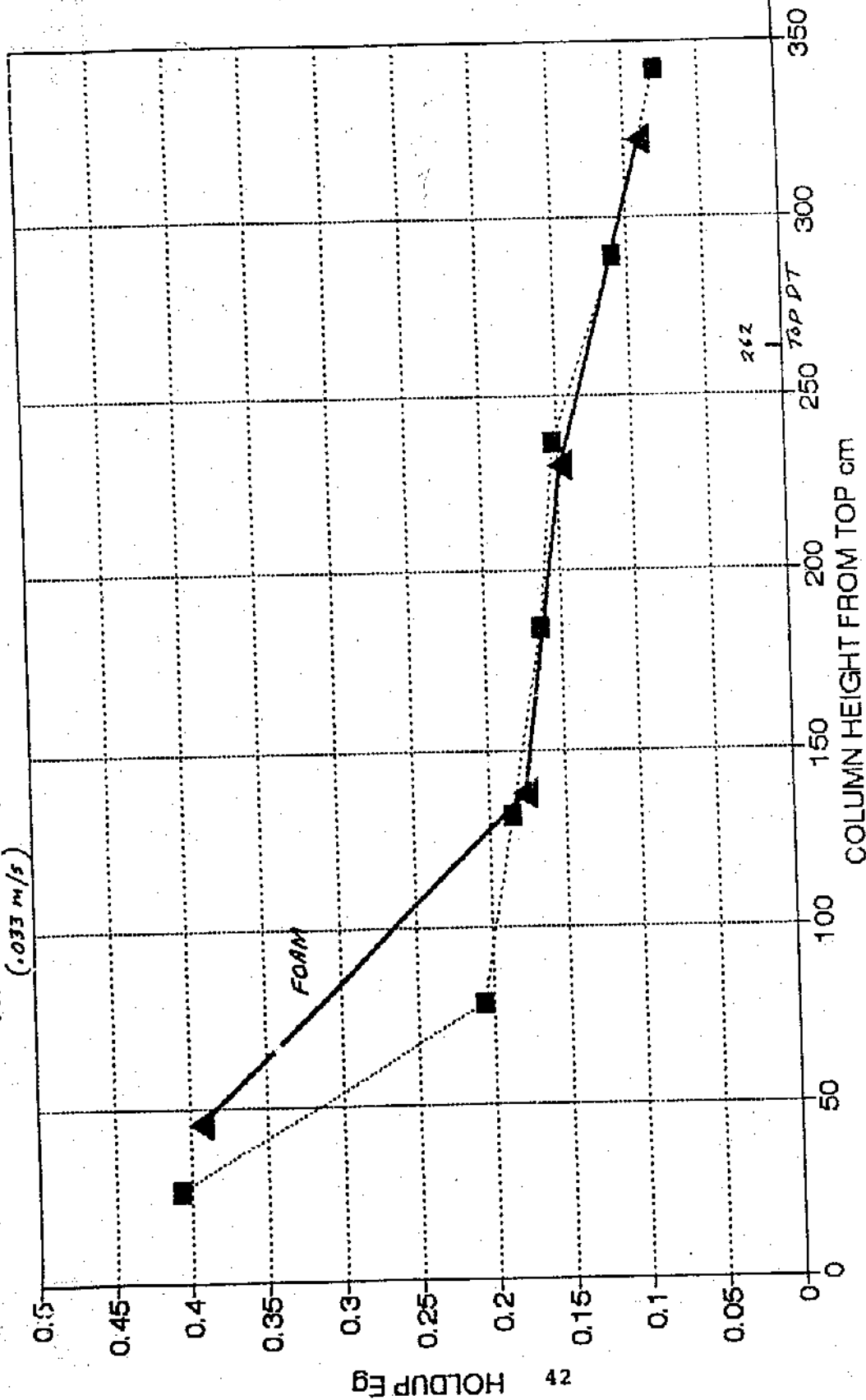


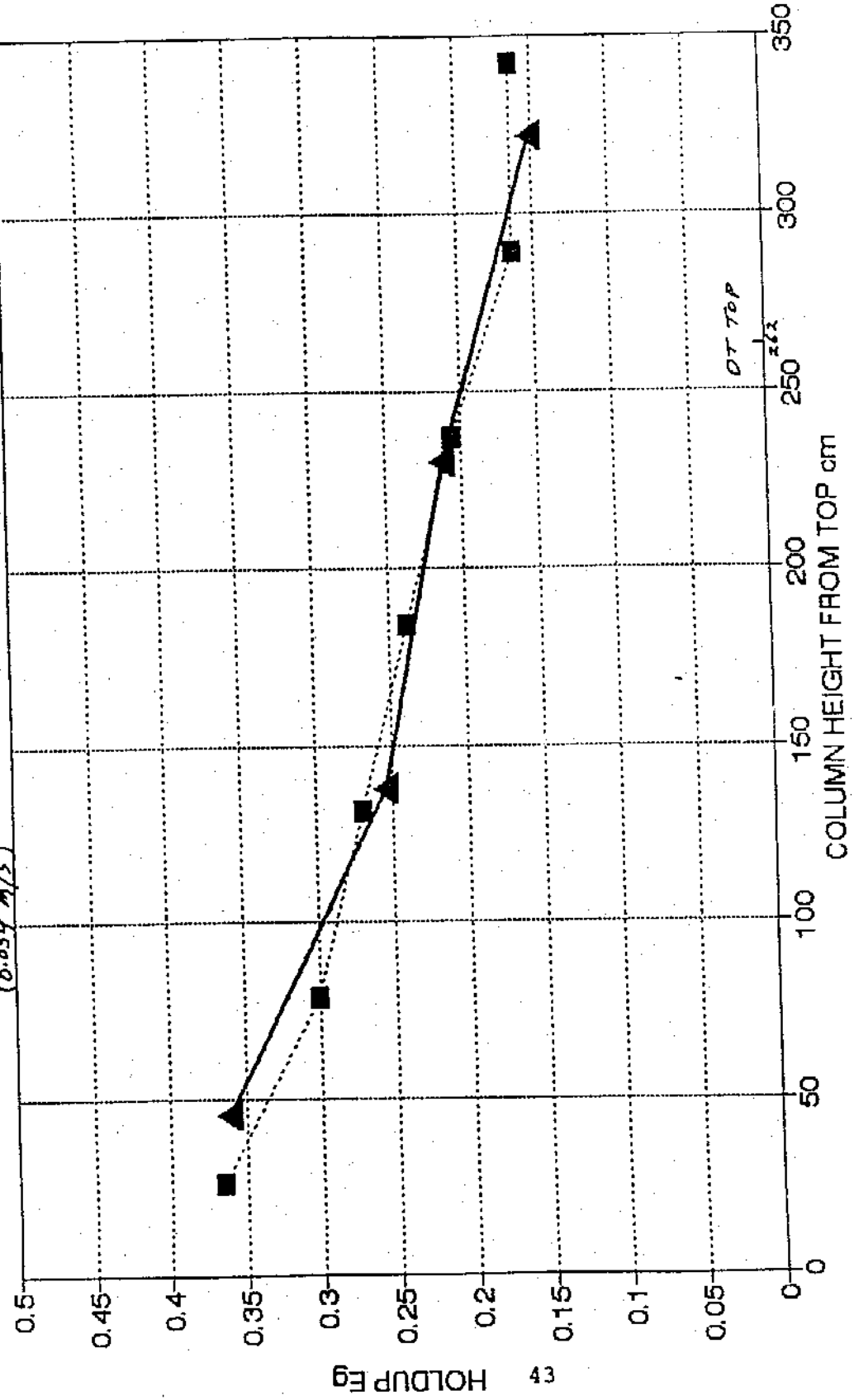
GAS HOLDUP IN .RSOL RUN#10  
 AT 5 SCFM AIR, PROBE INSIDE DRAFT TUBE  
 (.033 m/s)



▲ PROBE      ■ MANOMETER

GAS HOLDUP IN VOLSOL RUN#11  
8.8 SCFM AIR, PROBE INSIDE DRAFT TUBE  
(0.059 m/s)

