

APPENDIX A

COAL SEARCH

Appendix A
Coal Search

For PGW coal gasification plant GKT'S entrained bed coal gasification process was selected. The process utilizes high temperature (2700°F) atmospheric conditions with a continuous co-current stream of pulverized coal, oxygen and steam. The process can, in general, gasify all types of coal so long as it would allow normal pulverization; however, the coal should preferably have an ash fusion temperature of 2600°F or less, since coals with high ash fusion temperatures would require addition of fluxing agents. The following coal specifications were therefore developed to meet the process requirements:

Ash Fusion Temperature	2600°F max. (Reducing)
Sulfur (as received)	5.0 percent max.
Ash (as received)	15.0 percent max.
Moisture (as received)	10.0 percent max.
Size (as received)	2.0" x 0"

Specifications for sulfur, ash and moisture were so chosen to allow an evaluation of a wider range of coals. The coal size was so chosen to allow direct pulverization of coal without the need for preliminary crushing.

The search for candidate feed coals was initiated by providing to potential coal suppliers the above coal specifications. Forty-six (46) coal companies in the states of Pennsylvania, Ohio, West Virginia, Kentucky and Indiana were contacted and thirteen (13) companies responded with varied degrees of interest and information (see Table A-1).

An overall evaluation was then performed based on the coal data provided by these companies. Raw gas characteristics and cold gas efficiencies, and thereby the annual tonnage coal requirements and costs were estimated. Coal reserves, long term coal supply, oxygen plant costs, sulfur removal cost and ash disposal cost were also considered in the evaluation. Tables A-2 to A-6 show the various data for the candidate coals.

The analysis showed that the single factor which affects the plant economics most strongly is the delivered coal cost ($\$/10^6$ Btu). The five coals selected as potential feedstock for the gasification plant are from Centralia, Berwind, Keystone, C & K, and Bradford coal companies.

TABLE A-1
COAL COMPANIES RECEIVING PGW INQUIRY LETTER

<u>IN PENNSYLVANIA</u>	<u>DESIRE TO SUPPLY COAL</u>
Aloe Coal Company P.O. Box 50 Imperial, PA 15126	No Response
Consolidation Coal Company Consol Plaza 1800 Washington Rd. Pittsburgh, PA 15241	<u>Yes</u>
Allegheny & Eastern Coal Sales, Inc. 328 Allegheny Avenue Kittanning, PA 16201	No Response
Rochester & Pittsburgh Coal Co. 655 Church Street Indiana, PA 15701	<u>Yes</u>
Bradford Coal Company Bigler, PA 16825	<u>Yes</u>
North Cambria Fuels Co. 1st National Bank Bldg. Spangler, PA 15775	No Response
Reitz Coal Company 509 15th Street Windber, PA 15963	No Response
General Coal Company 2500 Fidelity Bldg. Philadelphia, PA 19106	<u>Yes</u>
United Eastern Coal Sales Corp. P.O. Box 685 Villanova, PA 19085	No Response
Avery Coal Company, Inc. P.O. Box 232 Philipsburg, PA 16866	No Response
C & K Coal Company P.O. Box 69 Clarion, PA 16214	<u>Yes</u>
Owens Coal Mining Co. R.D. 1 Penfield, PA 15849	No Response

TABLE A-1 (Cont'd)
COAL COMPANIES RECEIVING PGW INQUIRY LETTER

IN PENNSYLVANIA

DESIRE TO SUPPLY COAL

Universal Minerals, Inc. P.O. Box 307 Portage, PA 15946	No Response
Acme Coal Co. L. V. No. 5 Vein Slope Williamstown, PA 17098	No - Anthracite Coal Only
Berwind Coal Sales Co. 1500 Market Street Centre Square West Philadelphia, PA 19102	<u>Yes</u>
Centralia Coal Sales Co. P.O. Box 478 Wilkes-Barre, PA 18703	<u>Yes</u>
C and G Coal Company Washington, PA	No - Supplies only Consolidation National Gas Company
Dickson Fuel Corp. P.O. Box 831 Rosemont, PA 19010	No - No Coal Available
Slattery Brothers, Inc. 110 Bala Ave. Bala-Cynwyd, PA 19004	No Response
Alcon Coal & Land Co., Inc. 650 Blue Bell West Blue Bell, PA 19422	<u>Yes</u>
Westmoreland Coal Co. 123 S. Broad Street 2500 Fidelity Bldg. Philadelphia, PA 19109	No Response
Lehigh Valley Coal Sales Co. 800 Exeter Avenue West Pittston, PA 18643	No Response
FMC Corporation National Resource Div. 2000 Market Street Philadelphia, PA 19103	No Response

TABLE A-1 (Cont'd)
COAL COMPANIES RECEIVING PGW INQUIRY LETTER

<u>IN PENNSYLVANIA</u>	<u>DESIRE TO SUPPLY COAL</u>
Rafetto Coal Co., Inc. Aldan Park Manor Philadelphia, PA 19144	No Response
Keystone Coal Co. One East Market St. York, PA 17405	<u>Yes</u>
Hickman, Williams & Co. 1777 Walton Road Blue Bell, PA 19422	No Response
Miller Marketing Co. Suite 10-A 1445 City Line Avenue Philadelphia, PA 19151	<u>Yes</u> - Sent Coal Samples
Irish John K. Co., Inc. P.O. Box 885 Red Bank, NJ 07701	No Response
Universal Coal Co. 6411 Large Street Philadelphia, PA 19149	No Response
Russell L. Suender, Inc. P.O. Box 73 Port Carbon, PA 17965	No - Anthracite Coal Only
Eastern Association of Coal Corp. Kopper Bldg. Pittsburg, PA 15219	No Response

TABLE A-1 (Cont'd)
COAL COMPANIES RECEIVING FGW INQUIRY LETTER

IN OHIO

DESIRE TO SUPPLY COAL

Youghiogeny and Ohio Coal Company
4614 Prospect Avenue
Cleveland, OH 44103

No Response

Peabody Coal Company
225 Fairway Blvd.
Columbus, OH 43213

Yes

Valley Camp Coal Company
700 Westgate Tower
Cleveland, OH 44116

No Response

Ohio Coal and Construction Corp.
P.O. Box 2388
Wintersville, OH 43952

No Response

Central Ohio Coal Company
P.O. Box 98
Cumberland, OH 43732

No Response

North American Coal Corp.
12800 Shaker Blvd.
Cleveland, OH 44120

Yes

TABLE A-1 (Cont'd)
COAL COMPANIES RECEIVING PGW INQUIRY LETTER

IN WEST VIRGINIA

DESIRE TO SUPPLY COAL

Cannelton Industries, Inc.
P.O. Box 1226
1250 One Valley Square
Charlestown, WV 25324

Yes

Consolidated National Gas Company
Mr. I. M. Ovrr
C and G Coal Company
445 W. Main Street
Clarksburg, WV

No - Supply Only
to Gas Company

Pickards Mather and Company
322 70th Street
Charleston, WV 25009

No Response

Bishcp Coal Company
Pocahontas, WV 24635

Yes (See Consolidated
Coal Company)

Barbour Coal Company
P.O. Box 1744
Clarksburg, WV 26301

No Response

TABLE A-1 (Cont'd)
COAL COMPANIES RECEIVING PGW INQUIRY LETTER

IN KENTUCKY

DESIRE TO SUPPLY COAL

Addington Brother Mining, Inc. (Ashland)
P.O. Box 681
Ashland, KY 41101

No - Sells Only to
Ashland Oil

Island Creek Coal Co.
2355 Harrodsburg Road
P.O. Box 11430
Lexington, KY 40511

Yes

Sextet Mining Corporation
Madisonville, KY 42431

No Response

TABLE A-1 (Cont'd)
COAL COMPANIES RECEIVING PGW INQUIRY LETTER

IN INDIANA

Amax Coal Company
105 S. Meridean Street
Indianapolis, IN 46225

DESIRE TO SUPPLY COAL

No - Interest
Western Market
Only

TABLE A-2
SUMMARY OF COAL SEARCH RESULTS

Coal Supplier	Base	C&K	Consolidation	Bradford	General	R&P
Seam	Pittsburgh 8	Clarion, Kitt. Freeport	Pittsburgh	L. Kittaning	Brookville L. & U. Kitt.	L. Kitt.
Proximate Analysis, A.R.						
Moisture	4.58	6.0	5.00	5.33	9.62	4.5
FC + VM	87.59	85.3	83.11	80.83	77.98	82.5
Ash	7.83	8.7	11.89	13.84	12.40	13.0
Total	100.00	100.0	100.00	100.00	100.00	100.00
HHV, Btu/lb, A.R.	13,626	13,174	12,103	12,766	11,243	12,290
Delivered Coal Cost						
\$/Ton, A.R.	45.0	40.0	43.61	36.0	38.0	48.82
\$/Ton, MAF	51.38	46.89	52.47	44.54	48.73	59.18
\$/10 Btu	1.65	1.52	1.76	1.41	1.69	1.96
Pref. Candidate Coal (1)		X		X		

(1) X indicates preferred candidate coals

TABLE A-2 (Cont'd)
SUMMARY OF COAL SEARCH RESULTS

Coal Supplier	North American L. Kitt. PA "B Seam"	Island Creek Bakerstown & Freeport, WV	Contrailla Bakerstown, Freeport & KILL., WV	Berwind Brookville/ Clatton, VA	ACSL No. 8, PA	Keystone U. & L. Kitt. PA
Scam	5-11 None	73.9 0.875	100+ 0.6	15 (2)	5 (3)	10 0.30
Reserve, 10 ⁶ ton						
Production, 10 ⁶ ton/yr						
Proximate Analysis, A.R.						
Moisture	5.02	4.49	7.0	3	5	5
FC + VI	83.39	87.71	79.0	84	82	83
Ash	11.59	7.80	14.0	13	13	12
Sulfur	2.86	1.32	4.0	4	1.4	3
HIV, Btu/lb, A.R.	13,916	13,806	11,750	12,000 (4)	12,500	12,500
Ash Fusion Temp., °F (1)	2340	2670	2240	2500	2800+	2425
Delivered Coal Cost						
\$/Ton A.R.	46.06	56.58	38.58	0	39.0	38.58
\$/10 ⁶ Btu	55.23	64.51	48.84	7.62	47.56	46.48
1.77	2.05	1.64	1.67	1.56	1.56	1.54
Pref. Candidate Coal (5)			X	X		X

- (1) Fluid temperature under reducing condition.
- (2) Not in production at the present time.
- (3) Not available
- (4) Estimate
- (5) X indicates preferred candidate coals.
- (6) For 7000 ton unit train

TABLE A-3
SUMMARY OF COAL DATA

	<u>Coal Supplier</u>	<u>C&K</u>	<u>Consolidation</u>	<u>Bradford</u>	<u>General</u>	<u>R&P</u>
Seam	Clarion, Kitt. Freeport		Pittsburgh	L. Kitt.	Brookville L&U Kitt.	L. Kitt.
Reserve, 10 ⁶ Ton	60		800	15	50	25+
Production, 10 ⁶ Ton/Yr	5		50	0.1	0.3	0.8
Loading	Conrail		Conrail, B&O	Conrail	Conrail	Bessemer/Lake Erie
Freight Rate Group	Clearfield		W.V. (B&O)	Clearfield	Clearfield	Butler-Mercer
Coal Size	2" x 0"		2" x 0"	3/4" x 0"	1-1/2" x 0"	2" x 0"
Unit Coal Cost, \$/Ton						
FOB	29.0		31.75	25.0	27.0	35.54 ⁽²⁾
Freight ⁽¹⁾						
Single Car	-		15.83	15.07	15.07	-
Unit Train	-		-	-	-	15.22
4000 Ton	-		11.86	-	-	13.28
7000 Ton	-		-	-	-	12.26
9000 Ton	-		-	-	-	-

(1) From coal mines to City of Philadelphia
(2) April, 1979 price

TABLE A-3 (Cont'd)

SUMMARY OF COAL DATA

Coal Supplier	North American		Island Creek	
	L. Kitt., PA	U. Kitt., PA	Bakertown & Freeport, WV	Freeport, WV
Seam	"B" Seam	"E" Seam	73.9	54.1
Reserve, 10 ⁶ ton	5.11	8.94	0.875	1.375
Production, 10 ⁶ ton/yr	None	None	W. Maryland Rail	W. Maryland Rail
Loading	Chessie/Conrail	Chessie/Conrail	U. Potomac Dist.	U. Potomac Dist.
Freight Rate Group	-	-	1-1/2" x 0"	2.0" x 0"
Coal Size	3/4" or as req'd	3/4" or as req'd		
Unit Coal Cost, \$/ton ⁽¹⁾				
FOB	35.0	35.0	45.00	30.0
Freight ⁽²⁾			15.96 ⁽³⁾	15.96 ⁽³⁾
Single Car				
Unit Train				
4000 ton				
7000 ton	11.06	11.06	11.58 ⁽⁵⁾	11.58 ⁽⁵⁾
9000 ton				

-
- (1) 1st Quarter 1981 price.
 - (2) From coal mine to City of Philadelphia.
 - (3) Type of unit train not given in the letter responded.
 - (4) Not in production at the present time, but set up mining operations to produce up to 30,000 tons.
 - (5) Estimate

TABLE A-3 (Cont'd)

SUMMARY OF COAL DATA

Coal Supplier	Centralia	Berwind	AC&L	Keystone
Seam Reserve, 10 ⁶ ton	Bakerstown, Freeport & Kitt., WV	Brookville/Clarion, PA	No. 8, PA	U. & L. Kitt.
Production, 10 ⁶ ton/yr	100+	15 (4)	5	U. & L. Freeport, PA
Loading	0.60	Conrail-Windber, PA	Rail/Truck	10
Freight Rate Group	Cumberland- Piedmont Somerset 2.0" x 0"	2.0" x 0"	2.0" x 0"	0.30 Rail/Truck
Coal Size	27.0	29.0	26.0	27.0
Unit Coal Cost, \$/ton (1)	15.82	15.07	-	-
FOB	11.58	11.0 (5)	13.0	11.58 (3)
Freight (2)	-	-	-	-
Single Car	-	-	-	-
Unit Train	-	-	-	-
4000 ton	-	-	-	-
7000 ton	-	-	-	-
9000 ton	-	-	-	-

-
- (1) 2nd Quarter 1981 price
 - (2) From coal mine to City of Philadelphia
 - (3) Type of unit train not given in the letter responded
 - (4) Not in production at the present time, but set up mining operations to produce up to 30,000 tons per month
 - (5) Estimate

TABLE A-4
CHARACTERISTICS OF POTENTIAL CANDIDATE COALS

Seam	Coal Supplier	Base		C&K		Consolidation		Bradford		General		R&P	
		Pittsburgh No. 8	Clarion, Kitt. Freeports	Pickensburgh	I. Kittanning	Brookville 150 Kitt.	I. Kitt.	Brookville 150 Kitt.	R&P				
Proximate Analyses, A.R.													
Moisture (as-received)		4.58	5-7	4-6	5.33	<10	4.5						
Volatiles Matter		37.33	32-36	36-37	22.71	22-26	34.9						
Fixed Carbon		50.26	45-50	48-52	58.37	56-50	47.6						
Ash		7.83	8-10	6.8-7.8	13.59	12-14	13.0						
Total		100.00											
HHV Range, Btu/lb A.R.		13,442	12,600-12,800	13,400	12,503	12,000	12,400						
IGI		64	55-60	58-63	90	85-95	57						
FSI		7.5	7.0	7-8.5	9	5-7.5	7.5-8						
Ultimate Analysis, Wt. %													
Carbon		77.71	75.0	69.77	73.71	70.37	70.40						
Hydrogen		5.28	5.5	4.99	4.48	4.26	4.94						
Nitrogen		1.42	1.5	1.34	1.18	1.27	1.31						
Chlorine		-	0.2	-	-	0.11	0.16						
Sulfur		2.64	3.0	3.22	3.83	3.04	2.62						
Oxygen		4.74	5.5	8.16	2.18	7.23	6.95						
Ash		8.21	9.3	12.52	14.62	13.84	13.61						
Moisture		-	6.0	-	5.33	-	4.50						
Total		100.00	100.0	100.00	100.00	100.00	100.00						
HHV, Btu/lb, dry		14,087	13,511	14,105	13,207	12,503	12,984						
Reported (1)		14,280	14,015	12,740	13,485	12,766	12,870						
Calculated													

(1) Dulong formula

TABLE A-4 (Cont'd)
CHARACTERISTICS OF POTENTIAL CANDIDATE COALS

Seam	Coal Supplier	Base		C&K		Consolidation		Bradford		General		RRP	
		Pittsburgh No. 8	Pittsburgh No. 8	Clarion, Kitt. Freeports	Pittsburgh	I. Kittaning	Brookville I&H Kitt.	I. Kitt.					
Ash Mineral Composition, Wt. %													
Phos. Pentoxide		-	0.20		0.46		3.82		0.30		0.24		
Silica		47.19	38.31		41.04		37.09		47.00		37.00		
Ferric Oxide		16.23	30.31		19.61		27.30		18.20		26.80		
Alumina		22.40	22.28		18.90		22.34		28.72		24.60		
Titania		-	1.02		1.01		0.58		1.33		1.32		
Lime		4.11	1.43		6.89		4.20		1.00		1.51		
Magnesia		-	0.56		1.22		1.01		0.50		0.62		
Sulfur Trioxide		0.87	1.73		6.40		1.39		0.97		2.04		
Potassium Oxide		-	1.05		1.68		1.51		1.63		1.45		
Sodium Oxide		-	0.47 (3)		0.88 (3)		0.76		0.35		0.25 (3)		
Others		8.44 (2)	2.64 (3)		1.91 (3)		-		-		2.17 (3)		
Total		100.00	100.00		100.00		100.00		100.00		100.00		
Ash Fusibility Temp. °F													
Initial Deformation		2093	2000		2050		2090		2320		2090		
Softening		2138	2200		2150		2200		2410		2275		
Fluid		2156	2400		2350		2340		2520		2390		

