |
| Kondens.-Öl    | 1,80         | 14,6         | 62,6                   | 46,9                                | 35,6                  |
| Paraffingatsch | 3,60         | 29,3         | 34,5                   | 28,4                                | 16,0                  |
| Ges.-Prod.     | 2,20         | 100,0        | 13,3                   | 100,0                               | 10,0                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkand.     | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|-------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,626       | 0,826       | 0,81                |                | 0,984                |
| Olefine „SPL“ Vol. % |             |             |                     |                |                      |
| Jodzahl (Wijss)      |             |             |                     |                |                      |
| N Z / V Z            | 0,16 / 3,14 | 0,86 / 10,8 |                     |                | 11,54                |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 3,9    |        |
| 60 "          |        |        |        |        | 12,0   |        |
| 80 "          |        |        |        |        | 36,0   |        |
| 100 "         |        |        |        |        | 35,0   |        |
| 120 "         |        |        |        |        | 40,0   |        |
| 140 "         |        |        |        |        | 43,0   | 62,5   |
| 160 "         |        |        |        |        | 50,0   |        |
| 180 "         |        |        |        |        | 61,0   |        |
| 200 "         |        |        |        |        | 66,0   |        |
| 220 "         |        |        |        |        | 69,0   |        |
| 240 "         |        |        |        |        | 73,0   |        |
| 260 "         |        |        |        |        | 75,0   |        |
| 280 "         |        |        |        |        | 79,0   | 16,6   |
| 300 "         |        |        |        |        | 80,0   |        |
| 320 "         |        |        |        |        | 83,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 14,2   |
| Verlust       |        |        |        |        |        | 3,1    |

| Stockpunkt °C | Destill.-Prod.    | SPL | N Z | V Z  |
|---------------|-------------------|-----|-----|------|
|               | Benzin (bis 200°) |     |     | 0,16 |
|               | Öl (200-320°)     |     |     | 3,0  |
|               |                   |     |     | 6,5  |

Bemerkungen: *Wiederholung*

000420

DVA

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 16.12.1944 Zeit 11 Betr. Tage 8

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 4,30      | 31,3       | 46,6                   | 35,2                                | 34,0                  |
| Kondens.-Öl    | 6,35      | 45,4       | 57,1                   | 43,2                                | 34,8                  |
| Paraffingatsch | 2,30      | 16,3       | 26,8                   | 20,6                                | 17,9                  |
| Ges.-Prod.     | 13,75     | 100,0      | 129,5                  | 100,0                               | 76,7                  |

| Kondens.-Prod.       | A.K.-Benzin  | Ölkond.      | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|--------------|--------------|----------------|----------------|-----------------|
| Dichte bei 20° C     | 0,654        | 0,806        | 0,71           |                | 0,983           |
| Olefine „SPL“ Vol. % |              |              |                |                |                 |
| Jodzahl (Wijss)      |              |              |                |                |                 |
| N Z / V Z            | 0,57 / 2,994 | 9,94 / 18,64 |                |                | 844             |

| Siedeanalyse      | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|-------------|--------|--------|--------|--------|--------|--------|
|                   | - 40 °C     |        |        |        |        | 2,0    |        |
| 60 "              |             |        |        |        | 6,0    |        |        |
| 80 "              |             |        |        |        | 10,6   |        |        |
| 100 "             |             |        |        |        | 16,0   |        |        |
| 120 "             |             |        |        |        | 22,0   |        |        |
| 140 "             |             |        |        |        | 29,0   | 4,8    |        |
| 160 "             |             |        |        |        | 35,5   |        |        |
| 180 "             |             |        |        |        | 43,0   |        |        |
| 200 "             |             |        |        |        | 51,0   |        |        |
| 220 "             |             |        |        |        | 60,0   |        |        |
| 240 "             |             |        |        |        | 66,0   |        |        |
| 260 "             |             |        |        |        | 70,0   | 33,1   |        |
| 280 "             |             |        |        |        | 73,0   |        |        |
| 300 "             |             |        |        |        | 76,0   |        |        |
| 320 "             |             |        |        |        | 78,5   |        |        |
| 340 "             |             |        |        |        |        |        |        |
| 360 "             |             |        |        |        |        |        |        |
| Siede-Ende °C     |             |        |        |        |        |        |        |
| Rückstand         |             |        |        |        |        |        | 31,1   |
| Verlust           |             |        |        |        |        |        | 6,0    |
| Stockpunkt °C     |             |        |        |        |        |        |        |
| Destill.-Prod.    | SPL         | N Z    | V Z    |        |        |        |        |
| Benzin (bis 200°) |             |        |        |        | 11,0   |        |        |
| Öl (200-320°)     |             |        |        |        | 7,1    |        |        |
|                   |             |        |        |        | 6,6    |        |        |

