

## MASTER

TRANSITION METAL CHEMISTRY UNDER HIGH CARBON MONOXIDE PRESSURE: AN INFRARED SPECTROSCOPIC STUDY OF CATALYSIS IN THE FISCHER-TROPSCH REACTION

- R. B. King, Regents' Professor and Co-Principal Investigator
- A. D. King, Jr., Associate Professor and Co-Principal Investigator
- M. Z. Iqbal, Post-Doctoral Fellow
- C. C. Frazier, Post-Doctoral Fellow
- K. Tanaka, Post-Doctoral Fellow
- D. B. Yang, Post-Doctoral Fellow

Department of Chemistry University of Georgia Athens, Georgia 30602

This impact was perpared as an include of an exsense the second of the

January, 1979

PREPARED FOR THE U. S. DEPARTMENT OF ENERGY UNDER CONTRACT EY-76-S-09-0933

# **BLANK PAGE**

.

•

#### REFERENCES

- Annual progress report dated January, 1977, covering work performed under ERDA
   Contract E(38-1)-933 (now Contract EY-76-S-09-0933) during the period May 14, 1976, to December 31, 1976.
- (2) Annual progress report dated January, 1978, covering work performed under Department of Energy Contract EY-76-S-09-0933 during the period January 1, 1977, to December 31, 1977.
- (3) Research proposal entitled "Transition Metal Chemistry under High Carbon Monoxide Pressure: An Infrared Spectroscopic Study of Catalysis in the Fischer-Tropsch Reaction" submitted by R. B. King and A. D. King, Jr., to ERDA in 1975 on the basis of which Contract E(38-1)-933 (now Contract EY-76-S-09-0933) was awarded.
- (4) J. W. Rathke and H. M. Feder, J. Am. Chem. Soc., 100, 3623 (1978).
- (5) R. B. King, A. D. King, Jr., M. Z. Iqbal, and C. C. Frazier, <u>J. Am. Chem. Soc.</u>, 100, 1687 (1978).
- R. B. King, C. C. Frazier, R. M. Hanes, and A. D. King, Jr., <u>J. Am. Chem. Soc.</u>, 100, 2925 (1978).
- (7) D. Evans, J. A. Osborn, and G. Wilkinson, J. Chem. Soc.A, 3133 (1968).
- (8) C. K. Brown and G. Wilkinson, J. Chem. Soc. A, 2753. (1970).
- J. H. Craddock, A. Hershman, F. E. Paulik, and J. F. Roth, Ind. Eng. Chem. Prod. Res. Dev., 8, 291 (1969).
- (10) J. Faibe, J. Organometal. Chem., 94, 213 (1975).
- (11) L. Markó, G. Bor, G. Almásy, and P. Szabó, Brennstoff. Chem., 44, 184 (1963).
- (12) B. Heil and L. Marko, <u>Ber.</u>, <u>101</u>, 2209 (1968); <u>102</u>, 2238 (1969).
- (13) R. Whyman, J. Chem. Soc. Dalton, 1375 (1972).

#### PUBLICATIONS FROM THIS PROJECT

- R. B. King, A. D. King, Jr., M. Z. Iqbal, and C. C. Frazier, "Transition Metal Alkyl Chemistry at Elevated Carbon Monoxide Pressures: An Infrared Spectroscopic Study of Systems Related to Catalytic Intermediates in Homogeneous Hydroformylation Reactions," J. Am. Chem. Soc., 100, 1687 (1978).
- (2) R. B. King, A. D. King, Jr., M. Z. Iqbal, C. C. Frazier, and R. M. Hanes, "Metal Carbonyl Catalysis of Carbon Monoxide Reactions," chapter for a book based on papers presented at the 2nd International Workshop on "Fundamental Research in Homogeneous Catalysis" in Lake Biwa, Japan, during the period September 16–18, 1977, and to be published by Plenum Press.
- (3) R. B. King, C. C. Frazier, R. M. Hanes, and A. D. King, Jr., "Active Homogeneous Catalysts for the Water Gas Shift Reaction Derived from the Simple Mononuclear Carbonyls of Iron, Chromium, Molybdenum, andTungsten," J. Am. Chem. Soc., 100, 2925 (1978).
- (4) C. C. Frazier, R. M. Hanes, A. D. King, Jr., and R. B. King, "Homogeneous Catalysis of the Water Gas Shift Reaction: Pentacarbonyliron and the Metal Hexacarbonyls as Active Catalyst Precursors," Advan. Chem. Ser., in press.
- (5) R. B. King, M. Z. Iqbal, and A. D. King, Jr., "?entamethylcyclopentadienyl Derivatives of Transition Metals. VI. Carbonylation of Metal-Metal Triple Bonds: A High Pressure Infrared Spectroscopic Study," to be published in J. Organometal. Chem. after making minor revisions in the original version.
- (6) R. B. King, A. D. King, Jr., and M. Z. Iqbal, "Rhodium Carbonyl Derivatives as Catalytic Intermediates in Homogeneous Hydroformylation Reactions: An Infrared Spectroscopic Study," submitted for publication (J. Am. Chem. Soc.).