(1) Calculated from Dulong formula
(2) Only partial analysis was reported
(3) Unaccounted for

TABLE A-5
CHARACTERISTICS OF POTENTIAL CANDIDATE COALS

Seam	North American			Island Creek	
	L. Kitt., PA "B" Seam	U. Freeport, PA "G" Seam	1.60 Float	Bakertown & Freeport, WV	Freeport, WV
Proximate Analysis, A.R.					
Moisture (seam)	5.02 (2)	-	-	4.49	5.43
Volatile Matter	- (2)	26.58	26.26	20.42	17.46
Fixed Carbon	-	64.23	63.48	67.29	63.14
Ash	11.59	9.18	10.24	7.89	13.70
Total		99.95	99.98	100.00	100.00
HHV Range, Btu/lb., A.R.	13,016	14,100	13,910	13,806	12,536
HGI	-	-	-	105	100
FSI	-	-	-	9.0	9.0
Ultimate Analysis, Wt. %					
Carbon	A.R.	A.R.	A.R.	Dry 81.07	A.R. 71.82
Hydrogen	-	-	-	4.76	4.16
Nitrogen	-	-	-	1.52	1.41
Chlorine	-	-	-	0.15	0.11
Sulfur	2.86	1.74	2.02	1.38	1.96
Oxygen	-	-	-	2.95	1.95
Ash	-	-	-	8.17	14.49
Moisture	-	-	-	-	5.43
Total				100.00	100.00
HHV, Btu/lb, Dry					
Reported	13,016	14,100	13,910	-	12,536
Calculated (1)	-	-	-	13,806	12,815

(1) Dulong formula
(2) Not available

TABLE A-5 (Cont'd)
CHARACTERISTICS OF POTENTIAL CANDIDATE COALS

Seam	Coal Supplier	Centralia		Berwind	ACSL	Keystone
		Bakerstown, Freeport & Kitt., WV	Brookville/Clarion, PA			
Proximate Analysis, A.R.						
Moisture (seam)		6.0-8.0	3	No. 8, PA		U. & L. Kitt
Volatile Matter		24.0-26.0	17		5.0	U. & L. Freeport, PA
Fixed Carbon		50.0-55.0	67		20.0	5
Ash		13.0-15.0	13		60.6	23-24
Total			100		13.0	53
HHV Range, Btu/lb., A.R.		11,500-12,000	12,000		98.6	12
HGI		70-80			12,500	12,500
FSI		5-7				
Ultimate Analysis, Wt. %						
Carbon		Dry 68.0-72.0	A.R.		A.R.	A.R.
Hydrogen		4.6-4.8	65.0-67.0		-	-
Nitrogen		1.3-1.4	4.4-4.6		-	-
Chlorine		0.18-0.22	1.2-1.3		-	-
Sulfur		3.0-5.0	0.16-0.18		-	-
Oxygen		3.0-3.3	3.0-5.0	4.0	1.4	3.0
Ash		14.0-16.0	3.8-3.1		-	-
Moisture		-	13.0-15.0		-	-
Total		-	6.0-8.0		-	-
HHV, Btu/lb, dry						
Reported		12,234-13,043	11,500-12,000	12,000	12,500	12,500
Calculated (1)		12,859-13,652	12,087-12,560			

(1) Dulong formula

TABLE A-6
ASH CHARACTERISTICS OF POTENTIAL CANDIDATE COALS

Coal Supplier	North American		Island Creek	
	L. Kitt., PA "B" Seam	U. Freeport, PA "E" Seam	Batertown & Freeport, W. V.	Freeport, W. V.
Ash Mineral Composition,				
Wt. %	N.A. (2)	N.A. (2)		
Phos. Pentoxide	-	-	0.47	0.37
Silica	-	-	45.84	48.00
Ferric Oxide	-	-	13.02	14.33
Alumina	-	-	30.45	29.55
Titania	-	-	1.34	1.14
Lime	-	-	3.11	1.84
Magnesia	-	-	1.03	0.72
Sulfur Trioxide	-	-	2.68	1.49
Potassium Oxide	-	-	1.63	2.12
Sodium Oxide	-	-	0.32	0.29
Others	-	-	0.11	0.15
Total			100.00	100.00
Ash Fusibility Temp., °F	Red. Ox.	Red. Ox.	Red. Ox.	Red. Ox.
Initial Deformation	1.50 FI./1.60 FI. (3)	1.50 FI./1.60 FI.	2510	2500
Softening	2145	2550/2210	2560	2550
Fluid	2205	2380/2330	2670	2690
	2340	2510/2480		2700+
				2700+
				2709+

- (1) Unaccounted for
(2) N.A. = Not available
(3) FI. = float

TABLE A-6 (Cont'd)
ASH CHARACTERISTICS OF POTENTIAL CANDIDATE COALS

Coal Supplier	Centralia		Berwind		AC&L		Keystone	
	Bakerstown, Freeport & Kittanings, WV	Brookville/Clarion, PA	No. 8, PA	U. & L. Kitt.	U. & L. Freeport, PA	U. & L. Kitt.	U. & L. Freeport, PA	
Seam								
Ash Mineral Composition, Wt. %								
Phos. Pentoxide	0.3- 6.5	N.A.	N.A.	-	-	-	-	
Silica	48.0-52.0	-	-	-	-	-	-	
Ferric Oxide	16.0-18.0	-	-	-	-	-	-	
Alumina	25.0-27.0	-	-	-	-	-	-	
Titania	1.4- 1.6	-	-	-	-	-	-	
Lime	1.0- 1.2	-	-	-	-	-	-	
Magnesia	0.8- 1.0	-	-	-	-	-	-	
Sulfur Trioxide	1.0- 1.2	-	-	-	-	-	-	
Potassium Oxide	1.6- 1.8	-	-	-	-	-	-	
Sodium Oxide	0.8- 1.0	-	-	-	-	-	-	
Others	-	-	-	-	-	-	-	
Total	Red. 2020	Red. 2150	Red. 2700	Red. 2275	Red. 2350	Red. 2425	Ox. -	
Ash Fusibility Temp., °F	2090	2250	2800+	2800+	2800+	2800+	Ox. -	
Initial Deformation	2130	-	-	-	-	-	-	
Softening	2240	-	-	-	-	-	-	
Fluid								

(1) Unaccounted for
(2) N.A. = Not available
(3) Fl. = float

APPENDIX B
FLY ASH RECYCLE

Appendix B
Fly Ash Recycle

The GKI coal gasification process produces two types of solid wastes -granular slag and fine fly ash admixed with unburned carbon. Approximately 30% of the ash in the coal is recovered as quenched molten slag from the gasifier bottom while the remaining 70% (entrained in the raw gas) is recovered in the form of a filter cake from a downstream gas purification system consisting of wash column, settling basin, thickener, and rotary vacuum filter. When 1200 TPD of the Pittsburgh No. 8 coal is gasified in the usual manner, 33 TPD of slag (15% moisture) and 345 TPD of fly ash cake (50% moisture) are produced, and a total of 378 tons of solid wastes must be disposed of off-site. Furthermore, the fly ash cake contains a large fraction of unburned carbon (107 TPD) which is not an insignificant loss of carbon utilization.

In order to alleviate solid waste disposal problems and to reutilize some of the carbon contained in the fly ash cake, a scheme of recycling the fly ash cake back to the gasifier is incorporated in the present design. This is done by returning part of the fly ash cake via a conveyor system to pulverizers where it is mixed and pulverized with fresh coal. The mixture is dried to 1% moisture and gasified as in the non-recycle case.

Since the carbon in the fly ash cake is recovered and reutilized, fresh coal feed can be reduced by an amount equivalent to the carbon recycled. (In other words, the total carbon in the mixed feed remains the same as the straight feed.) As shown in Tables B-1 and B-2, the fresh coal feed can be steadily reduced and the overall carbon conversion efficiency improved as the fly ash recycle rate is increased. For example, at 50% recycle rate, fresh coal feed can be reduced from 1200 TPD to 1128 TPD and the carbon efficiency improved from 88% to 93.6%. In addition, the total solid wastes (slag and fly ash cake) can be reduced from 378 TPD to 250 TPD, and the quantities of carbon loss halved from 107 TPD to 54 TPD. With higher recycle rates, even better results can be achieved. However, as the recycle rate is increased, dust loading in the raw gas also increases (Table B-2), which will hamper the

TABLE B-1

EFFECT OF FLY ASH RECYCLE ON PULVERIZER PARAMETERS

Fly Ash Recycle Rate %	Fresh Coal (1) TPD	Recycled Fly Ash TPD (2)	Pulverizer		Moisture in Mixed Feed %	Drying (3) Duty 10 ⁹ Btu/D
			Mixed Feed TPD	Total Mixed Feed TPD		
0	1200	0	1200	4.58	0.150	
30	1157	112	1269	8.60	0.337	
40	1142	155	1297	10.00	0.409	
50	1128	202	1330	11.47	0.487	
60	1114	254	1368	13.02	0.576	
80	1085	387	1472	16.52	0.800	
100	1056	599	1655	21.03	1.161	

Notes: (1) Pittsburgh No. 8 coal, 4.58% moisture as received
 (2) 50% moisture filter cake
 (3) Mixed feed is dried to 1% moisture; 1750 Btu/lb water drying duty

TABLE B-2
EFFECT OF FLY ASH RECYCLE ON CARBON CONVERSION
AND THE QUANTITIES OF SOLID WASTES

Fly Ash Recycle Rate %	GKT Plant		Solid Waste Disposal			
	Overall Carbon Eff. %	Dust Loading in Raw Gas	Slag (1) TPD	Fly Ash (2) Cake TPD	Total Solid Wastes TPD	Carbon (3) Loss TPD
0	88.00	1 (base)	33	345	378	107
30	91.29	1.084	41	262	303	75
40	92.94	1.123	44	233	277	64
50	93.62	1.170	48	202	250	54
60	94.83	1.229	53	170	223	43
80	97.35	1.402	68	97	165	21
100	100.00	1.737	97	0	97	0

Notes: (1) 15% moisture granular slag
(2) 50% moisture filter cake
(3) Contained in the fly ash filter cake

capability of the wash column to remove fly ash from the gas. The capacity of pulverizers must also be increased to accommodate the increased throughput (Table B-1). More important, as the recycle rate is increased, the moisture in the mixed feed increases rapidly, since half of the fly ash cake recycled is water. At the 50% recycle rate, the moisture in the mixed feed reaches 11.47% or nearly equal to the design capacity (12%) of the air heaters associated with pulverizers. The required drying duty at this recycle rate is more than threefold (0.487×10^9 Btu/D) compared to the non-recycle case (0.150×10^9 Btu/D). Simple economic trade-off analysis also indicated that savings due to reduced coal feed would be about offset by the increase in the energy cost at the 50% recycle rate. For the present PGW coal gasification plant design, therefore, recycling of fly ash cake in the range of 0-50% is recommended.

APPENDIX C

STRETFORD PLANT SULFUR RECOVERY OPTIONS

Appendix C

Stretford Plant Sulfur Recovery Options

The Stretford plant is employed for removing H_2S from the raw gas coming from the GKT gasification plant. H_2S in the gas is converted to elemental sulfur which can be recovered as either filter cake or molten sulfur, the selection of which is dictated by the overall economics. The molten sulfur configuration generates a purge liquor stream which requires either on-site treatment by reductive incineration or disposal by hauling to a hazardous waste treatment facility.

In order to select the most economical and environmentally acceptable sulfur recovery option, the following five options were considered:

1. Filter cake disposal
2. Molten sulfur/purge disposal/sulfur credit
3. Molten sulfur/purge disposal/sulfur disposal
4. Molten sulfur/reductive incineration/sulfur credit
5. Molten sulfur/reductive incineration/sulfur disposal

The economic analysis was based on the C & K coal which is one of the selected candidate coals for gasification (Appendix A). The feed gas characteristics were predicted by the in-house combustion equilibrium (CEC) computer program. The comparative analysis is applicable to other candidate coals (including Pittsburgh No. 8 design coal) since the selection of the sulfur recovery option is based on the feed gas characteristics which are largely independent of the coal.

The basis and economic parameters along with the description of sulfur recovery options is described in the sections below. The molten sulfur/reductive incineration/sulfur credit option (case 5) was found to be most economical.

Basis for Comparative Analysis

Gas characteristics

Pressure: 4.5 Psig

Temperature: 105°F

Composition: (Mole %, wet)

CO	50.15
COS	0.04 (420 ppmv, dry)
CO ₂	8.40
H ₂	33.80
H ₂ O	5.57
H ₂ S	0.85 (9000 ppmv, dry)
N ₂	1.19
HCN	NA
CS ₂	NA

Mol Wt (wet) 20.075

Gas flow rate

Wet: 51,217 MM SCFM

Dry: 48,367 MM SCFM

Sulfur removal (assumed)

Efficiency: 95% of all H₂S, no COS removed

Sulfur Recovery Options - Description

Treatment of sulfur froth depends upon the amount to be handled. For small loads, filtration alone producing an impure sulfur cake might be an appropriate choice. Alternatively, filtration followed by batch autoclave

melting and separation may be used to recover sulfur in another form. Larger loads might require centrifuging followed by continuous sulfur melting and separation in a jacketed autoclave, or in a direct steam injection sulfur melter.

When the sulfur is to be recovered by filtration, a rotary vacuum drum filter is generally used. The filter cake produced contains approximately 50% solids. One or more wash cycles are employed to economically recover the maximum amount of Stretford solution components from the cake. The filtrate and the wash solution are sent to a surge tank and are then returned to the system. Sometimes, depending on the water balance for a particular design, it might be necessary to concentrate the wash solution leaving the filter. Centrifuges employed for larger loads are of the continuous type. Filtrate and wash solution are again returned to the system.

To produce molten sulfur, sulfur cake or sulfur cake re-slurried in recycled water can be fed to an autoclave melter-separator. The melter-separator is a vessel with a jacket or internal coil which is heated by steam at about 100 psig. Molten sulfur separated from the aqueous solution of residual salts is pumped to storage. Recovered water and salts are returned to the system. Sulfur recovered by the above separator/melter methods is of a high purity in the range of 99.5% or better.

Economics

Capital and operating costs for the Stretford process are affected by many variables. The major design parameters that have a direct effect on the economics include the allowable hydrosulfide loading of the solution (which sets the circulation rate, hence pumping costs, etc.) and the required residence times in the various parts of the plant (which governs equipment sizes). A solution circulation rate could be 125-175 gal/lb sulfur depending on the hydrosulfide loadings. A residence times of 10 to 20 min. is required in the base of the absorber or in a separate holding tank to permit maximum conversion of hydrosulfide to sulfur prior to entering the oxidizer. About 5-min. delay is necessary after oxygen addition in the oxidizer to complete reoxidation of ADA.

Another factor that affects the economics is the sulfur disposal and/or recovery option selected (see Table C-1). The sulfur filter cake option (case 1) has the advantage of low capital costs, but operating costs are high due to loss of chemicals and high tonnage disposal of sulfur cake (containing about 50% moisture). Molten sulfur and Stretford purge disposal options (cases 2 and 3) add 20% to the capital cost; however the chemicals loss is only about 60 percent of the filter cake option. Also, the amount of solution purged is less and the disposal cost is lower. If recovered sulfur can be sold then sulfur credit will help reduce the overall cost of operation (case 2). If sulfur cannot be sold and has to be disposed (case 3), the overall operating costs per ton of sulfur output will be about \$40 more than the filter cake disposal option (case 1).

With a sulfur melter, and reductive incineration for chemicals recovery added to the plant, the capital cost will be 35 percent higher than the filter cake option. This option with sulfur credit (case 4) shows improved economics over the base case. Compared with cases 2 and 3 the operating costs per ton of sulfur output are about \$17 and \$67 higher. With reductive incineration almost all NaVO_3 and Na_2CO_3 are recovered, minimizing the cost of chemicals. If no sulfur by-product credit is given (case 5) the operating cost is about \$53 higher per ton sulfur output than case 1 (base case).

Table C-1 shows the comparative economics of the sulfur plant options. The data shown in Table C-2 was used for estimating the operating costs. The results show that with no sulfur by-product credit considered, the overall cost of operation for cases 3 and 5 is higher than the base case. However, when sulfur by-product credit of \$60/ton is considered (cases 2 and 4) the overall cost of operation per ton of sulfur output is about \$20-40 lower than the filter cake disposal option (case 1).

Conclusions

- o If no sulfur by-product credit can be claimed, the filter-cake disposal option (case 1) should be considered.

