

Appendix A: ASPEN Plus Input File
 Gasifier Fortran Subroutine

Appendix A: ASPEN Plus Input File

DEF-STREAMS MIXCINC ALL

DIAGNOSTICS

HISTORY SYS-LEVEL=4 SIM-LEVEL=4 PROP-LEVEL=2 STREAM-LEVEL=4
MAX-PRINT SIM-LIMIT=5000 PROP-LIMIT=50

RUN-CONTROL MAX-ERRORS=500

DATABANKS PURECOMP / AQUEOUS / SOLIDS / INORGANIC / &
ASPENPCD

PROP-SOURCES PURECOMP / AQUEOUS / SOLIDS / INORGANIC / &
ASPENPCD .

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=====;  
; Components ;  
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COMPONENTS

TAR C10H8 TAR /
H2 H2 H2 /
O2 O2 O2 /
N2 N2 N2 /
CO2 CO2 CO2 /
CO CO CO /
H2O H2O H2O /
CH4 CH4 CH4 /
H2S H2S H2S /
NH3 H3N NH3 /
COS COS COS /
SO2 O2S SO2 /
SO3 O3S SO3 /
O2SI SIO2 O2SI /
NO2 NO2 NO2 /
NO NO NO /
PHENOL C6H6O PHENOL /
C6H6 C6H6 C6H6 /
C2H6 C2H6 C2H6 /
C2H4 C2H4 C2H4 /
C2H2 C2H2 C2H2 /
CARBON C CARBON /
SULFUR S SULFUR /
WOOD * WOOD /
ASH * ASH /
CHAR * CHAR

Flowsheet

FLOWSHEET MAIN

BLOCK FEEDMIX IN=GASIFSTM WOOD SAND OUT=GFEED
BLOCK GASIFIER IN=GFEED OUT=WOODGAS QGAS
BLOCK CHARSEP IN=WOODGAS OUT=CHAR SYNGAS
BLOCK CHARDEC IN=CHAR OUT=CHARCOMP QCHAR
BLOCK AIRHEAT IN=COMBAIR2 OUT=HCOMBAIR QAIR
BLOCK CHARFURN IN=CHARCOMP HCOMBAIR SANDSUPP QCHAR OUT= &
COMBPROD QCOMB
BLOCK COMBSPLT IN=COMBPROD OUT=CHARFLUE ASHSAND
BLOCK SANDSPLT IN=ASHSAND OUT=SAND SANDPURG
BLOCK SYNCOMPR IN=TOCOMPR OUT=SYNCOMPD 205
BLOCK PRIMARY IN=TOREFHOT REFSTM OUT=SYNREFRM 105
BLOCK HTSHIFT IN=TOHT OUT=FROMHT QHT
BLOCK LTSHIFT IN=TOLT OUT=FROMLT QLT
BLOCK REFHTR IN=207 OUT=TOREFHOT 198
BLOCK WATPUMP IN=REFSTMA OUT=REFSTMB
BLOCK WOODSEP IN=ARWOOD OUT=WOODWAT MIDWOOD
BLOCK DRY2 IN=MIDWOOD WETDAIR OUT=DRYWOOD
BLOCK DRY1 IN=WOODWAT FLUENAIR OUT=WETDAIR
BLOCK DRYRMIX IN=CHARFLUE DRYRAIR2 OUT=FLUENAIR
BLOCK PSA IN=TOPSAB OUT=H2PURIFY OFFGAS
BLOCK OFFCOMB IN=OFFGAS OFFAIR2 105 OUT=OFFFLUE1
BLOCK GSTMGEN IN=SYNREFRM GSTMIN OUT=FROMPRIM GASIFSTM
BLOCK AIRCOMP1 IN=COMBAIR OUT=COMBAIR2
BLOCK AIRCOMP2 IN=DRYRAIR OUT=DRYRAIR2
BLOCK DRYRSEP IN=DRYWOOD OUT=DRIED GASWAT
BLOCK MODEL1 IN=HOTIN COLDIN OUT=HOTOUT COLDOUT
BLOCK SYNCOOL1 IN=SYNGAS OUT=SYNCOLD 197
BLOCK MODEL2 IN=HI CI OUT=HO CO
BLOCK LTCOOL IN=FROMHT 196 OUT=TOLT STEAM6
BLOCK OFFCOMPR IN=OFFAIR1 OUT=OFFAIR2
BLOCK REFSTM IN=REFSTMB OUT=REFSTM 135
BLOCK COMBCOOL IN=OFFFLUE1 135 OUT=OFFFLUE2
BLOCK HTCOOL IN=FROMPRIM OUT=TOHT
BLOCK PUMP1 IN=BFW1A OUT=145
BLOCK INTER2A IN=GAS2A 160 OUT=COOLED2A STEAM2A
BLOCK INTER2B IN=GAS2B 165 OUT=COOLED2B STEAM2B
BLOCK PUMP4 IN=BFW2A OUT=160
BLOCK PUMP5 IN=BFW2B OUT=165
BLOCK RECMIX IN=TOPSAA H2RECYCL OUT=TOPSAB
BLOCK RECSPLT IN=H2PURIFY OUT=H2PROD H2RECYCL
BLOCK STMGEN6 IN=OFFFLUE2 188 OUT=OFFFLUE3 STEAM4
BLOCK B13 IN=BFW4 OUT=188
BLOCK B3 IN=BFW6 OUT=196
BLOCK B1 IN=SYNCOLD OUT=KOWATER TOCOMPR
BLOCK B2 IN=SYNCOMPD 208 205 OUT=207
BLOCK B5 IN=KOWATER OUT=208
BLOCK PSACOOOL IN=FROMLT 212 OUT=TOPSAA STEAM5 189

BLOCK B7 IN=BFW5 OUT=212
BLOCK B4 IN=GAS1A OUT=COOLED1A 213
BLOCK B6 IN=145 213 OUT=STMWAT
BLOCK STMFLASH IN=STMWAT OUT=STEAM1A WAT1A

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Physical Property Data

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PROPERTIES SYSOP3

PROP-REPLACE SYSOP3 RKS-BM
PROP MUVMX MUVMX02
PROP MULMX MULMX02
PROP KVMX KVMX02
PROP KLMX KLMX01
PROP DV DV01
PROP MUL MUL01
PROP MUV MUV01
PROP KV KV01
PROP KL KL01

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NC-COMPS WOOD ULTANAL SULFANAL PROXANAL
NC-PROPS WOOD ENTHALPY HCJ1BOIE / DENSITY DCOALIGT
NC-COMPS ASH GENANAL ULTANAL SULFANAL PROXANAL
NC-PROPS ASH ENTHALPY HCJ1BOIE / DENSITY DNSTYGEN
NC-COMPS CHAR ULTANAL SULFANAL PROXANAL
NC-PROPS CHAR ENTHALPY HCJ1BOIE / DENSITY DCHARIGT

PROP-DATA DATA1
IN-UNITS ENG
PROP-LIST DGSFRM / DHSFRM / MW
PVAL O2SI .0 / .0 / 60.0860
PVAL CARBON .0 / .0 / 12.0110
PVAL SULFUR .0 / .0 / 32.0640

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Conventional Component Property Data

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PROP-DATA DATA5
IN-UNITS SI TEMPERATURE=F
PROP-LIST VSPOLY

PVAL CARBON .005340 .0 .0 .0 .0 2500.0
PVAL SULFUR .01550 .0 .0 .0 .0 2500.0

PROP-DATA U-1

IN-UNITS ENG MOLE-HEAT-CA='CAL/MOL-K' TEMPERATURE=K
PROP-LIST CPSP01
PVAL CARBON 2.6730 .0026170 .0 .0 -116900.0 .0 273.0 &
1373.0
PVAL O2SI 12.80 .004470 .0 .0 -302000.0 .0 273.0 1973.0
PVAL SULFUR 3.630 .00640 0.0 0.0 0.0 0.0 1000.000

PROP-DATA U-2

IN-UNITS SI
PROP-LIST DENGEN
PVAL ASH 2000.0 .0 .0 .0

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; Stream Structure
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PROP-SET PS-1 CP RHO UNITS='BTU/LB-R' 'GM/CC' 'LB/CUFT' &
SUBSTREAM=MIXED COMPS=O2SI CARBON SULFUR PHASE=S

PROP-SET PS-2 DENSITY HEAT-CAP UNITS='LB/CUFT' 'GM/CC' &
'BTU/LB-R' 'CAL/GM-K' SUBSTREAM=NC COMPS=WOOD ASH CHAR &
PHASE=S

STREAM 207

STREAM ARWOOD

SUBSTREAM MIXED TEMP=59 PRES=14.696
MASS-FLOW H2O .78
SUBSTREAM NC TEMP=59 PRES=14.696
MASS-FLOW WOOD 1
COMP-ATTR WOOD ULTANAL (.920 50.880 6.04 .17 0 0.09 &
41.9)
COMP-ATTR WOOD SULFANAL (.450 .02250 .02250)
COMP-ATTR WOOD PROXANAL (11 15.29 83.52 .87)

STREAM BFW1A

SUBSTREAM MIXED TEMP=170 PRES=30
MASS-FLOW H2O .8

STREAM BFW2A

SUBSTREAM MIXED TEMP=59 PRES=30
MASS-FLOW H2O .0565

STREAM BFW2B

SUBSTREAM MIXED TEMP=59 PRES=30
MASS-FLOW H2O .04825

STREAM BFW4

SUBSTREAM MIXED TEMP=59 PRES=30
MASS-FLOW H2O .378

STREAM BFW5
SUBSTREAM MIXED TEMP=59 PRES=30
MASS-FLOW H2O .75

STREAM BFW6
SUBSTREAM MIXED TEMP=59 PRES=14.696
MASS-FLOW H2O .2

STREAM CI
SUBSTREAM MIXED TEMP=59 PRES=30
MASS-FLOW H2O .570

STREAM COLDIN
SUBSTREAM MIXED TEMP=228 PRES=530
MASS-FLOW TAR .014 / H2 .012 / CO2 .16 / CO .327 / &
H2O .51 / CH4 .069 / H2S .001 / NH3 .002 / C2H6 &
.004 / C2H4 .035 / C2H2 .003

