

IV. DOUBLE-BED Cs/Cu/ZnO/Cr₂O₃ CATALYST FOR HIGHER ALCOHOL SYNTHESIS

Catalytic Testing Results

A comparison of the results of the single-bed copper-based catalyst at high temperature (described in the previous section) with the copper-free catalyst reported by Beretta et al. [1996] suggested that the former could be effectively used as the bottom bed in a double-bed configuration. The relative stability of the cesium-doped copper-based catalyst at high temperatures, along with its high selectivity toward isobutanol synthesis, indicated that this catalyst could be used to improve upon the previous double-bed experiment by increasing the isobutanol yield. Indeed, the single-bed study of the copper-based catalyst demonstrated that this catalyst was more active toward isobutanol production at lower temperatures (613 and 643K) than the copper-free catalyst at high temperature (678K). In order to maximize isobutanol production, the copper-based catalyst was utilized in a double-bed configuration. In this manner, the temperatures of the two beds of equal volume could be controlled separately in order to achieve higher isobutanol productivity. Figure 20 shows the distribution of major products at two different bottom-bed temperatures (613 and 643K). It is seen that the space time yields of these products were lower at the higher bottom-bed temperature. As a group, the linear, primary alcohols showed the strongest temperature dependence. The remaining products (branched primary alcohols, secondary alcohols, and hydrocarbons) exhibited a weaker dependence upon temperature.

Table 9 lists all of the products observed under the HAS conditions specified in Figure 20. As can be seen, at the higher bottom-bed temperature of 643K, small amounts of butanol and pentanol were also produced. CO conversion, also listed in Table 9, was disfavored at the higher bottom-bed temperature. With the bottom-bed temperature maintained at 613K, CO conversion was 8.5%, but it decreased to 6.2% when the bed temperature was increased to 643K.

This experiment shows that by modifying the double-bed higher alcohol synthesis by using the Cs/Cu/ZnO/Cr₂O₃ catalyst in both beds but at different temperatures, isobutanol productivity increased significantly, as did the production of methanol. When the copper-based catalyst was used as the bottom bed and maintained at 340°C, isobutanol STY was 202 g/kg cat/hr, compared to 125 g/kg cat/hr (see Table 6) when the bottom bed consisted of the copper-free catalyst at 678K, an increase of 62%. Similarly, methanol production was greatly increased by the copper-containing bottom bed, reaching a value of 574 g/kg cat/hr. Product distribution was influenced by the temperature of the copper-based bottom bed. High yields of methanol are expected at the lower reactant temperature due to equilibrium constraints at higher temperatures. Lower temperature is also expected to increase the overall productivity of the copper-based catalyst. This was

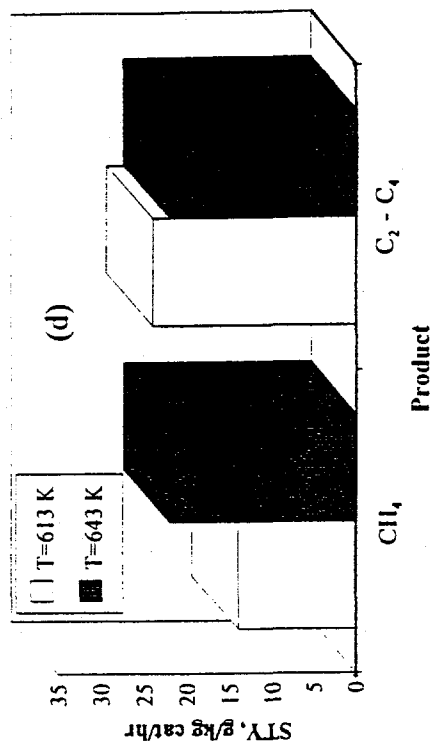
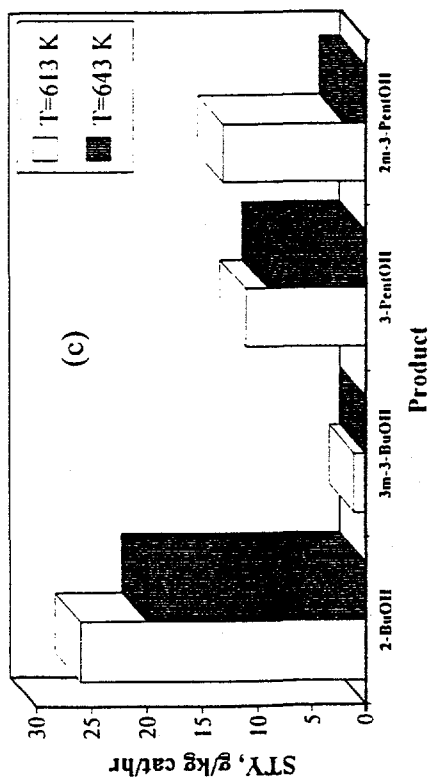
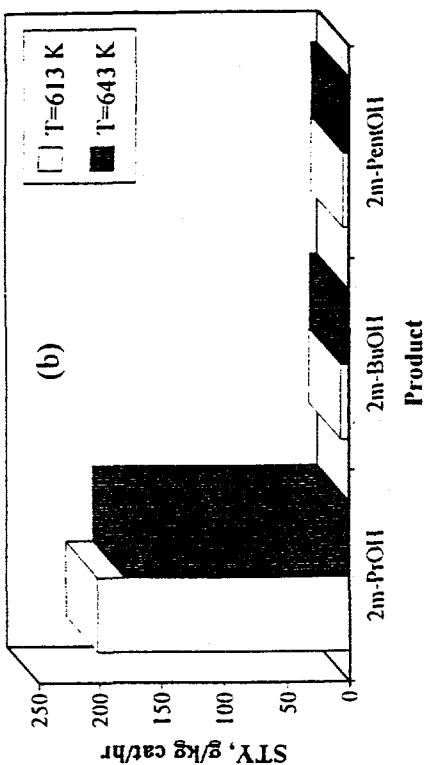
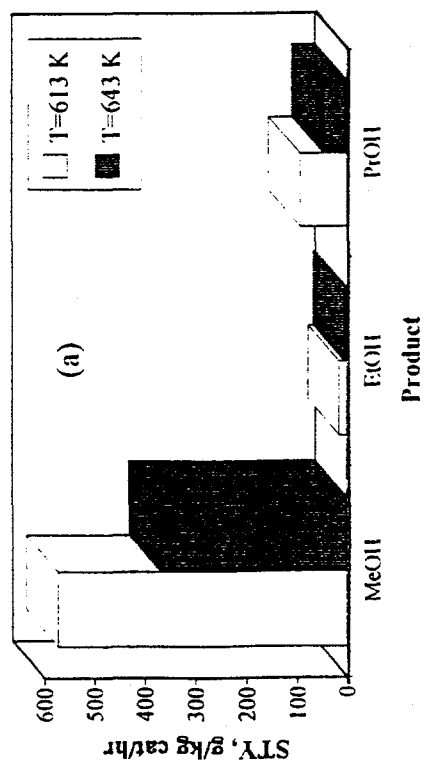