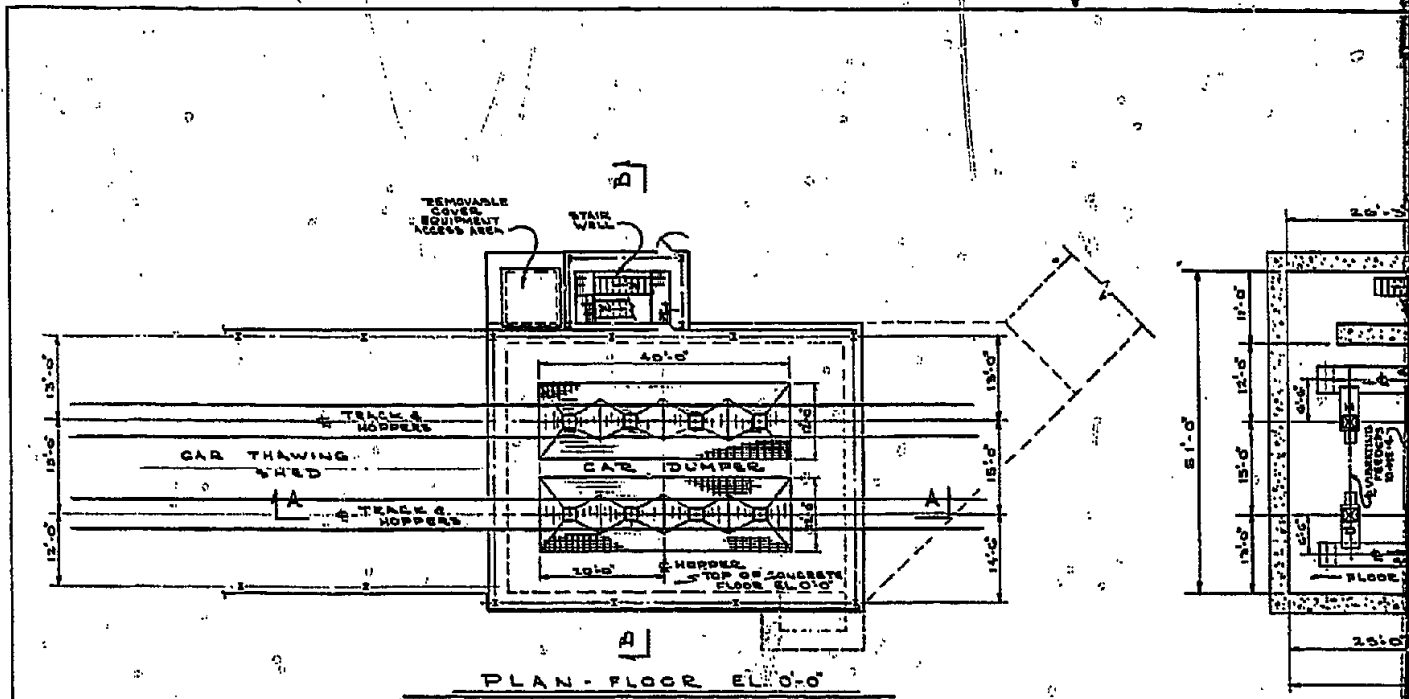
TABLE C-1
ECONOMIC EVALUATION OF STRETTFORD SULFUR PLANT OPTIONS

Case	1 (Base)	2	3	4	5
Sulfur Plant Options	Filter Cake Disposal	Molten Sulfur-Purge Disposal-Sulfur Credit	Molten Sulfur-Purge Disposal-Sulfur Disposal	Molten Sulfur-Red. Incineration-Sulfur Credit	Molten Sulfur-Red. Incineration-Sulfur Disposal
Total Plant Invest., MM\$	7.400	8.880	8.880	9.990	9.990
Yearly Operating Cost, MM\$					
Chemicals	0.492	0.312	0.312	0.193	0.193
Electricity	0.618	0.767	0.767	0.767	0.767
Steam	None	0.048	0.048	0.048	0.048
Fuel	None	None	None	0.166	0.166
Labor	0.114	0.114	0.114	0.114	0.114
Maintenance (2% of TPI)	0.148	0.178	0.178	0.200	0.200
Depreciation (20% of TPI)	1.480	1.776	1.775	1.998	1.998
Filter Cake Disposal	0.366	None	None	None	None
Purge Liquor Disposal	None	0.185	0.185	None	None
Sulfur Disposal	None	None	0.166	None	0.166
Sulfur Credit	None	-(0.498)	None	-(0.498)	None
Total	3.218	2.882	3.546	2.988	3.652
Overall Cost of Operation \$/Ton Sulfur Output	387.83	347.35	427.35	360.15	440.14

(1) Plant investment is based on the conceptual cost estimates performed during Phase I of the current project.

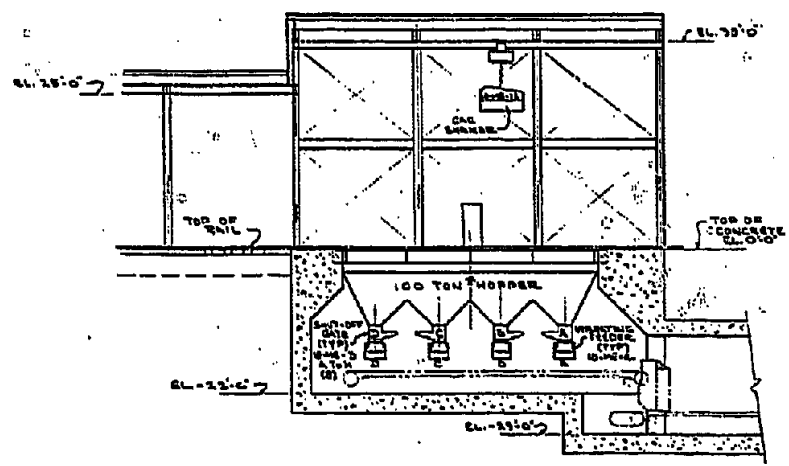
- o If sulfur can be sold at about \$60/ton or higher, the molten sulfur options (cases 2 and 4) should be considered. Reductive incineration (case 4) may be preferable to case 2 (purge disposal) because of marginal benefits of case 2 over case 4.

APPENDIX D
LAYOUT DRAWINGS

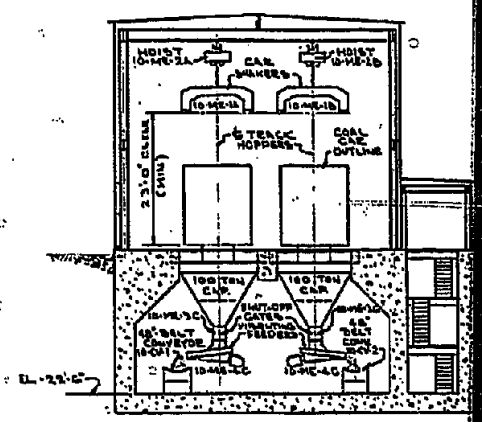


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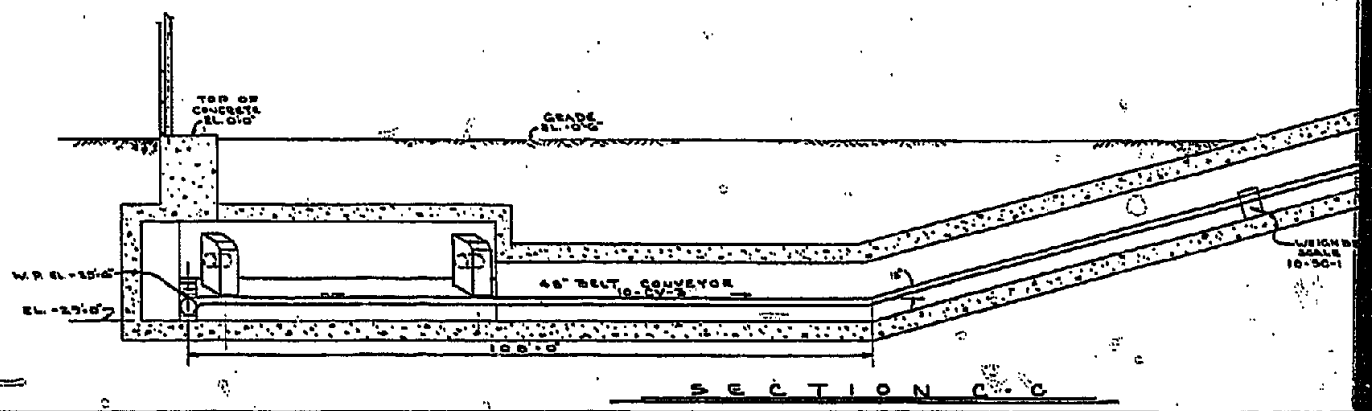
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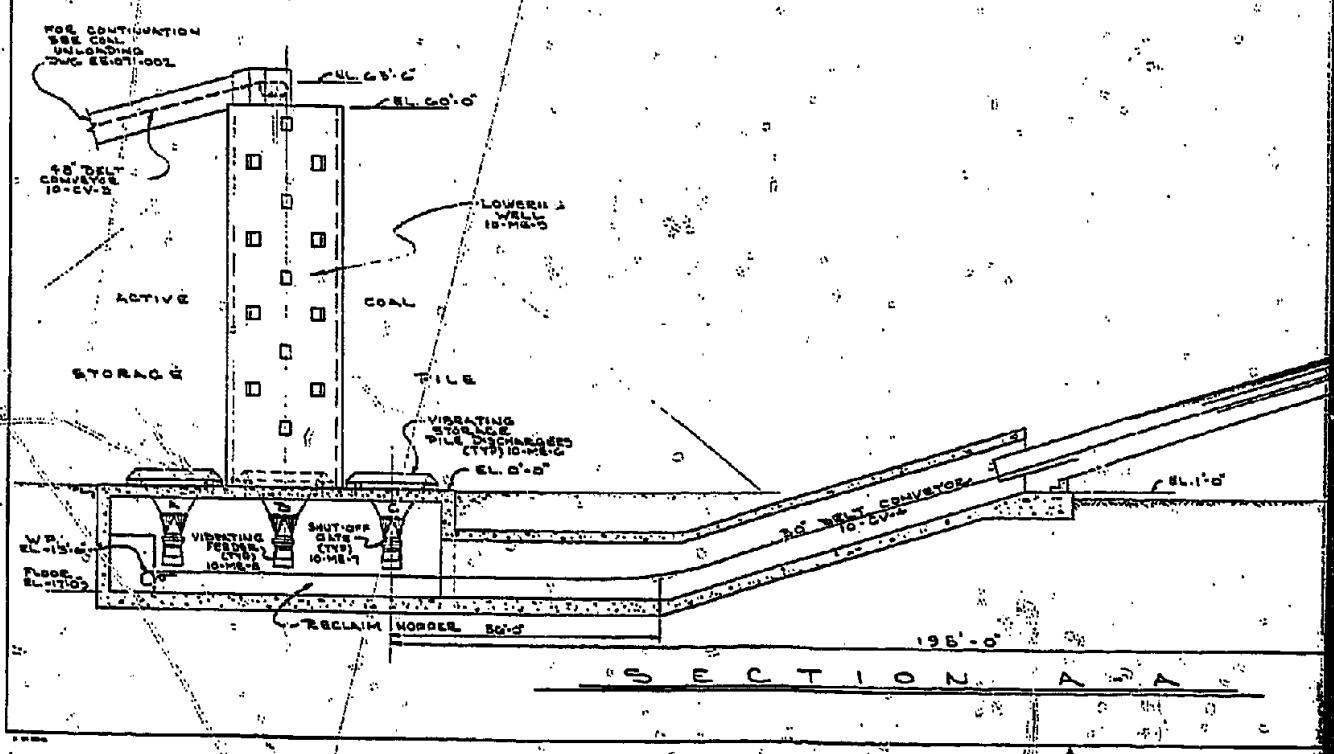
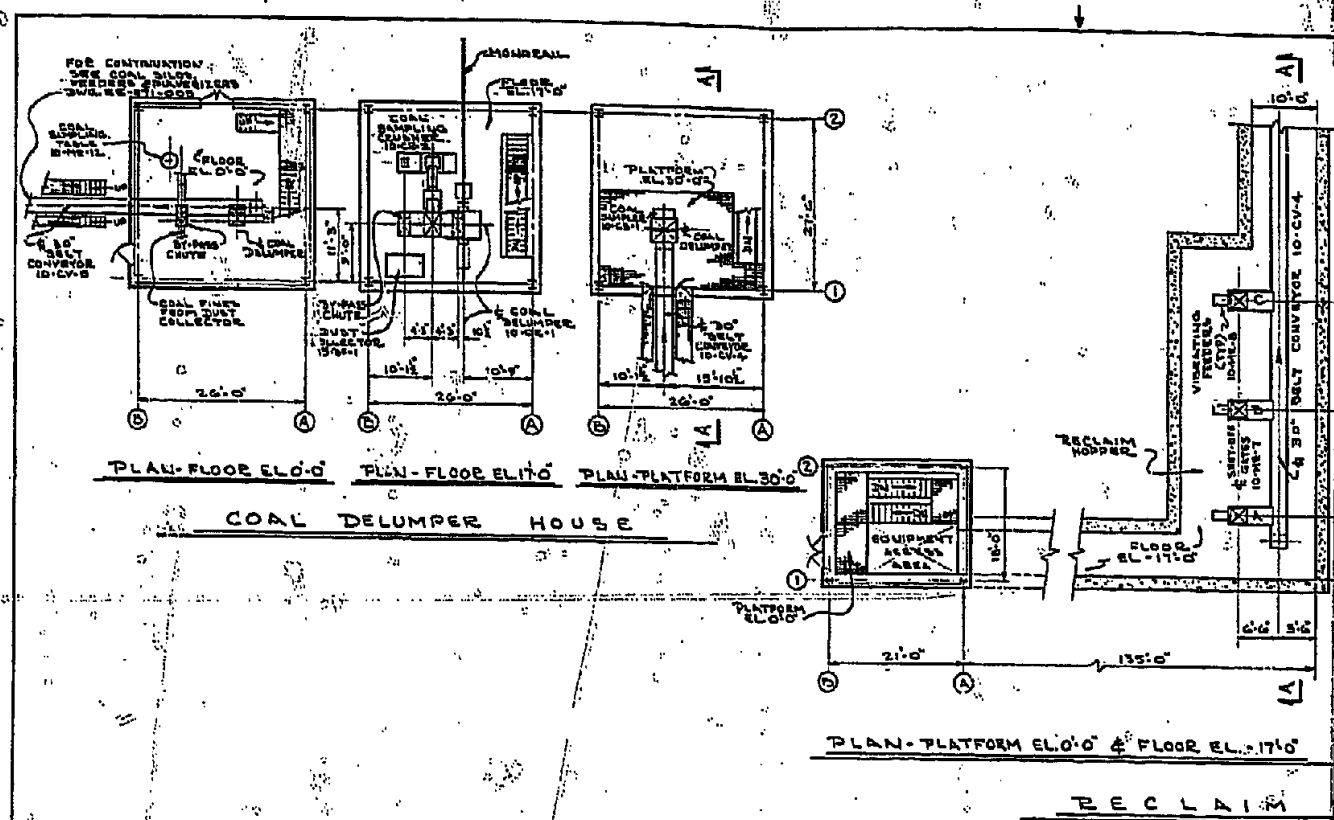


