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Aromatic hydrocarbon prodn. from carbon monoxide and hydrogen - using a catalyst mixt. of an acyclic oxygen contg. hydrocarbon prodn. catalyst and a crystalline gallium silicate

Aromatic hydrocarbon mixts. are prepd. from synthesis gas (CO + H₂) using a mixt. of two catalysts. One catalyst (X) is capable of converting the H₂/CO mixt. into acyclic oxygen-contg. hydrocarbons, while the other (Y) is a crystalline gallium silicate having (a) a characteristic X-ray powder diffraction diagram (radiation Cu-K alpha 2 theta/relative intensity, wavelength 0.15418 nm; where ZS= very strong; S = strong; M = medium; Z = weak; theta = Bragg angle) 7.8-8.2, S; 8.7-9.1, M; 11.8-12.1, Z; 12.4-12.7, Z; 14.6-14.9, Z; 15.4-15.7, Z; 15.8-16.1, Z; 17.6-17.9, Z; 19.2-19.5, Z; 20.2-20.6, Z; 20.7-21.1, Z; 23.1-23.4, ZS; 23.8-24.1, ZS; 24.2-24.8, S; 29.7-30.1, M., and (b) a formula, expressed as the oxides (omitting those of H and alkali(ne earth) metals), in which the Ga₂O₃/SiO₂ mol. ratio is less than 0.1.

Component (X) is pref. a Zn/Cr catalyst in which the atomic percentage Zn/Zn+Cr is at least 60 (pref. 60-80)%. The catalysts pref. contain 1-5 pts. vol. (X) per pt. vol. (Y).

ADVANTAGE

E(10-J2B3) H(4-E1, 4-E5, 4-F2E) J(4-E1, 4-E4) N(1-D, 3-D, 3-F)

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The catalysts have high activity and high selectivity.

DETAILS

The H₂/CO mixt. pref. has a mol. ratio of 0.25-1.0. Conversion is pref. carried out at 200-500 (esp. 300-450) deg.C, 1-150 (esp. 5-100) bars, and a GHSV of 300-3000.

EXAMPLE

Crystalline silicates were prepd. from mixts. of SiO₂, NaOH, ((C₃H₇)₃N)OH and Ga(NO₃)₃ in water, heated in an autoclave for 24 hours at 150 deg.C. The prods. were filtered off, washed, dried and calcined at 500 deg.C. A typical prod. had a Ga₂O₃/SiO₂ ratio of 0.0185. This was boiled with 1 M NH₄OH, dried and calcined at 500 deg.C again, then 1 pt. of the silicate was mixed with 10 pts. of a ZnO-Cr₂O₃ catalyst contg. 70 atom% Zn.

The catalyst was used for conversion of a H₂/CO mixt. having a H₂/CO mol. ratio of 0.5, at 375 deg.C, 60 bars and a GHSV of 1000. After 10 hours' operation, the conversion was 67% with a selectivity of C₅+ material of 77%. Over 50% of the C₅+ fraction was aromatic. (15pp513).

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of 50 deg.C. After 15 mins the foam was removed from the mould and treated in a forced air circulation oven for 2 hrs. at a wet bulb temp. of 55 deg.C. and a dry bulb temp. of 65 deg.C. A rigid foam with a smooth surface and uniform cell structure throughout was obtd. The prod. had a compressive strength of 207 kPa at 23 deg.C/50% R.H. (29pp513).