Figure 20. Product distribution over the double-bed 3 mol % Cs-Cu/ZnO/Cr₂O₃ (both beds) catalyst with $T_{\text{top bed}} = 598\text{K}$, $\text{H}_2/\text{CO} = 0.75$ and $\text{GHSV} = 18,375 \text{ l(STP)/kg cat/hr}$ at a reaction pressure of 7.6 MPa with bottom-bed temperatures of 613 and 643K for (a) primary alcohols, (b) secondary alcohols, and (d) hydrocarbons.

TABLE 9. Higher alcohol synthesis over two portions of the 3 mol% Cs/Cu/ZnO/Cr₂O₃ catalyst held in a double-bed configuration, where the top bed (1 g) was held at 598K and the lower bed (1 g) was maintained at 613 or 643K. The synthesis gas consisted of H₂/CO = 0.75 at 7.6 MPa with GHSV = 18,375 l(STP)/kg cat/hr. The productivities of aldehydes and ketones have been added to those of the corresponding primary and secondary alcohols. Abbreviations used are Me = methyl, Et = ethyl, Pr = propyl, Bu = butyl, Pent = pentyl, 2m = 2-methyl, 3m = 3-methyl, and HC = hydrocarbon.

	Top = 598K Bottom = 613K (g/kg cat/hr)	Top = 598K Bottom = 643K (g/kg cat/hr)
MeOH	574	369
EtOH	15	5
PrOH	93	47
BuOH	0	1
PentOH	0	1
2m-PrOH	202	180
2m-BuOH	7	6
2m-PentOH	5	5
2-BuOH	26	20
3m-2-BuOH	1	0
3-PentOH	11	9
2m-3-PentOH	13	2
CH ₄	14	22
C ₂ -C ₄ HC	24	22
%CO Conv. (CO ₂ -free)	8.5	6.2

reflected in the CO conversion level, which increased from 6.2 to 8.5% when the reaction temperature was decreased. With the copper-based bottom bed, the selectivity of isobutanol among the other 2-methyl alcohols was greatly increased, as well.

Conclusions

This study used the recently demonstrated concept of employing two sequential catalysts at different reaction temperatures to enhance the productivity of isobutanol from synthesis gas. It was shown that the Cs/Cu/ZnO/Cr₂O₃ catalyst could be utilized to advantage as the second-bed catalyst at 613-643K instead of the previously used copper-free Cs-ZnO/Cr₂O₃ catalyst at the higher temperature of 678K. High space time yields of 202 g/kg cat/hr for isobutanol and high selectivity toward isobutanol/methanol mixtures were achieved by coupling two beds of the Cs/Cu/ZnO/Cr₂O₃ catalyst at different reaction temperatures in a double-bed configuration. The isobutanol/methanol mass ratios were about 0.35 and 0.5 for the lower bed temperatures of 613 and 643K, respectively. The selectivity of the isobutanol and methanol products was notable. At the lower bed temperature of 613K, 67% of the C in the products shown in Table 9 was in the isobutanol and methanol products. If n-propanol is included along with isobutanol and methanol, then 80% of the carbon found in the alcohol and hydrocarbon products was obtained in these three alcohols.