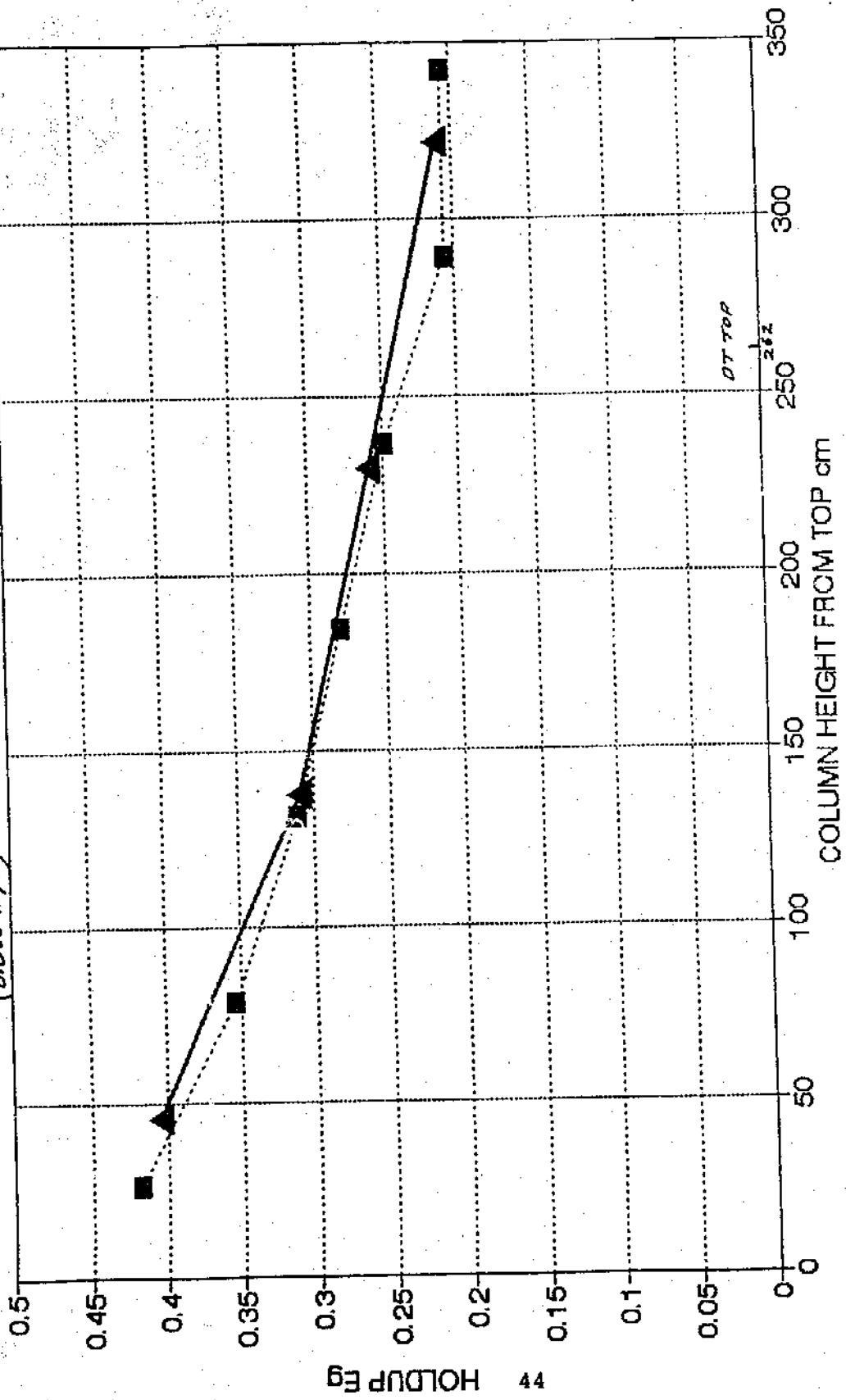
Not re-calibrated



▲ PROBE    ■ MANOMETER

GAS HOLDUP IN VAPORISOL RUN#12  
12 SCFM AIR, PROBE INSIDE DRAFT TUBE  
(0.080 m/s)

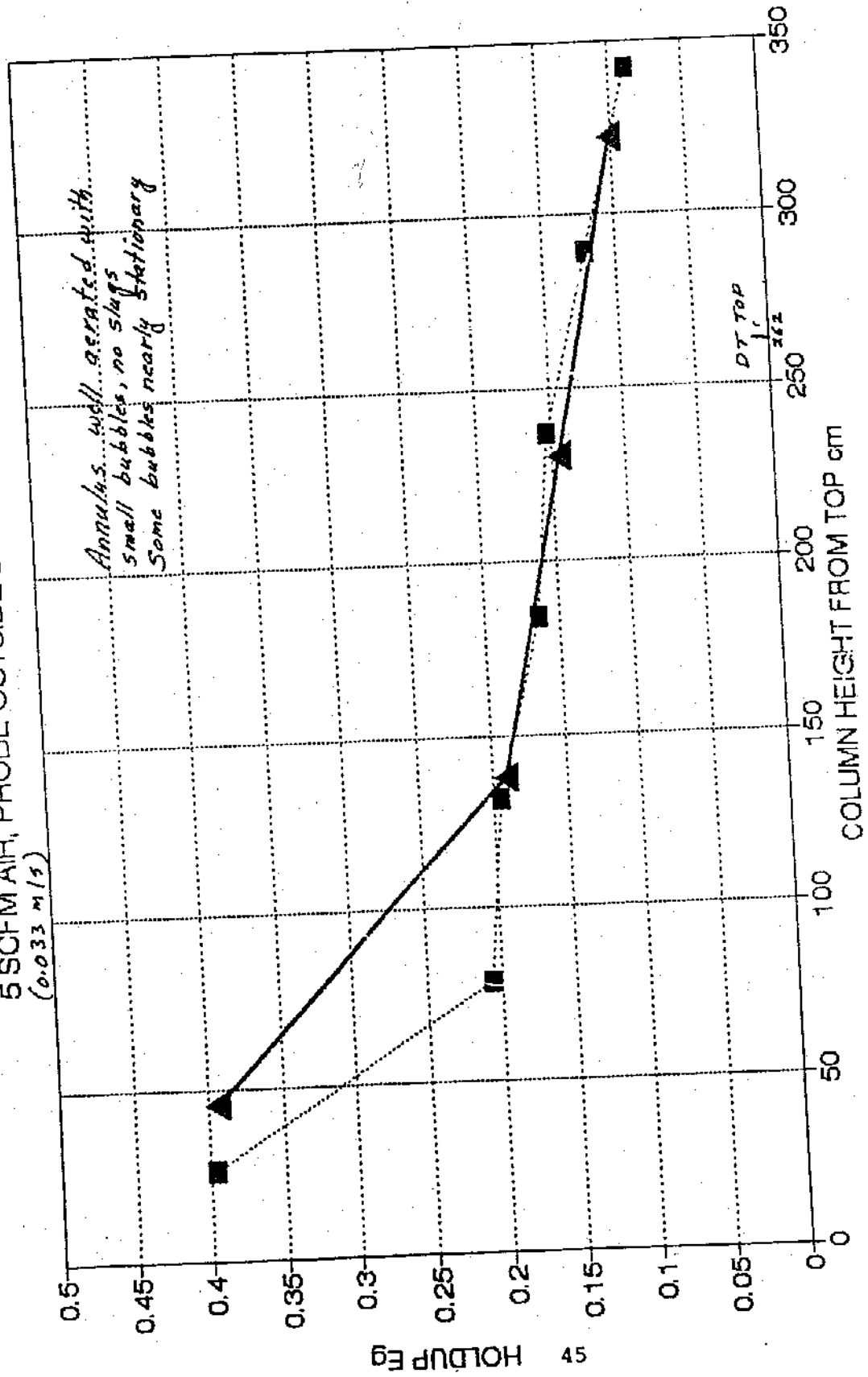
Not re-calibrated



▲ PROBE    ■ MANOMETER

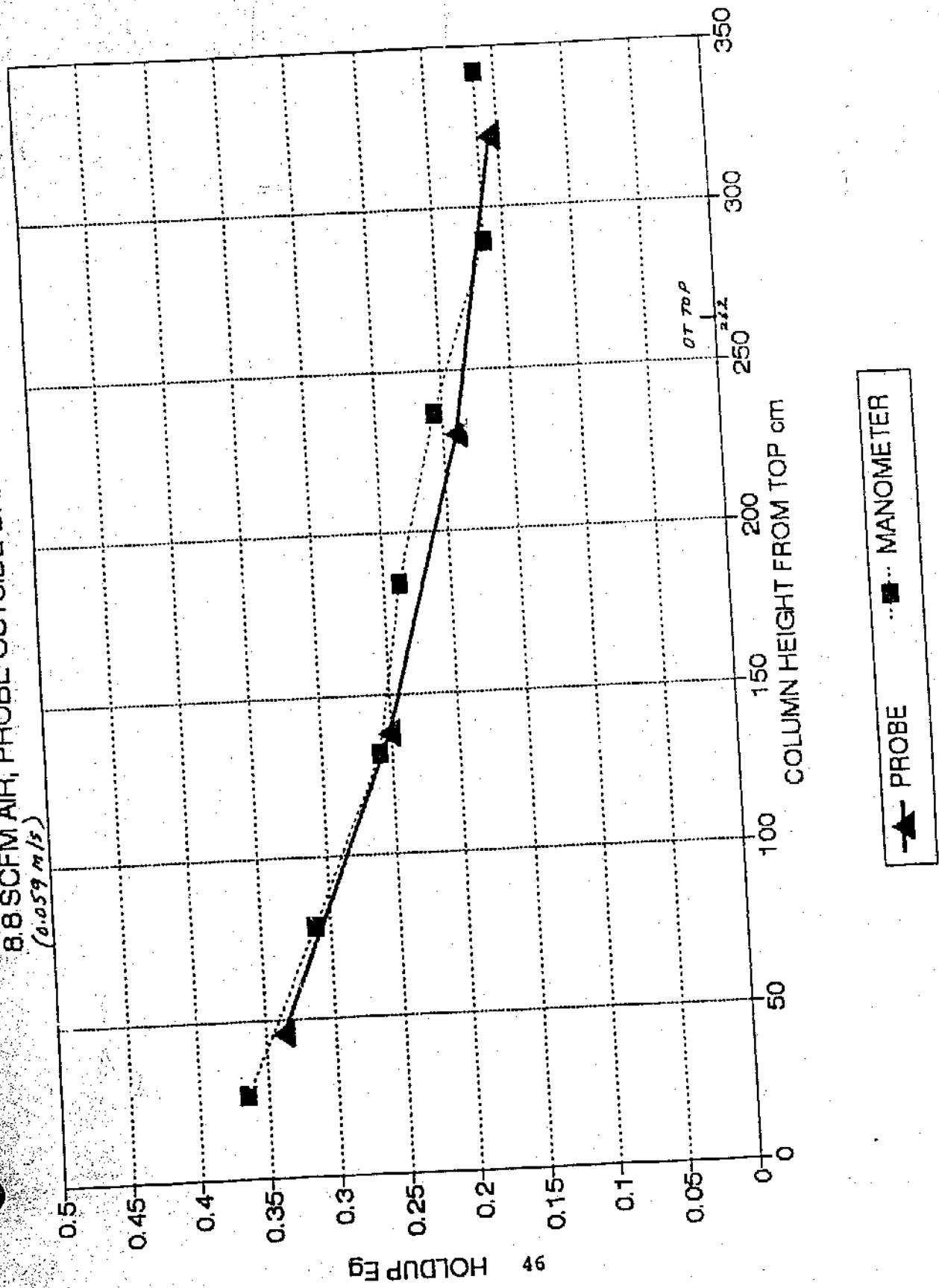
**GAS HOLDUP IN CARSOL RUN #13**  
**5 SCFM AIR, PROBE OUTSIDE DRAFT TUBE**  
*(0.033 m/s)*