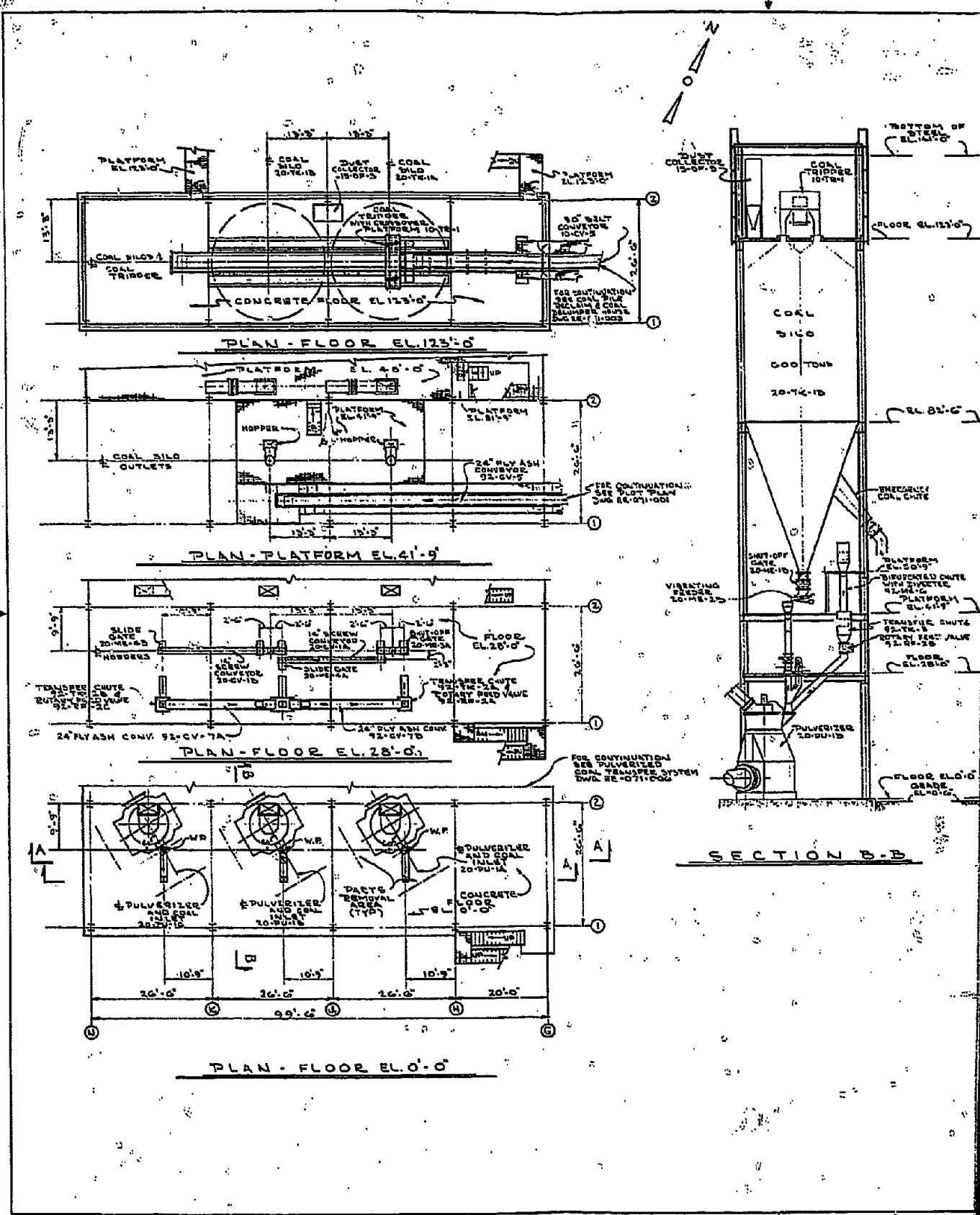
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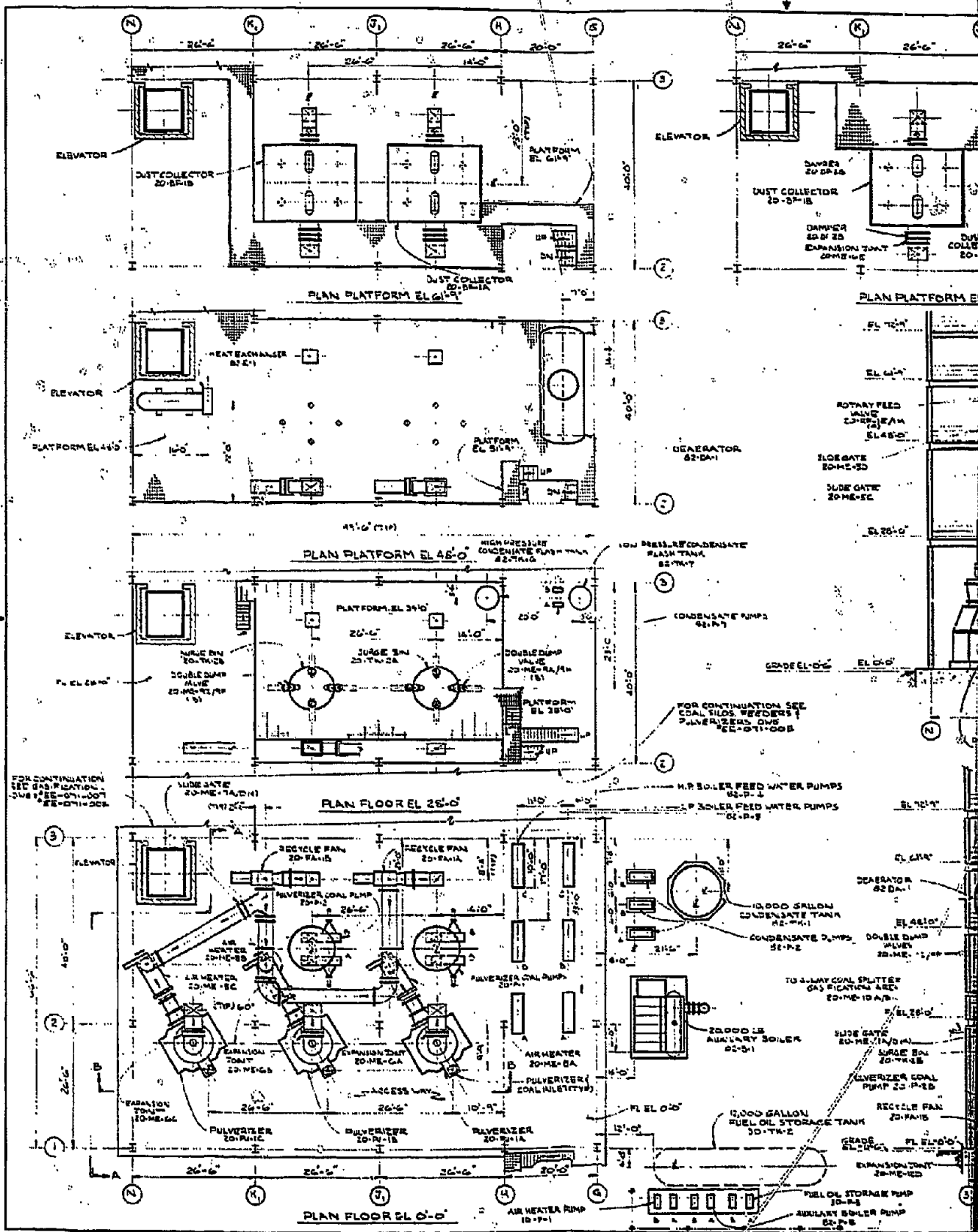


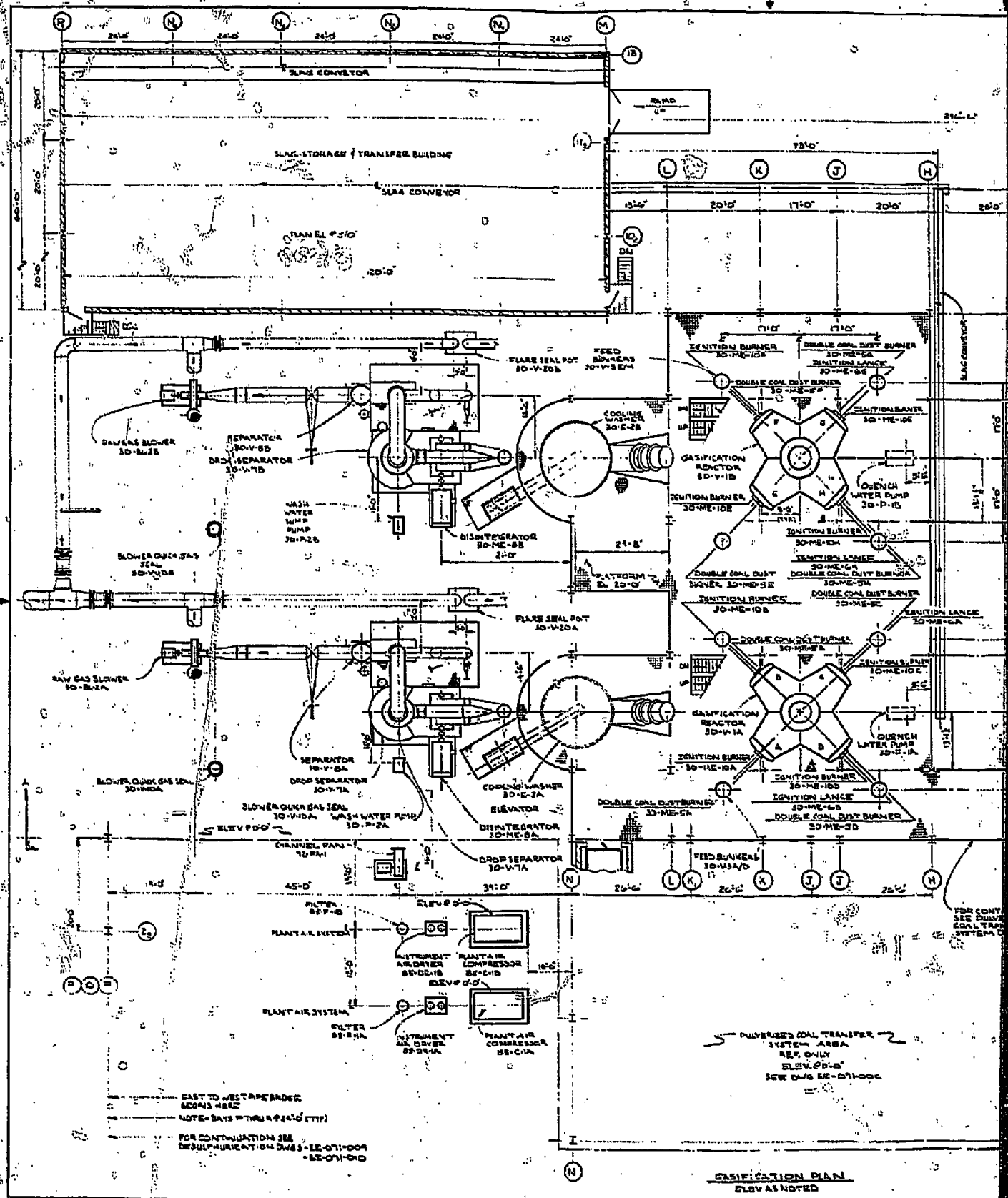
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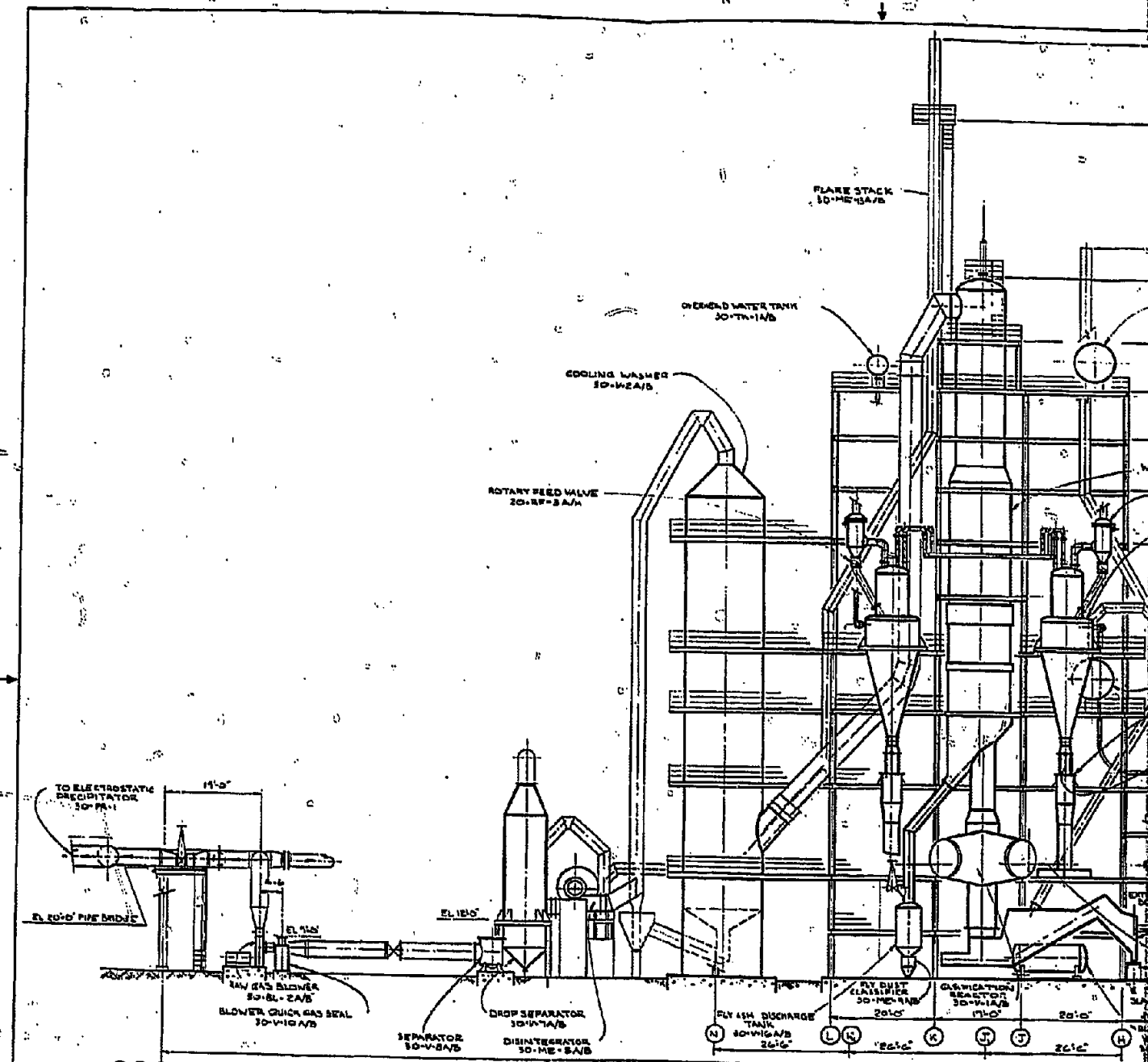
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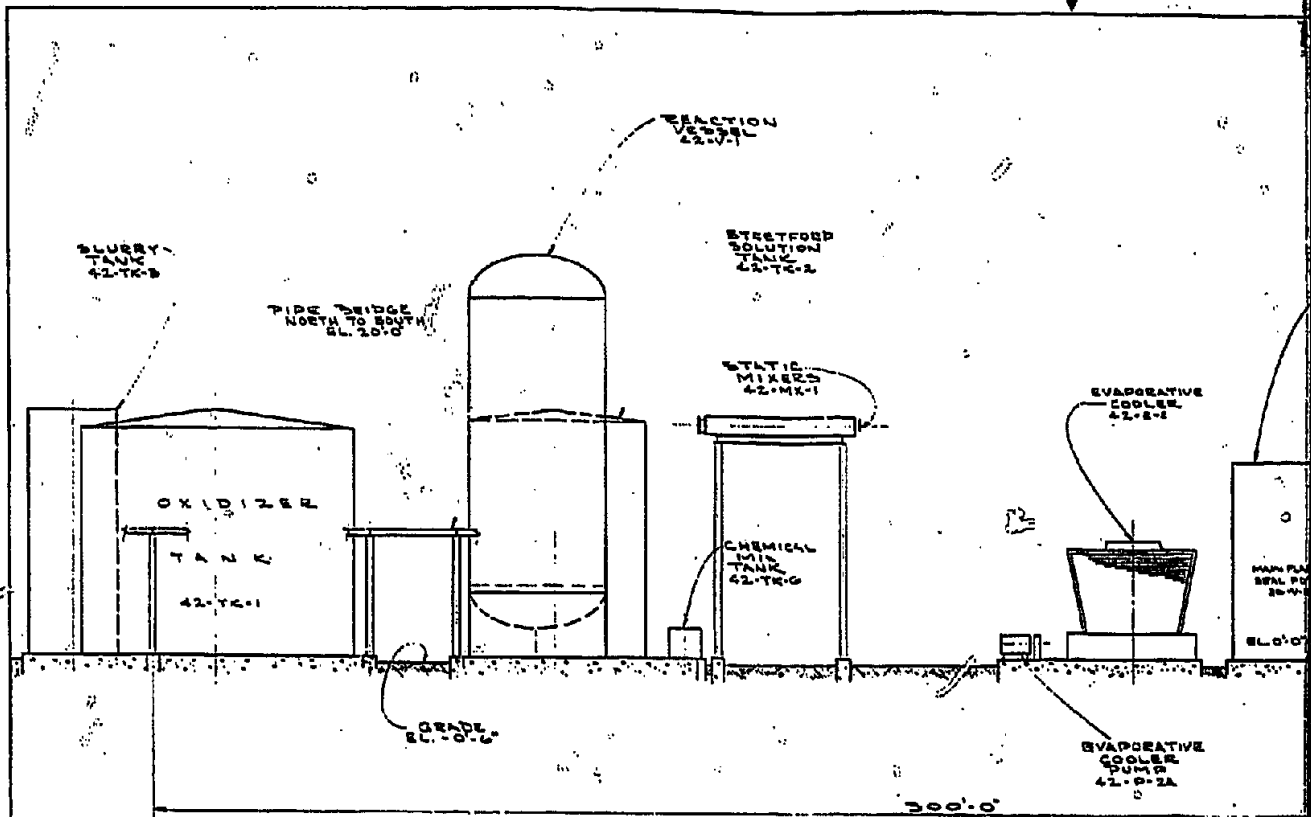