#### MEETING PRESENTATIONS FROM THIS PROJECT

- R. B. King, A. D. King, Jr., M. Z. Iqbal, and C. C. Frazier, "Infrared Spectroscopy at High Pressures for the Investigation of Catalysis of Carbon Monoxide Reactions," presented by R. B. King at the 2nd joint conference of the Chemical Institute of Canada and the American Chemical Society, Montreal, P. Q., Canada, May 29-June 2, 1977: paper COLL25 in abstracts.
- (2) R. B. King, M. Z. Iqbal, C. C. Frazier, and A. D. King, Jr., "Infrared Spectroscopy at High Pressures for the Investigation of Reactions of Cycloper.tadienylmetal Derivatives with Carbon Monoxide," presented by R. B. King at the Eighth International Conference on Organometallic Chemistry, Kyoto, Japan, September, 1977.
- R. B. King, A. D. King, Jr., M. Z. Iqbal, C. C. Frazier, and R. M. Hanes, "Metal Carbonyl Catalysis of Carbon Monoxide Reactions," presented by R. B.
   <u>Ring-at the 2nd International Workshop on "Fundamental Research in Homogeneous</u> Catalysis, "Lake Biwa, Japan, September, 1977.
- (4) C. C. Frazier, R. Hanes, A. D. King, Jr., and R. B. King, "Homogeneous Catalysis of the Water Gas Shift Reaction: Pentacarbonyliron and the Metal Hexacarbonyls as Active Catalyst Precursors," presented by C. C. Frazier at a symposium on "In organic Compounds with Unusual Properties. II. Molecular Catalysis and the Conversion, Production, and Storage of Energy," Athens, Georgia, February, 1978.
- (5) R. B. King, A. D. King, Jr., R. M. Hanes, and C. C. Frazier, "Metal Carbonyls as Catalysts in the Water Gas Shift Reaction," presented by R. B. King at the 175th National Meeting of the American Chemical Society, Anaheim, California, March, 1978; paper INOR 119 in abstracts.
- (6) A. D. King, Jr., R. B. King, and M. Z. Iqbal, "The Relative Reactivities of Metal-Metal Triple Bonds Towards Addition of Carbon Monoxide: A High Pressure Infrared Spectroscopy Study," presented by A. D. King, Jr., at the 176th National Meeting of the American Chemical Society, Miami Beach, Florida, September, 1978, paper INOR 50 in abstracts.
- (7) R. B. King, M. Z. lqbal, and A. D. King, Jr., "Rhodium Carbonyl Derivatives as Catalytic Intermediates in Homogeneous Hydroformylation Reactions: an Infrared Spectroscopy Study," presented by R. B. King at the Symposium on Rhodium in Homogeneous Catalysis, Veszprém, Hungary, September, 1978: abstracts p. 84.

- (8) R. B. King, D. B. Yang, C. C. Frazier, and A. D. King, Jr., "Kinetics of the Water Gas Shift Reaction Catalyzed by Iron Carbonyls," paper scheduled for presentation by A. D. King, Jr., at the Sixth North American Meeting of the Catalysis Society, Chicago, Illinois, March, 1979.
- (9) R. B. King, A. D. King, Jr., M. Z. Iqbal, and K. Tanaka, "Intermediates in the Rhodium-Catalyzed Hydroiomylation of Olefins," paper scheduled for presentation by R. B. King at the New York Academy of Sciences Conference on Transition Metal Mediated Organic Syntheses, New York, New York, April, 1979.