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STREAM COMBAIR
SUBSTREAM MIXED TEMP=59.0 PRES=14.696 MASS-FLOW=1.80
MOLE-FRAC O2 .207340 / N2 .782180 / CO2 .000330 / H2O &
.010150

STREAM DRYRAIR
SUBSTREAM MIXED TEMP=59 PRES=14.696 MASS-FLOW=6
MOLE-FRAC O2 .207340 / N2 .782180 / CO2 .000330 / H2O &
.010150

STREAM GAS1A
SUBSTREAM MIXED TEMP=397.8549 PRES=45.37759
MASS-FLOW TAR .013804 / H2 .011585 / CO2 .160307 / CO &
0.327241 / H2O .50999 / CH4 .068728 / H2S .000781 / &
NH3 .001718 / C2H6 .003747 / C2H4 .035058 / C2H2 &
.00254

STREAM GAS2A
SUBSTREAM MIXED TEMP=414.9241 PRES=72.99842
MASS-FLOW O2 .250564 / N2 .827514 / CO2 .000548 / H2O &
.006906

STREAM GAS2B
SUBSTREAM MIXED TEMP=373.9805 PRES=162.6937
MASS-FLOW O2 .250564 / N2 .827514 / CO2 .000548 / H2O &
.006906

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STREAM GASIFSTM
SUBSTREAM MIXED TEMP=1000 PRES=25

MASS-FLOW H2O .4

STREAM GSTMIN

SUBSTREAM MIXED TEMP=59 PRES=30
MASS-FLOW H2O .4

STREAM HI

SUBSTREAM MIXED TEMP=1736 PRES=362.6
MASS-FLOW O2 .038 / N2 .99 / CO2 1.041 / H2O .227

STREAM HOTIN

SUBSTREAM MIXED TEMP=1517.5 PRES=20
MASS-FLOW TAR .014 / H2 .012 / CO2 .16 / CO .327 / &
H2O .51 / CH4 .069 / H2S .001 / NH3 .002 / C2H6 &
.004 / C2H4 .035 / C2H2 .003

STREAM OFFAIR1

SUBSTREAM MIXED TEMP=59 PRES=14.696 MASS-FLOW=5
MOLE-FRAC O2 .207340 / N2 .782180 / CO2 .000330 / H2O &
.010150

STREAM OFFFLUE1

SUBSTREAM MIXED TEMP=1915 PRES=362
MASS-FLOW O2 .058983 / N2 1.197313 / CO2 1.040337 / CO &
.266843

STREAM REFSTMA

SUBSTREAM MIXED TEMP=59 PRES=30
MASS-FLOW H2O .544

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STREAM SAND

SUBSTREAM MIXED TEMP=1822.0 PRES=25.0
MASS-FLOW H2O 1.000E-05
SUBSTREAM CISOLID TEMP=1740.0 PRES=25.0
MASS-FLOW O2SI 21.0
SUBSTREAM NC TEMP=1740.0 PRES=25.0
MASS-FLOW ASH .00780
COMP-ATTR ASH GENANAL (100.0 0.0 0.0 0.0 0.0 0.0 0.0 &
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 &
0.0)
COMP-ATTR ASH ULTANAL (100.0 0.0 0.0 0.0 0.0 0.0)
COMP-ATTR ASH SULFANAL (0.0 0.0 0.0)
COMP-ATTR ASH PROXANAL (0.0 0.0 0.0 100.0)

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STREAM SANDSUPP

SUBSTREAM MIXED TEMP=59.0 PRES=20
MASS-FLOW H2O 1.000E-05
SUBSTREAM CISOLID TEMP=59.0 PRES=20
MASS-FLOW O2SI .080

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;=====
;                               Streams
;=====
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;                               CoalMisc (8476.0 0.0 0.0 0.0 0.0)
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STREAM WOOD

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SUBSTREAM MIXED TEMP=155 PRES=25
SUBSTREAM CISOLID TEMP=220 PRES=25
MASS-FLOW CARBON 1.000E-05
SUBSTREAM NC TEMP=220 PRES=25
MASS-FLOW WOOD 1.0 / ASH 1.000E-05 / CHAR 1.000E-05
COMP-ATTR WOOD ULTANAL ( .920 50.880 6.040 .170 .0 .090 &
41.90 )
COMP-ATTR WOOD SULFANAL ( .450 .02250 .02250 )
COMP-ATTR WOOD PROXANAL ( 11.0 15.290 83.520 .870 )
COMP-ATTR ASH GENANAL ( 100.0 .0 .0 .0 .0 .0 .0 &
.0 .0 .0 .0 .0 .0 .0 .0 .0 .0 )
COMP-ATTR ASH ULTANAL ( 100.0 .0 .0 .0 .0 .0 )
COMP-ATTR ASH SULFANAL ( .0 .0 .0 )
COMP-ATTR ASH PROXANAL ( .0 .0 .0 100.0 )
COMP-ATTR CHAR ULTANAL ( .0 86.0 4.0 .0 .0 .030 9.970 &
)
COMP-ATTR CHAR SULFANAL ( .010 .010 .010 )
COMP-ATTR CHAR PROXANAL ( .0 87.180 12.810 .010 )
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DEF-STREAMS HEAT 105

DEF-STREAMS HEAT 135

DEF-STREAMS HEAT 197

DEF-STREAMS HEAT 198

DEF-STREAMS HEAT 213

DEF-STREAMS HEAT QAIR

DEF-STREAMS HEAT QCHAR

DEF-STREAMS HEAT QCOMB

DEF-STREAMS HEAT QGAS

DEF-STREAMS HEAT QHT

DEF-STREAMS HEAT QLT

BLOCK B2 MIXER
PARAM PRES=530

BLOCK DRY1 MIXER

BLOCK DRY2 MIXER

BLOCK DRYRMIX MIXER

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BLOCK FEEDMIX MIXER
PARAM PRES=25

BLOCK RECMIX MIXER

BLOCK RECSPLT FSPLIT
FRAC H2RECYCL .1

BLOCK SANDSPLT FSPLIT
FRAC SANDPURG .0050

BLOCK B1 SEP

FRAC STREAM=KOWATER SUBSTREAM=MIXED COMPS=TAR H2 O2 N2 &
CO2 CO H2O CH4 H2S NH3 COS SO2 SO3 O2SI NO2 NO &
PHENOL C6H6 C2H6 C2H4 C2H2 CARBON SULFUR FRACS=0 0 &
0 0 0 0 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
FRAC STREAM=KOWATER SUBSTREAM=CISOLID COMPS=O2SI CARBON &
FRACS=0 0
FRAC STREAM=KOWATER SUBSTREAM=NC COMPS=WOOD ASH CHAR &
FRACS=0 0 0

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BLOCK CHARSEP SEP

FRAC STREAM=CHAR SUBSTREAM=CISOLID COMPS=O2SI CARBON &
FRACS=1.0 1.0
FRAC STREAM=CHAR SUBSTREAM=NC COMPS=WOOD ASH CHAR FRACS= &
1.0 1.0 1.0
FRAC STREAM=SYNGAS SUBSTREAM=MIXED COMPS=TAR H2 O2 N2 &
CO2 CO H2O CH4 H2S NH3 COS SO2 SO3 O2SI NO2 NO &
PHENOL C6H6 C2H6 C2H4 C2H2 CARBON SULFUR FRACS=1.0 &
1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 &
1.0 1.0 1.0 1.0 1.0 1.0 1.0 0.0 0.0

;

BLOCK COMBSPLT SEP

FRAC STREAM=ASHSAND SUBSTREAM=MIXED COMPS=TAR H2 O2 N2 &
CO2 CO H2O CH4 H2S NH3 COS SO2 SO3 O2SI NO2 NO &
PHENOL C6H6 C2H6 C2H4 C2H2 CARBON SULFUR FRACS=.0 .0 &
.0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 1.0 .0 .0 .0 &
.0 .0 .0 .0 .0 .0
FRAC STREAM=ASHSAND SUBSTREAM=CISOLID COMPS=O2SI FRACS= &
1.0
FRAC STREAM=ASHSAND SUBSTREAM=NC COMPS=WOOD ASH CHAR &
FRACS=.0 1.0 .0

BLOCK DRYRSEP SEP

FRAC STREAM=DRIED SUBSTREAM=MIXED COMPS=TAR H2 O2 N2 &
CO2 CO H2O CH4 H2S NH3 COS SO2 SO3 O2SI NO2 NO &
PHENOL C6H6 C2H6 C2H4 C2H2 CARBON SULFUR FRACS=0 0 &
0 0

FRAC STREAM=DRIED SUBSTREAM=CISOLID COMPS=O2SI CARBON &
FRACS=0 0

FRAC STREAM=DRIED SUBSTREAM=NC COMPS=WOOD ASH CHAR &
FRACS=1 0 0

BLOCK PSA SEP

FRAC STREAM=H2PURIFY SUBSTREAM=MIXED COMPS=TAR H2 O2 N2 &
CO2 CO H2O CH4 H2S NH3 COS SO2 SO3 O2SI NO2 NO &
PHENOL C6H6 C2H6 C2H4 C2H2 CARBON SULFUR FRACS=0 .85 &
0 0