Bemerkungen: *Handwritten notes*

000421

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# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 14.15.144 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 4,10         | 30,8           | 45,6                   | 35,0                                 | 33,6                  |
| Kondens.-Öl    | 6,10         | 45,8           | 57,7                   | 44,3                                 | 35,3                  |
| Paraffingatsch | 3,10         | 23,4           | 26,9                   | 20,7                                 | 18,0                  |
| Ges.-Prod.     | 13,30        | 100,0          | 130,2                  | 100,0                                | 76,8                  |

| Kondens.-Prod.       | A.K. Benzin   | Ölkond.      | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|---------------|--------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,626         | 0,795        | 0,87                |                | 0,993                |
| Olefine „SPL“ Vol. % |               |              |                     |                |                      |
| Jodzahl (Wijss)      |               |              |                     |                |                      |
| N Z / V Z            | 0,104 / 0,544 | 8,26 / 16,56 |                     |                | 8,41                 |

| Siedeanalyse  | Siedebeginn | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |  |
|---------------|-------------|--------|--------|--------|--------|--------|--------|--|
|               | — 40 °C     |        |        |        |        | 3,6    |        |  |
|               | 60 „        |        |        |        |        | 9,0    |        |  |
|               | 80 „        |        |        |        |        | 31,0   |        |  |
|               | 100 „       |        |        |        |        | 36,0   |        |  |
|               | 120 „       |        |        |        |        | 33,0   |        |  |
|               | 140 „       |        |        |        |        | 40,0   | 56,3   |  |
|               | 160 „       |        |        |        |        | 45,0   |        |  |
|               | 180 „       |        |        |        |        | 53,0   |        |  |
|               | 200 „       |        |        |        |        | 59,0   |        |  |
|               | 220 „       |        |        |        |        | 63,0   |        |  |
|               | 240 „       |        |        |        |        | 67,0   |        |  |
|               | 260 „       |        |        |        |        | 70,5   |        |  |
|               | 280 „       |        |        |        |        | 73,5   | 20,5   |  |
|               | 300 „       |        |        |        |        | 76,5   |        |  |
| 320 „         |             |        |        |        | 79,0   |        |        |  |
| 340 „         |             |        |        |        |        |        |        |  |
| 360 „         |             |        |        |        |        |        |        |  |
| Siede-Ende °C |             |        |        |        |        |        |        |  |
| Rückstand     |             |        |        |        |        |        | 31,1   |  |
| Verlust       |             |        |        |        |        |        | 3,1    |  |

|                   |     |     |     |  |        |
|-------------------|-----|-----|-----|--|--------|
| Stockpunkt °C     |     |     |     |  |        |
| Destill.-Prod.    | SPL | N Z | V Z |  | Obfium |
| Benzin (bis 200°) |     |     |     |  | 73     |
| Öl (200—320°)     |     |     |     |  | 66     |

Bemerkungen: *früheres Paraffin*

000423

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 13.14.44 Zeit            Betr. Tage           