### Metal Carbonyls as Catalysts for the Water Gas Shift Reaction

An important discovery during the previous project period<sup>2,6</sup> was the observation that simple mononuclear metal carbonyls, specifically  $M(CO)_6$  (M = Cr, Mo, and W) and  $Fe(CO)_5$ , were active catalysts for the water gas shift reaction (equation 2). In fact, the high activity of these simple and inexpensive catalyst systems at temperatures around 150°C makes such systems of considerable interest for hydrogen production. During the present project period

$$CO + H_2O \xrightarrow{} CO_2 + H_2 \qquad (2)$$

we have improved the accuracy and convenience of our gas chromatographic analytical technique: by the installation of an automated chromatographic data system. We have investigated the catalyst system derived from treatment of Fe(CO)<sub>5</sub> with a base (hydroxide, carbonate, or formate) in greatest detail and have observed the following effects of the indicated variables on this reaction:

(1) Solvent: Experiments using various methanol/water solvent mixtures and potassium hydroxide as the base indicate that an approximately 3:1 methanol/water solvent mixture gives the maximum rate of hydrogen production.

(2) Temperature: A series of runs in the temperature range 120°C to 160°C using the optimum 3:1 methanol/water solvent mixture indicates an activation energy of ca. 29 kcal/mole.

3) Basicity: If the initial hydroxide concentration is greater than 0.1 M, reaction of hydroxide with CO to give formate occurs in preference to the water gas shift reaction. However, as the hydroxide concentration falls to ca. 0.1 M, this reaction ceases and the water gas shift reaction (equation 2) begins. The latter mode of reaction dominates until all reaction ceases at a phi of approximately 7. The water gas shift reaction is catalytic in base, however, in that the moles of H<sub>2</sub> produced far exceed the moles of base initially introduced into the system. Presumably the CO<sub>2</sub> produced in the H<sub>2</sub>Fe (CO)<sub>4</sub>/HFe (CO)<sub>4</sub><sup>-</sup>/Fe (CO)<sub>4</sub><sup>-</sup> system over the pH range in which the water gas shift reaction occurs is HFe (CO)<sub>4</sub> suggesting that HFe (CO)<sub>4</sub><sup>-</sup> is the catalytically active species in these mixtures.

(4) Base Counterion: Using bases containing an alkaline-earth metal counterion  $(Ca(OH)_2 o: Ba(OH)_2)$  in 3:1 methanol/water leads to a reaction rate about 10% that of corresponding reaction: using a base with an alkali metal counterion (e.g. KOH). Furthermore, the reaction stops completely after a relatively short time with a final pH of approximately 5. This is no doubt a consequence of the insolubility of divalent metal carbonates (i.e. CaCO<sub>3</sub> or BaCO<sub>3</sub>) in the aqueous methanol reaction medium which removes base irreversibly from the reaction solution by the following equation:

 $M^{2+} + 2OH^{-} + CO_2 \longrightarrow MCO_3 \checkmark + H_2O$  (3)

Removal of base according to this process results in cessation of the reaction after a short time.

-3-

(5) CO pressure: The rate of the reaction is independent of the CO pressure, at least to the pressure range 7 to 30 atmospheres and using potassium hydroxide or sodium carbonate as the base. This suggests that reaction with CO is not involved in the rate-determining step of the reaction mechanism.

Recently we have begun a similar detailed investigation of the  $W(CO)_6$ /base system as a catalyst for the water gas shift reaction (equation 2) in order to assess the effects on the above observation of changing the central metal atom to one having significantly different chemistry. In these studies the role of the solvent system is more pronounced due to the relative insolubility of  $W(CO)_6$ . Nevertheless,  $W(CO)_6$  generates rather active catalyst systems whose detailed features currently are being investigated.