FRAC STREAM=H2PURIFY SUBSTREAM=CISOLID COMPS=O2SI CARBON &
FRACS=0 0

FRAC STREAM=H2PURIFY SUBSTREAM=NC COMPS=WOOD ASH CHAR &
FRACS=0 0 0

BLOCK WOODSEP SEP

FRAC STREAM=WOODWAT SUBSTREAM=MIXED COMPS=TAR H2 O2 N2 &
CO2 CO H2O CH4 H2S NH3 COS SO2 SO3 O2SI NO2 NO &
PHENOL C6H6 C2H6 C2H4 C2H2 CARBON SULFUR FRACS=1 1 &
1 1

FRAC STREAM=WOODWAT SUBSTREAM=CISOLID COMPS=O2SI CARBON &
FRACS=1 1

FRAC STREAM=WOODWAT SUBSTREAM=NC COMPS=WOOD ASH CHAR &
FRACS=0 1 1

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BLOCK AIRHEAT HEATER

PARAM TEMP=60.0 PRES=0

BLOCK B4 HEATER

PARAM TEMP=190 PRES=0

BLOCK B6 HEATER

PARAM PRES=0

BLOCK COMBCOOL HEATER

PARAM PRES=0

BLOCK HTCOOL HEATER

PARAM TEMP=370 <C> PRES=0

BLOCK REFHTR HEATER

PARAM TEMP=800 <C> PRES=0

BLOCK REFSTM HEATER

PARAM TEMP=1000 PRES=0

BLOCK SYNCOOL1 HEATER

PARAM TEMP=195 PRES=0

BLOCK STMFLASH FLASH2
PARAM PRES=130 DUTY=0

BLOCK GSTMGEN HEATX
PARAM T-COLD=1000 PRES-COLD=0
FEEDS HOT=SYNREFRM COLD=GSTMIN
PRODUCTS HOT=FROMPRIM COLD=GASIFSTM

BLOCK INTER2A HEATX
PARAM T-HOT=150
FEEDS HOT=GAS2A COLD=160
PRODUCTS HOT=COOLED2A COLD=STEAM2A

BLOCK INTER2B HEATX
PARAM T-HOT=150
FEEDS HOT=GAS2B COLD=165
PRODUCTS HOT=COOLED2B COLD=STEAM2B

BLOCK LTCOOL HEATX
PARAM T-HOT=392
FEEDS HOT=FROMHT COLD=196
PRODUCTS HOT=TOLT COLD=STEAM6
FLASH-SPECS TOLT FREE-WATER=YES MAXIT=100
FLASH-SPECS STEAM6 MAXIT=100

;This block is used to model the syngas cooler prior to compression. Note
;that this block is really only representative of SYNCOOL1 and REFHTR;
;SYNCOOL2 is a separate cooler, modelled by MODEL2.

BLOCK MODEL1 HEATX
PARAM T-HOT=1472
FEEDS HOT=HOTIN COLD=COLDIN
PRODUCTS HOT=HOTOUT COLD=COLDOUT

;This block models the heat exchanger which connects blocks SYNCOOL2
;DECANTHT. SYNCOOL1 is modeled by MODEL1.

BLOCK MODEL2 HEATX
PARAM T-COLD=1000
FEEDS HOT=HI COLD=CI
PRODUCTS HOT=HO COLD=CO

BLOCK PSACOOOL HEATX
PARAM T-HOT=75
FEEDS HOT=FROMLT COLD=212
PRODUCTS HOT=TOPSAA COLD=STEAM5
DECANT-STREA HOT=189
FLASH-SPECS TOPSAA FREE-WATER=YES

BLOCK STMG6 HEATX
PARAM T-HOT=82
FEEDS HOT=OFFFLUE2 COLD=188
PRODUCTS HOT=OFFFLUE3 COLD=STEAM4

;

BLOCK CHARFURN RSTOIC

PARAM TEMP=1800.0 PRES=-1.0
STOIC 1 MIXED H2 -1.0 / O2 -.50 / H2O 1.0
STOIC 2 MIXED O2 -1.0 / CISOLID CARBON -1.0 / MIXED &
CO2 1.0
STOIC 3 MIXED O2 -1.0 / CISOLID SULFUR -1.0 / MIXED &
SO2 1.0
CONV 1 MIXED H2 1.0
CONV 2 CISOLID CARBON 1.0
CONV 3 CISOLID SULFUR 1.0

BLOCK HTSHIFT RSTOIC

PARAM PRES=0 DUTY=0
STOIC 1 MIXED TAR -1 / H2O -20 / CO2 10 / H2 24
STOIC 2 MIXED CO -1 / H2O -1 / H2 1 / CO2 1
CONV 1 MIXED TAR 1
CONV 2 MIXED CO .7

BLOCK LTSHIFT RSTOIC

PARAM PRES=0 DUTY=0
STOIC 1 MIXED CO -1 / H2O -1 / H2 1 / CO2 1
CONV 1 MIXED CO .75

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BLOCK GASIFIER RYIELD

SUBROUTINE YIELD=BATYD
USER-VECS NREAL=6
REAL VALUE-LIST=1500.0 360.0 6.60 8.30 .04650 4.0
PARAM TEMP=1500.0 PRES=20
BLOCK-OPTION SIM-LEVEL=4

BLOCK OFFCOMB RGIBBS

PARAM PRES=0

BLOCK PRIMARY RGIBBS

PARAM TEMP=850 <C> PRES=0 TAPP=-20

BLOCK B3 PUMP

PARAM PRES=500

BLOCK B5 PUMP

PARAM PRES=530

BLOCK B7 PUMP

PARAM PRES=115

BLOCK B13 PUMP

PARAM PRES=115

BLOCK PUMP1 PUMP

PARAM PRES=180

BLOCK PUMP4 PUMP
PARAM PRES=115

BLOCK PUMP5 PUMP
PARAM PRES=115

BLOCK WATPUMP PUMP
PARAM PRES=363

BLOCK AIRCOMP1 COMPR
PARAM TYPE=POLYTROPIC PRES=20

BLOCK AIRCOMP2 COMPR
PARAM TYPE=POLYTROPIC PRES=19 TEMP=59

BLOCK OFFCOMPR MCOMPR
PARAM NSTAGE=4 TYPE=POLYTROPIC PRES=362.6
FEEDS OFFAIR1 1
PRODUCTS OFFAIR2 4
COOLER-SPECS 1 TEMP=180 / 2 TEMP=150 / 3 TEMP=150 / 4 &
TEMP=372.8

BLOCK SYNCOMPR MCOMPR
PARAM NSTAGE=4 TYPE=POLYTROPIC PRES=530
FEEDS TOCOMPR 1
PRODUCTS SYNCOMP 4 / 205 GLOBAL L
COOLER-SPECS 1 TEMP=190 / 2 TEMP=190 / 3 TEMP=190 / 4 &
TEMP=393.1852
BLOCK-OPTION FREE-WATER=YES

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BLOCK CHARDEC USER
DESCRIPTION "CHAR IS DECOMPOSED INTO ITS ELEMENTS"
SUBROUTINE USRDEC
BLOCK-OPTION SIM-LEVEL=4

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Design Specifications

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DESIGN-SPEC ADIABAT
DEFINE GAST INFO-VAR INFO=HEAT VARIABLE=DUTY STREAM=QGAS
SPEC "GAST" TO "0.D0"
TOL-SPEC "5."
VARY BLOCK-VAR BLOCK=GASIFIER VARIABLE=TEMP SENTENCE=PARAM
LIMITS "1200." "2000."

DESIGN-SPEC AIRTOFLU
DEFINE WOODT STREAM-VAR STREAM=DRYWOOD SUBSTREAM=MIXED &
VARIABLE=TEMP
SPEC "WOODT" TO "155"

TOL-SPEC "1.0"
VARY STREAM-VAR STREAM=DRYRAIR SUBSTREAM=MIXED &
VARIABLE=MASS-FLOW
LIMITS "12" "40"

DESIGN-SPEC RECYCLE

DEFINE H2FRAC MOLE-FRAC STREAM=TOPSAB SUBSTREAM=MIXED &
COMPONENT=H2
SPEC "H2FRAC" TO ".7"
TOL-SPEC ".01"
VARY BLOCK-VAR BLOCK=RECSPLT SENTENCE=FRAC VARIABLE=FRAC &
ID1=H2RECYCL
LIMITS ".1" ".5"

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DESIGN-SPEC SANDREC

DEFINE QNONE INFO-VAR INFO=HEAT VARIABLE=DUTY STREAM=QCOMB
SPEC "QNONE" TO "0.D0"
TOL-SPEC "10."
VARY STREAM-VAR STREAM=SANDSUPP SUBSTREAM=CISOLID &
VARIABLE=MASS-FLOW
LIMITS "0.01" "40."