*Annulus well aerated with small bubbles, no slugs  
 Some bubbles nearly stationary*

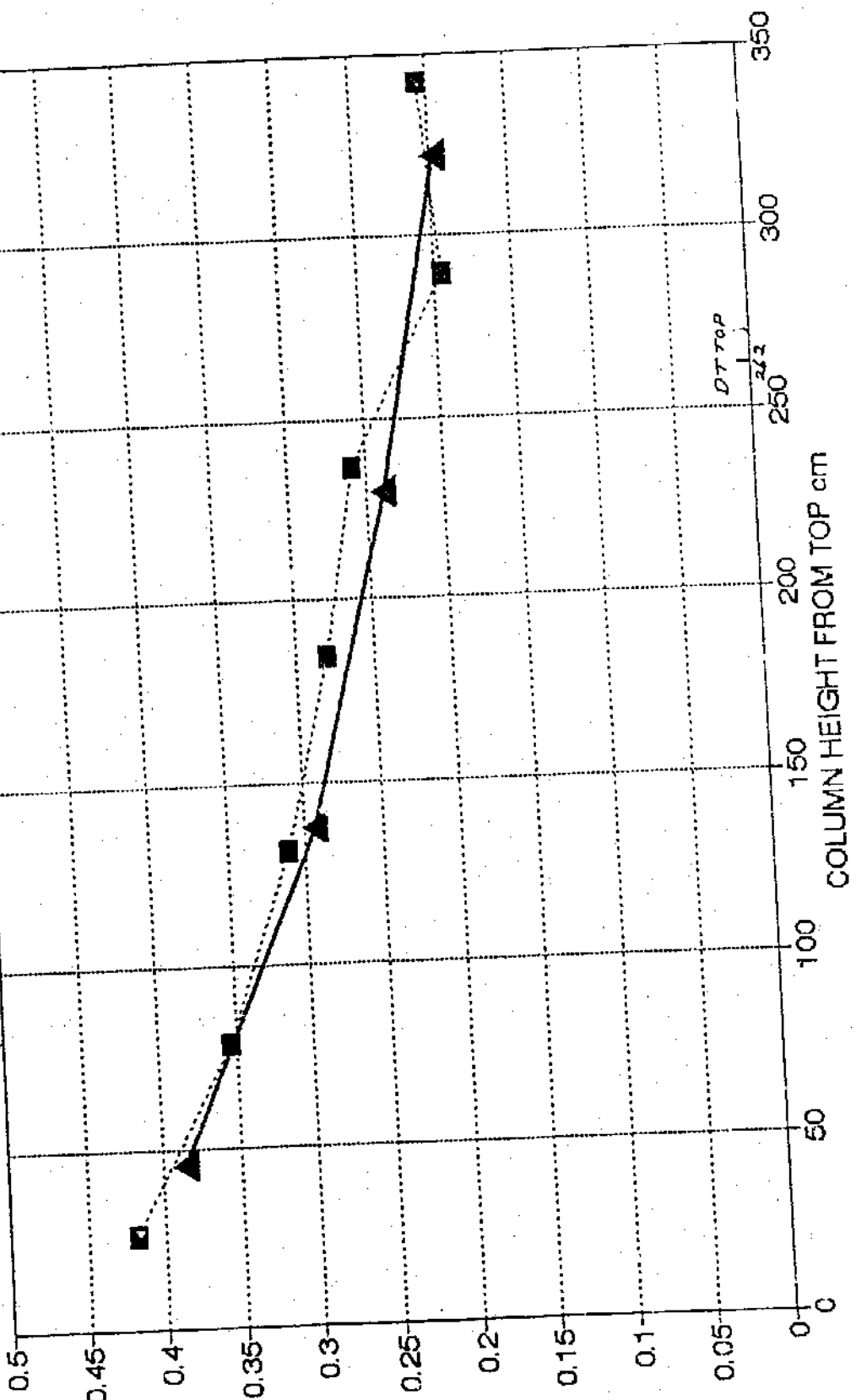


▲ PROBE    ■ MANOMETER

GAS HOLDUP IN  $\text{H}_2\text{O}$  RESOL RUN#14  
8.8 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
(0.059 m/s)



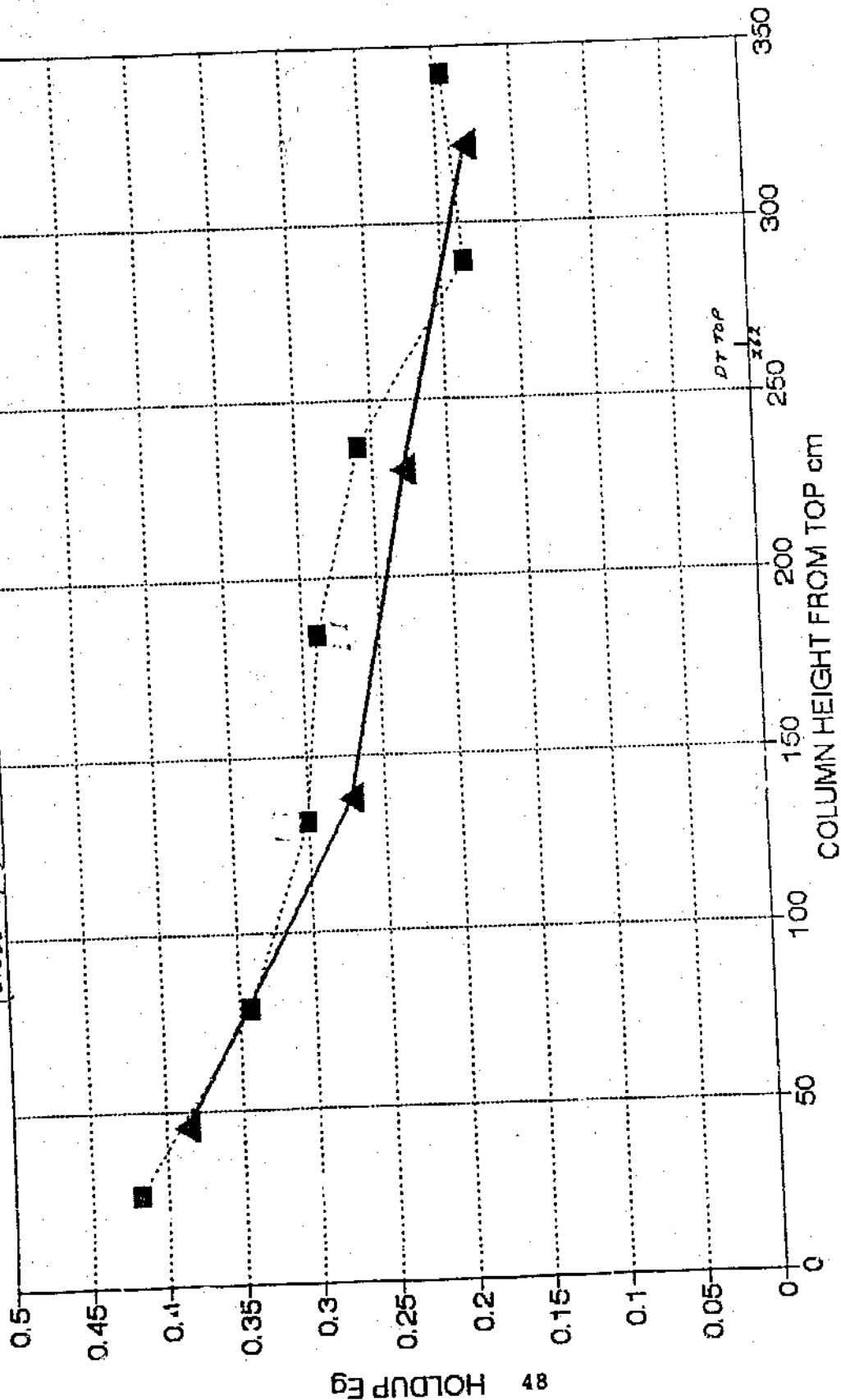
GAS HOLDUP IN PERSOL RUN#15  
 12 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.080 m/s)



▲ PROBE      ■ MANOMETER

GAS HOLDUP IN VIOSOL RUN#16  
 12 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.080 m/s)