#### Rhodium Hydroformylation Catalysts

Certain rhodium compounds are known to be active catalysts for the hydroformylation of olefins (e.g. equation 4 in the case of ethylene).<sup>7,8,9,10</sup> The currently accepted mechanism for such hydroformylation reactions can be summarized by the following

$$C_2H_4 + CO + H_2 \longrightarrow C_2H_5C(O)H$$
(4)

series of equations for the hydroformylation of ethylene with a rhodium catalyst (5a-5h):

$HRh(CO)_4  HRh(CO)_3 + CO$	(5 <b>a</b> )
$HRh(CO)_3 + C_2H_4$ HRh(CO) <sub>3</sub> (C <sub>2</sub> H <sub>4</sub> )	(5b)
$HRh(CO)_{3}(C_{2}H_{4})  C_{2}H_{5}Rh(CO)_{3}$	(5c)
$C_2H_5Rh(CO)_3 + CO_2H_5Rh(CO)_4$	(5d)
$C_2H_5Rh(CO)_4$ $C_2H_5CORh(CO)_3$	(5e)
$C_2H_5CORh(CO)_3 + H_2  C_2H_5CORh(CO)_3H_2$	(5f)
$C_2H_5CORh(CO)_3H_2 \longrightarrow C_2H_5C(O)H + HRh(CO)_3$	(5g)
$HRh(CO)_3 + CO_{} HRh(CO)_4$	(5h)

In an attempt to obtain more direct evidence for some of these intermediates we have now investigated reactions of a variety of rhodium complexes with 1:1:1  $CO/C_2H_4/H_2$  mixtures in our high pressure infrared cell.

Diverse rhadium (I) carbonyl derivatives including  $[Rh(CO)_2CI]_2$ ,  $C_5H_5NRh(CO)_2C1$ ,  $[CH_3CO_2Rh(CO)_2]_2$ , and  $C_5H_7O_2Rh(CO)_2$  were found in the high pressure infrared cell to generate systems that catalyse the hydroformylation of ethylene under mild conditions (e.g.  $35^{\circ}C$  and 20 to 100 atmospheres total pressure). More interestingly, in several such systems, the infrared  $\nu$  (CO) frequencies (2115 w, 2037 s, 2019 s cm.<sup>-1</sup>) assigned to an unstable RRh (CO)<sub>4</sub> rhodium alkyl were found. The assignments of these frequencies were based on analogy with the reported<sup>11</sup>  $\nu$  (CO) frequencies of an analogous cobalt compound CH<sub>3</sub>Co(CO)<sub>4</sub> (2105 w, 2036 m, 2019 vs cm.<sup>-1</sup>). This is the first direct evidence for the existence of rhodium alkyls of the type RRh(CO)<sub>4</sub>, apparently a very unstable class of compounds. Unfortunately, Infrared spectroscopy does not provide information on the exact alkyl group attact commodium in the RRh (CO)<sub>4</sub> derivative. However, the similarity in the positions of the v(CO) frequencies in this RRh (CO)<sub>4</sub> derivative to those listed above for the CH<sub>3</sub>Co (CO)<sub>4</sub> model compound suggests that the electronic properties of the R group in the RRh (CO)<sub>4</sub> derivative must be fairly close to those of the methyl group. It therefore is highly likely that this unknown RRh (CO)<sub>4</sub> derivative is C<sub>2</sub>H<sub>5</sub>Rh (CO)<sub>4</sub>, which is involved in steps 5d and 5e of the hydroformylation mechanism. This work is an interesting application of the use of infrared spectroscopy at elevated pressures to detect metal carbonyl intermediates unstable at atmospheric pressure as was suggested in our original research proposal.<sup>3</sup>