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,70         | 35,3           | 51,9                   | 39,8                                | 86,9                  |
| Kondens.-Öl    | 2,90         | 37,3           | 46,7                   | 35,8                                | 11,5                  |
| Paraffingatsch | 2,90         | 37,6           | 31,7                   | 24,4                                | 21,4                  |
| Ges.-Prod.     | 10,50        | 100,2          | 130,3                  | 100,0                               | 70,6                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.  | Paraffn-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|----------|--------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,677       | 0,786    | 0,81               |                | 0,904                |
| Olefine „SPL“ Vol. % |             |          |                    |                |                      |
| Jodzahl (Wijss)      |             |          |                    |                |                      |
| N Z / V Z            | 0154/3399   | 884/1924 |                    |                |                      |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C -     |        |        |        |        | 39     |        |
| 60 "          |        |        |        |        | 80     |        |
| 80 "          |        |        |        |        | 81,0   |        |
| 100 "         |        |        |        |        | 82,0   |        |
| 120 "         |        |        |        |        | 84,0   |        |
| 140 "         |        |        |        |        | 87,0   | 54%    |
| 160 "         |        |        |        |        | 47,0   |        |
| 180 "         |        |        |        |        | 58,0   |        |
| 200 "         |        |        |        |        | 59,0   |        |
| 220 "         |        |        |        |        | 62,0   |        |
| 240 "         |        |        |        |        | 68,0   |        |
| 260 "         |        |        |        |        | 69,0   |        |
| 280 "         |        |        |        |        | 71,0   |        |
| 300 "         |        |        |        |        | 74,0   |        |
| 320 "         |        |        |        |        | 75,0   |        |
| 340 "         |        |        |        |        | 75,0   |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 34%    |
| Verlust       |        |        |        |        |        | 1,9    |

| Stockpunkt °C     |     |     |     |     |
|-------------------|-----|-----|-----|-----|
| Destill.-Prod.    | SPL | N Z | V Z | 0,6 |
| Benzin (bis 200°) |     |     |     | 71  |
| Öl (200-320°)     |     |     |     | 0,6 |

Bemerkungen: *Paraffin*

000424



# Untersuchung der flüssigen Produkte

Ofen Nr. *11* Füllung *13* Dat. *12. 13. 1942* Zell *11* Betr. Tage

| Produkt        | Anfall kg | Gewichts-% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|-----------|------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 2,80      | 29,0       | 42,6                   | 33,0                                | 22,4                  |
| Kondens.-Öl    | 6,10      | 46,6       | 57,7                   | 45,5                                | 36,3                  |
| Paraffingatsch | 3,30      | 24,4       | 27,7                   | 21,5                                | 12,9                  |
| Ges.-Prod.     | 12,20     | 100,0      | 139,0                  | 100,0                               | 77,5                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.     | Paraffingatsch | Gesamt-Produkt | Reaktionswasser |
|----------------------|-------------|-------------|----------------|----------------|-----------------|
| Dichte bei 20 °C     | 0,681       | 0,795       | 0,89           |                |                 |
| Olefine „SPL“ Vol.-% |             |             |                |                | 0,982           |
| Jodzahl (Wijss)      |             |             |                |                |                 |
| N Z / V Z            | 0,091/0,336 | 0,301/0,495 |                |                |                 |

Siedeanalyse

| Siedebeginn   | Vol.-% | Vol.-% | Vol.-% | Vol.-% | Vol.-% | Gew.-% |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 40     |        |
| 60 "          |        |        |        |        | 80     |        |
| 80 "          |        |        |        |        | 20,0   |        |
| 100 "         |        |        |        |        | 36,0   |        |
| 120 "         |        |        |        |        | 33,0   |        |
| 140 "         |        |        |        |        | 40,0   | 56,3   |
| 160 "         |        |        |        |        | 47,0   |        |
| 180 "         |        |        |        |        | 53,0   |        |
| 200 "         |        |        |        |        | 59,0   |        |
| 220 "         |        |        |        |        | 63,0   |        |
| 240 "         |        |        |        |        | 67,0   |        |
| 260 "         |        |        |        |        | 71,5   |        |
| 280 "         |        |        |        |        | 76,0   | 19,9   |
| 300 "         |        |        |        |        | 78,0   |        |
| 320 "         |        |        |        |        | 79,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 23,3   |
| Verlust       |        |        |        |        |        | 0,2    |