Re-calibrated

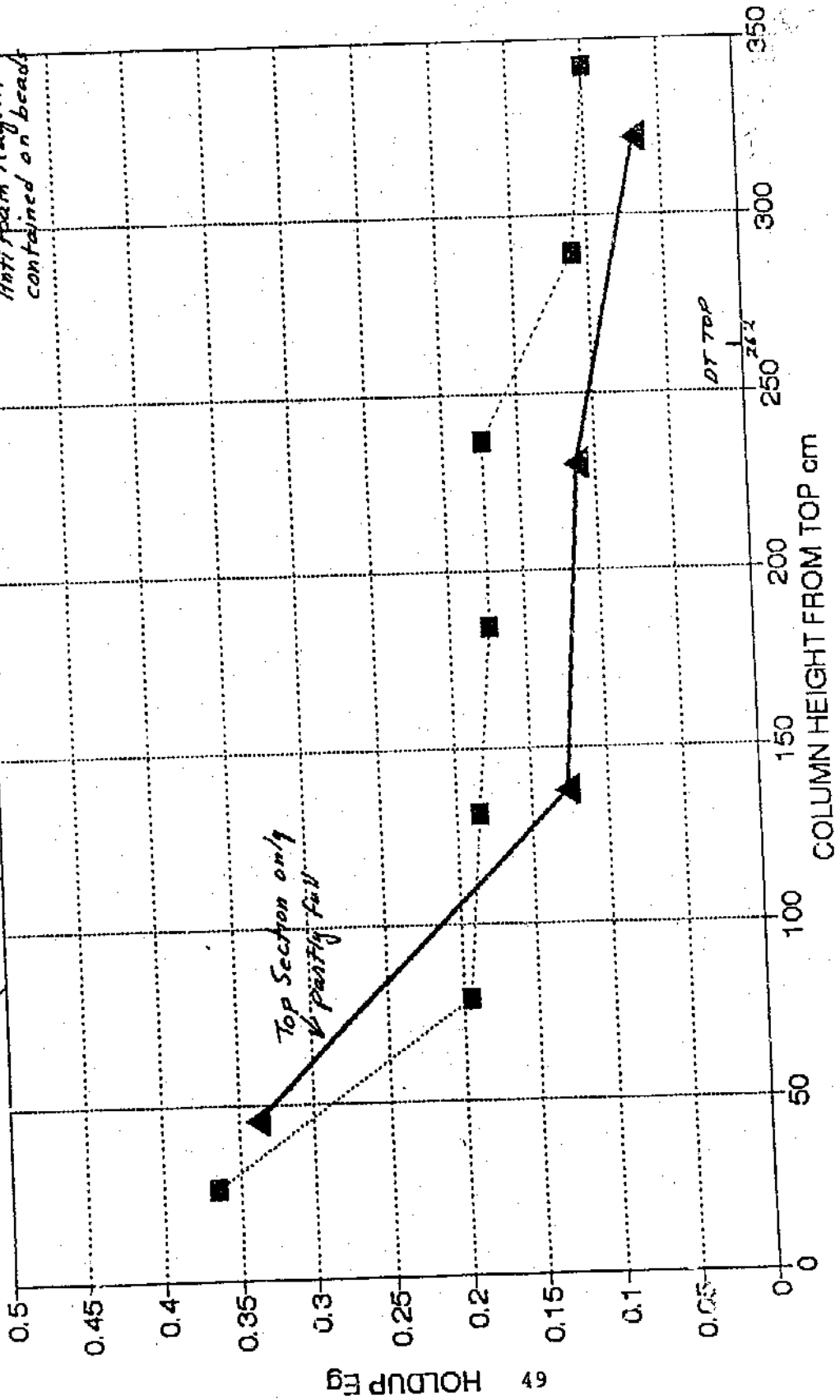


GAS HOLDUP IN VARSOL + SOLIDS RUN#17  
 12 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.080 m/s)

(170-230 glass solids)

Not Re-calibrated

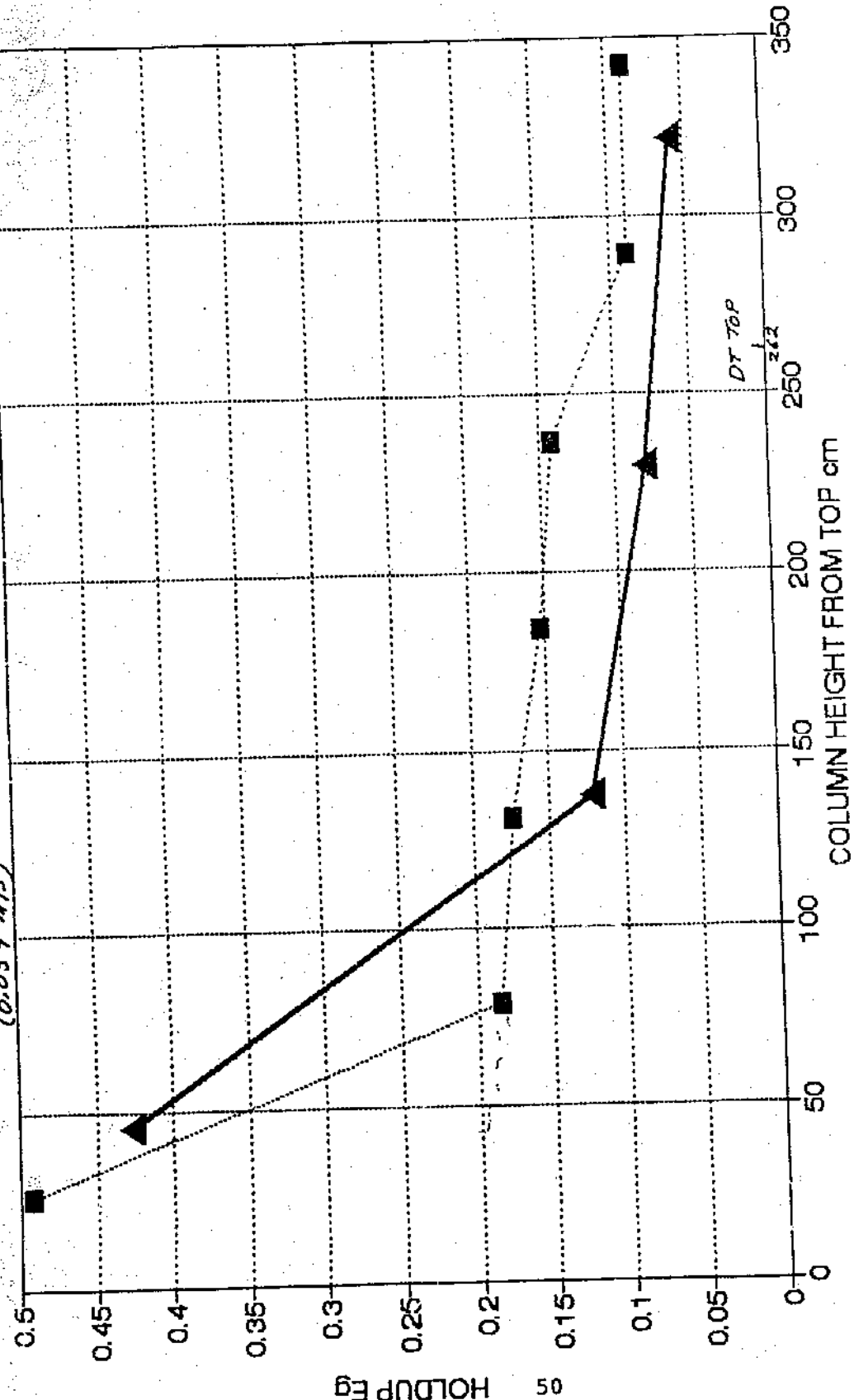
Anti foam reagent  
 contained on beads



▲ PROBE  
 ■ MANOMETER



GAS HOLDUP IN VARS ● + SOLIDS RUN #18 (170-230 glass 1/5)  
 8.8 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.057 m/s)  
 Not Re-calibrated