DESIGN-SPEC STMGEN6

DEFINE STMT STREAM-VAR STREAM=STEAM5 SUBSTREAM=MIXED &
VARIABLE=TEMP
SPEC "STMT" TO "360"
TOL-SPEC "1"
VARY STREAM-VAR STREAM=BFW5 SUBSTREAM=MIXED &
VARIABLE=MASS-FLOW
LIMITS ".70" ".85"

DESIGN-SPEC STMGEN8

DEFINE STMT STREAM-VAR STREAM=STEAM6 SUBSTREAM=MIXED &
VARIABLE=TEMP
SPEC "STMT" TO "490"
TOL-SPEC "1"
VARY STREAM-VAR STREAM=BFW6 SUBSTREAM=MIXED &
VARIABLE=MASS-FLOW
LIMITS ".2" ".3"

FORTRAN COMBAIRT

DEFINE BLTEMP BLOCK-VAR BLOCK=AIRHEAT VARIABLE=TEMP &
SENTENCE=PARAM
DEFINE STRTEM STREAM-VAR STREAM=COMBAIR2 SUBSTREAM=MIXED &
VARIABLE=TEMP
F BLTEMP=STRTEM
EXECUTE AFTER BLOCK AIRCOMPI

;

FORTRAN GASTEMP

DEFINE TGAS BLOCK-VAR BLOCK=GASIFIER VARIABLE=TEMP &

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    SENTENCE=PARAM
    DEFINE TLIST BLOCK-VAR BLOCK=GASIFIER VARIABLE=VALUE-LIST &
        SENTENCE=REAL ELEMENT=1
F    TLIST = TGAS
F    WRITE(NHSTRY,*) 'WRITE: TLIST = ',TLIST
F    WRITE(NHSTRY,*) 'WRITE: TGAS = ',TGAS
    READ-VARS TGAS
    WRITE-VARS TLIST

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FORTRAN OFFAIR
    DEFINE H2 MOLE-FLOW STREAM=OFFGAS SUBSTREAM=MIXED &
        COMPONENT=H2
    DEFINE CO MOLE-FLOW STREAM=OFFGAS SUBSTREAM=MIXED &
        COMPONENT=CO
    DEFINE CH4 MOLE-FLOW STREAM=OFFGAS SUBSTREAM=MIXED &
        COMPONENT=CH4
    DEFINE C2H6 MOLE-FLOW STREAM=OFFGAS SUBSTREAM=MIXED &
        COMPONENT=C2H6
    DEFINE C2H4 MOLE-FLOW STREAM=OFFGAS SUBSTREAM=MIXED &
        COMPONENT=C2H4
    DEFINE C2H2 MOLE-FLOW STREAM=OFFGAS SUBSTREAM=MIXED &
        COMPONENT=C2H2
    DEFINE AIRFLO STREAM-VAR STREAM=OFFAIR1 SUBSTREAM=MIXED &
        VARIABLE=MOLE-FLOW
    DEFINE O2FRAC MOLE-FRAC STREAM=OFFAIR1 SUBSTREAM=MIXED &
        COMPONENT=O2
F    O2MOL=(.5*H2+.5*CO+2*CH4+3.5*C2H6+3*C2H4+2.5*C2H2)
F    AIRFLO=1.15*O2MOL/O2FRAC
    EXECUTE BEFORE BLOCK OFFCOMB

```

```

FORTRAN PRESDROP
    DEFINE P1 STREAM-VAR STREAM=SYNCOMP D SUBSTREAM=MIXED &
        VARIABLE=PRES
    DEFINE HTPRES BLOCK-VAR BLOCK=HTSHIFT VARIABLE=PRES &
        SENTENCE=PARAM
    DEFINE LTPRES BLOCK-VAR BLOCK=LTSHIFT VARIABLE=PRES &
        SENTENCE=PARAM
    DEFINE PRIMP BLOCK-VAR BLOCK=PRIMARY VARIABLE=PRES &
        SENTENCE=PARAM
F    PRIMP = 0.95 * P1
F    HTPRES = 0.85 * PRIMP
F    LTPRES = 0.85 * HTPRES
    EXECUTE AFTER BLOCK PRIMARY

```

```

FORTRAN REFSTM
    DEFINE STM MOLE-FLOW STREAM=REFSTMA SUBSTREAM=MIXED &
        COMPONENT=H2O
    DEFINE TAR MOLE-FLOW STREAM=TOREFHOT SUBSTREAM=MIXED &
        COMPONENT=TAR
    DEFINE CO MOLE-FLOW STREAM=TOREFHOT SUBSTREAM=MIXED &
        COMPONENT=CO
    DEFINE CH4 MOLE-FLOW STREAM=TOREFHOT SUBSTREAM=MIXED &
        COMPONENT=CH4
    DEFINE C2H6 MOLE-FLOW STREAM=TOREFHOT SUBSTREAM=MIXED &

```

```

    COMPONENT=C2H6
    DEFINE C2H4 MOLE-FLOW STREAM=TOREFHOT SUBSTREAM=MIXED &
        COMPONENT=C2H4
    DEFINE C2H2 MOLE-FLOW STREAM=TOREFHOT SUBSTREAM=MIXED &
        COMPONENT=C2H2
    DEFINE EXIST MOLE-FLOW STREAM=TOREFHOT SUBSTREAM=MIXED &
        COMPONENT=H2O
F   STM=3*(10*TAR+CO+1*CH4+2*C2H6+2*C2H4+2*C2H2)-EXIST
    EXECUTE BEFORE BLOCK PRIMARY

```

FORTRAN SETCSEP

```

    DEFINE TEMPIN STREAM-VAR STREAM=WOODGAS SUBSTREAM=MIXED &
        VARIABLE=TEMP
    DEFINE TSEP BLOCK-VAR BLOCK=CHARSEP VARIABLE=TEMP &
        SENTENCE=FLASH-SPECS ID1=CHAR
    DEFINE TSEPG BLOCK-VAR BLOCK=CHARSEP VARIABLE=TEMP &
        SENTENCE=FLASH-SPECS ID1=SYNGAS
F   TSEP = TEMPIN
F   TSEPG = TEMPIN
    READ-VARS TEMPIN
    WRITE-VARS TSEP TSEPG

```

;

FORTRAN STEAMAMT

```

    DEFINE STEAM MASS-FLOW STREAM=GASIFSTM SUBSTREAM=MIXED &
        COMPONENT=H2O
    DEFINE WOOD MASS-FLOW STREAM=WOOD SUBSTREAM=NC &
        COMPONENT=WOOD
F   STEAM = 0.4 * WOOD
    READ-VARS WOOD
    WRITE-VARS STEAM

```

FORTRAN WOODDRY