| Stockpunkt °C     | SPL | N Z | V Z  |
|-------------------|-----|-----|------|
| Destill.-Prod.    |     |     |      |
| Benzin (bis 200°) |     |     | 0,12 |
| Öl (200-320°)     |     |     | 73   |
|                   |     |     | 68   |

Bemerkungen: *kein Paraffin*

000425

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 11.11.44 Zeit ..... Betr. Tage .....

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|-------------------------------------|-----------------------|
| A.K.-Benzin    | 3,50         | 37,0           | 39,6                   | 30,9                                | 31,1                  |
| Kondens.-Öl    | 6,05         | 46,7           | 58,9                   | 45,8                                | 36,4                  |
| Paraffingatsch | 3,40         | 26,3           | 39,9                   | 33,3                                | 20,5                  |
| Ges.-Prod.     | 12,95        | 100,0          | 129,4                  | 100,0                               | 78,0                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.    | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,683       | 0,795      | 0,82                |                |                      |
| Olefine „SPL“ Vol. % |             |            |                     |                | 0,984                |
| Jodzahl (Wijss)      |             |            |                     |                |                      |
| N Z / V Z            | 15 / 399    | 933 / 1844 |                     |                |                      |

**Siedeanalyse**

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 44     |        |
| 60 "          |        |        |        |        | 7,0    |        |
| 80 "          |        |        |        |        | 19,0   |        |
| 100 "         |        |        |        |        | 34,0   |        |
| 120 "         |        |        |        |        | 31,0   |        |
| 140 "         |        |        |        |        | 39,0   | 53,3   |
| 160 "         |        |        |        |        | 45,9   |        |
| 180 "         |        |        |        |        | 51,0   |        |
| 200 "         |        |        |        |        | 57,0   |        |
| 220 "         |        |        |        |        | 61,9   |        |
| 240 "         |        |        |        |        | 66,0   |        |
| 260 "         |        |        |        |        | 70,9   | 32,4   |
| 280 "         |        |        |        |        | 74,0   |        |
| 300 "         |        |        |        |        | 77,0   |        |
| 320 "         |        |        |        |        | 79,0   |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 33,3   |
| Verlust       |        |        |        |        |        | 1,0    |

| Stockpunkt °C     | SPL | N Z | V Z |        |
|-------------------|-----|-----|-----|--------|
| Destill.-Prod.    |     |     |     |        |
| Benzin (bis 200°) |     |     |     | Ölfirn |
| Öl (200-320°)     |     |     |     | 73     |
|                   |     |     |     | 68     |

Bemerkungen: *hervorgehoben Paraffin*

000426

Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 13 Dat. 10.11.1.44 Zeit Betr. Tage

| Produkt        | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|----------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 3,40         | 27,0           | 39,6                   | 30,2                                 | 31,0                  |
| Kondens.-Öl    | 5,90         | 46,8           | 59,1                   | 46,1                                 | 36,6                  |
| Paraffingatsch | 2,30         | 18,2           | 19,7                   | 13,1                                 | 20,3                  |
| Ges.-Prod.     | 11,60        | 100,0          | 118,4                  | 100,0                                | 77,9                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond. | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|---------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,681       | 0,793   | 0,88                |                | 0,982                |
| Olefine „SPL“ Vol. % |             |         |                     |                |                      |
| Jodzahl (Wijss)      |             |         |                     |                |                      |
| N Z / V Z            | 915         | 96      | 1908                |                | 869                  |