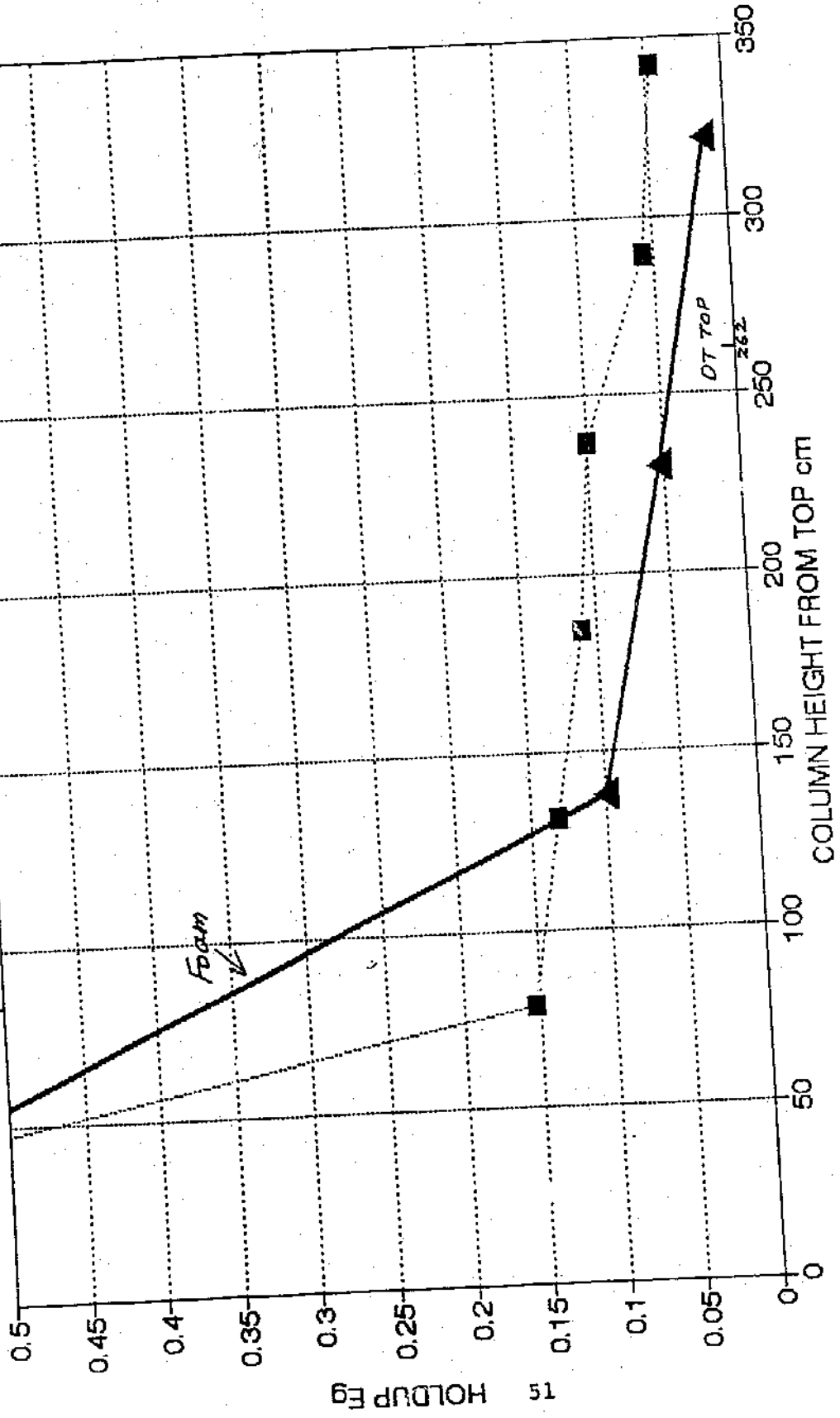
▲ PROBE     ■ MANOMETER

● (170-230 glass ds.) ●

# GAS HOLDUP IN VARSOL + SOLIDS RUN#19 (170-230 glass ds.)

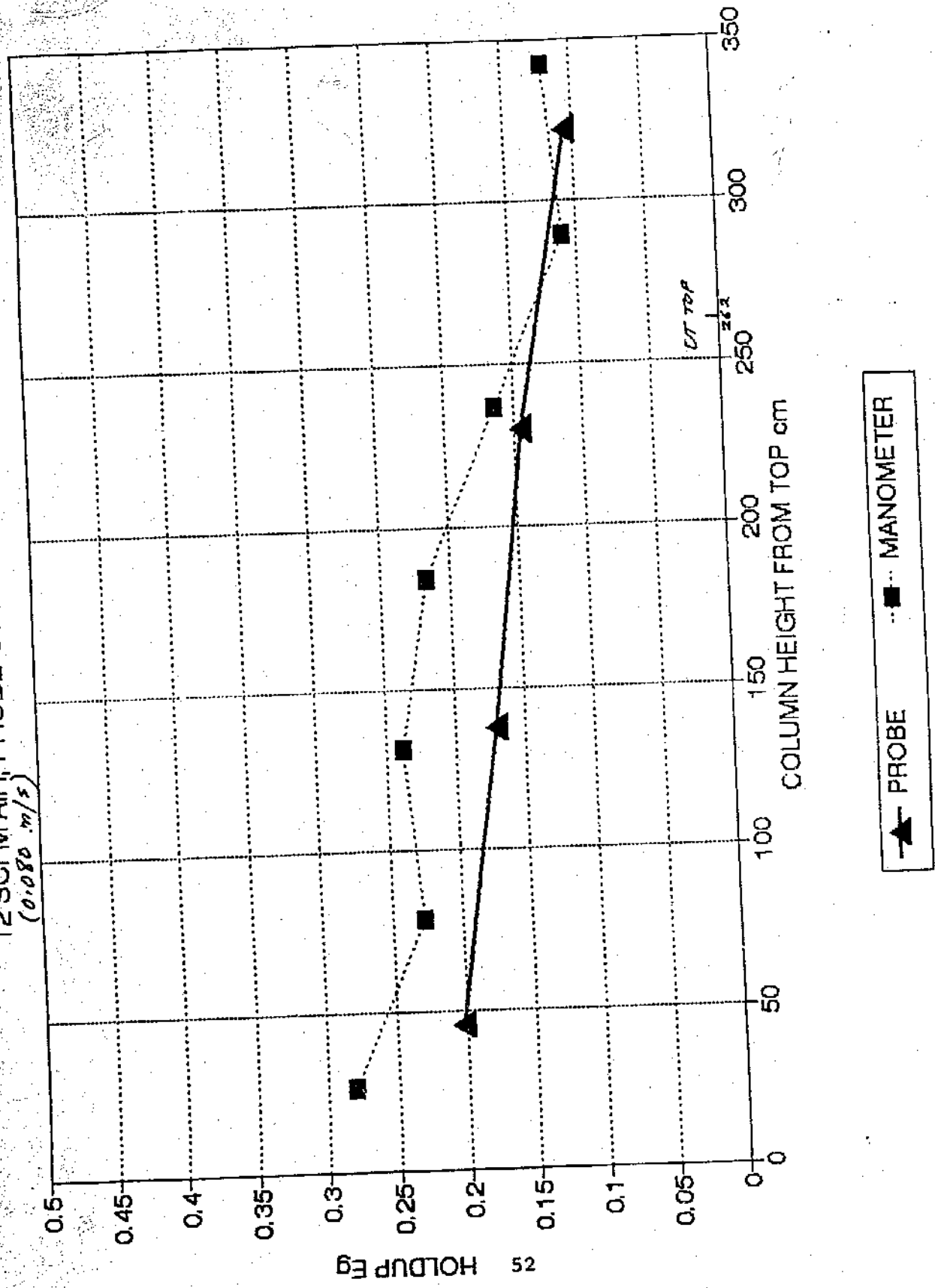
5 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
(0.033 m/s)

Not Re-calibrated



▲ PROBE    ■ MANOMETER

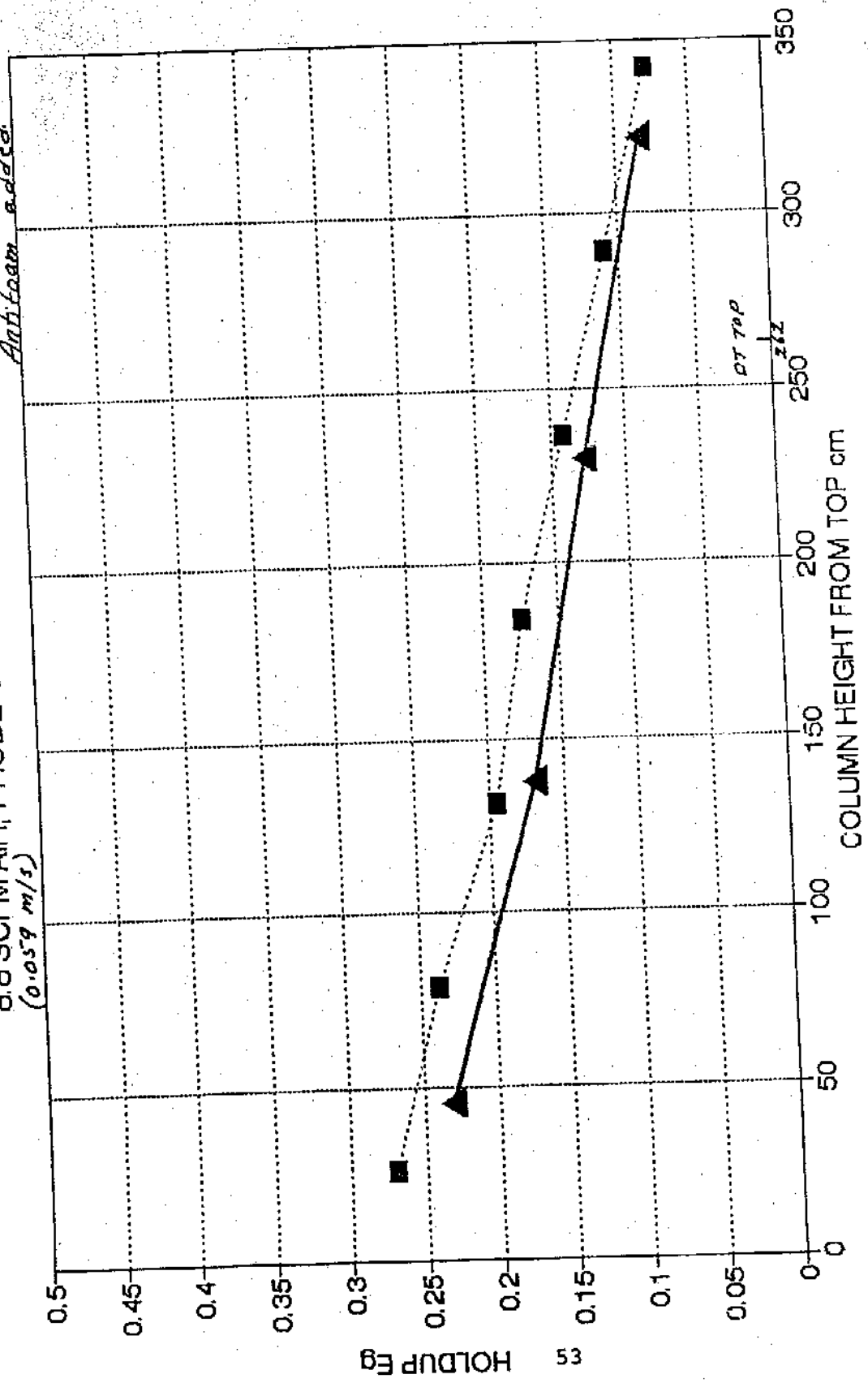
GAS HOLDUP IN VARSOL + SOLIDS RUN#20 (170-230 g loss 2ds)  
 12 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.080 m/s)



GAS HOLDUP IN VARSOL + SOLIDS RUN#21  
 8.8 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.059 m/s)