```

    DEFINE REALNC STREAM-VAR STREAM=WOOD SUBSTREAM=NC &
        VARIABLE=MASS-FLOW
    DEFINE REALMI STREAM-VAR STREAM=WOOD SUBSTREAM=MIXED &
        VARIABLE=MASS-FLOW
    DEFINE REALCI STREAM-VAR STREAM=WOOD SUBSTREAM=CISOLID &
        VARIABLE=MASS-FLOW
    DEFINE NEWNC STREAM-VAR STREAM=ARWOOD SUBSTREAM=NC &
        VARIABLE=MASS-FLOW
    DEFINE NEWMIX STREAM-VAR STREAM=ARWOOD SUBSTREAM=MIXED &
        VARIABLE=MASS-FLOW
    DEFINE NEWCI STREAM-VAR STREAM=ARWOOD SUBSTREAM=CISOLID &
        VARIABLE=MASS-FLOW
    DEFINE NEWH2O MASS-FLOW STREAM=ARWOOD SUBSTREAM=MIXED &
        COMPONENT=H2O
F   NEWNC = REALNC
F   NEWH2O = 0.78 * REALNC
F   NEWMIX = REALMI + NEWH2O
F   NEWCI = REALCI
    EXECUTE BEFORE BLOCK WOODSEP

```


;

FORTRAN XSAIR

DEFINE PCARB MOLE-FLOW STREAM=CHARCOMP SUBSTREAM=CISOLID &
COMPONENT=CARBON
DEFINE PHYDRO MOLE-FLOW STREAM=CHARCOMP SUBSTREAM=MIXED &
COMPONENT=H2
DEFINE PSULF MOLE-FLOW STREAM=CHARCOMP SUBSTREAM=CISOLID &
COMPONENT=SULFUR
DEFINE AIRFLO STREAM-VAR STREAM=COMBAIR SUBSTREAM=MIXED &
VARIABLE=MOLE-FLOW
DEFINE O2FRAC MOLE-FRAC STREAM=COMBAIR SUBSTREAM=MIXED &
COMPONENT=O2
F O2MOL = PCARB + 0.5*PHYDRO + PSULF
F AIRFLO = 1.2 * O2MOL / O2FRAC
READ-VARS PCARB PHYDRO PSULF O2FRAC
WRITE-VARS AIRFLO

CONV-OPTIONS

PARAM CHECKSEQ=NO

CONVERGENCE C-GASSTM WEGSTEIN

TEAR GASIFSTM

CONVERGENCE C-H2REC WEGSTEIN

TEAR H2RECYCL

CONVERGENCE C-SAND WEGSTEIN

TEAR SAND .0010

PARAM MAXIT=50 QMIN=-5.0

CONVERGENCE MIXTEAR WEGSTEIN

TEAR 207

CONVERGENCE C-AIRFLU SECANT

SPEC AIRTOFLU

;

CONVERGENCE C-QGAS SECANT

SPEC ADIABAT

CONVERGENCE C-SANDR SECANT

SPEC SANDREC

CONVERGENCE H2SPLT SECANT

SPEC RECYCLE

CONVERGENCE STMGEN6 SECANT

SPEC STMGEN6

CONVERGENCE STMGEN8 SECANT

SPEC STMGEN8

SEQUENCE S-1 STEAMAMT C-GASSTM C-SAND FEEDMIX C-QGAS GASTEMP &
GASIFIER (RETURN C-QGAS) SETCSEP CHARSEP CHARDEC XSAIR &
AIRCOMP1 COMBAIRT AIRHEAT C-SANDR CHARFURN &
(RETURN C-SANDR) COMBSPLT SANDSPLT (RETURN C-SAND) &
SYNCOOL1 MIXTEAR B1 B5 SYNCOMPR B2 (RETURN MIXTEAR) &
REFHTR REFSTM WATPUMP REFSTM PRESDROP PRIMARY GSTMGEN &
(RETURN C-GASSTM) C-AIRFLU AIRCOMP2 DRYRMIX WOODDRY &
WOODSEP DRY1 DRY2 DRYRSEP (RETURN C-AIRFLU) HTCOOL &
HTSHIFT STMGEN8 B3 LTCOOL (RETURN STMGEN8) LTSHIFT B7 &
PSACOO H2SPLT C-H2REC RECMIX PSA RECSPLT &
(RETURN C-H2REC) (RETURN H2SPLT) OFFAIR OFFCOMPR OFFCOMB &
COMBCOOL B13 STMGEN6 MODEL1 MODEL2 PUMP1 B4 B6 &
STMFLASH PUMP4 INTER2A PUMP5 INTER2B

STREAM-REPOR ZEROFLOW MOLEFLOW MASSFLOW MOLEFRAC MASSFRAC &
NOCOMP-ATTR

PROPERTY-REP NOPARAMS

REPORT-SCALE

DEFINE WOOD STREAM-VAR STREAM=WOOD SUBSTREAM=NC &
VARIABLE=MASS-FLOW
SCALE "WOOD" TO "1"

PROP-TABLE PT-1 PROPS

STREAM COMBAIR
VARY TEMP
RANGE LOWER=100.0 UPPER=2400.0 INCR=100.0
TABULATE "PROPERTIES TABLE FOR CONV. COMPS" PROPERTIES=PS-1

PROP-TABLE PT-2 PROPS

STREAM WOOD
VARY TEMP
RANGE LOWER=100.0 UPPER=2400.0 INCR=100.0
TABULATE "PROPS FOR NC COMPS" PROPERTIES=PS-2

Appendix A (cont'd): Gasifier Fortran Subroutine

C\$ #2 BY: MKMANN 6/08/94 MODIFIED TO MODEL THE BATTELLE GASIFIER
 C\$ #1 BY: KRCRAIG 5/21/93 NEW

C
 C-----

C **** NOTICE ****
 C-----

C
 C
 C
 C
 C
 C
 C

C THIS CODE IS PART OF THE SYSTEM DEVELOPED AT
 C NATIONAL RENEWABLE ENERGY LABORATORY, GOLDEN, COLORADO

C
 C
 C
 C
 C
 C
 C

C SUBROUTINE BATYD (SIN ,SOUT , NSUBS,IDXSUB,ITYPE,NINT,INT,NREAL,
 C 1 REAL,IDS,NPO,NBOPST,NIW,IW,NW,W)

C NAME OF MODULE: USRDEV

C MODULE TITLE: WOOD DEVOLATILIZATION AND PYROLYSIS

C PURPOSE: USER ROUTINE TO MODEL FIXED-BED GASIFICATION WOOD
 C DEVOLATILIZATION BASED ON THE ULTIMATE ANALYSIS OF
 C THE WOOD, TAR, OIL, NAPHTHA, PHENOL, AND CHAR.

C WRITTEN BY: K. R. CRAIG DATE WRITTEN: 5/21/93

C BASED ON NYLD ROUTINE WRITTEN BY M.I.T. FOR CONOCO STUDY (12/15/81)

C VARIABLES IN ARGUMENT LIST

VAR	I/O	TYPE	DIM	DESCRIPTION
SIN	I/O	R		INLET MATERIAL STREAM VECTOR
SOUT	O	R		OUTLET MATERIAL STREAM VECTOR
NSUBS	I	I		NUMBER OF SUBSTREAMS
IDXSUB	I	I	NSUBS	SUBSTREAM INDEX VECTOR
ITYPE	I	I	NSUBS	SUBSTREAM TYPE VECTOR
NINT	I	I		LENGTH OF INTEGER VECTOR
INT	I/O	I	NINT	INTEGER VECTOR
NREAL	I	I		LENGTH OF REAL VECTOR
REAL	I	R	NREAL	REAL ARRAY
REAL(1)	I	R		OUTLET TEMPERATURE
REAL(2)	I	R		OUTLET PRESSURE
IDS	I	I	2,NCC	ID VECTOR
NPO	I	I		NUMBER OF PHYSICAL PROPERTY OPTIONS
NBOPST	I	I	3,NPO	PHYSICAL PROPERTY OPTION SET POINTERS

C NIW I I LENGTH OF THE INTEGER WORK VECTOR
C IW I I NIW INTEGER WORK VECTOR
C NW I I LENGTH OF THE REAL WORK VECTOR
C W I R NW REAL WORK VECTOR

C
C

C IMPORTANT INTERNAL VARIABLES

C

C VAR TYPE DIM DESCRIPTION

C

C HYDCAR R 6 HYDROCARBON YIELD FROM DRY ASH-FREE WOOD

C

HYDCAR(1) = TAR

C

HYDCAR(2) = PHENOL

C

HYDCAR(3) = NAPHTHA

C

HYDCAR(4) = OIL

C

HYDCAR(5) = CHAR

C

HYDCAR(6) = C2H6

C

C SDIST R 3 DISTRIBUTION OF SULFUR COMPOUNDS (SUM=1.0)

C

SDIST(1) = H2S

C

SDIST(2) = COS

C

SDIST(3) = CS2

C

C RNDIST R 2 DISTRIBUTION OF NITROGEN COMPOUNDS (SUM=1.0)

C

RNDIST(1) = NH3

C

RNDIST(2) = N2

C

C IDX I 99 COMPONENT INDEX VECTOR

C

C X R 99 COMPONENT MOLAR FRACTION VECTOR

C

C L1 I POINTER TO MIXED SUBSTREAM

C

C L2 I POINTER TO CISOLID SUBSTREAM

C

C L3 I POINTER TO NC SUBSTREAM

C

C

C ERROR CONDITIONS:

C

C NUMBER LEVEL

C

C 860000 0

C

C IMPROPER STREAM STRUCTURE.

C

C STREAM STRUCTURE MUST BE MIXED + CISOLID + NC, IN THAT ORDER.

C

C 860001 1

C

C ULTIMATE ANALYSIS IS MISSING FOR ONE OR MORE OF THESE COMPONENTS:

C

C TAR, OIL, PHENOL, NAPHTHA, CHAR.

C

C 860002 2

C

C ULTANAL MUST NOT CONTAIN CHLORINE. MASS BALANCE WILL BE IN ERROR.

C

C

C SUBROUTINES CALLED:

C

C NAME - LOCATI (FUNCTION)

C

C DESC - INTEGER BEAD LOCATOR

C
 C NAME - LOCATS
 C DESC - STREAM BEAD LOCATOR
 C
 C NAME - APSCPY
 C DESC - STREAM COPIER
 C
 C NAME - UCONV1
 C DESC - CONVERTS VALUE TO SI UNITS
 C
 C NAME - NSQCC
 C DESC - FINDS SEQUENCE NUMBER OF A CONVENTIONAL COMPONENT
 C
 C NAME - NSQNCC
 C DESC - FINDS SEQUENCE NUMBER OF A NONCONVENTIONAL COMPONENT
 C
 C NAME - CPACK
 C DESC - CONVENTIONAL PHASES PACKING
 C
 C NAME - AVEMW (FUNCTION)
 C DESC - AVERAGE SUBSTREAM MOLECULAR WEIGHT
 C
 C NAME - TOTENT
 C DESC - TOTAL STREAM ENTHALPY
 C
 C NAME - FLASH
 C DESC - GENERAL PURPOSE FLASH INTERFACE ROUTINE
 C
 C NAME - MERRPT (FUNCTION)
 C DESC - ERROR MESSAGE CHECKING
 C
 C NAME - ERROR
 C DESC - ERROR HANDLING ROUTINE
 C

C USING THIS MODEL:

C WOOD, CHAR, TAR, OIL, PHENOL, AND NAPHTHA ARE EXPECTED TO HAVE
 C ULTIMATE ANALYSES. ANY CHLORINE IN THE ULTIMATE ANALYSES WILL
 C BE IGNORED, RESULTING IN A MASS BALANCE ERROR. TAR, OIL, PHENOL,
 C AND NAPHTHA SHOULD BE IN THE MIXED SUBSTREAM. THE ASSUMED STREAM
 C STRUCTURE IS MIXED + CISOLID + NC.

C *****
 C * *
 C * THE COMPONENTS LISTED BELOW ARE REQUIRED. *
 C * ALL OTHERS ARE CONSIDERED INERT. *
 C * *
 C * WOOD CO *
 C * ASH H2 *
 C * CHAR N2 *
 C * CARBON H2O *
 C * TAR H2S *

```

C *      OIL      CS2      *
C *      PHENOL   COS      *
C *      NAPHTHA  NH3      *
C *              C2H6      *
C *              *
C *****

```

C DECLARATIONS & COMMONS

```

C IMPLICIT REAL*8(A-H,O-Z)
C DIMENSION SIN(1), SOUT(1), IDXSUB(NSUBS), ITYPE(NSUBS),
1 INT(NINT), REAL(NREAL), NBOPST(3,NPO),
2 IW(NIW), W(NW), IDS(2,12)
C DIMENSION RETN(337),IRETN(6)
C DIMENSION IPROG(2)
C DIMENSION ITAR(2),IOIL(2),IPHNOL(2),INAPTH(2),ICHAR(2),IWOOD(2),
1 IH2S(2),INH3(2),ICARB(2),ICOS(2),ICO(2),IH2(2),
2 IN2(2),IC2H6(2),IASH(2),ICS2(2),IH2O(2),IC2H4(2),
3 IC6H6(2),IO2(2),ICH4(2),ICO2(2), IC2H2(2)
C DIMENSION IDX(99),X(99)
C DIMENSION XH2(3),XCO(3),XCO2(3),XCH4(3),XC2H2(3),XC2H4(3),
1 XC2H6(3),XC6H6(3),XCHAR(3),XTAR(2),XDGAS(3)
C COMMON /USER/ RMISS, IMISS, NGBAL, IPASS, IRESTR, ICONVG, LMSG,
1 LPMSG, KFLAG, NHSTRY, NRPT, NTRMNL
C COMMON /NCOMP/ NCC, NNCC
C DIMENSION B(1)
C EQUIVALENCE (IB(1), B(1))
C INTEGER XMW
C COMMON / IPOFF1 / IPOFF1(1)
C COMMON /RGLOB/ DUMMY1, RMIN
C INTEGER IDXCC
C COMMON / IPOFF8 / IPOFF8(1)
C INTEGER IDXNCC
C INTEGER IPROX
C COMMON / IPOFF2 / IPOFF2(1)
C INTEGER IULT
C COMMON /PLEX/ IB(1)

```

C DATA STATEMENTS