Our studies in the high pressure infrared cell on the hydroformylation of ethylene by various rhodium complexes using a 1:1:1 CO/C<sub>2</sub>H<sub>4</sub>/H<sub>2</sub> mixture indicated that diverse rhodium(1) complexes are active hydroformylation catalysts under mild conditions but that rhodium complexes containing the metal in other formal oxidation states such as 0 (i.e.  $Rh_4(CO)_{12}$ ) or +2 (i.e. modium(II) acetate) were inactive catalysts under similar conditions. The results with  $Rh_4(CO)_{12}$  were initially somewhat difficult to reconcile with earlier reported observations<sup>12</sup> that  $Rh_4(CO)_{12}$  is an active hydroformylation catalyst for 1-heptene and related liquid substituted olefins. In order to clarify this inconsistency reactions of Rh<sub>4</sub>(CO)<sub>12</sub> were investigated in n-tetradecane solution using  $CO/C_2H_4/H_2$  mixtures where the ratio of CO<sup>i</sup> to the other gases was varied within a wide range. The results from these experiments are summarized in Table 2. These experiments showed that the maximum rate of hydroformylation was obtained with a CO/C<sub>2</sub>H<sub>4</sub>/H<sub>2</sub> ratio of 0.2/1.0/1.0. Gas mixtures appreciably richer or poorer in CO led to far slower reaction rates. These data indicate that carbon monoxide, although a necessary reactant for the hydroformylation reaction, is also a catalyst poison possibly by diverting one of the 16-electron intermediates in the catalytic cycle 5a-5h to an inactive 18-electron intermediate by CO addition to the "free" coordination site of the 16-electron intermediate.

Other observations suggest that this CO catalyst poisoning involves diversion of the HRh(CO)<sub>3</sub> intermediate required for step 5b to HRh(CO)<sub>4</sub> (e.g. step 5h). However, HRh(CO)<sub>4</sub> is unstable with respect to Rh<sub>4</sub>(CO)<sub>12</sub>, since both of the equilibria below (6a and 6b) lie predominantly to the right under our reaction conditions in accord with earlier high pressure infrared spectroscopic work by Whyman.<sup>13</sup> Thus treatment of Rh<sub>4</sub>(CO)<sub>12</sub> with a 1:1 C<sub>2</sub>H<sub>4</sub>/H<sub>2</sub>

$2 \text{ HRh}(CO)_4  \text{Rh}_2(CO)_8 + \text{H}_2$	(6a)
$2 \operatorname{Rh}_{2}(\operatorname{CO})_{8}  \operatorname{Rh}_{4}(\operatorname{CO})_{12} + 4 \operatorname{CO}$	(6b)

mixture in the absence of CO at 35°C and 50 atmospheres results in gradual disappearance of the  $Rh_4(CO)_{12}$  bridging  $\nu(CO)$  frequency at 1818 cm.<sup>-1</sup> with the production of a new species exhibiting  $\nu(CO)$  frequencies at 2075w and 2026s cm.<sup>-1</sup>. This species (conveniently designated as Compound X) persists in n-tetradecane solution upon release of the  $C_2H_4/H_2$  pressure. Solutions containing compound X, as shown by comparison of the  $\nu(CO)$  spectra,

-3-

#### TABLE 2

×.

EFFECT OF THE COMPOSITION OF THE CO/C2H4/H2 MIXTURE ON THE HYDRC-FORMYLATION OF ETHYLENE CATALYZED BY  $Rh_4(CO)_{12}^{\circ}$ 

-,

CO/C2H4/H2 Ratios	Production of Fropionaldehyde (+(CO) 1/38 cm. <sup>1</sup> )			
1.0/1.0/1.0	none			
0.4/1.0/1.0	none			
0.3/1.0/1.0	slow			
0.2/1.0/1.0	fast			
0.1/1.0/1.0	slow			

a) Temperature 37°C, solvent n-tetradecane, partial pressures of C<sub>2</sub>H<sub>4</sub> and H<sub>2</sub> each 12 atmospheres.

have also been obtained on the preparative scale by reaction of  $Rh_4(CO)_{12}$  with  $C_2H_4/H_2$ under pressure at room temperature in an autoclave in pentane solution. A solution of compound X catalyzes the hydroformylation of ethylene using a 1:1:1 CO/C<sub>2</sub>H<sub>4</sub>/H<sub>2</sub> mixture under conditions where  $Rh_4(CO)_{12}$  is ineffective as a catalyst. Furthermore, treatment of compound X with CO alone results in the regeneration of  $Rh_4(CO)_{12}$ .

