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Synthesis gas from prodn. hydrocarbon esp. methane - by conversion with steam to prod. contg. hydrogen and carbon monoxide, catalytic partial oxidn. of prod. and removal of carbon dioxide

C87-024287 E(AT BE CH DE FR GB IT NL)

E(10-J2D, 31-A1) H(4-E4, 4-F2E) N(2-C)

Synthesis gas is prepd. from a hydrocarbon-contg. feed (I) by

- (a) converting at least part of (I) at elevated temp. and pressure with steam to a product (II) containing  $H_2$  and  $CO$ ;  
 (b) subjecting (II) and any remaining (I) to catalytic partial oxidn. with an  $O_2$ -contg. gas (III); and  
 (c) removing  $CO_2$  from the prod. of step (b).

#### ADVANTAGE

By carrying out step (b) after step (a), extreme conditions in (a) are avoided. (I) is esp. methane or natural gas. Synthesis gas obtd. may be converted to hydrocarbons with a Fischer-Tropsch catalyst.

#### PREFERRED CONDITIONS

Step (a) takes place at 500-900° C, 15-30 bar, with a catalyst, e.g. Ni supported on alumina, or at higher temp. in

absence of a catalyst; space velocity of hydrocarbon is 700-1000 and that of steam is 3800-4200 l. (S.T.P.)l. catalyst/hr. Step (b) takes place at 600-1100° C, 10-50 bar, space velocity 5000-10000 l./l./hr., with a nickel on alumina catalyst.

$CO_2$  removed in step (c) may be fed to step (a) and/or step (b); further  $CO_2$  for feed to these stages may be obtd. by additional steps of converting hydrocarbon + steam to a prod., contg.  $CO_2$  and  $H_2$ , partial oxidn., and recovery of  $CO_2$ . Some of the synthesis gas produced in the reaction may be converted to light hydrocarbons which are added to the feed of step (a).

#### EXAMPLE

Natural gas (800 l./l./hr.) and steam (4000 l./l./hr.) are contacted at 500-850° C, 38 bar, with a supported nickel catalyst; 90 vol. % of the natural gas is converted. The product, containing 85 vol. %  $H_2$  +  $CO$ , is contacted with oxygen and a supported nickel catalyst at 8500 l./l./hr., temp. up to 950° C, 35 bar.  $CO_2$  is separated from the product by absorption with a liquid organic amino cpd. After  $CO_2$  removal, product is 97 vol. %  $H_2$  +  $CO$ , in

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molar H<sub>2</sub>/CO ratio 3.9:1. (9pp1644RKMHDwgNo0/7).  
(E)ISR: No Search Report.

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