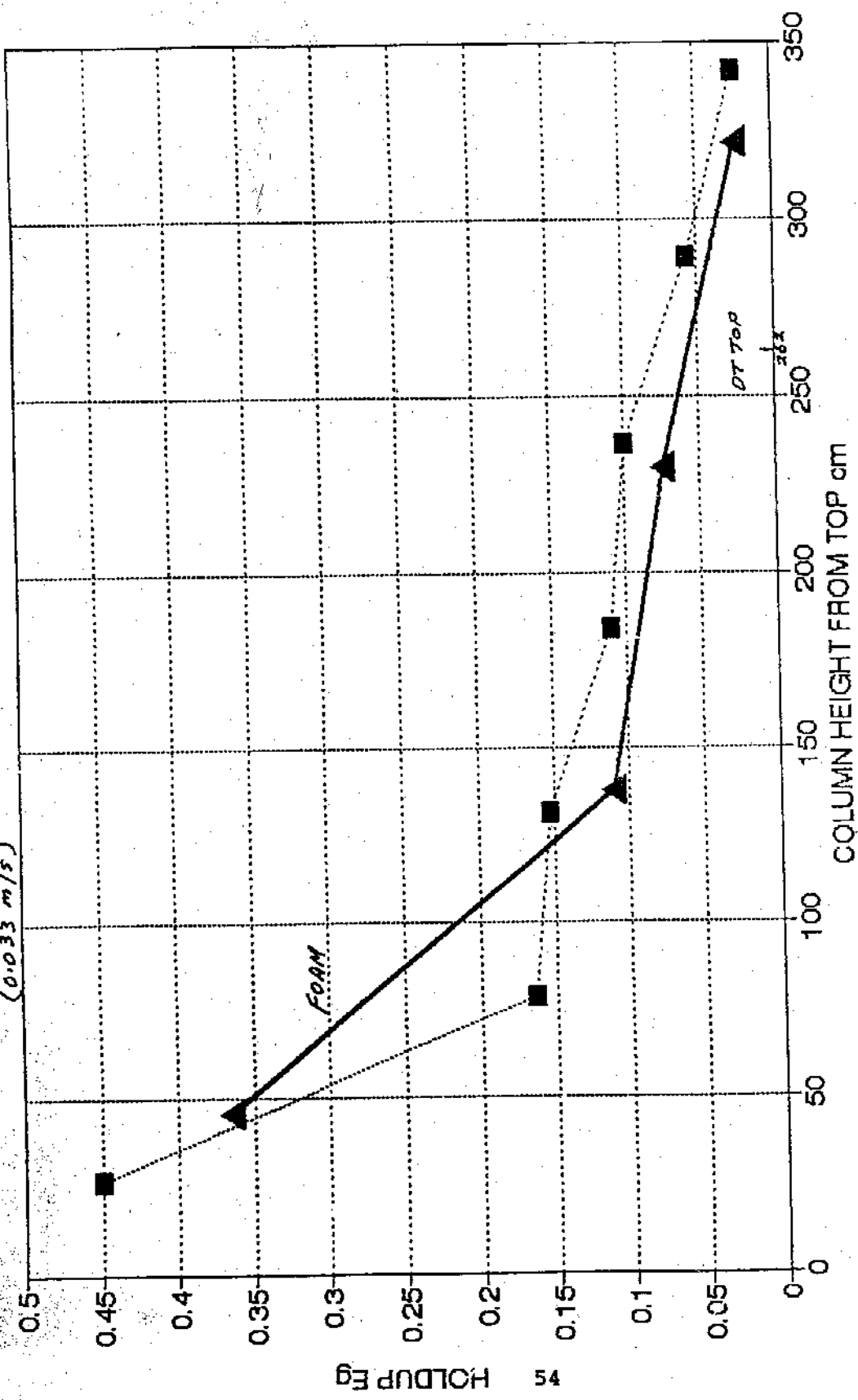
(170-230 glass balls)

Anti-foam added



▲ PROBE  
 ■ MANOMETER

GAS HOLDUP IN VAPOROL + SOLIDS RUN#22 (170-230 g/l (0.15 mds))  
 5 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.1033 m/s)

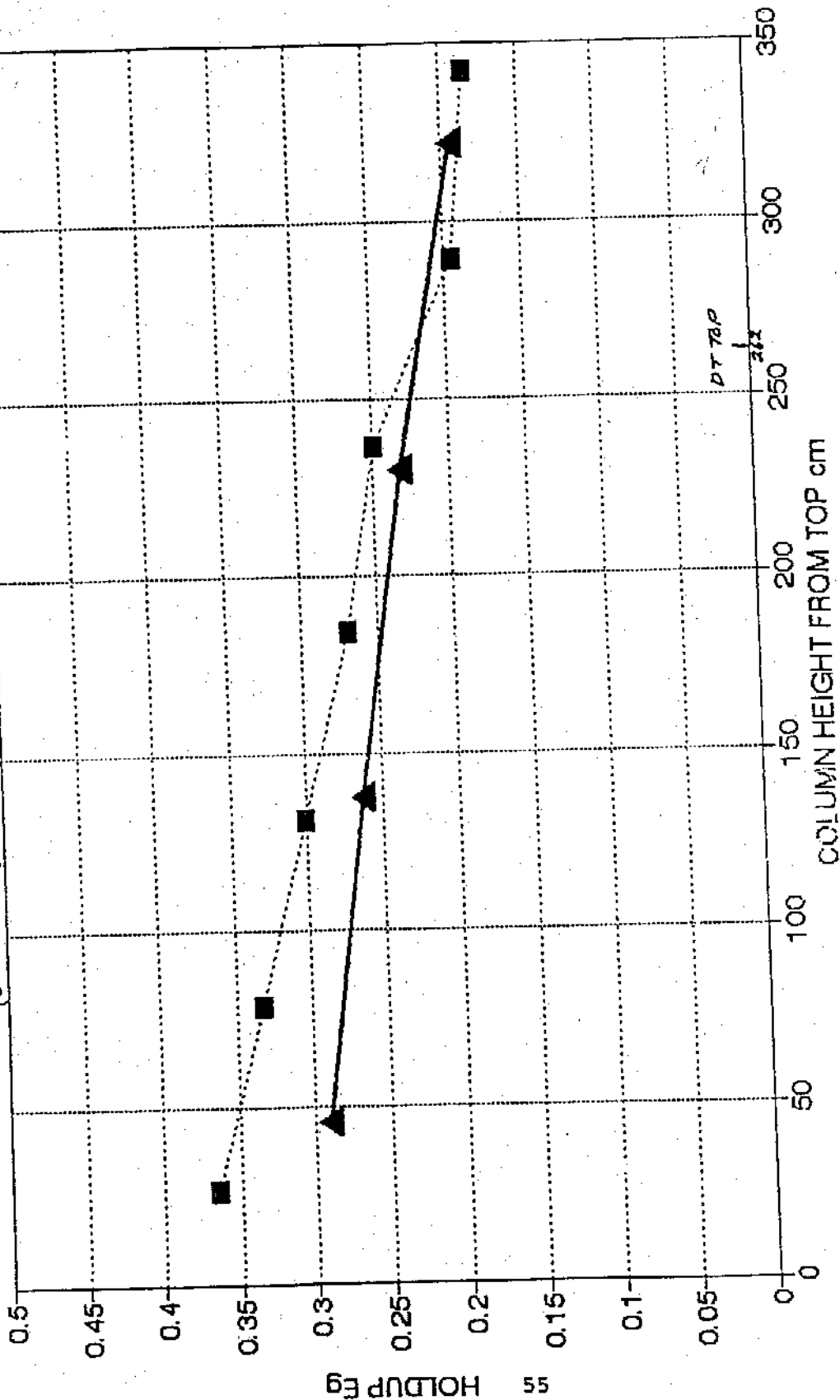


▲ PROBE      ■ MANOMETER

GAS HOLDUP IN ARSOL RUN#23  
 12 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.080 m/s)