Siedeanalyse

| Siedebeginn   | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|---------------|--------|--------|--------|--------|--------|--------|
| - 40 °C       |        |        |        |        | 43     |        |
| 60 "          |        |        |        |        | 60     |        |
| 80 "          |        |        |        |        | 118,0  |        |
| 100 "         |        |        |        |        | 133,0  |        |
| 120 "         |        |        |        |        | 139,0  |        |
| 140 "         |        |        |        |        | 177,0  | 54,3   |
| 160 "         |        |        |        |        | 144,0  |        |
| 180 "         |        |        |        |        | 151,0  |        |
| 200 "         |        |        |        |        | 157,0  |        |
| 220 "         |        |        |        |        | 161,0  |        |
| 240 "         |        |        |        |        | 165,0  |        |
| 260 "         |        |        |        |        | 169,0  |        |
| 280 "         |        |        |        |        | 173,0  | 21,2   |
| 300 "         |        |        |        |        | 176,0  |        |
| 320 "         |        |        |        |        | 178,5  |        |
| 340 "         |        |        |        |        |        |        |
| 360 "         |        |        |        |        |        |        |
| Siede-Ende °C |        |        |        |        |        |        |
| Rückstand     |        |        |        |        |        | 23,0   |
| Verlust       |        |        |        |        |        | 1,0    |

| Stockpunkt °C | Destill.-Prod.    | SPL | N Z | V Z |              |
|---------------|-------------------|-----|-----|-----|--------------|
|               | Benzin (bis 200°) |     |     |     | Ölbin<br>102 |
|               | Öl (200-320°)     |     |     |     | 26           |

Bemerkungen: *benzini Paraffin*

000427

# Untersuchung der flüssigen Produkte

Ofen Nr. 11 Füllung 1 Dat. 9.10.1944 Zeit          Betr. Tage         

| Produkt        | Anfall<br>kg | Gewichts-<br>% <sub>100</sub> | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100 cm <sup>3</sup> | g/100 cm <sup>3</sup> |
|----------------|--------------|-------------------------------|------------------------|--------------------------------------|-----------------------|
| A.K.-Benzin    | 2,90         | 64,8                          | 36,0                   | 38,4                                 | 10,5                  |
| Kondens.-Öl    | 5,70         | 41,7                          | 51,4                   | 48,0                                 | 38,3                  |
| Paraffingatsch | 3,10         | 86,5                          | 89,9                   | 33,4                                 | 20,8                  |
| Ges.-Prod.     | 11,70        | 100,0                         | 137,4                  | 100,0                                | 78,6                  |

| Kondens.-Prod.       | A.K.-Benzin | Ölkond.    | Paraffin-<br>gatsch | Gesamt-Produkt | Reaktions-<br>wasser |
|----------------------|-------------|------------|---------------------|----------------|----------------------|
| Dichte bei 20° C     | 0,686       | 0,795      | 0,89                |                | 0,994                |
| Olefine „SPL“ Vol. % |             |            |                     |                |                      |
| Jodzahl (Wijss)      |             |            |                     |                |                      |
| N Z / V Z            | 0,88 / 8336 | 907 / 1948 |                     |                | 842                  |

**Siedeanalyse**

| Siedebeginn       | Vol. % | Vol. % | Vol. % | Vol. % | Vol. % | Gew. % |
|-------------------|--------|--------|--------|--------|--------|--------|
| - 40 °C           |        |        |        |        |        |        |
| - 60 „            |        |        |        |        | 41     |        |
| 80 „              |        |        |        |        | 60     |        |
| 100 „             |        |        |        |        | 19,0   |        |
| 120 „             |        |        |        |        | 34,9   |        |
| 140 „             |        |        |        |        | 31,7   |        |
| 160 „             |        |        |        |        | 39,0   | 54,8   |
| 180 „             |        |        |        |        | 45,0   |        |
| 200 „             |        |        |        |        | 70,0   |        |
| 220 „             |        |        |        |        | 19,0   |        |
| 240 „             |        |        |        |        | 67,0   |        |
| 260 „             |        |        |        |        | 71,0   | 38,3   |
| 280 „             |        |        |        |        | 24,0   |        |
| 300 „             |        |        |        |        | 75,0   |        |
| 320 „             |        |        |        |        | 10,5   |        |
| 340 „             |        |        |        |        |        |        |
| 360 „             |        |        |        |        |        |        |
| Siede-Ende °C     |        |        |        |        |        |        |
| Rückstand         |        |        |        |        |        | 36,5   |
| Verlust           |        |        |        |        |        | 0,4    |
| Stockpunkt °C     |        |        |        |        |        |        |
| Destill.-Prod.    | SPL    | N Z    | V Z    |        |        |        |
| Benzin (bis 200°) |        |        |        | Ölfine |        |        |
| Öl (200-320°)     |        |        |        | 24     |        |        |
|                   |        |        |        | 64     |        |        |