```

C DATA IPROG /4HBTY,4HD /
C DATA ITAR/4HTAR ,4H /,IOIL/4HOIL ,4H /,IPHNOL/4HPHEN,4HOL /
1,INAPTH/4HNAPH,4HTHA /,ICHAR /4HCHAR,4H /,IWOOD /4HWOOD,4H /
2,ICARB/4HCARB,4HON /,ICOS /4HCOS ,4H /,IH2S /4HH2S ,4H /
3,INH3 /4HNH3 ,4H /,ICO /4HCO ,4H /
4,IH2 /4HH2 ,4H /,IN2 /4HN2 ,4H /,IC2H6 /4HC2H6,4H /
5,IASH /4HASH ,4H /,ICS2 /4HCS2 ,4H /,IH2O /4HH2O ,4H /
6,IO2 /'O2 ' ; /,IC2H4 /'C2H4' ; /,IC6H6 /'C6H6' ; /
7,ICH4 /'CH4 ' ; /,IC2H2 /'C2H2' ; /
8,ICO2 /'CO2 ' ; /

```

```

C DATA XDGAS / 2.8993D+01, -4.3325D-02, 2.0966D-05 /
2, XCO / 133.46, -0.10290, 2.8792D-5 /

```

4, XCO2 / -9.5251, 0.037889, -1.4927D-5 /
6, XCH4/ -13.82, 0.044179, -1.6167D-5 /
8, XC2H4/ -38.258, 0.058435, -1.9868D-5 /
1, XC2H6/ 11.114, -0.011667, 3.064D-6 /
3, XH2 / 17.996, -0.026448, 1.8930D-5 /
9, XC2H2 / -4.3114, 5.4499D-3, -1.561D-6 /
5, XCHAR/ 0.75503, -3.0212D-4; -3.1178D-8 /
7, XTAR/ 0.045494, -1.9759D-5 /

C

C CHECK FOR REPORT PASS

C

C

C STATEMENT FUNCTIONS FOLLOW

C

XMW(I) = LMW + I

C

IDXCC(I) = LIDXC + I

IDXNCC(I) = LIDXN + I

IPROX(I) = LPRXA + I

IULT(I) = LULTA + I

C

C SET PLEX OFFSETS

C

LMW = IPOFF1(306)

LIDXC = IPOFF8(4)

LIDXN = IPOFF8(5)

LPRXA = IPOFF2(10)

LULTA = IPOFF2(12)

IF (IPASS.EQ.4) RETURN

C

C INITIALIZE VARIABLES AND POINTERS

C

IULTTR = 0

IULTOI = 0

IULTPH = 0

IULTNA = 0

IULTCH = 0

IPRXWD = 0

IPRXCH = 0

IULTWD = 0

C

C COPY INLET STREAM INTO OUTLET STREAM

C

C LOCATE BLOCK BEAD

LPROC = LOCATI(2)

LBSMB = LOCATI(IB(LPROC+3))

LBLK = IB(LBSMB+5)

C LOCATE STREAM BEADS

NBSIN = IB(LBLK + IB(LBLK+17))

NBSOUT = IB(LBLK + IB(LBLK+19))

CALL LOCATS(NBSIN,LV11,LVR1,LD,NBD)

CALL LOCATS(NBSOUT,LV12,LVR2,LD,NBD)

C COPY THE STREAM

CALL APSCPY(LD,LVR1,LVR2)

C

```

C CHECK FOR IMPROPER STREAM STRUCTURE
C
  IF (NSUBS.NE.3) GOTO 820
  IF (ITYPE(1).NE.1 .OR. ITYPE(2).NE.2 .OR. ITYPE(3).NE.3) GOTO 820
C
C SET OUTLET TEMPERATURE AND PRESSURE (IN SI UNITS)
C
  TOUTF= REAL(1)
  TOUT = REAL(1)
  POUT = REAL(2)
  CALL UCONV1(22,TOUT)
  CALL UCONV1(20,POUT)
  IF (POUT.LE.0.0) POUT=SIN(NNCC+3)+POUT
C
C FIND COMPONENT INDEX NUMBERS
C
  CALL NSQCC(ITAR,NTAR)
C   CALL NSQCC(IOIL,NOIL)
C   CALL NSQCC(IPHNOL,NPHNOL)
C   CALL NSQCC(INAPTH,NNAPTH)
  CALL NSQCC(ICARBN,NCARBN)
C   CALL NSQCC(ICOS,NCOS)
C   CALL NSQCC(ICS2,NCS2)
  CALL NSQCC(IH2S,NH2S)
  CALL NSQCC(IH2O,NH2O)
  CALL NSQCC(INH3,NNH3)
  CALL NSQCC(ICO,NCO)
  CALL NSQCC(ICO2,NCO2)
  CALL NSQCC(IH2,NH2)
  CALL NSQCC(IN2,NN2)
  CALL NSQCC(IO2,NO2)
  CALL NSQCC(IC2H6,NC2H6)
  CALL NSQCC(IC2H4,NC2H4)
  CALL NSQCC(IC2H2,NC2H2)
  CALL NSQCC(IC6H6,NC6H6)
  CALL NSQCC(ICH4,NCH4)
  CALL NSQCC(IWOOD,NWOOD)
  CALL NSQCC(IASH,NASH)
  CALL NSQCC(ICHAR,NCHAR)
C
C ATOMIC (NOT MOLECULAR) WEIGHTS FOR CARBON, HYDROGEN, NITROGEN,
C SULFUR, AND OXYGEN.
C
  CAW = B(XMW(NCARBN))
  HAW = B(XMW(NH2))/2
  RNAW = B(XMW(NN2))/2
  SAW = 32.064
  OAW = 16.0
C
C FIND OUT WHERE ATTRIBUTES ARE STORED FOR ATTRIBUTED COMPONENTS.
C
  DO 150 I=1,NSUBS
    ILOC = ITYPE(I)
    NCT = NCC

```



```

      IF (ILOC .EQ. 3) NCT = NNCC
      IATLST = IDXSUB(I) + NCT + 8
      GOTO (120,130,140), ILOC
120  CONTINUE
      L1 = IDXSUB(I) - 1
C     IULTTR = IATLST + IULT(IDXCC(NTAR))
C     IULTOI = IATLST + IULT(IDXCC(NOIL))
C     IULTPH = IATLST + IULT(IDXCC(NPHNOL))
C     IULTNA = IATLST + IULT(IDXCC(NNAPTH))
      GOTO 150
130  CONTINUE
      L2 = IDXSUB(I) - 1
      GOTO 150
140  CONTINUE
      L3 = IDXSUB(I) - 1
      IULTCH = IATLST + IB(IULT(IB(IDXNCC(NCHAR))))
      IPRXWD = IATLST + IB(IPROX(IB(IDXNCC(NWOOD))))
      IPRXCH = IATLST + IB(IPROX(IB(IDXNCC(NCHAR))))
      IULTWD = IATLST + IB(IULT(IB(IDXNCC(NWOOD))))
      TOTAL = SIN(L3 + NWOOD)
150  CONTINUE
C
C     CHKSUM = IULTTR + IULTOI + IULTPH + IULTNA + IULTCH
      CHKSUM = IULTCH
      IF (CHKSUM.LT.RMISS) GOTO 170
      ISEV=1
      IF (MERRPT(IPROG,IDS,ISEV,8600001,LMSG,KFLAG).NE.0)
        & WRITE(NHSTRY,160)
160  FORMAT(6X,'ULTIMATE ANALYSIS IS MISSING FOR ONE OR MORE OF '
        & 'THESE COMPONENTS:'/9XTAR, OIL, PHENOL, NAPHTHA, CHAR.)
C     CALL ERRSP(ISEV,3)
170  CONTINUE
C
C     CHKSUM = SIN(IULTTR+5) + SIN(IULTOI+5) + SIN(IULTPH+5)
C     & + SIN(IULTNA+5) + SIN(IULTCH+5)
      CHKSUM = SIN(IULTCH+5)
      IF (CHKSUM.LT.RMIN) GOTO 190
      ISEV=2
      IF (MERRPT(IPROG,IDS,ISEV,8600002,LMSG,KFLAG).NE.0)
        & WRITE(NHSTRY,180)
180  FORMAT(6X,'ULTANAL MUST NOT CONTAIN CHLORINE. MASS BALANCE '
        & 'WILL BE IN ERROR.')
C     CALL ERRSP(ISEV,3)
190  CONTINUE
C
C GET MOISTURE CONTENT OF WOOD. GET DRY WEIGHT OF WOOD.
C
      WATER = SIN(IPRXWD+1)*TOTAL/100.
      BDW = TOTAL - WATER
      H2O = WATER / B(XMW(NH2O))
      TMULT = BDW/100.
      write(nhstry,992) total,water,(sin(iultwd+i),i=1,7),caw,haw,
        & rnaw,saw,oaw
992 format(/,' wood flow=',g12.5, ' moisture=',g12.5,

```