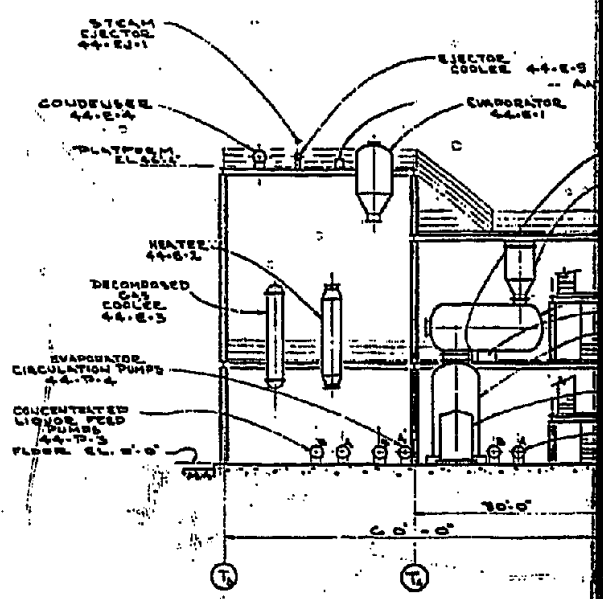
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GASIFICATION SECTION AA

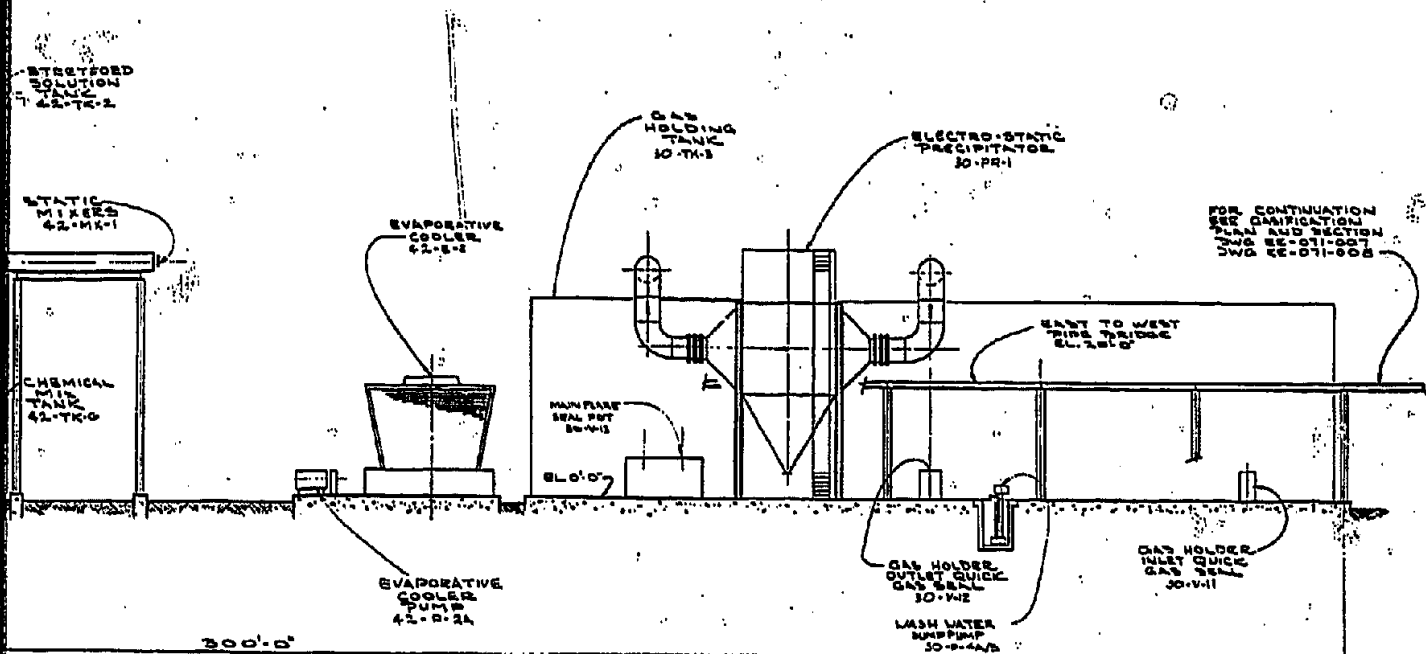


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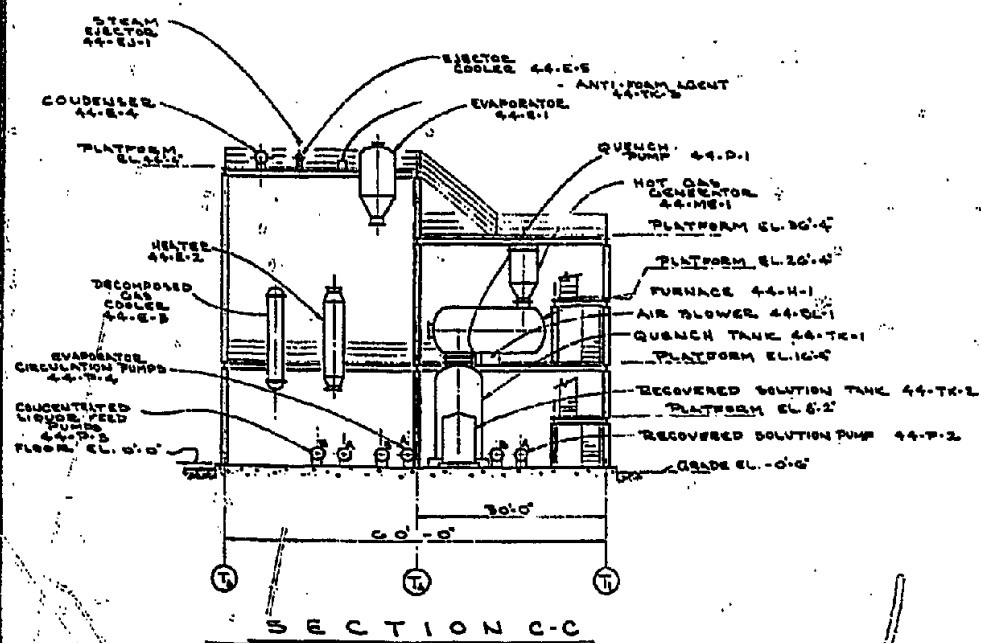
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A-A



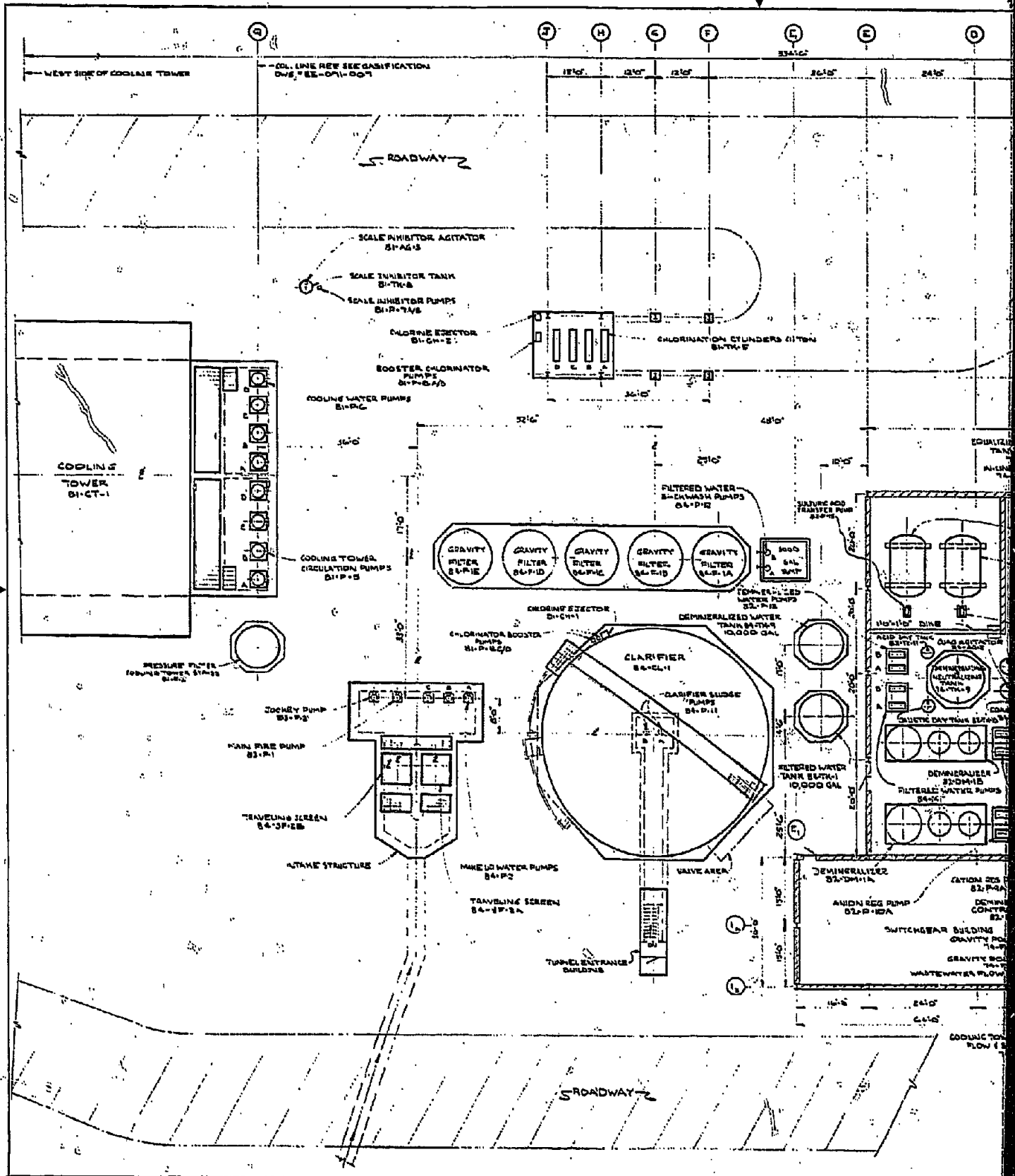
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DWS EE-071-008

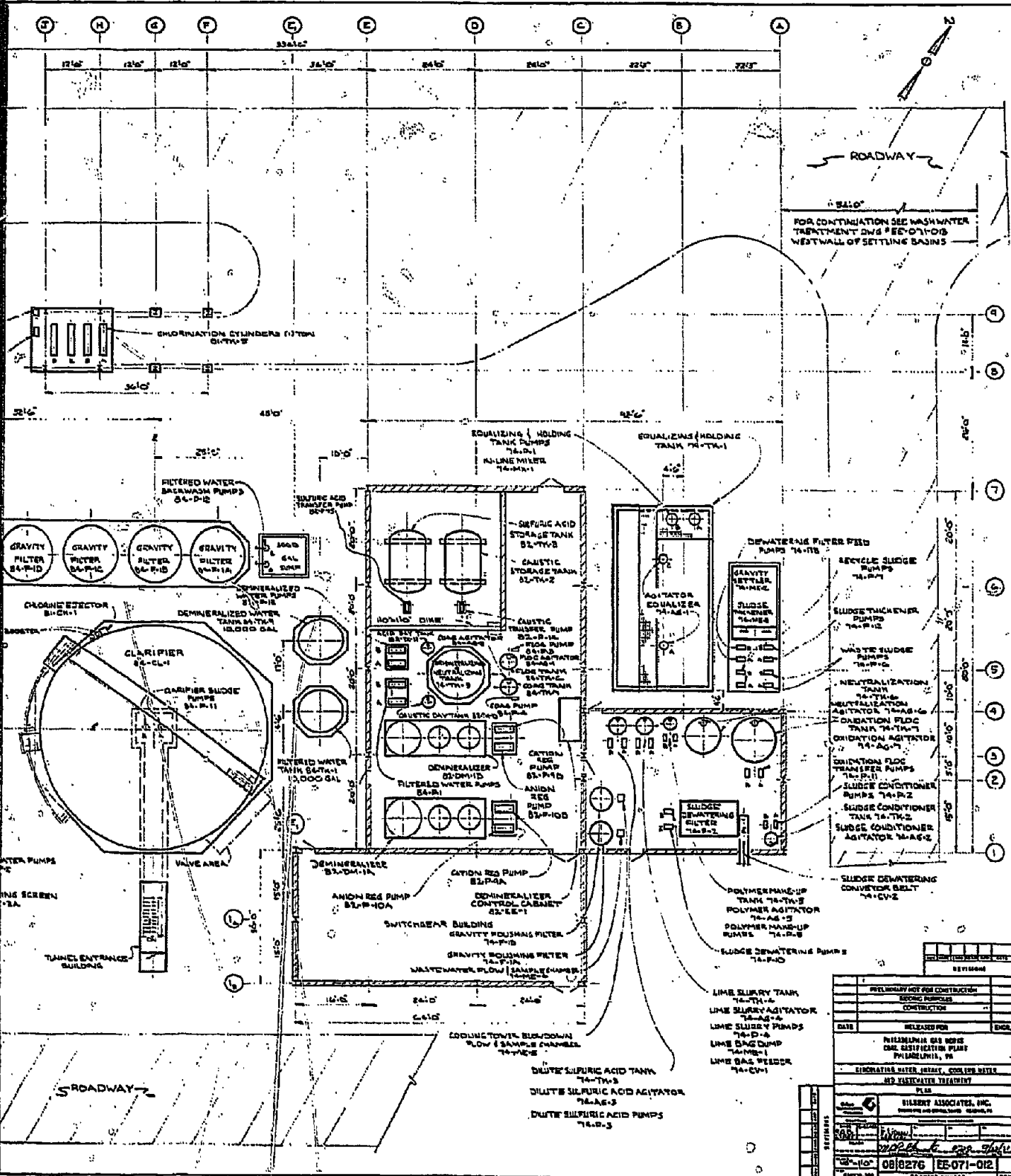
SECTION B-B



SECTION C-C

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CPL. DESIGNATION PLANT	
PHILADELPHIA, PA.	
REVISIONS	
DESCRIPTION	
GILBERT ASSOCIATES, INC.	
DATE	
08/27/68	EE-071-010





FOR CONTINUATION SEE WASH WATER TREATMENT DWG # EE-071-03 WEST WALL OF SETTLING BASINS

- RECYCLE SLUDGE PUMPS 74-R-1
- SLUDGE THICKENER PUMPS 74-R-2
- WASTE SLUDGE PUMPS 74-R-3
- NEUTRALIZATION TANK 74-T-1
- NEUTRALIZATION AGITATOR 74-A-1
- OXIDATION FLOC TANK 74-T-2
- OXIDATION AGITATOR 74-A-2
- OXIDATION FLOC TRANSFER PUMPS 74-T-3
- SLUDGE CONDITIONER PUMPS 74-R-4
- SLUDGE CONDITIONER TANK 74-T-3
- SLUDGE CONDITIONER AGITATOR 74-A-3
- SLUDGE DEWATERING CONVEYOR BELT 74-CV-2

- POLYMER MAKE-UP TANK 74-T-4
- POLYMER AGITATOR 74-A-4
- POLYMER MAKE-UP PUMPS 74-R-5
- SLUDGE DEWATERING PUMPS 74-F-1

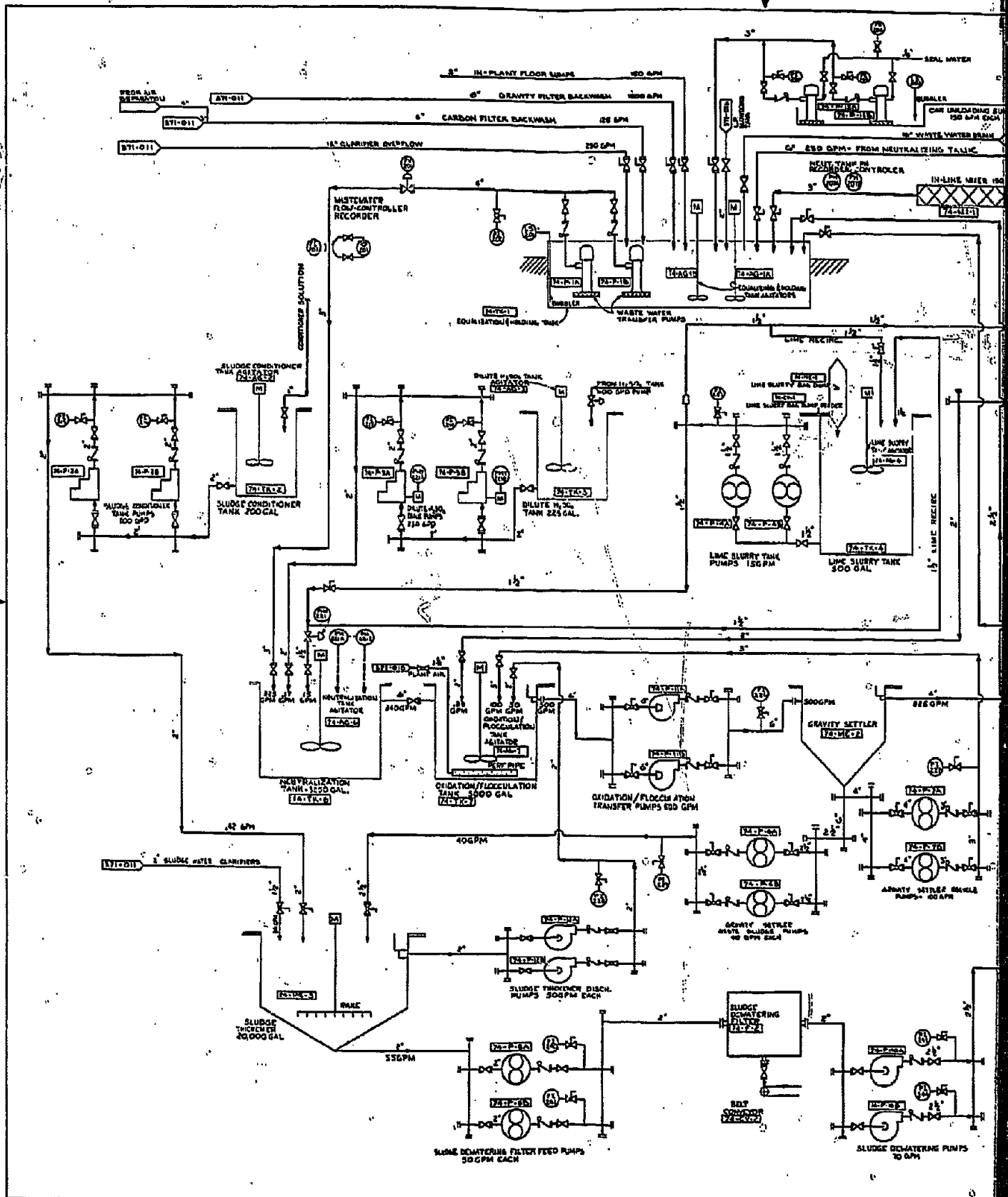
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- LIME SLURRY AGITATOR 74-A-5
- LIME SLURRY PUMPS 74-R-6
- LIME SAG DUMP 74-M-1
- LIME SAG FEEDER 74-CV-1

