

APPENDIX A

Co Catalyst Formulations

Catalyst Prep #	WGS.09	Date Tech	Jul-13-94	Amount	500.0 g
Compound (%wt)		Cu	Cr		Al ₂ O ₃
		5	4		

Support	y-Alumina VISTA B	Amount	455.00 g
Particle Size	400 - 0 mesh	Treatment	500°C / 10 hrs
Metal I	Copper (II) Nitrate	Amount	95.03 g
Metal II	Chromium (III) Nitrate	Amount	153.85 g
Promoter		Amount	
Promoter		Amount	
Promoter		Amount	

PROCEDURE			
Preparation	X	Incipient Wetness Ion Exchange	Wet Impregnation Other
Notes	Incipient wetness: aqueous solution Cu + Cr, ca. 1.2 ml/g Dry catalyst precursor in an oven 110°C / 16 hrs		
Calcination	Temperature	<u>500°C</u>	Time <u>24 hrs</u>
Notes			

WGS.09 5 wt% Cu
 4 wt% Cr
 γ -alumina

Preparation Procedure of Cu-Cr/ γ -alumina

Calcine γ -alumina at 500°C for 10 hrs. Use Vista B alumina. Presieve to >38 microns (400-0 mesh).

Impregnate the support with an aqueous solution of $\text{Cu}(\text{NO}_3)_2 \cdot x\text{H}_2\text{O}$, and $\text{Cr}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ using appropriate quantities to yield 5 wt% Cu, and 4 wt% Cr and to get incipient wetness (ca. 1.2 ml/g).

Dry the catalyst precursor in an oven for 16 hours at 110°C.

The dried catalyst is then calcined in air by raising its temperature at a heating rate of ca. 1°C/min to 500°C and holding for 24 hours.

Reduction Procedure before Reaction:

Heat the catalyst in inert gas to 120°C at a rate of 1°C/min then start adding hydrogen to give a concentration of 0.5% at the bed inlet. Raise the catalyst bed temperature to 165°C at a rate of ca. 30°C/hr. When the temperature of the bed has reached 165°C increase the hydrogen concentration in the carrier gas to 1.0%. As the reduction proceeds and the temperature rise begins to diminish, the inlet temperature may be raised to 200°C. The inlet hydrogen concentration can then be increased to about 3-5%, provided that the maximum temperature limit of 230°C is not exceeded. When the reduction appears to be complete the inlet temperature should be raised to 230°C and the inlet hydrogen concentration raised to ca. 20%.

Catalyst Handbook 2nd ed. Martyn V. Twigg
J. Catal. 137, 408-422 (1992)

Catalyst Prep #	Co.055	Date Tech	July 12-1994	Amount	200.0 g
Compound (%wt)		Co	Re	La2O3	Al2O3
		20	1	1	

Support	γ -Alumina / Vista-B	Amount	156.00 g
Particle Size	400 - 0 mesh	Treatment	500°C / 10 hr
Cobalt	Cobalt Nitrate	Amount	197.29 g
Metal	Perrhenic Acid	Amount	3.67 g
Promotor	La-Nitrate / Molycorp C5247	Amount	5.31 g
Promotor		Amount	
Promotor		Amount	

PROCEDURE

Preparation	X	Incipient Wetness	Wet Impregnation
		Ion Exchange	Other
Notes	Incipient wetness: aqueous solution - ca. 1.2 ml/g support Dry catalyst precursor in an oven at 115°C / 5 hr		

Calcination	Temperature	300°C	Time	2 hr
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Notes: 50g of the catalyst precursor are not to be calcined !!