```

1      ' ash %=' ,g12.5/, ' carb%=' ,g12.5,
2      ' hyd%=' ,g12.5, ' nitr%=' , g12.5,
3      /, ' cl%=' ,g12.5, ' sulf%=' ,g12.5,
4      ' oxygen%=' ,g12.5/, ' caw=' ,g12.5,
5      ' haw=' ,g12.5, ' rnaw=' ,g12.5,
6      /, ' saw=' ,g12.5, ' oaw=' ,g12.5/)

```

C

C GET INDIVIDUAL ELEMENT TOTAL FLOWS

C

SANDIN = SIN(L2+NO2SI)

C

SANDOUT = SOUT(L2+NO2SI)

C

SANDDIF = SANDOUT-SANDIN

TASH = SIN(IULTWD+1) * TMULT

TCARB = SIN(IULTWD+2) * TMULT / CAW

THYD = SIN(IULTWD+3) * TMULT / HAW

TRNIT = SIN(IULTWD+4) * TMULT / RNAW

TSULF = SIN(IULTWD+6) * TMULT / SAW

TOXY = SIN(IULTWD+7) * TMULT / OAW

WRITE(NHSTRY,999) TASH,TCARB,THYD,TRNIT,TSULF,TOXY

999 FORMAT(/, ' WRITE: WOOD ELEMENTS',/

1 ' MOLES OF ATOMS',/ ' ASH ',G12.5, ' CARBON ',G12.5,

2 ' HYDROGEN ',G12.5/, ' NITROGEN ',G12.5, ' SULFUR ',

3 G12.5, ' OXYGEN ',G12.5)

C

C YIELD OF HYDROCARBONS BASED ON A MOISTURE AND ASH FREE BASIS

C DGAS AND GAS COMPONENTS IN SCF (59 F, 1 ATM)

C CHAR AND TAR IN LB

ZMAF = BDW - TASH

C

ZMAF = MOISTURE AND ASH FREE WOOD (KG/SEC)

WRITE(NHSTRY,*) ZMAF = 'ZMAF

ZLBMAF = ZMAF*2.20462*3600

C

ZLBMAF = MOISTURE AND ASH FREE WOOD (LB/HR)

WRITE(NHSTRY,*) ZLBMAF = 'ZLBMAF

ZLBBDW = BDW * 2.20462 *3600

WRITE(NHSTRY,*) ZLBBDW = 'ZLBBDW

T2 = TOUTF**2

T1 = TOUTF

WRITE(NHSTRY,*) TOUT = 'TOUT

WRITE(NHSTRY,*) T1 = 'T1

WRITE(NHSTRY,*) T2 = 'T2

DGAS = (XDGAS(1) + T1*XDGAS(2) + T2*XDGAS(3)) * ZLBMAF

WRITE(NHSTRY,*) 'DGAS IN SCF = 'DGAS

WRITE(NHSTRY,*) 'MAF IN LB = 'ZLBMAF

H2 = (XH2(1) + T1*XH2(2) + T2*XH2(3)) * DGAS/100

write(nhstry,*) ' WRITE: bdw= 'bdw,' h2= 'h2,' DGAS= 'DGAS

CO = (XCO(1) + T1*XCO(2) + T2*XCO(3)) * DGAS/100

write(nhstry,*) ' WRITE: CO(scf)='CO

CO2 = (XCO2(1) + T1*XCO2(2) + T2*XCO2(3)) * DGAS/100

write(nhstry,*) ' WRITE: CO2(scf)='CO2

CH4 = (XCH4(1) + T1*XCH4(2) + T2*XCH4(3)) * DGAS/100

write(nhstry,*) ' WRITE: CH4(scf)='CH4

C2H2 = (XC2H2(1) + T1*XC2H2(2) + T2*XC2H2(3)) * DGAS/100

write(nhstry,*) ' WRITE: C2H2(scf)='C2H2

```

C2H4 = (XC2H4(1) + T1*XC2H4(2) + T2*XC2H4(3)) * DGAS/100
write(nhstry,*) ' WRITE: C2H4(scf)=',C2H4
C2H6 = (XC2H6(1) + T1*XC2H6(2) + T2*XC2H6(3)) * DGAS/100
write(nhstry,*) ' WRITE: C2H6(scf)=',C2H6
CHAR = (XCHAR(1) + T1*XCHAR(2) + T2*XCHAR(3)) * ZLBBDW
WRITE(NHSTRY,*) 'WRITE: CHAR (LB) = ',CHAR
TAR = (XTAR(1) + T1*XTAR(2)) * ZLBBDW
write(nhstry,*) ' WRITE: TAR(LB)=',TAR

```

C CONVERT PRODUCT GAS FLOWS IN SCF AND TAR AND CHAR IN LB TO MOLAR BASI

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H2MOL = H2 / 379.4630 / 2.20462 / 3600
write(nhstry,*) ' WRITE: mwh2= ',B(xmw(nh2)), ' h2mol= ',h2mol
COMOL = CO / 379.4630 / 2.20462 / 3600
write(nhstry,*) ' WRITE: mwCO= ',B(xmw(nCO)), ' COMol= ',COMol
CO2MOL = CO2 / 379.4630 / 2.20462 / 3600
write(nhstry,*) ' WRITE: mwCO2 = ',B(xmw(nCO2)), ' CO2mol= ',CO2mol
CH4MOL = CH4 / 379.4630 / 2.20462 / 3600
write(nhstry,*) ' WRITE: mwCH4 = ',B(xmw(nCH4)), ' CH4mol= ',CH4mol
C2H2MOL = C2H2 / 379.4630 / 2.20462 / 3600
C2H4MOL = C2H4 / 379.4630 / 2.20462 / 3600
C2H6MOL = C2H6 / 379.4630 / 2.20462 / 3600
C   C6H6MOL = C6H6 / 379.4630 / 2.20462 / 3600
TARMOL = TAR/B(XMW(NTAR)) / 2.20462 / 3600
write(nhstry,*) ' WRITE: mwTAR = ',B(xmw(nTAR)), ' TARMol= ',TARMol
if (h2mol .lt. 0.d0) h2mol = 0.d0
if (h2mol .lt. 0.d0) WRITE(NHSTRY,*) ' WRITE: H2MOL = 0 (407)'
if (comol .lt. 0.d0) comol = 0.d0
if (comol .lt. 0.d0) WRITE(NHSTRY,*) ' WRITE: COMOL = 0 (409) '
if (co2mol .lt. 0.d0) co2mol = 0.d0
if (co2mol .lt. 0.d0) WRITE(NHSTRY,*) ' WRITE: CO2MOL = 0 (411) '
if (ch4mol .lt. 0.d0) ch4mol = 0.d0
if (ch4mol .lt. 0.d0) WRITE(NHSTRY,*) 'WRITE: CH4MOL = 0 (413) '
if (c2h4mol .lt. 0.d0) c2h4mol = 0.d0
if (c2h4mol .lt. 0.d0) WRITE(NHSTRY,*) 'WRITE: CH24MOL = 0 (415) '
if (c2h2mol .lt. 0.d0) c2h2mol = 0.d0
if (c2h2mol .lt. 0.d0) WRITE(NHSTRY,*) 'WRITE: C2H2MOL = 0 (415) '
if (c2h6mol .lt. 0.d0) c2h6mol = 0.d0
if (c2h6mol .lt. 0.d0) WRITE(NHSTRY,*) 'WRITE: C2H6MOL = 0 (417) '
C   if (c6h6mol .lt. 0.d0) c6h6mol = 0.d0
C   if (c6h6mol .lt. 0.d0) WRITE(NHSTRY,*) 'WRITE: C6H6MOL = 0 (419) '
if (TARMol .lt. 0.d0) TARMol = 0.d0
if (TARMol .lt. 0.d0) WRITE(NHSTRY,*) 'WRITE: TARMOL = 0 (421) '
WRITE(NHSTRY,998)H2MOL,COMOL,CO2MOL,CH4MOL,C2H4MOL,
1      C2H6MOL,TARMOL
998 FORMAT(/,' GASIF. PRODUCTS',/
1      ' MOLES ',/ H2 ',G12.5,' CO ',G12.5,
2      ' CO2 ',G12.5,/, ' CH4 ',G12.5,' C2H4 ',
3      G12.5,' C2H6 ',G12.5,G12.5,/,
4      ' TAR ',G12.5)
C
C
C DETERMINE THE AMOUNT OF STEAM FED TO GASIFIER
STM = SIN(L1 + NH2O)

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```

WRITE(NHSTRY,*) 'STEAM FED TO GASIFIER = ', STM
C
C CALCULATE THE TOTAL AMOUNT OF WATER IN GASIFIER
H2OTOT = H2O + STM
C
C
C *** CARBON BALANCE ***
C
GCARB = COMOL + CO2MOL + CH4MOL + 2.D0*(C2H4MOL+C2H6MOL) +
&      10.D0*TARMOL + 2.D0*(C2H2MOL)
CCARB = TCARB - GCARB
WRITE(NHSTRY,996) TCARB,GCARB,CCARB
996 FORMAT(/, ' TOTAL CARBON= ',G12.5,/, ' GASEOUS CARBON= ',G12.5,
&      /, ' CHAR CARBON= ',G12.5)
IF ( CCARB LE. 0.D0) THEN
  CFACT = TCARB/GCARB
  CCARB = 0.D0
  ISEV=3
  IF (MERRPT(IPROG,IDS,ISEV,8600001,LMSG,KFLAG).NE.0)
& WRITE(NHSTRY,162) CFACT
162 FORMAT(6X,'PREDICTED GASEOUS CARBON YIELD EXCEEDS CARBON
& AVAILABLE ',/,
& 6X,' GASEOUS CARBON COMPOUND YIELD ADJUSTED BY A FACTOR OF ',
& G12.5,' AND CHAR CARBON SET TO ZERO')
C CALL ERRSP(ISEV,3)
163 COMOL = CFACT * COMOL
CO2MOL = CFACT * CO2MOL
CH4MOL = CFACT * CH4MOL
C2H4MOL = CFACT * C2H4MOL
C2H6MOL = CFACT * C2H6MOL
C C6H6MOL = CFACT * C6H6MOL
TARMOL = CFACT * TARMOL
END IF
C
C *** OXYGEN BALANCE ***
C
C write(nhstry,*) ' oxy1 = ',oxy
OAVAIL = 2.D0*SIN(L1 + NO2) + TOXY + H2OTOT
C REAL(6) IS MOL% OF O IN WOOD RETAINED IN CHAR
COXY = TOXY * (REAL(6)/100.D0)
OREQD = COMOL + 2.D0*CO2MOL + COXY
WRITE(NHSTRY,993) COMOL,CO2MOL,COXY,OAVAIL,OREQD
993 FORMAT(/, ' COMOL = ',G12.5, ' CO2MOL = ',G12.5, ' COXY = ',G12.5,
&      /, ' OAVAIL = ',G12.5, ' OREQD = ',G12.5,/)
IF (OREQD .GT. TOXY) THEN
  STMDEC = (OREQD - TOXY)
  H2OTOT = H2OTOT - STMDEC
  IF (H2OTOT LT. 0) THEN
    WRITE(NHSTRY,*) 'NEED MORE STEAM '
  ENDIF
  WRITE (NHSTRY,994) STMDEC
994 FORMAT(/, ' STEAM DECOMPOSITION = ',G12.5, ' MOLES',/)
  OXY = 0
  ELSE IF (OREQD LT. TOXY) THEN

