Isotopic Tracer Studies of Fischer-Tropsch Synthesis over Ru/TiO₂ Catalysts

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by

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ABSTRACT

react to give predominantly liquid hydrocarbons. The reaction can be considered a special type of polymerization in which the monomer is produced *in situ*, and chain growth occurs by a sequence of independently repeated additions of the monomer to the growing chain. An investigation has been conducted to study the CO hydrogenation reaction in order to better understand catalyst deactivation and the elementary surface processes involved in chain growth.

Isotopic tracers are used in conjunction with transient-response techniques in this study of Fischer-Tropsch synthesis over Ru/TiO₂ catalysts. Experiments are conducted at a total pressure of 1 atmosphere, reaction temperatures of 453-498 K and D₂/CO (or H₂/CO) ratios of 2-5. Synthesis products are analyzed by gas chromatography or isotope-ratio gas chromatography-mass spectrometry.

Ru/TiO₂ catalysts deactivate with no change of product selectivity and the rate of deactivation correlates with initial

catalyst activity. Deactivation occurs at an initial rapid rate, followed by a slower activity loss. Deactivation is accompanied by a loss in CO uptake and the accumulation of various types of carbonaceous species. The long-term loss of activity is attributed to the buildup of long chain hydrocarbon product species.

Rate constants for chain initiation, propagation and termination are evaluated under steady-state reaction conditions by using transients in isotopic composition. The activation energy for chain termination is much higher than that for propagation, accounting for the observed decrease in the chain growth parameter with increasing temperature. Coverages by reaction intermediates are also estimated. The dominant reactive surface species are monomeric building units, which occupy 0.2-0.6 ML. Alkyl species that are the direct hydrocarbon product precursors occupy < 0.2 ML. Adsorbed CO covers 0.7 ML.

When small amounts of ¹²C-labelled ethylene are added to ¹³CO/H₂ synthesis gas, ethylene acts as the sole chain initiator. Ethylene-derived carbon also accounts for 45 % of the C₁ monomer pool.

To

my parents,

my parents-in-law,

Ashok,

and

Ananth.

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List of Symbols

ASF	Anderson-Schulz-Flory
C_{α}	Carbidic carbon (ML)
C_{β}	Alkyl carbon chains (ML)
C _β '	Alkyl carbon chains that are precursors to the C2+
	hydrocarbon products (ML)
C _β "	Unreactive alkyl chains, of longer chain length than C_{β}
	(ML)
F ₁	Fraction of labelled carbon in the surface precursor to
	methane
F _m	Fraction of labelled carbon in the monomer pool
Fn	Fraction of labelled carbon in the pool of carbon chain
	length n
K	Equilibrium constant for CO adsorption
k	Rate parameter
k _i	Initiation rate constant (s-1)
k _p	Intrinsic Rate constant for propagation (s-1)
k _p '	Apparent rate constant for propagation (s-1)
k _t	Rate constant for termination (s-1)
k ₁	Rate constant
k ₂	Rate constant
kз	Rate constant
ML_	Monolayer, unit of coverage based on hydrogen
	chemisorption to estimate the number of surface exposed

Ru atoms

	nu atoms
No	Turnover frequency of CO (s-1) i.e., moles of CO converted
	per moles of surface-exposed metal atoms per sec
N∞°	Apparent turnover frequency of CO at $t_r = 0$ min
N _{C1}	Turnover frequency of methane (s-1)
N _C ,	Turnover frequency of products of carbon chain length n
	(S-1)
n	Carbon number
n _{av}	Average carbon number of hydrocarbon products
P∞	Partial pressure of CO
t _r	Time onstream after reaction startup
α	ASF chain growth probability or chain growth parameter
Ө	Surface coverage
θω	CO coverage (ML)
θm	Coverage by monomer building block
θ ₁	Coverage by methane precursor
Θ_{Π}	Coverage by precursor to hydrocarbon products of chain
	length n
θ_{α}	Coverage by $C_{\alpha} + C_{\beta}$ (ML)
Θ _β "	Coverage by C _β " (ML)
τ	Lifetime of surface alkyl chains
τ_{m}	Lifetime of monomer pool

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