acid.

E(31-N4C, 35-U5) H(4-E5, 4-F2E) J(4-E4) N(2-A, 4-A)

91-149895/21 E17 H04 J04 (H08) SASO- 14.11.89 *DE 4035-544-A SASOL IND PTY LTD 14.11.89-ZA-008668 (16.05.91) B01j-21/18 B01j-23/74 C07c-01/04 C07c-09/22 Solid-bed fischer-tropsch catalyst for wax prodn. - obtd. by adding 1-80 wt. per cent active carbon, w.r.t. Iron content of catalyst at any stage before extrusion C91-064806 Catalyst (1) for Fischer-Tropsch process contains active carbon (11). Prodn. of an Fe-based catalyst (I) is also claimed and comprises adding 1 - 80 wt. % (II) (w.r.t. amt. of Fe) to one of the catalyst precursors at any stage before extrusion. Pareffin wax obtd. by the process is further claimed. USE/ADVANTAGE (I) is useful for the prodn. of hydrocarbon waxes with improved colour, by contacting a suitable synthesis gas with (I) in a solid-bed reactor at elevated temp. and pressure. Catalyst (I) gives wax with a high Saybolt no. (pref. at least 20) directly, without the need for subsequent hydrogenation.

MORE SPECIFICALLY
(1) is useful for the low-temp, variant of the Fischer-Tropsch, esp, as a solid-bed catalyst.

Amt. of (II) is 1 - 80 (5-10) wt. % w.r.t. Fe, and (II) is uniformly distributed in (I). At least 50 (at least 90) wt. % of the particles of (II) are smaller than 100 μ, pref. with at least 90 wt. % smaller than 45 μ, or the same proportion is in the size range 850 - 1200 μ.
(II) is produced from pinewood tanniferous acacia or coconut shells, and is preactivated with steam or mineral

FURTHER DETAILS
Incorporation of (II) with the above particle size gives catalyst grains with a higher side-crushing strength. A suitable active carbon (II) is Ceca 2S (RTM).

(II) is pref. preactivated with steam at 600°C before incorporation into (I).

EXAMPLE

A solid-bed iron-based Fischer-Tropsch catalyst was produced as described by Frohning et al. in DE4035544-A+