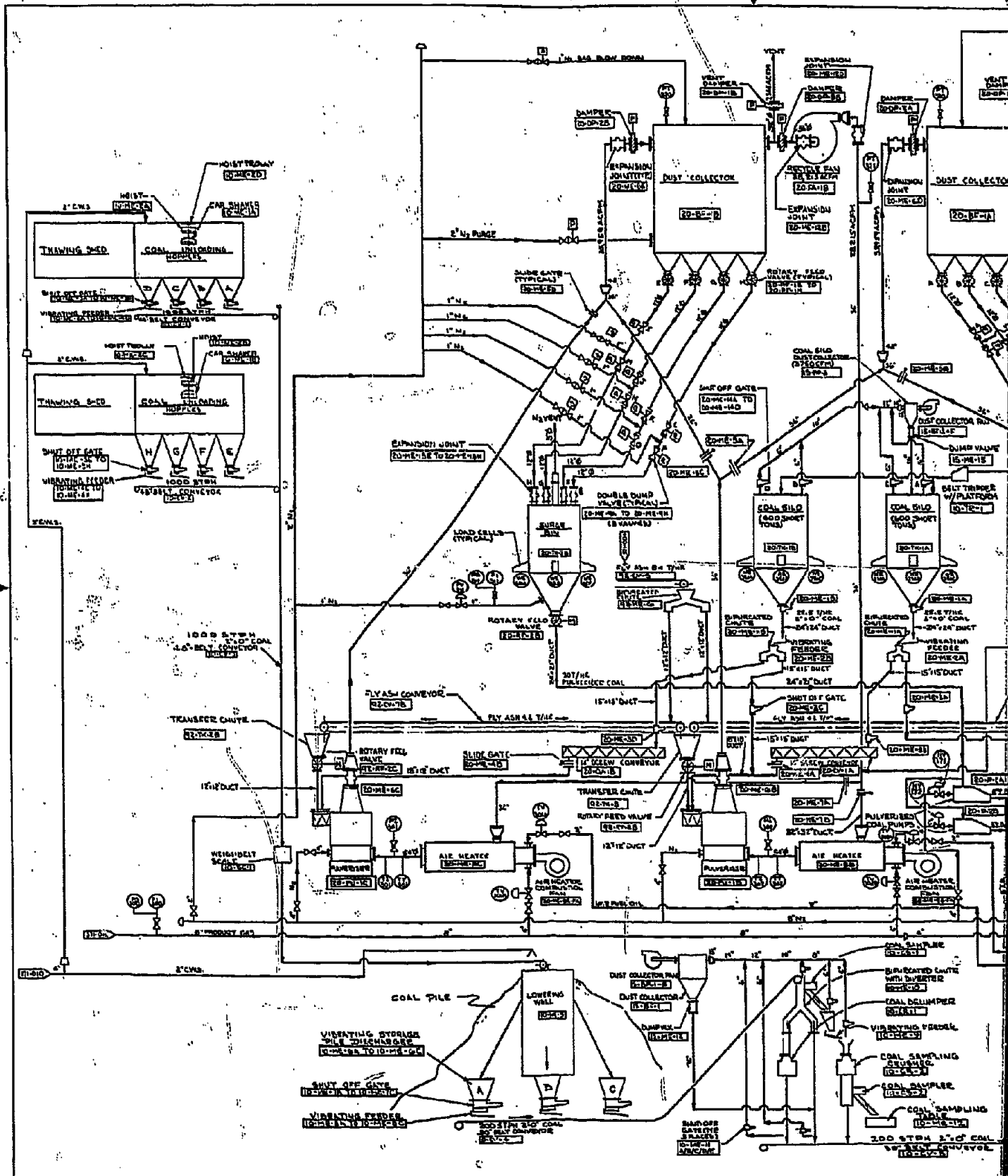
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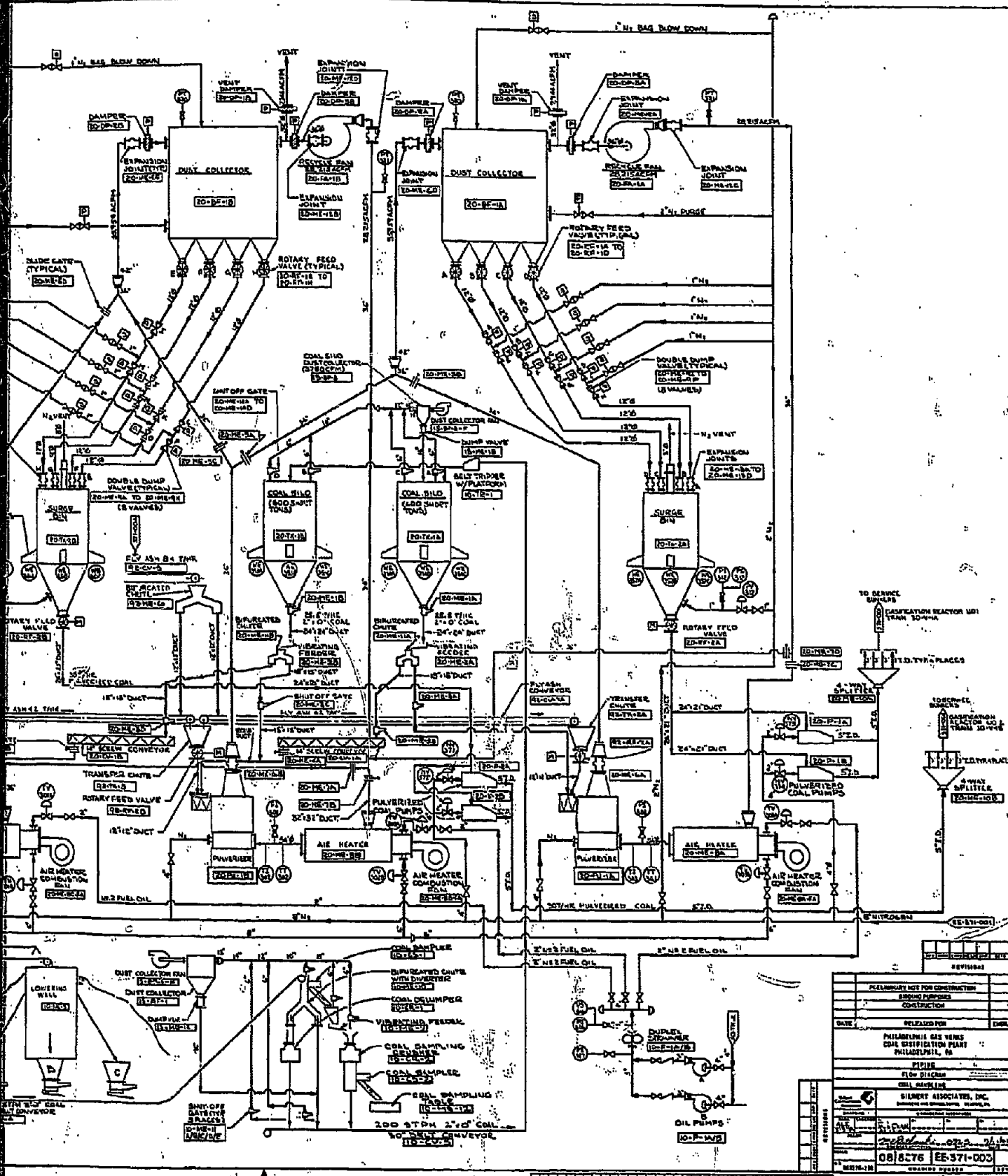
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SHEET NO.: 02		