Our current hypothesis is that compound X is  $HRh(CO)_3(C_2H_4)$ , a proposed intermediate in the hydroformylation reaction (i.e. steps 5b and 5c). This idea is supported by the following observations:

- (1) Its high activity as a hydroformylation catalyst as noted above.
- (2) Its formation from Rh<sub>4</sub>(CO)<sub>12</sub>/C<sub>2</sub>H<sub>4</sub>/H<sub>2</sub> under mild conditions, possibly by the reaction

$$\operatorname{Rh}_{4}(\operatorname{CO})_{12} + 4\operatorname{C}_{2}\operatorname{H}_{4} + 2\operatorname{H}_{2} \longrightarrow 4\operatorname{HRh}(\operatorname{CO})_{3}(\operatorname{C}_{2}\operatorname{H}_{4})$$
(7)

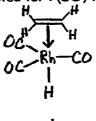
(3) Its reaction with CO to give  $Rh_4(CO)_{12}$  possibly through the following reaction sequence:

$$HRh(CO)_{a}(C_{2}H_{d}) + CO \xrightarrow{} HRh(CO)_{d} + C_{2}H_{d}$$
(8)

$$2 \text{ HRh}(CO)_4 \longrightarrow \text{Rh}_2(CO)_8 + H_2$$
 (6a)

$$2 \operatorname{Rh}_{2}(\operatorname{CO})_{8} \longrightarrow \operatorname{Rh}_{4}(\operatorname{CO})_{12} + 4 \operatorname{CO}^{-1}$$
(6b)

(4) The pattern of its  $\nu$  (CO) frequencies is consistent with a trigonal bipyramidal structure 1 for HRh (CO)<sub>3</sub> (C<sub>2</sub>H<sub>4</sub>) (Calculated for  $\nu$  (CO) frequencies: A<sub>1</sub> (weak IR) + E (strong IR)).

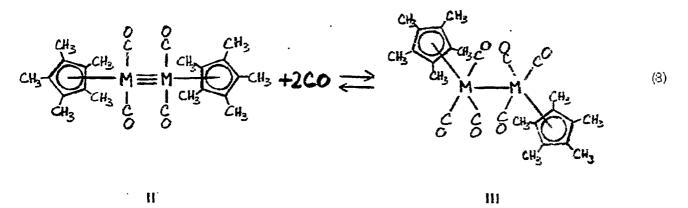


(5) The substitution of CO in HRh (CO)<sub>4</sub> with the weaker  $\pi$ -acceptor ethylene should make HRh (CO)<sub>3</sub> (C<sub>2</sub>H<sub>4</sub>) more stable in accord with the ability to detect but not isolate HRh (CO)<sub>3</sub> (C<sub>2</sub>H<sub>4</sub>) as noted above.

This type of evidence for the formulation of Compound X as  $HRh(CO)_3(C_2H_4)$  is not particularly convincing. Accordingly, we are in the process of investigating the reactions of the other  $M_4(CO)_{12}$  derivatives (M = Co and Ir) with  $C_2H_4/H_2$  mixtures hoping to obtain analogous  $HM(CO)_3(C_2H_4)$  (M = Co and Ir) derivatives which might be stable enough to isolate and therefore to characterize by more convincing chemical and spectroscopic methods.

#### Additions of Carbon Monoxide to Metal-Metal Triple Bonds

We have now completed our study of the addition of CO to the metal-metal triple bonded derivatives [(CH<sub>3</sub>)<sub>5</sub>C<sub>5</sub>M(CO)<sub>2</sub>]<sub>2</sub> (II: M = Cr, Mo, and W) to give the corresponding metal-metal single bonded derivatives-[(CH<sub>3</sub>)<sub>5</sub>C<sub>5</sub>M(CO)<sub>3</sub>]<sub>2</sub> (III: M = Cr, Mo, and W) as summarized in the following equation:



Studies of this reaction in the high pressure infrared cell indicate that the ease of CO addition in n-tetradecane solution to the metal-metal triple bond in the analogous compounds II (M = Cr, Mo, and W) increases in the sequence Cr < W < Mo. This is the first time that such a comparison between analogous 3d, 4d, and 5d transition metals has been possible. Furthermore, these carbonylations (equation 8) have all been carried out on the preparative scale leading to the isolation of the three metal-metal single bonded [ $(CH_3)_5C_5M(CO)_3$ ]<sub>2</sub>, derivatives (M = Cr, Mo, and W) in the solid state. The chromium derivative [ $(CH_3)_5C_5Cr(CO)_3$ ]<sub>2</sub>, which was obtained for the first time, is the least stable of these compounds and is red-purple in contrast to the green  $[C_5H_5Cr(CO)_3]_2$ . were the communication by Rathke and Feder' reporting that cobalt carbony! deress and were active catalysts for the synthesis of methanol, ethanol, and propanol from carbon monoxide and hydrogen. Accordingly, we have begun a systematic study of selected metal carbonyl derivatives as catalysts for the synthesis of alcohols from carbon monoxide and hydrogen using the following two techniques:

(1) Selected metal carbonyl derivatives were heated up to ca. 200°C in n-tetradecane solution under 200 atmospheres of a 1:1 H2/CO mixture in our high pressure infrared cell.<sup>5</sup> Infrared spectra were taken periodically in order to determine the metal carbonyl species present at a given temperature. This provides a method for establishing what types of metal carbonyl species are present under conditions resembiling those used in the actual catalytic reaction. This is important since it establishes which metal carbonyl precursors lead to different catalytic systems under a given set of reaction conditions.

(2) Catalytic reactions were carried out in an autoclave at 200°C and 200 atmospheres of a 1:1  $H_2$ /CO mixture. Samples were periodically withdrawn over a period of one week and analyzed by gas chromatography. p-Dioxane was used as a solvent in accord with the work of Rathke and Feder.<sup>4</sup>

Our experiments of this type are summarized in Table 1. The highlights of these results up to the present time can be summarized as follows:

#### (1) Cobalt Derivatives

The cobalt complexes which have been investigated up to the present time fail into two categories: (a) Complexes which form an equilibrium HCo(CO),/Co2(CO), mixture under the reaction conditions us shown by infrared spectroscopy (e.g. CH3CCo3 (CO), and (C6H5)2C2Co2-(CO), produce essentially the same mixture of methanol, ethanol, propanol, methyl formate, and ethyl formate as the  $Co_2(CO)_8$  catalyst precursor of Rathke and Feder<sup>4</sup>; (b) Complexes which decompose to carbonyl-free species under the reaction conditions (e.g.  $[CH_3N(PF_2)_2]_3$ - $Co_2(CO)_2$  and  $(CH_3)_3$  Sr(Co(CO)\_4) are inactive as catalysts for the hydrogenation of carbon monoxide.

#### (2) Ruthenium Derivatives

The ruthenium cluster Ru3(CO)12 forms Ru(CO)5 as the major product under the reaction conditions as shown by infrared spectroscopy. This ruthenium system is significantly more active than the active cobalt system for the production of methanol from carbon monoxide and hydroge: but is inactive for the production of higher alcohols such as ethanol and isopropanol.

We plan to continue work of this type during the next project period as discussed in detail in our research proposal.

#### TABLE 1: CAVALYSIS FOR THE HYDRO MAY HIS OF CARBON MONOXIDE TO ALCOHOLS

-	Metal Complexes formed by a reaction with 200 atm 1:1 CO/H <sub>2</sub>		Organic Products formed by the catalyzed reaction of 200 ata: 'CO/H2 in dioxane solution'			
Catalyst Precursor	Temp.	Products	mmoles/liter	Temp.	Product (ramoles) <sup>c</sup>	
Co <sub>2</sub> (CO) <sub>8</sub> <sup>d</sup>		HCo(CO)₄		182°C	MeOH, MeOCOH, EtOH, EtOCOH PrOH	
MeCCo <sub>3</sub> (CO) <sub>9</sub>	200 <sup>0</sup> C	Co <sub>2</sub> (CO) <sub>3</sub> <sup>e</sup>	5.5	200 <sup>°</sup> C	MeOH(33.5), MeOCOH (2.8) EIOH (16.4), EIOCOH (2.0) PrOH (10.0)	
$Ph_2C_2Co_2(CO)_6$	180°C	HCo(CO)4/Co2(CO)3	5.4	173°C	MeOH, MeOCOH, EtOH, EtOCOH, PrOH	
(PhP) <sub>2</sub> Co <sub>4</sub> (CO) <sub>10</sub>	>195°C	HCo(CO)4/Co2(CO)8	3.3	~190°C	МеОН, МеОСОН, ЕЮН, ЕЮСОН, РЮН	
[MeN(PF2)2]3Co2(CO)2	160°C	dec.f		~200°C	no reaction	
$Me_3SnCo(CO)_4$	>180°C	dec. <sup>f</sup>		~200°C	no reaction	
C <sub>3</sub> F <sub>7</sub> Co(CO) <sub>4</sub>	~115℃	HCo(CO)4/Co2(CO)8 + C3F7CHO(?)	g			
Ru3(CO)12	>90°C	Ru (CO) <sub>5</sub>	1.5	180°C	MeOH (48), MeOCOH (4.4)	