Catalyst Prep #	Co.056	Date Tech	Jul-12-94	Amount	200.0 g
Compound (%wt)	Co	La		SiO ₂	
	20	8.5			

Support	Silica Davison Grade 952	Amount	143.00 g
Particle Size	400 - 250 mesh	Treatment	500°C / 10 hrs
Cobalt	Cobalt Nitrate	Amount	197.29 g
Metal		Amount	
Promotor	La-Nitrate/Molycorp	Amount	105.91 g
Promotor		Amount	
Promotor		Amount	

PROCEDURE

Preparation	X	Incipient Wetness Ion Exchange	Wet Impregnation Other
Notes	Incipient wetness: aqueous solution of La Dry catalyst precursor in an oven 115°C / 5 hrs with stirring/calcine at 300 °C/2hrs Incipient wetness: aqueous solution of Co with catalyst precursor Dry catalyst precursor in an oven 115°C / 5 hrs with stirring		

Calcination	Temperature	300°C	Time	2 hrs
Notes	50g of the catalyst precursor are not to be calcined !!			

Co.056: 20 wt% Co
 8.5 wt% La
 SiO₂

La-promoted SiO₂-supported catalyst comparable to Co.025 where Zr is replaced by La. One-step impregnation of silica with lanthanum nitrate followed by one-step impregnation with cobalt nitrate solution.

Preparation Procedure:

Calcine the SiO₂ at 500°C for 10 hrs. Presieve to >38 microns (400-0 mesh).

Impregnate the support with an aqueous solution of La nitrate using an appropriate quantity to get incipient wetness with the desired loading of La.

Dry the La-loaded SiO₂ in an oven for 5 hrs at 115°C with moderate stirring.

Calcine the dried support in air by raising its temperature at a heating rate of ca. 1°C/min to 300°C and holding for 2 hrs.

Impregnate the La-loaded silica with an aqueous solution of Co nitrate [Co(NO₃)₂·6H₂O] using an appropriate quantity to get incipient wetness with the desired loading of Co.

Dry the catalyst precursor in an oven for 5 hrs at 115°C with moderate stirring.

Calcine the dried catalyst in air by raising its temperature at a heating rate of ca. 1°C/min to 300°C and holding for 2 hrs.

Reduction Procedure before Reaction:

Reduce the catalyst in a pure hydrogen flow of 3000 cc/g/hr by heating at 1°C/min to 250°C and holding for 10 hrs.

CoW.07

20 wt% Co
5 wt% Cu
4 wt% Cr
Silica

Cobalt impregnation on calcined Cu-Cr/Silica. Similar to CoW.06, but Cu-Cr/SiO₂ calcined at 750°C.

Preparation Procedure

Calcine silica at 500°C for 10 hrs. Use Davison Grade 952 silica. Presieve to > 38 microns (400-0 mesh).

Impregnate the support with an aqueous solution of Cu(NO₃)₂·xH₂O, and Cr(NO₃)₃·9H₂O using appropriate quantity to get incipient wetness (ca. 1.2 ml/g) with the desired loading of Cu and Cr.

Dry the catalyst precursor in an oven for 16 hours at 110°C.

The dried catalyst precursor is then calcined in air by raising its temperature at a heating rate of ca. 1°C/min to 750°C and holding for 24 hours.

Impregnate the Cu-Cr/SiO₂ with an aqueous solution of Co nitrate [Co(NO₃)₂·6H₂O] using an appropriate quantity to get incipient wetness with the desired loading of Co.

Dry the catalyst precursor in an oven for 5 hrs at 115°C with moderate stirring.

Calcine the dried catalyst in air by raising its temperature at a heating rate of ca. 1°C/min to 300°C and holding for 10 hrs.

Reduction Procedure before Reaction:

Heat the catalyst in inert gas to 120°C at a rate of 1°C/min then start adding hydrogen to give a concentration of 0.5% at the bed inlet. Raise the catalyst bed temperature to 165°C at a rate of ca. 30°C/hr. When the temperature of the bed has reached 160°C increase the hydrogen concentration in the carrier gas to 1.0%. As the reduction proceeds and the temperature rise begins to diminish, the inlet temperature may be raised to 200°C. The inlet hydrogen concentration can then be increased to about 3-5%, provided that the maximum temperature limit of 230°C is not exceeded. When the reduction appears to be complete the inlet temperature should be raised to 230°C and the inlet hydrogen concentration raised to ca. 20%.