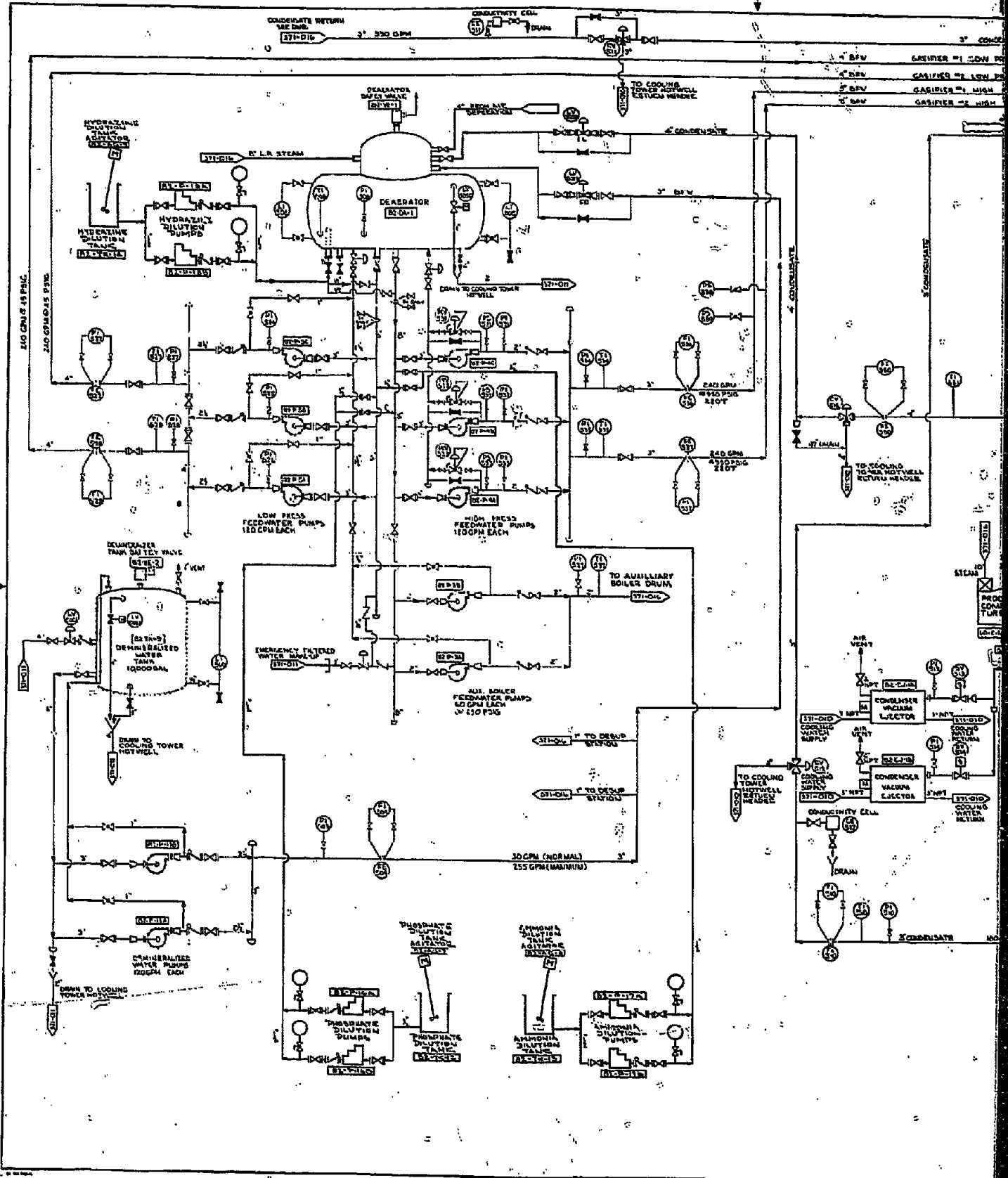
SEE OTHER SHEETS FOR CONTINUATION

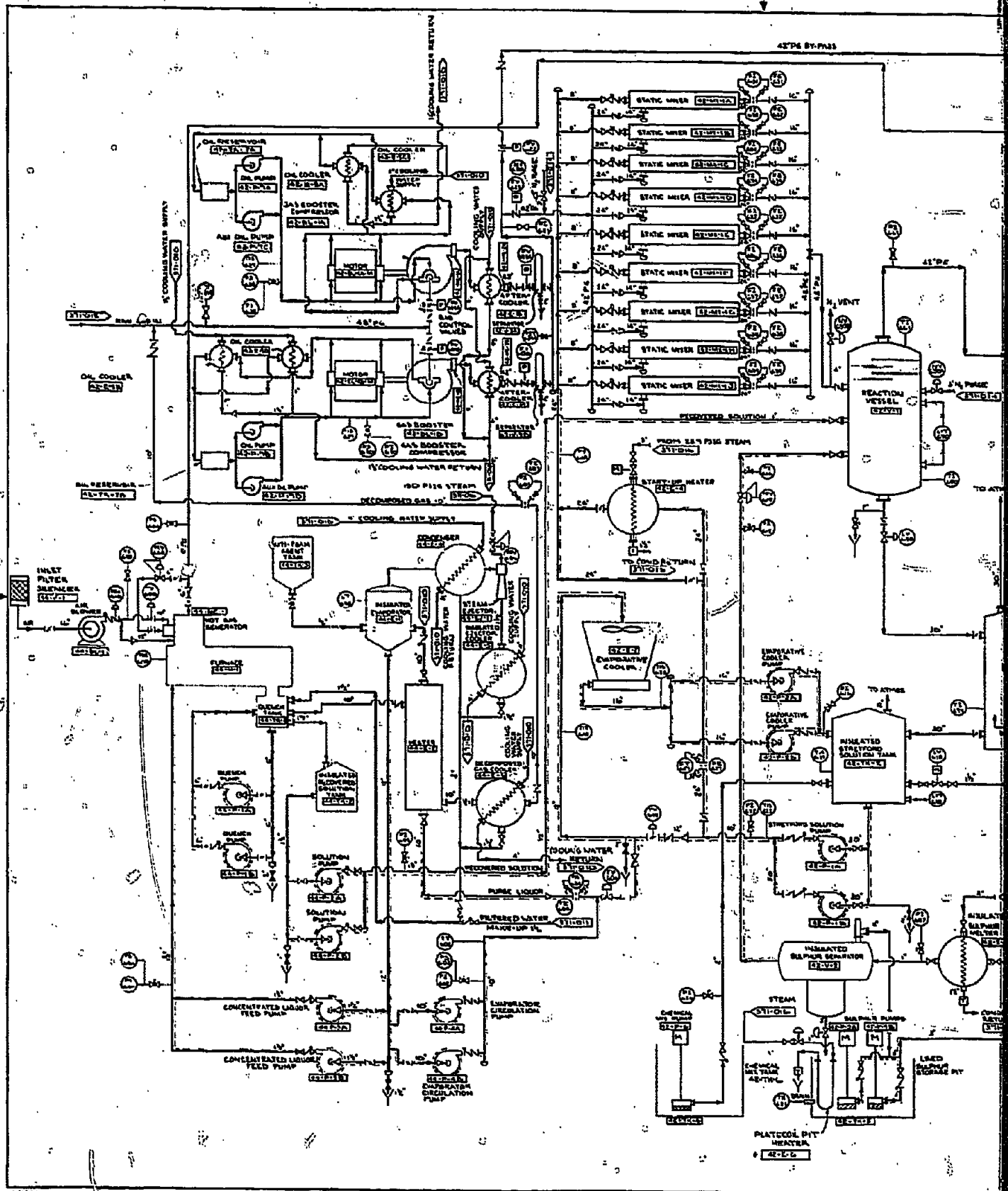
APPENDIX E
PIPING FLOW DIAGRAMS

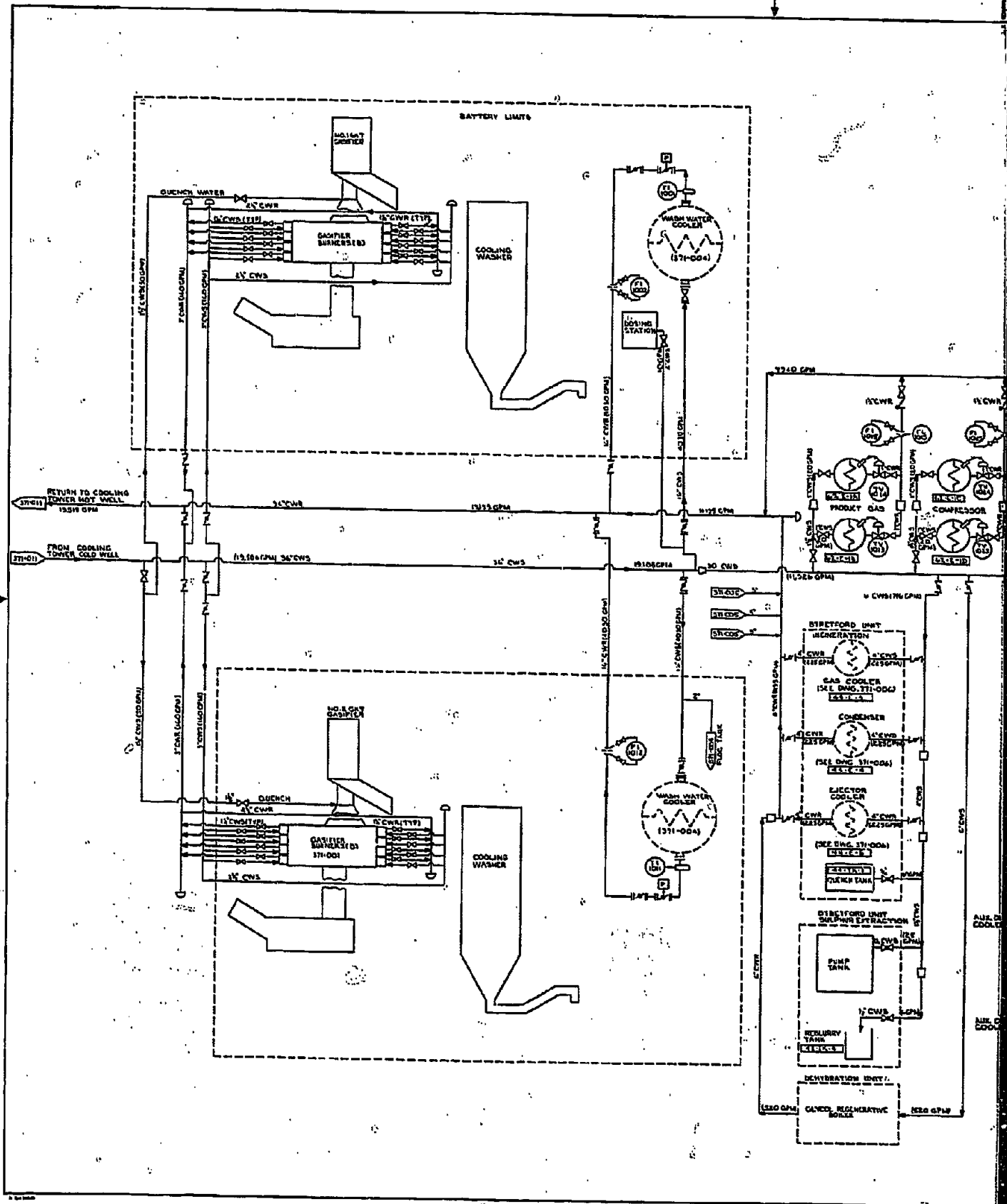


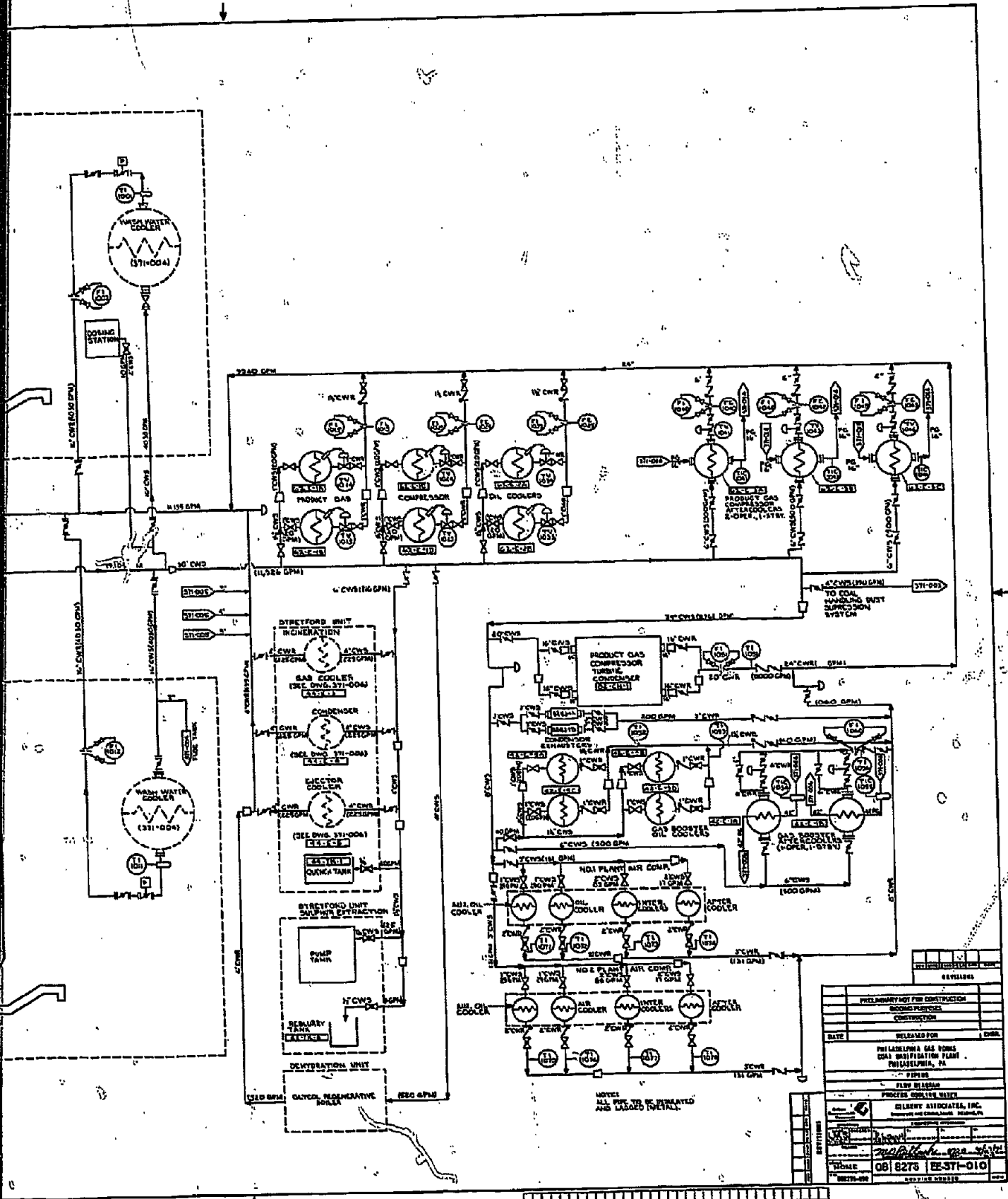




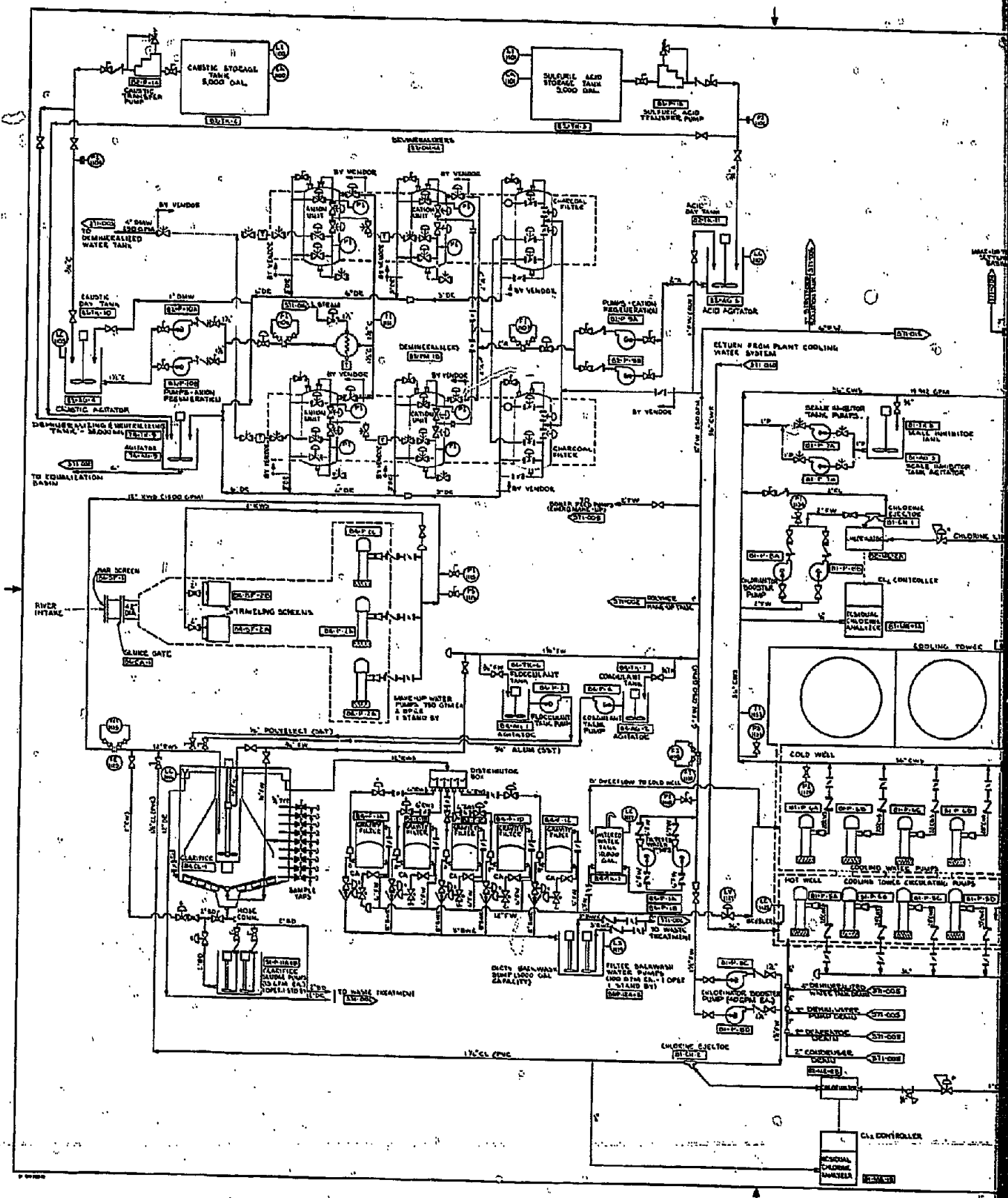


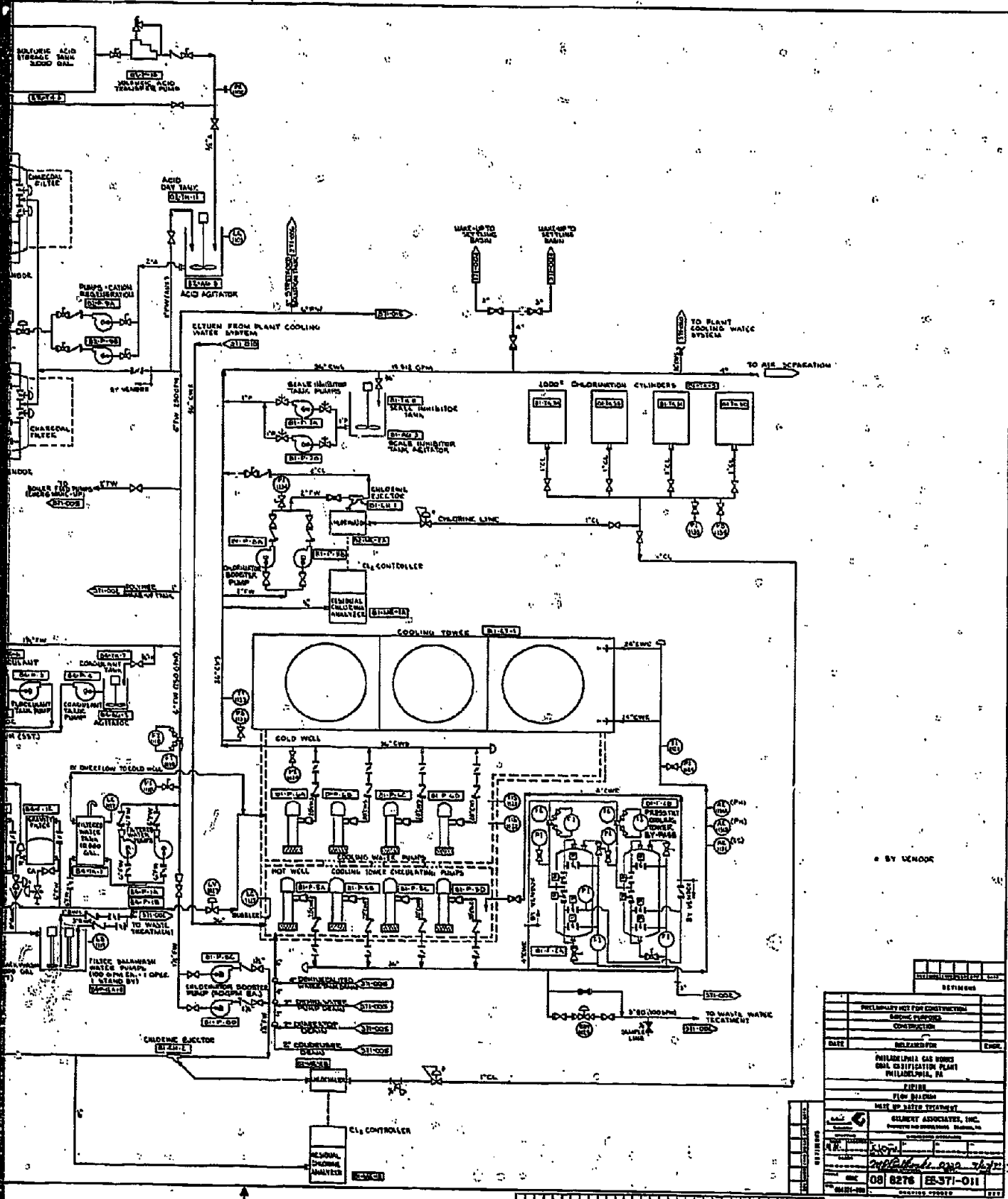




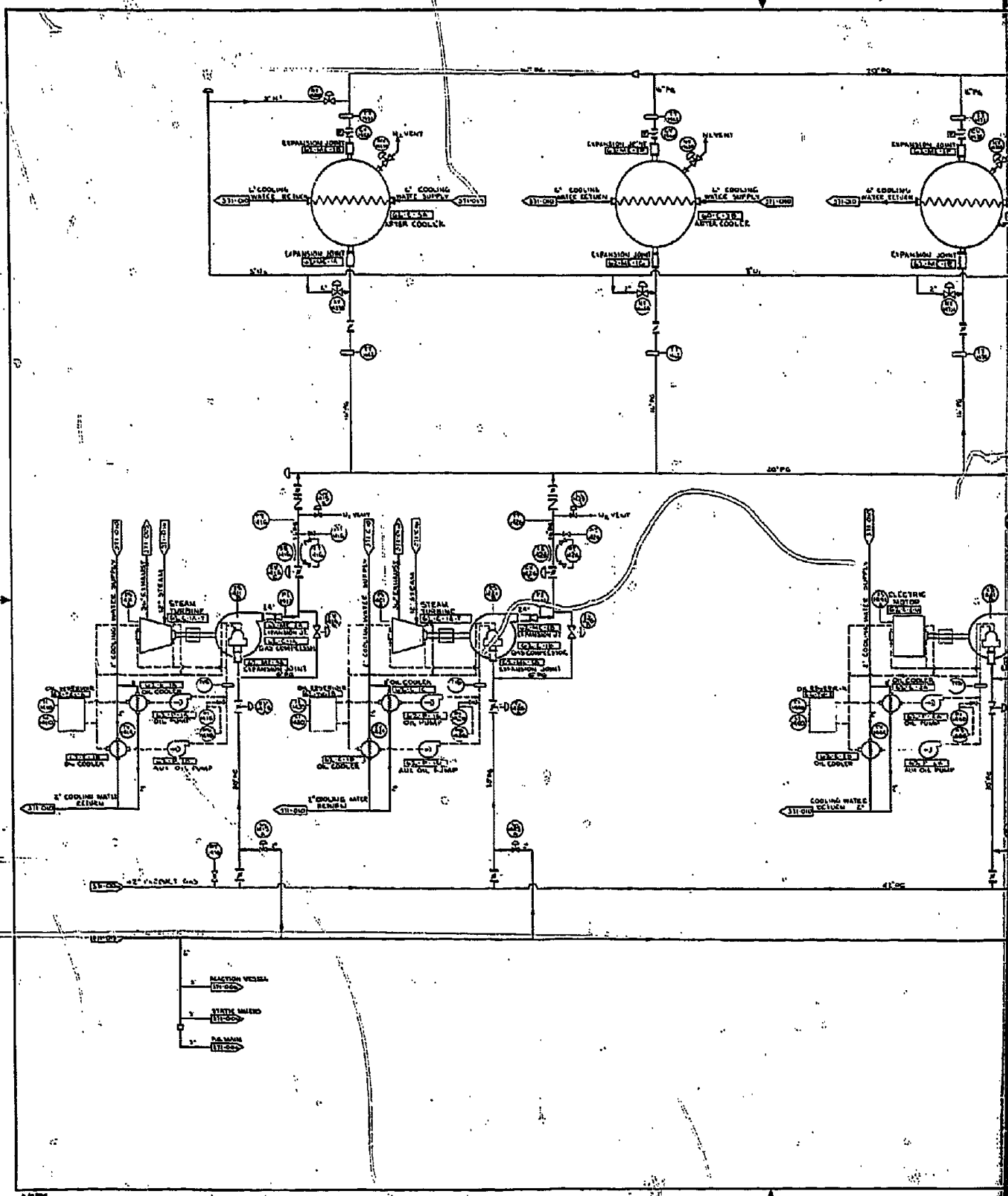


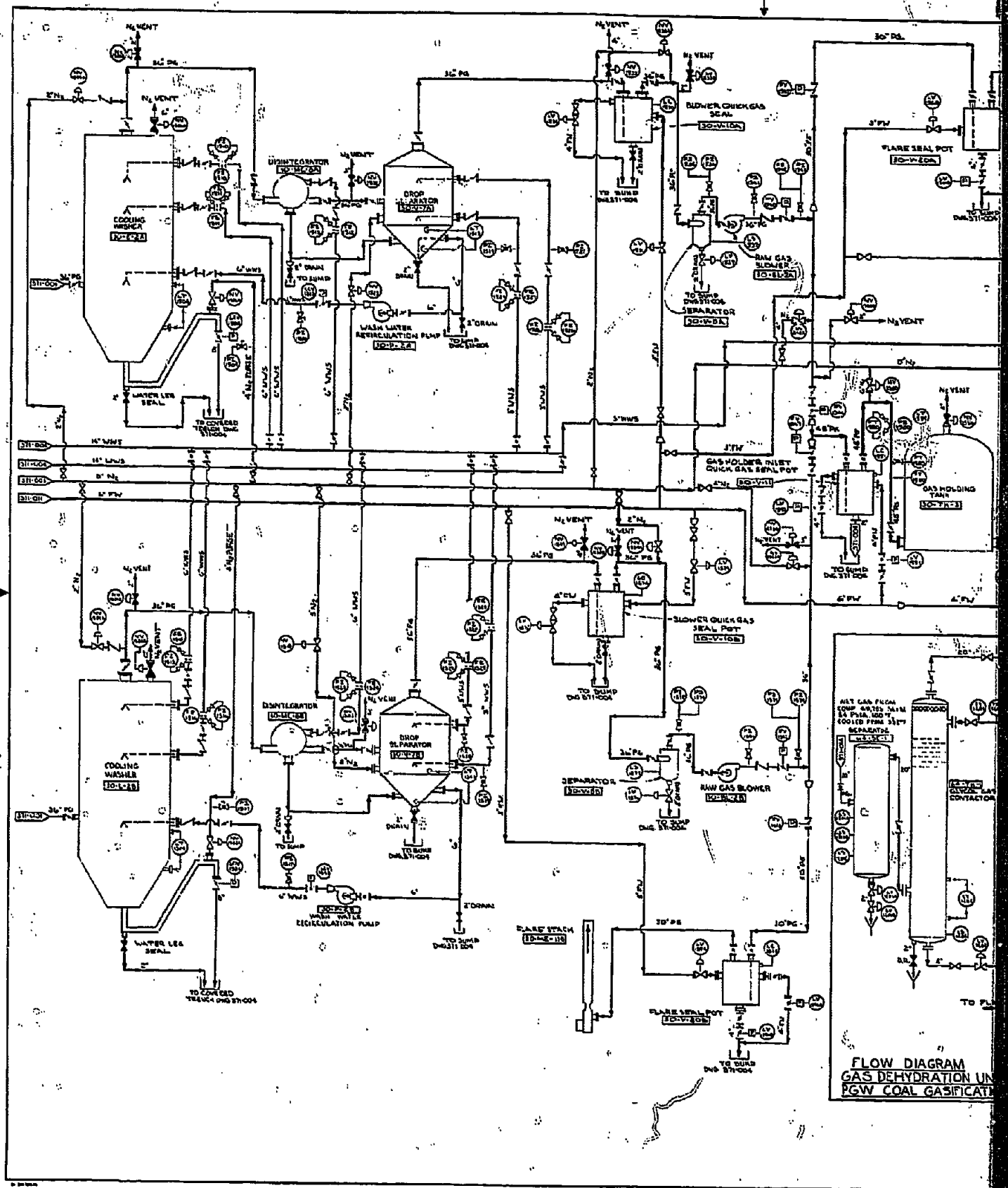
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P. 1010 FLOW SHEET PROCESS CONDENSER UNIT PHILADELPHIA GAS WORKS, INC. PHILADELPHIA, PA.	
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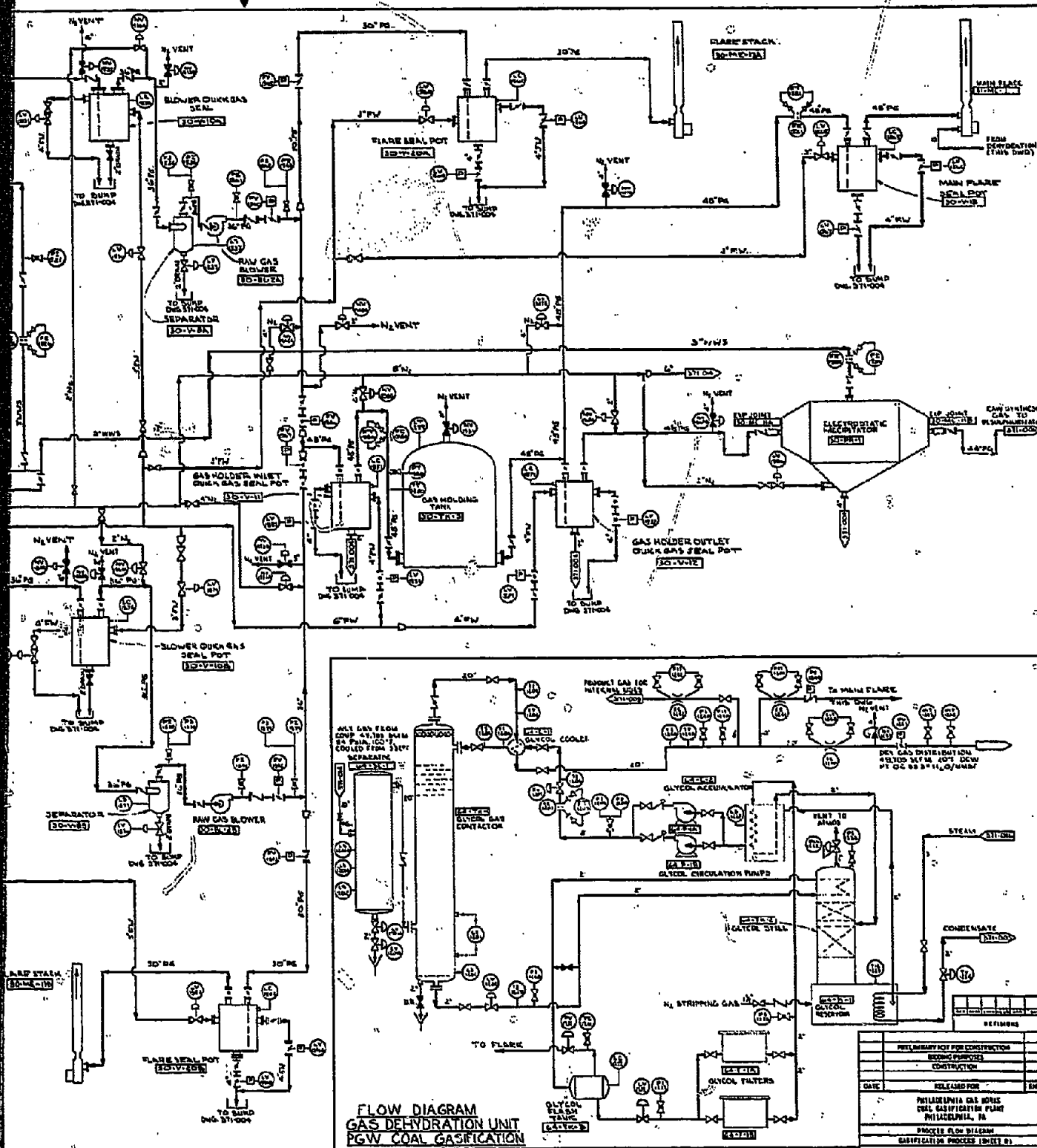


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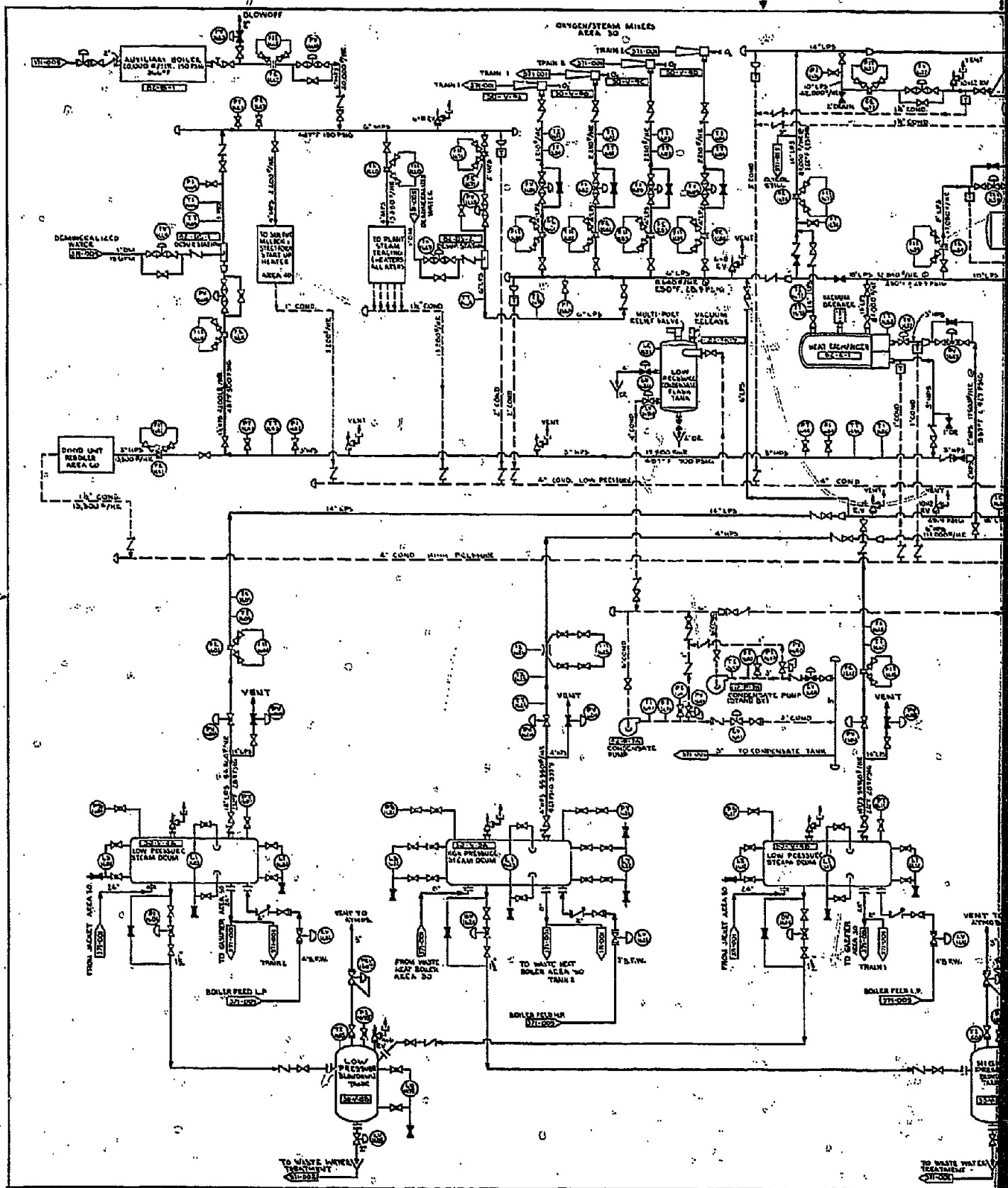