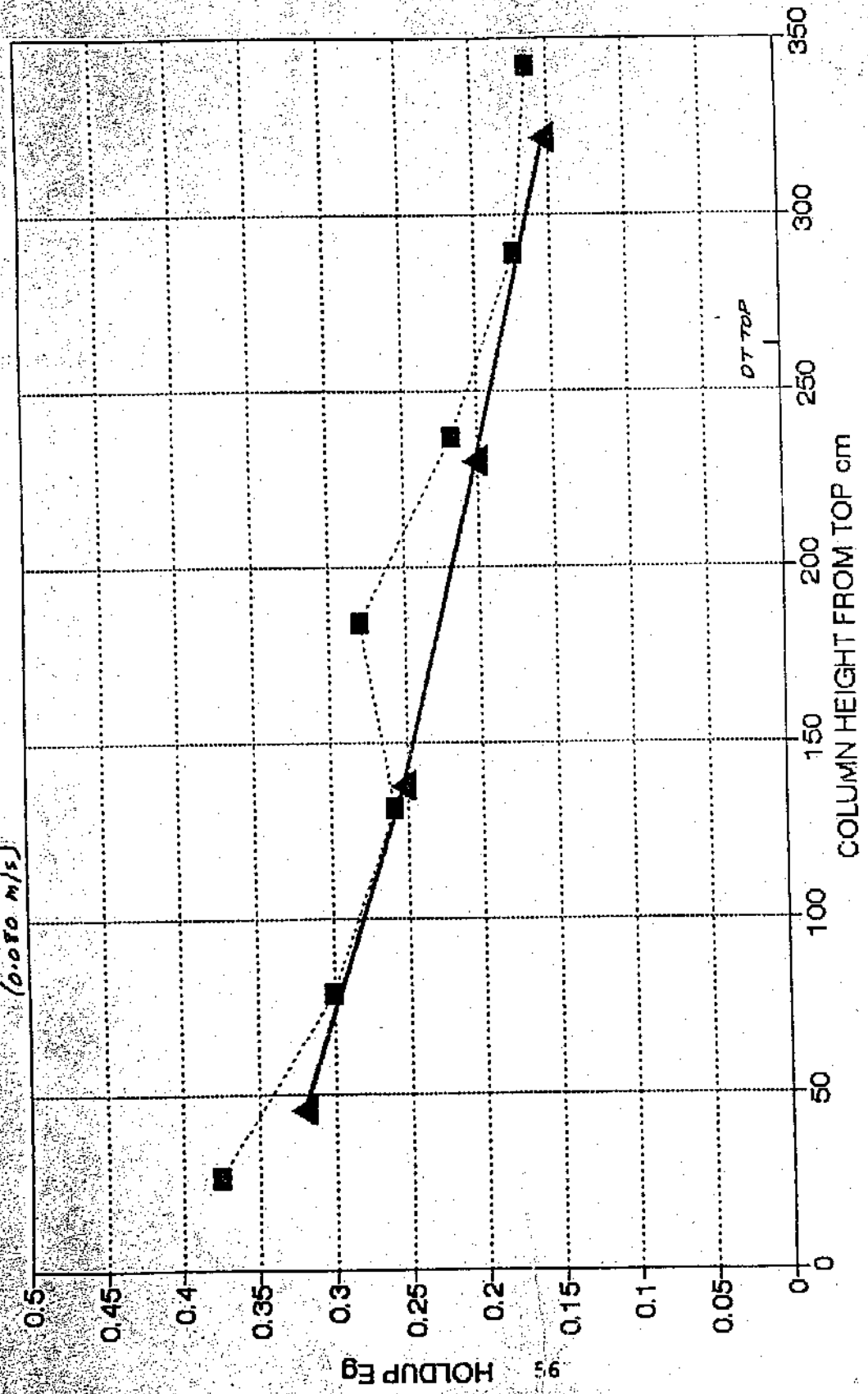
(no solids)

Re-Calibrated



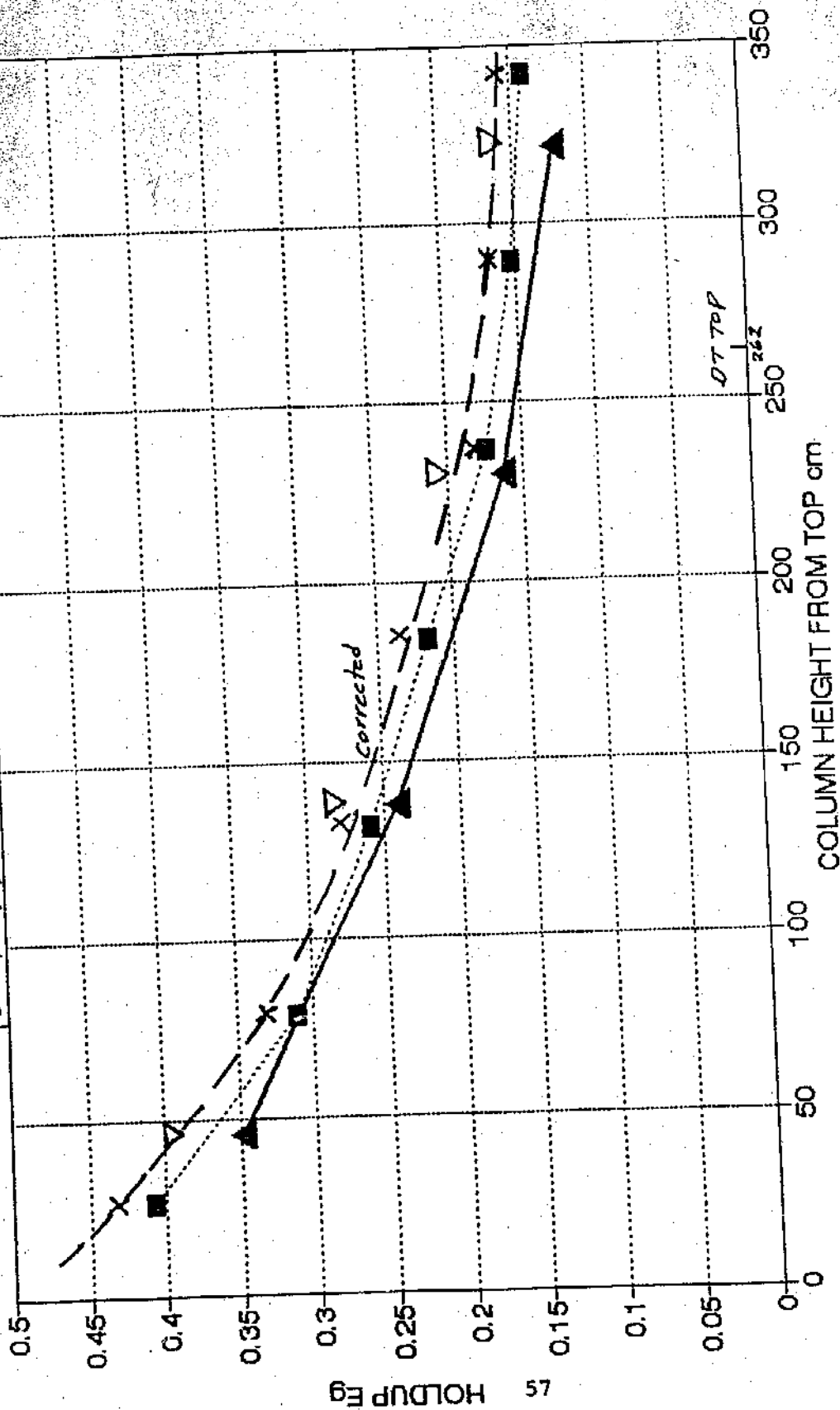
▲ PROBE    ■ MANOMETER

GAS HOLDUP IN VARIOUS IRON OXIDE RUN #24  
 12 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
*(0.080 m/s)*



▲ PROBE      ■ MANOMETER

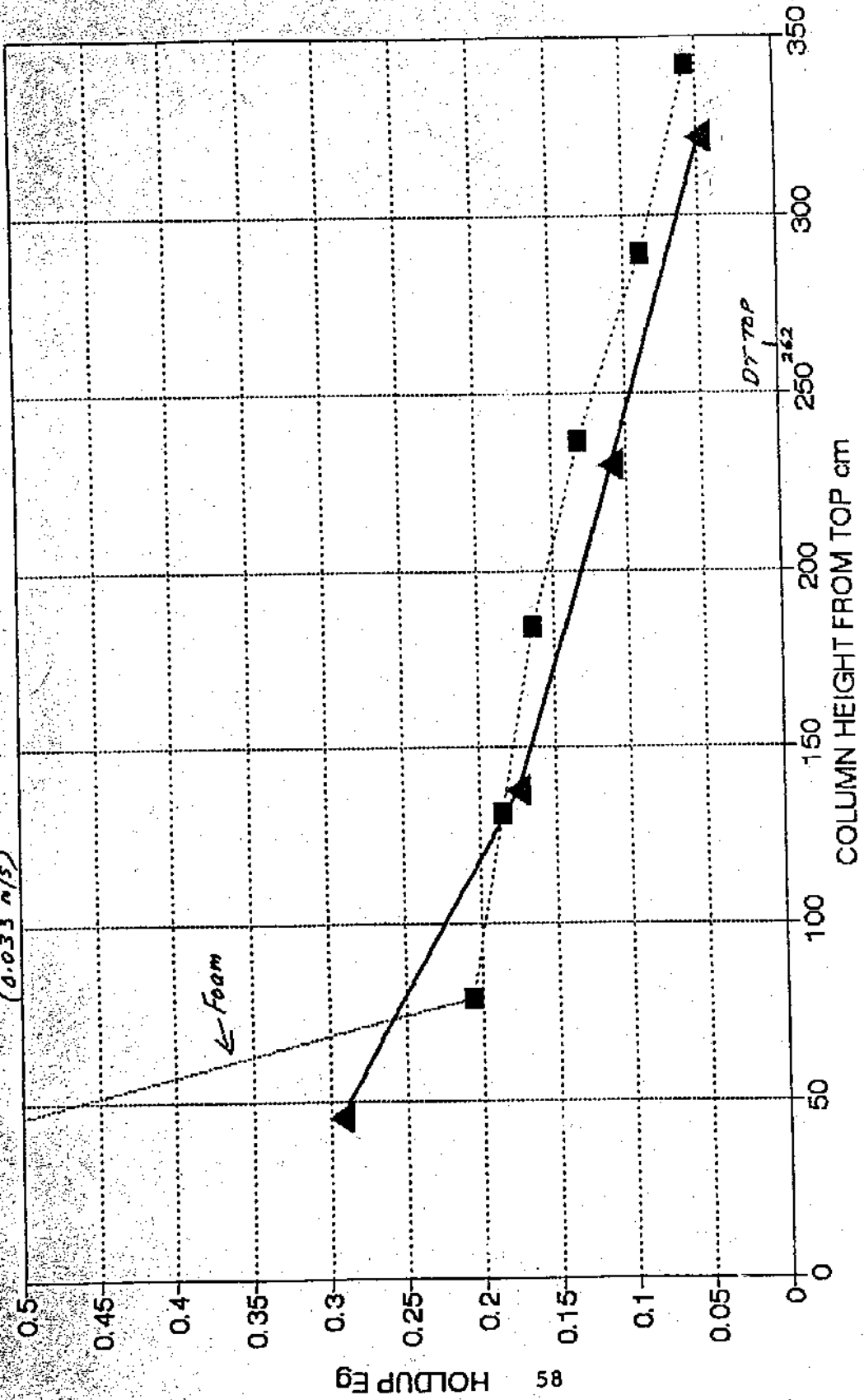
GAS HOLDUP IN VARS + IRON OXIDE RUN #25  
 8.8 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.059 m/s)