Bemerkungen: *paraffin / paraffin*

000428

Nr.

# Drucksynthese B.-V.-A.

Ofen-Nr.: 11 Datum u. Zeit: *Thunwaldstraße* *Frankfurt* Nr. 507/508

|          | Anfall<br>kg | Gewichts-<br>% | cm <sup>3</sup> /100 g | cm <sup>3</sup> /100cm <sup>3</sup> | g/100cm <sup>3</sup> |
|----------|--------------|----------------|------------------------|-------------------------------------|----------------------|
| Benzin   |              |                |                        |                                     |                      |
| Öel      |              |                |                        |                                     |                      |
| Paraffin |              |                |                        |                                     |                      |

|   | 507<br>Benzin | 508<br>Öel | Paraffin | Gesamt-Produkt |        | Reaktions-<br>wasser |   |
|---|---------------|------------|----------|----------------|--------|----------------------|---|
|   | Vol. %        | Vol. %     | Vol. %   | Vol. %         | Gew. % |                      |   |
| 1   | 2             | 3          | 4        | 5              | 6      | 7                    | 8 |
| Dichte bei 15 °C  | 0,691         | 0,794      |          |                |        |                      |   |
| Olefine (H <sub>2</sub> SO <sub>4</sub> -P <sub>2</sub> O <sub>5</sub> ) Vol. % |               |            |          |                |        |                      |   |
| Jodzahl (Wijs)  |               |            |          |                |        |                      |   |
| N. Z. KZ.   | 1621446       | 1861904    |          |                |        |                      |   |
| Siede-Beginn °C   | 34            | 123        |          |                |        |                      |   |
| - 40  | 3,0           |            |          |                |        |                      |   |
| 60  | 34,0          |            |          |                |        |                      |   |
| 80  | 40,0          |            |          |                |        |                      |   |
| 100   | 50,0          |            |          |                |        |                      |   |
| 120   | 59,0          |            |          |                |        |                      |   |
| 140   | 70,0          |            |          |                |        |                      |   |
| 160   | 87,0          |            |          |                |        |                      |   |
| 180   | 90,0          |            |          |                |        |                      |   |
| 195   | 93,0          |            |          |                |        |                      |   |
| 220   | 94,0          |            |          |                |        |                      |   |
| 240   |               |            |          |                |        |                      |   |
| 260   |               |            |          |                |        |                      |   |
| 280   |               |            |          |                |        |                      |   |
| 300   |               |            |          |                |        |                      |   |
| 320   |               |            |          |                |        |                      |   |
| 340   |               |            |          |                |        |                      |   |
| 360   |               |            |          |                |        |                      |   |
| Siede-Ende °C   | 108           |            |          |                |        |                      |   |
| Rückstand   | 3,2           |            |          |                |        |                      |   |
| Verlust   | 1,2           |            |          |                |        |                      |   |
| Stockpunkt °C   |               |            |          |                |        |                      |   |
| Eisen mg/l  |               |            |          |                |        |                      |   |
| Analysen-Nr.  | 78            | 63         |          |                |        |                      |   |
| Zeichen des Laboranten  |               |            |          |                |        |                      |   |

Siede-Analyse:

Bemerkungen:

000429