

91-000634/11 H04 MOB 29.12.89  
 MOBIL OIL CORP \*US 4995-962-A

29.12.89-US-459154 (26.02.91) C10g-47/20  
 Hydroisomerisation of paraffin wax with catalyst comprising a  
 pillared layered titanate and hydrogenation metal  
 C91-034300

H(4-E, 4-F2E) N(2,3-C,3-D)

#### PROCESS

The wax is pref. deoiled microcrystalline, intermediate, or paraffin wax, esp. a hydroprocessed or synthetic (e.g. Fischer-Tropsch) wax product.

The process takes place at 200 - 3000 psig, 232 - 454°C  
 LHSV 0.05 - 10, hydrogen circulation 500 - 10,000 scf/bbl.

#### EXAMPLE

A silicotitanate catalyst containing 0.99 wt. % Pt was prep'd. by forming an octylammonium swollen trititanate, treated there of with tetraethylorthosilicate to produce a pillared material, and exchange of the latter with a  $Pt(NH_3)_4Cl_2$  solution.

This catalyst was used to convert a hydrotreated paraffin wax at 400 psig, 0.5 LHSV. Fig. shows lube oil yield for a given pour point. Yields were 5 - 10 wt. % higher than obtained with a comparison catalyst consisting of Pt on silica-alumina. The Pt/silicotitanate catalyst was ca. 25°F more active than the Pt/silica-alumina catalyst on the same LHSV basis.

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A petroleum wax or synthetic paraffin wax is hydroisomerised to reduce its pour point by contact with a hydroisomerisation catalyst comprising:

- (a) a layered titanate containing interspathic polymeric oxide; and  
 (b) a hydrogenation component selected from Fe, Co, Ni, Ru, Rh, Pd, Os, Ir and Pt.

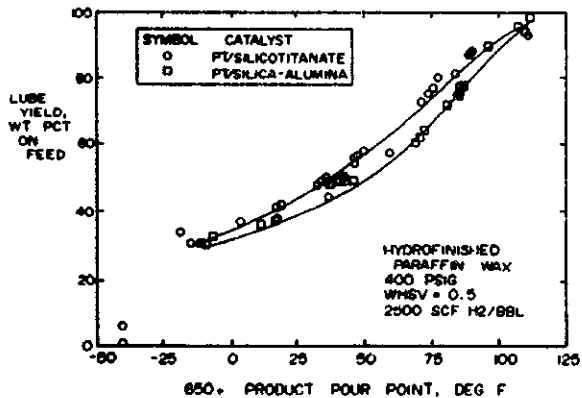
#### ADVANTAGE/USE

The pour point of the wax is lowered to give a salable high VI product of lube oil boiling range. Overcracking to lower mol. wt. materials outside this range is minimised.

#### CATALYST

Suitable catalysts are described in US 4600503. The polymeric oxide is esp. silica and (b) is esp. Pt. The catalyst may further comprise a binder, e.g. alumina.

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