▲ PROBE  
 ■ MANOMETER  
 △ - Corrected  
 × - Corrected



GAS HOLDUP IN VARS + IRON OXIDE RUN #26  
 5 SCFM AIR, PROBE OUTSIDE DRAFT TUBE  
 (0.033 n/s)



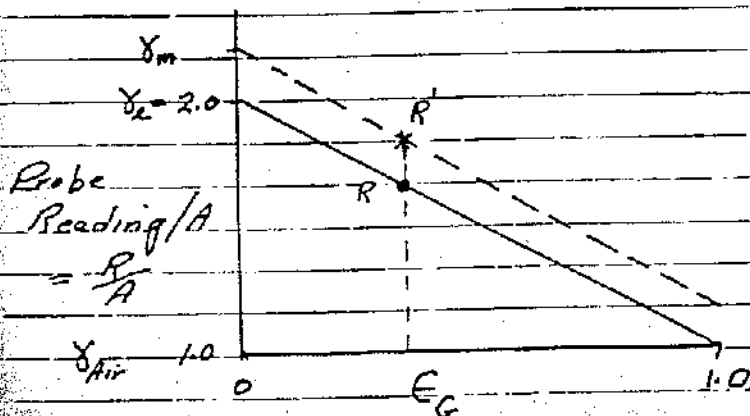
▲ PROBE    ■ MANOMETER

**APPENDIX**

## APPENDIX

## 1. Correction of Probe Readings for Presence of Solids

A method is developed to correct the probe reading for the increase in dielectric caused by the presence of solids (glass beads)



- $\delta_m$  - dielectric of slurry
- $\delta_l$  - dielectric of liquid = 2.0
- $\delta_a$  - dielectric of air = 1.0
- A - calibration factor
- $\delta_s$  - dielectric of glass beads = 4.7

When a slurry is present, at a gas holdup of  $\epsilon_G$ , reading of probe is at  $R'$ . However, calibration is the solid line, so  $R'$  must be corrected so calibration factor for air-liquid only can be used to calculate the corrected reading,  $R$ .

$$\delta_m = \delta_l \epsilon_l' + \delta_s \epsilon_s'$$

where  $\epsilon_l'$ ,  $\epsilon_s'$  are volume fractions of liquid and solids resp. in slurry

$$\text{But } \epsilon_l' + \epsilon_s' = 1.0$$

$$\text{so } \delta_m = \delta_l (1 - \epsilon_s') + \delta_s \epsilon_s' = \delta_l + \epsilon_s' (\delta_s - \delta_l)$$

$$\epsilon_s' = \frac{\epsilon_G}{1 - \epsilon_G}$$

$\epsilon_G$  = volume fraction of solids in the bubble column.

$$\text{and } \delta_m = \delta_l + \frac{\epsilon_G}{1 - \epsilon_G} (\delta_s - \delta_l)$$

With solids present, readout is

$$\frac{R'}{A} = \epsilon_G \delta_a + (1 - \epsilon_G) \delta_m = \epsilon_G \delta_a + (1 - \epsilon_G) \left[ \delta_l + \frac{\epsilon_G}{1 - \epsilon_G} (\delta_s - \delta_l) \right]$$

With no solids present, readout is

$$\frac{R}{A} = \gamma_e (1 - E_c) + \gamma_a E_c$$

$$= E_c (\gamma_a - \gamma_e) + \gamma_e$$

At the same value of  $E_c$ , correction is

$$\frac{R' - R}{A} = E_c \gamma_a + (1 - E_c) \left[ \gamma_e + \frac{E_s}{1 - E_c} (\gamma_s - \gamma_e) \right]$$

$$- \left[ E_c (\gamma_a - \gamma_e) + \gamma_e \right]$$

$$= (1 - E_c) \left[ \frac{E_s}{1 - E_c} (\gamma_s - \gamma_e) \right] = E_s (\gamma_s - \gamma_e)$$

For the tests with glass beads

$$12.5 \text{ kg of beads @ } 2450 \text{ kg/m}^3 = 0.00510 \text{ m}^3$$

$$\text{Column volume} = 300 \text{ l}$$

$$E_s' = \frac{0.00510 \text{ m}^3}{(0.300 \text{ m}^3)(1 - E_c)} = \frac{0.0170}{1 - E_c}$$

$$\text{and since } E_c' = \frac{E_s}{1 - E_c} = \frac{0.0170}{1 - E_c} \quad E_c = 0.0170$$

$$\text{Then } \frac{R' - R}{A} = 0.0170 (47 - 3.0) = 0.0459$$

Correction is  $0.0459 A$ , where  $A$  is the experimental span. If a constant solids concentration is assumed, as a first approximation, then the above correction is constant because  $E_c$  is constant.

The assumption of constant  $E_c$  is less in error for tests with a draft tube because of the improved mixing.

The true correction factor would be smallest at the top of the column and greatest at the bottom.

Since for the conditions used the solids concentration (no draft tube) may vary by a factor of 2 from top to bottom, this means that the correction factor could vary from the mean values used by  $\pm 33\%$ .

For tests with iron oxide

$$\text{Dielectric of hematite} = 14.2$$

$$\text{Density of hematite} = 4900 - 5300 \text{ kg/m}^3$$

$$\text{Amount of hematite used} = 5.835 \text{ kg}$$

$$\text{Assuming } \rho = 5200 \text{ kg/m}^3$$

$$\text{Volume of iron oxide} = \frac{5.835}{5200} = 0.001122 \text{ m}^3$$

$$E_s = \frac{0.001122 \text{ m}^3}{1.300 \text{ m}^3} = 0.00374$$

Then correction to probe reading

$$\frac{R' - R}{A} = 0.001122 (14.2 - 2.0) = 0.0456$$

This value is almost identical to that for the glass beads

However, because of the small diameter of the iron oxide, solids concentrations especially with a draft tube will tend to be more axially uniform

## Corrections to Manometer Readings due to Solids

Total column volume (7.5 sections, bottom) = 300 litres

Solids samples were not taken, so the same assumption as previously will be made, that is, axial solids concentration is uniform. This assumption will give to ~~too~~ small a correction (+) near the bottom and too large a correction (+) near the top.

Liquid void fraction calculated with solids ( $E_c$ ), and assuming no solids ( $E_c'$ ). The no solids assumption uses the liquid density and is the one reported on the data sheets.

$$E_c = \frac{\rho_{man} g \Delta h_{man}}{\rho_{sl} \Delta h g}$$

$$E_c' = \frac{\rho_{man} g \Delta h_{man}}{\rho_l \Delta h g}$$

where  $\rho_{man}$  = manometer fluid density  
 $\Delta h_{man}$  = manometer reading  
 $\rho_{sl}$  = density of the slurry (average)  
 $\rho_l$  = density of the liquid  
 $\Delta h$  = column increment between measuring points

$$\text{Then } \frac{E_c'}{E_c} = \frac{\rho_{sl}}{\rho_l} = \frac{1 - E_{c, calc}}{1 - E_{c, corr}}$$

For the Vapour used  $\rho = 798 \text{ kg/m}^3$

$$\text{and } E_{c, corr} = \frac{1 - 798 (1 - E_{c, calc})}{\rho_{sl}}$$

$$\text{To find } \rho_{sl} \rightarrow E_c = \frac{12.5 \text{ kg}}{(2450)(0.30 \text{ m}^3)} = 0.017$$

$$\text{Volume of slurry} = 0.300 (1 - E_g)$$

$$\text{Volume of liquid} = 0.300 (1 - E_g - E_s) = 0.295 (1 - E_g)$$

$$\begin{aligned} \text{Then } \rho_{se} &= \frac{798 (0.295)^{(1-E_g)} + 12.5}{0.300 (1 - E_g)} = 784.7 + \frac{12.5}{(1-E_g)} \\ &= 784.7 + \frac{41.67}{(1-E_g)} \end{aligned}$$

The Table below gives values of this manometric correction factor for the 170/230 glass beads.

True $E_g$	$\rho_{se} \text{ kg/m}^3$	$E_{g \text{ calc.}}$	$E_{g \text{ con}}$	$\Delta$ (+)
0.05	828	0.05	0.084	0.034
0.10	831	0.10	0.136	0.036
0.15	834	0.15	0.187	0.037
0.20	837	0.20	0.237	0.037
0.25	840	0.25	0.288	0.038
0.30	844	0.30	0.338	0.038
0.40	854	0.40	0.439	0.039

As can be seen, this correction factor is nearly constant over a wide range of gas holdups and slurry solid concentrations.

The value of the correction factor is nearly equal to that for the dielectric effect (about 80% as much). As a result, both probe and manometric readings of the gas holdup are corrected (increased) by nearly the same amount.

### Manometric Correction for Iron Oxide Slurry:

For the iron oxide (5.835 kg, density 5200 kg/m<sup>3</sup>)

as developed earlier

$$P_{sc} = \frac{(798)(.298)(1 - E_G) + 5.835}{(0.300)(1 - E_G)}$$

The Table below gives calculated gas holdup corrections

True $E_G$	$P_{sc}$ kg/m <sup>3</sup>	$E_G$ calc.	$E_G$ corr.	$\Delta$ (+)
.05	813	.05	.0675	.0175
.10	814	.10	.118	.018
.15		.15		
.20	817	.20	.219	.019
.25		.25		
.30	820	.30	.319	.019
.40	825	.40	.420	.020

This is a considerably smaller correction to the manometric reading than that for glass beads.