. •

(a) Unless otherwise indicated these species were identified from their v(CO) frequencies in spectra taken in the high pressure infrared cell under the indicated conditions using n-tetradecane as the solvent.

These reactions were carried out in an autoclave under the indicated conditions. Liquid samples were removed periodically at 60°C and (b) analyzed by gas chromatography.

The mmoles of the Indicated products obtained after 1 week reaction time are given in parentheses. (c)

(d) (e) This information was taken from J. W. Rathke and H. M. Feder, J. Am. Chem. Soc., 100, 3623 (1978).

These products were detected by infrared spectroscopy of the solutions obtained after carrying out the catalytic reactions. These compounds decomposed under the indicated conditions to give carbonyl-free products as indicated by the absence of v(CO) frequencies.

(f) (g) Since this cobalt precursor was shown to give HCo(CO), /Co2 (CO), under the reaction conditions, the catalytic reactions were not rur. Figure ultimate aim of this research project is the discovery of fundamental charges with which will provide a basis for the substitution of coal for petroleum as a raw material. Since the carbon in coal can be converted to carbon monoxide by the water gas reaction (equation 1), the specific chemistry involved in this project focusses on the basic chemistry behind tech-

nology using carbon monoxide as a raw material. During the period covered by this progress report, various aspects of the fundamental chemistry of the following reactions of carbon monoxide were studied:

(1) The manufacture of alcohols from carbon monoxide/and hydrogen: Alcohols can serve as clean fuels for-motor vehicles ("gasohol"). Furthermore, if coal-derived carbon monoxide can be substituted for petroleum as a raw material for the manufacture of methanol, ethanol, etc., the scarce petroleum can be conserved for other purposes.

2) The manufacture of hydrogen from carbon monoxide and water ("water gas shift reaction"): Hydrogen is another candidate for a clean fuel. However, if coal-derived carbon monoxide carbe used to liberate the hydrogen from water, then the water gas shift reaction effectively represents a method of getting a clean fuel from coal.

(3) The manufacture of aldehydes from olefins, carbor monoxide, and hydrogen (the hydroformylation reaction): This reaction is important in connection with the manufacture of organic chemicals and uses coal, rather than petroleum, as the source of the aldehyde carbon atom.

Such fundamental chemistry could provide the basis for new and improved molecular catalysts for the above reactions. In the case of both carbon monoxide hydrogenation and the water gas shire reaction, such catalysts might allow industrial processes to be carried out under much milder courditions than those required for the currently used heterogeneous catalysts.

All of the three reactions listed above involve catalysis by transition metal complexes with metal carbonyls as reaction intermediates. Therefore, the high pressure infrared spectroscopic techniques developed during the previous years of this project<sup>1</sup>,<sup>2</sup> are very suited to the study of their fundamental chemistry.

#### The Manufacture of Alcohols from Carbon Monoxide und Hydrogen

The ultimate objective of this research project as envisioned in the original research proposal<sup>3</sup> was the development of new transition metal catalysts for the manufacture of hydrorarbon fuels from carbon monoxide and hydrogen (Fischer-Tropsch reaction). Therefore any reaction involving metal carbonyl catalysts which leads to hydrocarbon derivatives is of potential interest to this work. In this connection an interesting report during the past year

> Reproduced from best available copy

"This report was prepared as an account of work sponsored by the United States Government. Neither the United States nor the United State Department of Energy, nor any of their employees, nor any of their contractors, subcontractors, or their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately-owned rights."

.