```

```

C   write(nhstry,*) ' oxy2 = ',oxy
      OXY = TOXY - OREQD
C   write(nhstry,*) ' oxy3 = ',oxy
      ELSE
        WRITE(NHSTRY,*) 'OXYGEN BALANCE ALL MESSSED UP '
      ENDIF
      IF (OXY .GT. 0) THEN
        WRITE(NHSTRY,*) 'MOLES OF ADDITIONAL OXYGEN (O) TO CHAR = ',OXY
        COXY = COXY + OXY
        OXY = 0
      ENDIF
C
C
C *** HYDROGEN BALANCE ***
C
      AMMOL = TRNIT * (1.D0 - REAL(3)/100.D0)
      CNIT = TRNIT * (REAL(3)/100.D0)
      H2SMOL = TSULF * ( 1.D0 - REAL(4)/100.D0 )
      CSULF = TSULF * (REAL(4)/100.D0)
C
C REAL(5) IS H/C MASS RATIO IN CHAR
C
      CHRHYD = ( CCARB*CAW * REAL(5) ) / HAW

      GASHYD = 2.D0*H2MOL + 4.D0*CH4MOL + 6.D0*(C2H6MOL) +
&      3*AMMOL + 2*H2SMOL + 8*TARMOL + 4*C2H4MOL + 2*C2H2MOL
      HREQD = GASHYD + CHRHYD
      HAVAIL = THYD + STMDEC*2.D0
      WRITE(NHSTRY,995)AMMOL,H2SMOL,GASHYD,CHRHYD,HAVAIL,HREQD
995 FORMAT(/,' MOLES',/, ' NH3 ',G12.5,' H2S ',G12.5,
&      ' GASEOUS HYDROGEN',G12.5,/, ' CHAR HYDROGEN ',G12.5,
&      ' AVAIL. HYDROGEN',G12.5,
&      ' REQ. HYDROGEN',G12.5)
      IF (HREQD .GT. HAVAIL) THEN
        WRITE(NHSTRY,*) ' ERROR: NOT ENOUGH HYDROGEN AVAILABLE'
        ISEV=1
        IF (MERRPT(IPROG,IDS,ISEV,8600001,LMSG,KFLAG).NE.0)
& WRITE(NHSTRY,164)
164  FORMAT(6X,'PREDICTED HYDROGEN YIELD EXCEEDS HYDROGEN AVAILABLE '
&      ',/6X,' STEAM TO WOOD RATIO SHOULD BE INCREASED ')
C      CALL ERRSP(ISEV,3)
      ELSE IF (HREQD .GT. THYD) THEN
        WRITE (NHSTRY,950) STMDEC
950  FORMAT(/,' NOTE: H2 BALANCE NEEDED ',G12.5, ' MOLES OF STEAM',/)
      END IF
C
C
C FILL IN OUTLET FLOWS
C
      DO 250 I=1,NSUBS
        GOTO (200,210,220), ITYPE(I)
C
C MIXED SUBSTREAM
C

```

200 CONTINUE

SOUT(L1 + NO2) = OXY/2.D0

C write(nhstry,*) 'oxy/2.0 = ',sout(l1 + no2)

SOUT(L1 + NCO) = SOUT(L1 + NCO) + COMOL

WRITE(NHSTRY,*) 'COMOLS OUT = ',SOUT(L1+NCO)

SOUT(L1 + NCO2) = SOUT(L1 + NCO2) + CO2MOL

SOUT(L1 + NH2) = SOUT(L1 + NH2) + H2MOL + STMDEC

C SOUT(L1 + NN2) = SOUT(L1 + NN2) + RN2

SOUT(L1 + NH2O) = H2OTOT

SOUT(L1 + NH2S) = SOUT(L1 + NH2S) + H2SMOL

SOUT(L1 + NNH3) = SOUT(L1 + NNH3) + AMMOL

SOUT(L1 + NTAR) = SOUT(L1 + NTAR) + TARMOL

SOUT(L1 + NC2H2) = SOUT(L1 + NC2H2) + C2H2MOL

SOUT(L1 + NC2H6) = SOUT(L1 + NC2H6) + C2H6MOL

SOUT(L1 + NC2H4) = SOUT(L1 + NC2H4) + C2H4MOL

C SOUT(L1 + NC6H6) = SOUT(L1 + NC6H6) + C6H6MOL

SOUT(L1 + NCH4) = SOUT(L1 + NCH4) + CH4MOL

C

C FILL IN TOTAL FLOW AND AVERAGE MOLECULAR WEIGHT

C

CALL CPACK(SOUT(IDXSUB(1)),NCP,IDX,X,FLOW)

SOUT(L1+NCC+1)=FLOW

SOUT(L1+NCC+9)=AVEMW(NCP,IDX,X)

GOTO 250

C

C CISOLID SUBSTREAM

C

210 CONTINUE

DO J=1 ,NCC

SOUT(L2 + J) = SIN(L2 + J)

ENDDO

CALL CPACK(SOUT(IDXSUB(2)),NCP,IDX,X,FLOW)

SOUT(L2+NCC+1)=FLOW

SOUT(L2+NCC+9)=AVEMW(NCP,IDX,X)

GOTO 250

C

C NC SUBSTREAM

C

220 CONTINUE

C

C CALCULATE CHAR FLOW AND ULTIMATE ANALYSIS

C

CHAR = TASH+CCARB*CAW+CHRHYD*HAW+COXY*OAW+CNIT*RNAW+CSULF*SAW

SOUT(IULTCH+1) = TASH / CHAR * 100.D0

WRITE(NHSTRY,*) 'CHAR ASH = ',SOUT(IULTCH+1)

SOUT(IULTCH+2) = CCARB*CAW / CHAR * 100.D0

WRITE(NHSTRY,*) 'CHAR CARBON = ',SOUT(IULTCH+2)

SOUT(IULTCH+3) = CHRHYD*HAW / CHAR * 100.D0

WRITE(NHSTRY,*) 'CHAR HYDROGEN = ',SOUT(IULTCH+3)

SOUT(IULTCH+4) = CNIT*RNAW / CHAR * 100.D0

WRITE(NHSTRY,*) 'CHAR NITROGEN = ',SOUT(IULTCH+4)

SOUT(IULTCH+6) = CSULF*SAW / CHAR * 100.D0

WRITE(NHSTRY,*) 'CHAR SULFUR = ',SOUT(IULTCH+6)

SOUT(IULTCH+7) = COXY*OAW / CHAR * 100.D0

```

WRITE(NHSTRY,*) 'CHAR OXYGEN = ',SOUT(IULTCH+7)
C
SOUT(L3 + NWOOD) = 1.D-10
SOUT(L3 + NASH) = 1.D-10
SOUT(L3 + NCHAR) = SOUT(L3 + NCHAR) + CHAR
TOTNC = 0.D0
DO 230 J=1,NNCC
    TOTNC = TOTNC + SOUT(L3+J)
230 CONTINUE
    SOUT(L3+NNCC+1) = TOTNC
250 CONTINUE
C
C
C ADD UP INLET ENTHALPY
C
    CALL TOTENT(SIN,NSUBS,IDXSUB,ITYPE,ENTHIN)
C
C FIND OUTLET STREAM ENTHALPY (TP FLASH)
C
C    GUESS=1.0
C    if (SOUT(1) .lt. 0.d0) SOUT(1) = 0.d0
C    WRITE(NHSTRY,*) ' SOUT(O2)= ',SOUT(L1+NO2)
C    WRITE(NHSTRY,*) 'SOUT AND POUT WRITES'
C    DO J=1,NCC
C        WRITE(NHSTRY,*) SOUT(J)
C    ENDDO
C    WRITE(NHSTRY,*) POUT
C    CALL FLASH(SOUT,NSUBS,IDXSUB,ITYPE,NBOPST,2,2,1,30,1.D-4,
&    TOUT,POUT,GUESS,LMSG,LPMSG,IRESSTR,2,RETN,IRETN,LCFLAG)
    CALL TOTENT(SOUT,NSUBS,IDXSUB,ITYPE,ENTOUT)
C
C CALCULATE DUTY AND RETURN
C
    Q = ENTHIN-ENTOUT
    IF (LMSG.GE.4) WRITE(NHSTRY,300) ENTHIN,ENTOUT,Q
300 FORMAT(6X,'HIN =',E13.5,' HOUT =',E13.5,' Q =',E13.5)
    RETURN
C
C TERMINAL ERROR SECTION -----
C
820 ISEV=0
    IF (MERRPT(IPROG,IDS,ISEV,8600000,LMSG,KFLAG).EQ.0) GOTO 840
    WRITE(NHSTRY,825)
825 FORMAT(6X,'IMPROPER STREAM STRUCTURE.',/6X,'STREAM STRUCTURE ',
1 'MUST BE MIXED + CISOLID + NC, IN THAT ORDER.')
C 830 CALL ERRSP(ISEV,3)
840 RETURN
    END

```