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MONSANTO CO *EP --61-259
13.03.81-US-243273 (+243220) (29.09.82) C01b-03/50 C10g-47
C10g-49/22
Hydrocracking process with increased hydrogen utilisation - with recycle of hydrogen-rich stream obtd. by passing vapour from hydrocrackate through polymeric membrane

D/S: E(DE FR GB IT NL)

A catalytic hydrocracking process is claimed in which (a) a hydrocarbonaceous feed is hydrocracked in the presence of a catalyst and H₂ at at least 250°C and 45 ata, the reaction zone contg. a vapour phase (I) and a liquid phase and the H₂ being supplied by a feed gas contg. > 75 vol.% H₂ in such amounts that the H₂ concn. in (I) is > 65 vol.%, (b) the hydrocrackate is sepd. into liquid (II) and vapour (III) phases, (III) being at such a temp. and pressure that it is in equilibrium with (II) and has a greater H₂ concn. than the minimum H₂ concn. of (I), (c) contacting (III) with a polymeric membrane which is selectively permeable to H₂ compared with nitrogen or methane, and (d) withdrawing H₂ permeate from the low-pressure side of the membrane, compressing it and recycling it to the hydrocracking zone.

ADVANTAGES

The hydrogen utilisation efficiency is increased without

H(4-B3, 4-E6)

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deleterious effects on the operation of the hydrocracker. Furthermore, the throughput of hydrocarbon feedstock can be increased and the C5+ yield is also increased.

DETAILS

The pressure of (III) is pref. at least 0.5 (esp. 0.9-1) times the pressure in the hydrocracking zone. The temp. of (III) is pref. < 70°C and (III) pref. contains at > 75 vol.% H₂. At least 5% of (III), and pref. all of it, is contacted with the membrane.

The membrane pref. operates with a pressure difference

of \$20 atmospheres, and \$50% of the H₂ in the vapour on the feed side should permeate the membrane.

To produce (III), the hydrocrackate is pref. separated at elevated temp. into vapour and liq. and the vapour is cooled to below 70°C to form (II) and (III).(26pp909).
(E) ISR:- US3471397; US3733260; FR2265673.