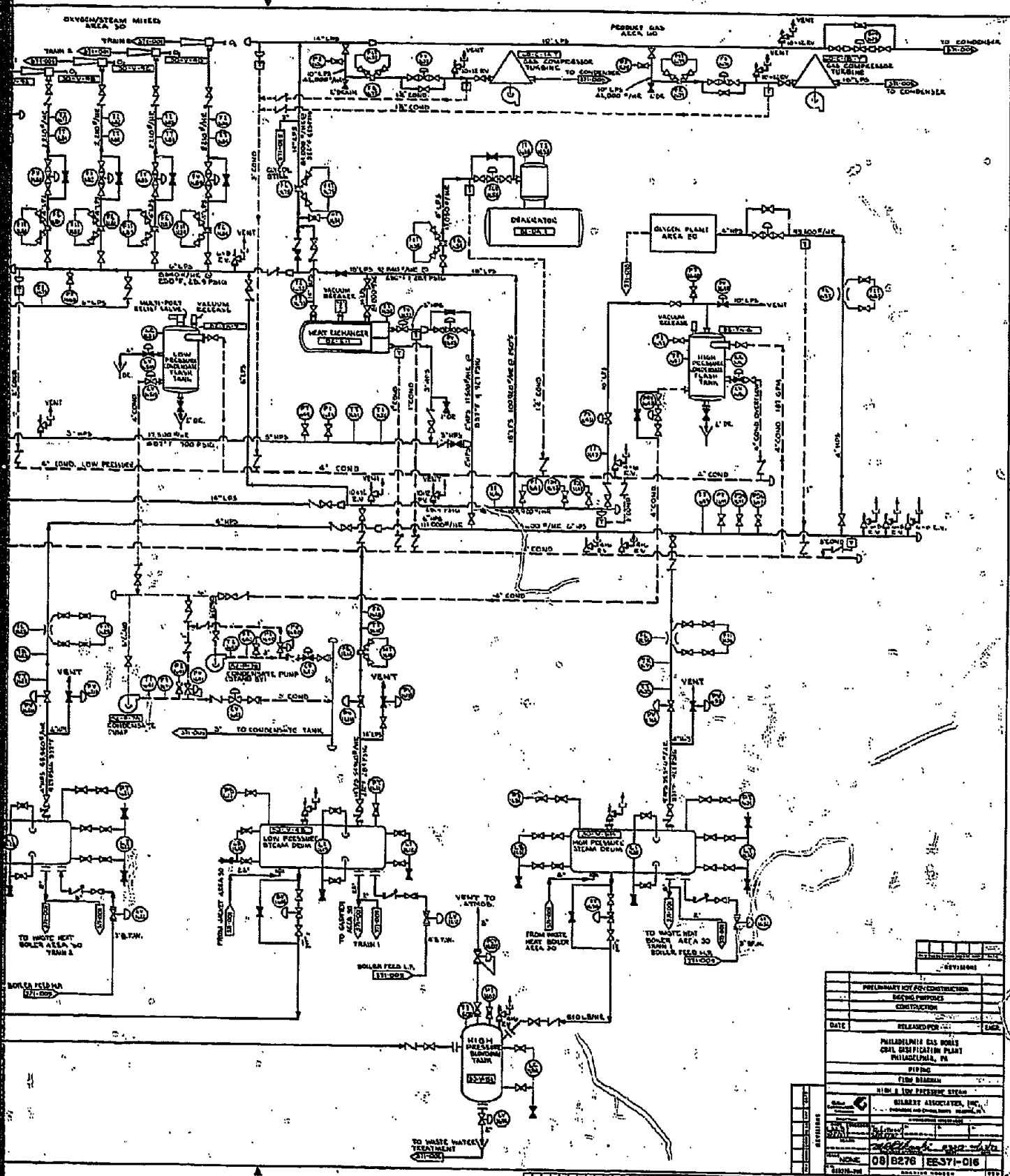


FLOW DIAGRAM
 GAS DEHYDRATION IN
 PGW COAL GASIFICATION



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DESIGNED BY	CONSTRUCTION
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PROJECT FLOW DIAGRAM GASIFICATION PROCESS (SHEET 8)	
& GAS DEHYDRATION	
GILBERT ASSOCIATES, INC. ENGINEERS AND ARCHITECTS PHILADELPHIA, PA.	
PROJECT NO. 08/8276 E-571-015	
SHEET NO. 8276-015	





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COAL GASIFICATION PLANT			
PHILADELPHIA, PA			
FIELD NO.			
FIELD DRAWING			
HIGH & LOW PRESSURE STEAM			
SILBERT ASSOCIATES, INC.			
ENGINEERS AND ARCHITECTS			
PHILADELPHIA, PA			
DRAWN BY			
CHECKED BY			
DATE			
NO. 081276 EE-37-016			
SHEET NO.			