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Present addresses of co-workers on this research project are:

Dr. Alessandra Beretta, Dipartimento di Chimica Industriale e Ingegneria Chimica "G. Natta," Piazza Leonardo da Vinci 32, Politecnico di Milano, 20133 Milano, Italy.

Maria Burcham, Department of Chemistry, S. B. Mudd Bldg., 6 Packer Avenue, Lehigh University, Bethlehem, PA 18015.

Dr. Yeping Cai, Zettlemoyer Center for Surface Studies, Sinclair Laboratory, 7 Asa Drive, Lehigh University, Bethlehem, PA 18015.

Dr. Marie Johansson, STC Technologies, Inc., 1745 Eaton Avenue, Bethlehem, PA 18018-1799.

Dr. Biswanath Roy, Department of Chemical Engineering, Iacocca Hall, 111 Research Drive, Lehigh University, Bethlehem, PA 18015.

Dr. Qun Sun, Dupont CR&D, Experimental Station, P.O. Box 80356, Wilmington, DE 19880-0356.

LIST OF PUBLICATIONS TO-DATE

• Publications Based on the Research Carried out During this Project:

"Higher Alcohol Synthesis Over Cs-Doped Cu/Zn/Cr Oxide Catalysts: Effect of Reaction Temperature on the Product Distribution and Catalyst Stability," A. Beretta, Q. Sun, R. G. Herman, and K. Klier, Preprints, Div. Fuel Chem., ACS, **40(1)**, 142-147 (1995).

"Synthesis of 2-Methylpropan-1-ol/Methanol Mixtures From H₂/CO Synthesis Gas Over Double-Bed Cs/Cu/ZnO/Cr₂O₃ and Cs/ZnO/Cr₂O₃ Catalysts," A. Beretta, Q. Sun, R. G. Herman, and K. Klier, J. Chem. Soc., Chem. Commun., 2525-2526 (1995).

"Catalytic Synthesis of Methanol, Higher Alcohols and Ethers," K. Klier, A. Beretta, Q. Sun, O. C. Feeley, and R. G. Herman, in *"Proc. of the Workshop on Environmental Catalysis: The Role of IB Metals,"* Osaka, Japan, Osaka National Research Institute, AIST-MITI, 6-15 (1995).

"Production of Methanol and Isobutanol Mixtures Over Double-Bed Cs-Promoted Cu/ZnO/Cr₂O₃ and ZnO/Cr₂O₃ Catalysts," A. Beretta, Q. Sun, R. G. Herman, and K. Klier, Ing. Eng. Chem. Res., **35**, 1534-1542 (1996).

"Surface Acidity (Brønsted and Lewis) by High Resolution X-Ray Photoelectron Spectroscopy," M. Johansson and K. Klier, Catal. Lett. (1996); in press.

"High Pressure Methanol Synthesis Over Zirconia Supported Copper Catalysts," Y. Cai, M. M. Burcham, B. Roy, R. G. Herman, and K. Klier, J. Catal., manuscript under revision.

"Higher Alcohol Synthesis Over Cesium-Promoted Cu/ZnO/Cr₂O₃ and ZnO/Cr₂O₃ Catalysts in a Double Bed Reactor Configuration at High Temperatures and Pressures," M. M. Burcham, Y. Cai, R. G. Herman, and K. Klier, Ing. Eng. Chem. Res., manuscript under revision.

• Recent Publications Resulting From the Ether Synthesis Research carried out during the Previous Research Period:

"Coupling of Alcohols to Ethers: the Dominance of the Surface S_N2 Reaction Pathway," K. Klier, Q. Sun, O. C. Feeley, M. Johansson, and R. G. Herman, in *"11th Intern. Congr. Catal.-40th Ann.,"* (Studies in Surface Science and Catalysis), **101A**, ed. by J. W. Hightower, W. N. Delgass, E. Iglesia, and A. T. Bell, Elsevier, Amsterdam, 601-610 (1996).

"Kinetic Evaluation of the Direct Synthesis of Ethers from Alcohols over Sulfonated Resin Catalysts," L. Lietti, Q. Sun, R. G. Herman, and K. Klier, Catal. Today, **27**, 151-158 (1996).

"Chirality Inversion in HZSM-5 and Nafion-H Solid Acid-Catalyzed Synthesis of Ethers from Alcohols *via* Surface S_N2 Reaction," Q. Sun, R. G. Herman, and K. Klier, J. Chem. Soc., Chem. Commun., 1849-1850 (1995).

"Selective Isotopic Oxygen Incorporation into C_5 and C_6 Ethers *via* Solid Acid Catalyzed Reaction of Methanol and Ethanol with Isobutanol," O. C. Feeley, Q. Sun, R. G. Herman, M. Johansson, L. Lietti, and K. Klier, Catal. Letters, **35**, 13-22 (1995).

"Mechanistic Studies of the Pathways Leading to Ethers *via* Coupling of Alcohols," Q. Sun, L. Lietti, R. G. Herman, and K. Klier, Preprints, Div. Fuel Chem., ACS, **40(1)**, 138-141 (1995).

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