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76143 D/42 E17 H09 (H04) MOBI 24.03.80
 MOBIL OIL CORP *EP--37-213
 24.03.80-US-133384 (07.10 81) B01i-29/30 C07c-01/04
 Conversion of synthesis gas into hydrocarbon rich in alpha-olefin -
 using non-active ZSM-5 type zeolite contg. carbon oxide-reducing
 component in its pores

E(10-J2C3) H(4-E5) N(6-B)

086

0.5-2 (esp. 1) : 1; and a pressure of 3.4-68 (esp. 10.2-27.2)
 atm.g.

EXAMPLE

ZSM-5 having a $\text{SiO}_2/\text{Al}_2\text{O}_3$ ratio of 1600, a Na content of
 1.6 wt.% and K content of 1 wt.% was impregnated with aq.
 soln, contg. 1 wt.% Fe. Conversion of syngas was at 27.2 -
 54.4 atm.g., 288-316 °C and 520-740 GHSV. Conversion
 was 10% and the prod. contained 67.04% linear α -olefins.
 (24pp959)

(E)ISR: US4172843 US4086262

D/S: E(BE DE FR GB IT NL)

Synthesis gas is converted into hydrocarbons by contact at
 elevated temp. with a non-active ZSM-5 type zeolite having
 a carbon oxide-reducing component (I) in its pores.

USE/ADVANTAGES

The use of the above catalyst enhances the selectivity of
 the product to linear alpha-olefins (esp. 4-6C olefins) which
 can be used in the prodn. of soaps and lubricants.

DETAILS

(I) is esp. a Fischer-Tropsch catalyst (e.g. Fe, Co or
 Ru). The acidity, if any, of the zeolite is eliminated by
 base exchange e.g. with Na. (I) is included in the pores of
 the zeolite by impregnation with an aq. soln. of a salt of the
 desired metal (e.g. a nitrate).

The process is carried out at 260-343 (esp. 287-316)°C;
 a GHSV of 400-20,000 (esp. 500-6,000); a H_2 : COx ratio of

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